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Pretreatment Applied Engineering, Corrosion Assessment for Tank Materials: 1995 Final Report

Graham T. MacLean

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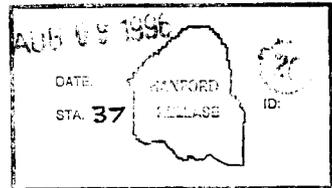
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**PRETREATMENT APPLIED ENGINEERING,
CORROSION ASSESSMENT
FOR TANK MATERIALS:
1995 FINAL REPORT**

July 1996

G. T. MacLean

Prepared by:

Pacific Northwest National Laboratory
Richland, Washington

for:

Westinghouse Hanford Company
Richland, Washington

SUMMARY

For sludge washing to be conducted in existing Hanford carbon steel tanks, there must be an assurance that the tanks will be safe from failure by pitting, stress-corrosion cracking or other failure processes when the corrosion inhibitors present in the waste are diluted during the sludge washing operation. Testing has been conducted previously to define safe operating regimes in concentrated waste environments and moderately dilute waste environments. Due to identification of unsafe operating regimes for moderately dilute waste environments, testing was conducted in more dilute environments to adequately capture the range of possible chemistries during sludge washing operations. Additionally, a small scoping study was performed to identify the corrosion effects of high levels of chloride in the waste environments.

Six month exposure coupon tests, slow strain rate tests, and potentiodynamic scans have been completed on a statistically designed test matrix of twenty-four tests. Stress-corrosion cracking was not found for the specimens in the static tests or the slow strain rate tests. Pitting and crevice corrosion was found for many of the solutions, but primarily in the vapor phase. Waterline attack at the vapor space/solution interface was common for the range of solutions tested. Gross general attack was found for the specimens exposed to the vapor space of the high chloride solutions.

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ACRONYMS AND ABBREVIATIONS

ASTM	American Society for Testing Materials
E_{cor}	open circuit potential
E_{pit}	pitting potential
E_{prot}	protection potential
HLW	high-level waste
PNNL	Pacific Northwest National Laboratory
WHC	Westinghouse Hanford Company
SCC	stress corrosion cracking
SSR	slow strain rate

PRETREATMENT APPLIED ENGINEERING,
CORROSION ASSESSMENT
FOR TANK MATERIALS:
1995 FINAL REPORT

1.0 INTRODUCTION

Pretreatment of the radioactive tank waste in storage at the Hanford site will be used to minimize the volume of the high-level waste (HLW), and thereby reduce the attendant costs of disposal. One step in the pretreatment of HLW is sludge washing, which may be performed in the existing double-shell carbon steel tanks. Sludge washing will include pumping the supernatant liquid out of the tank, adding water to the sludge volume, mixing the contents, settling the contents, and then pumping off the aqueous phase. Multiple washing steps are planned in order to remove the soluble constituents.

Currently, the **concentrated** wastes are maintained to compositional specifications (Ondrejcin 1978, Kirch 1984) that prevent stress corrosion cracking (SCC). There is a major concern that the washing operations using raw water (without inhibitors) could jeopardize the tank integrity by SCC and pitting attack, because the corrosion-inhibiting effect of hydroxide and nitrite ions would be lost through excessive dilution. Ideally, the wash water should contain sufficient levels of corrosion inhibitor to minimize pitting, cracking, or uniform attack and at the same time add very little additional burden to the amount of dissolved solids that must be processed.

Corrosion testing began at the Pacific Northwest National Laboratory (PNNL) in FY 94 to provide experimental data to guide in adding the minimum amount of inhibitor chemicals to the wash water, consistent with avoiding tank failures by SCC, pitting, and uniform attack (Danielson and Bunnell 1994). Stress-corrosion cracking and potentially serious pitting in the vapor phase were observed in specimens exposed to two of the sixteen statistically designed solution environments investigated in these FY 94 studies. Based on these test results, testing in FY 95 focused on the following: (1) better definition of prototypical waste solution environments, (2) better definition of the compositional regime that separates the corrosive chemical environments from the benign chemical environments, and (3) examination of the effects of chloride ion which was not evaluated in FY 94. The FY 95 solution compositions were selected by coordination with Westinghouse Hanford Company (WHC) process engineers and a PNNL statistician. Corrosion test results are reported for the FY 95 electrochemical tests, slow strain rate tests, and coupon tests.

2.0 TEST APPROACH

Three types of tests at $93\pm 3^{\circ}\text{C}$ (200°F) were carried out: slow strain rate tests to evaluate SCC propensity: static tests with totally-immersed and half-immersed U-bends and plain coupon specimens to evaluate the SCC, pitting, crevice, and uniform corrosion attack behavior; and electrochemical tests. Crevice corrosion was evaluated by using serrated polytetrafluoroethylene washers under the bolts loading the U-bends. Test specimens were A-515 steel that were given a twenty-four hour heat treatment at 593°C (1100°F). The tanks were originally given a one hour heat treatment, but the longer heat treatment given to the specimens increases their propensity for SCC (Sarafian 1975), resulting in a more conservative test condition. The chemical and physical properties (before the heat treatment) of the A-515 steel are shown in Tables 1 and 2 for the FY 94 and FY 95 materials. The supplier was unable to duplicate the same heat of A515 for the FY 95 testing.

A-515 steels were studied because a good possibility exists that the earliest washed tanks (constructed of A-515) will be used as the long-term sludge washing containers for the other tanks. Consequently, the A-515 tanks will have the longest exposure to the washed environments and the greatest chance for some slow failure process to occur. A-537 carbon steel was used in later-built tanks. It is hypothesized that the corrosion behavior of A-515 can be used as an accurate predictor for that of A-537.

Nitrate, nitrite, and free hydroxide are the three independent variables that have the most effect on the corrosion response. A statistical experimental design was used to define the test solution compositions because of the expected complexity of the interaction among these variables and the wide variety in the tank solution compositions. The range of each variable is shown below:

Nitrate:	0.025 to 1.00 <u>M</u>
Nitrite:	0.01 to 0.393 <u>M</u>
Hydroxide:	0.01 to 0.389 <u>M</u>
Chloride:	<0.001 to 0.500 <u>M</u>

Additional minor waste components were maintained at a low level in each solution to better simulate actual waste solutions:

Sodium carbonate:	0.01 <u>M</u>
Sodium sulfate:	0.01 <u>M</u>
Sodium phosphate:	0.001 <u>M</u>

Table 1. A-515 Chemical Properties.

C	Cr	Cu	Mn	Mo	Ni	P	S	Si	Other
FY 94 Specimen Material:									
0.21	0.20	0.25	0.54	0.07	0.24	0.02 3	0.01 3	0.22	V 0.003 Cb 0.001
FY 95 Specimen Material:									
0.24	0.11	0.28	0.51	0.05	0.11	0.00 8	0.01 5	0.18	V 0.001 Cb 0.002

Table 2. A-515 Physical Properties.

Alloy	Heat	Tensile, MPa	Yield, MPa	Elong, %	UNS	Supplier
FY 94 Specimen Material:						
A515, Gr 60	J567	551	405	23	K02401	Metal Samples
FY 95 Specimen Material:						
A515, Gr 60	K604	525	341	23	K02401	Metal Samples

The composition of the 24 statistically designed test solutions is shown in Tables 3 and 4 (solutions 12 and 20, as well as 7 and 19, are identical for the statistical purpose of measuring the standard error). Chloride was not added for the 'low' chloride solutions represented in Table 3, because chloride is an impurity in sodium hydroxide; so some chloride will be present in every solution. The chloride concentrations for the low chloride solutions varied from <5 mg/L to 30 mg/L for the range of sodium hydroxide in the test solutions. The high chloride solutions, shown in Table 4, containing 0.5 M chloride, were used to perform a scoping test on the effects of chloride on the corrosion susceptibility of the A-515 steel. The solution compositions are more clearly shown in the three-dimensional plots of Figures 1 and 2. Figure 1 shows only the 1995 test matrix while Figure 2 shows the integrated test matrix containing the test concentrations from both the 1994 and 1995 test matrices.

Table 3. Test Solutions, Constrained Test Design for Studying the Effects of Nitrate, Nitrite, and Hydroxide in Dilute Waste Environments.

Solution	Nitrite, M	Nitrate, M	Hydroxide, M
1	0.03	0.10	0.03
2	0.01	0.10	0.03
3	0.10	1.00	1.00
4	0.30	1.00	0.10
5	0.03	0.30	0.03
6	0.03	0.10	0.01
7	0.01	0.10	0.10
8	0.30	1.00	0.30
9	0.10	0.30	0.03
10	0.01	0.10	0.01
11	0.10	0.10	0.01
12	0.10	1.00	0.10
13	0.30	0.30	0.03
14	0.10	1.00	0.30
15	0.03	0.30	0.30
16	0.03	0.30	0.10
17	0.10	0.30	0.30
18	0.10	0.30	0.10
19	0.01	0.10	0.10
20	0.10	1.00	0.10

Table 4. Test Solutions, One-Half Fractional Factorial Test Design for Studying the Effect of Chloride in Dilute Waste Environments.

Solution	Nitrite, <u>M</u>	Nitrate, <u>M</u>	Hydroxide, <u>M</u>	Chloride, <u>M</u>
21	0.025	0.025	0.389	0.500
22	0.025	0.393	0.026	0.500
23	0.393	0.025	0.026	0.500
24	0.393	0.393	0.389	0.500

1995 Test Matrix Corrosion Assessment for Sludge Washing

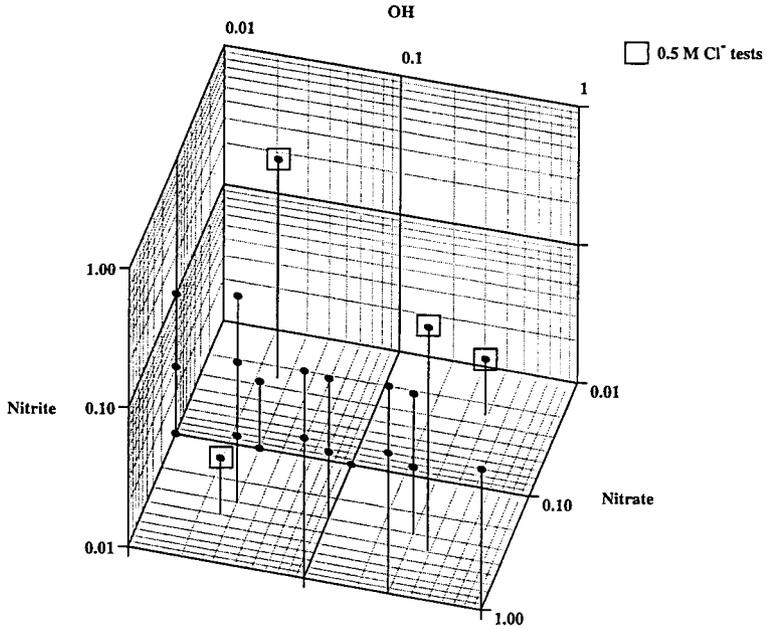


Figure 1. 1995 Test Matrix for Sludge Washing Corrosion Assessment.

3.0 EXPERIMENTAL DESIGN AND SETUP

SCC propensity was evaluated from slow strain rate tests in each of the 24 solutions by time to failure, percent elongation, reduction in tensile strength, reduction of area, and fractographic indications of brittle fracture. A slow strain rate apparatus with a nickel-base alloy vessel was used as schematically shown in Figure 3. Care was taken to electrically isolate the A-515 steel specimens from the test machine to eliminate galvanic effects with the nickel-base alloy. The dogbone-shaped specimens had a gage width and thickness of 0.635 cm (0.25 inches) with a gage length of 2.54 cm (1.0 inches). The slow strain rate tests were carried out at a strain rate of 1.3E-6/sec, the same rate as Ondrejcin (1984) used in his Savannah River Laboratory study on the cracking of carbon steels in concentrated simulated waste solutions. The only exception to this strain rate was the one test performed in solution 12, at a strain rate of 3.25E-7/sec. This test was performed to investigate the cause of the discrepancy between results from the FY 94 testing and current FY 95 test results. A test would typically last three days. Air was continually sparged through the solution, which was maintained at $93 \pm 3^\circ\text{C}$. No welded specimens were evaluated.

Pitting propensity was evaluated in each test solution using the potentiodynamic method to determine the pitting and protection potential. These tests involve polarizing the specimen with a potentiostat according to American Society for Testing Materials (ASTM) standards G-3 and G-5 at a scan rate of 0.2 mV/s. The test set-up is shown schematically in Figure 4. Potentials were measured relative to a Ag, AgCl reference electrode (4.0 M KCl electrolyte) at the $93 \pm 3^\circ\text{C}$ (200°F) solution temperature. The electrochemical tests reveal pitting propensity by determining the existence and value of an electrochemical pitting potential (potential at which pitting starts) and protection potential (potential at which pits stop growing).

Additionally, there were 24 static solution tests containing A-515 coupons. Tests were performed in two-liter polypropylene bottles containing three totally immersed U-bends and three totally immersed flat, uniform corrosion specimens. Three U-bends and three flat specimens were also mounted at the solution/vapor interface in each bottle. Each U-bend (shown schematically in Figure 5) at the solution/vapor interface was positioned with the maximum stressed region at the interface. Polytetrafluoroethylene crevice washers were used under the stressing bolts for all the U-bends to serve as a crevice corrosion test. The test bottles were maintained at $93 \pm 3^\circ\text{C}$ in three air ovens (eight bottles/oven). Each bottle was sparged with carbon dioxide-free air at 1.3 L/day to maintain the oxygen concentration (the carbon dioxide was scavenged with Ascarite). An air condenser was fitted to each of the 24 containers. Deionized water was added to each container as needed to compensate for evaporation losses.

The testing program was conducted according to the Tank Waste Remediation System Test Plan, TWRS-95-6.2, Revision 1.

Slow Strain Rate Test System

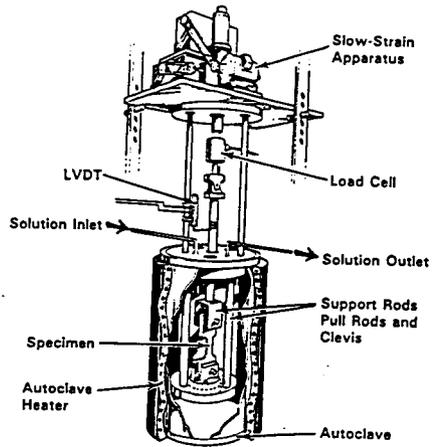


Figure 3. Schematic of the Slow-strain-rate Test Apparatus.

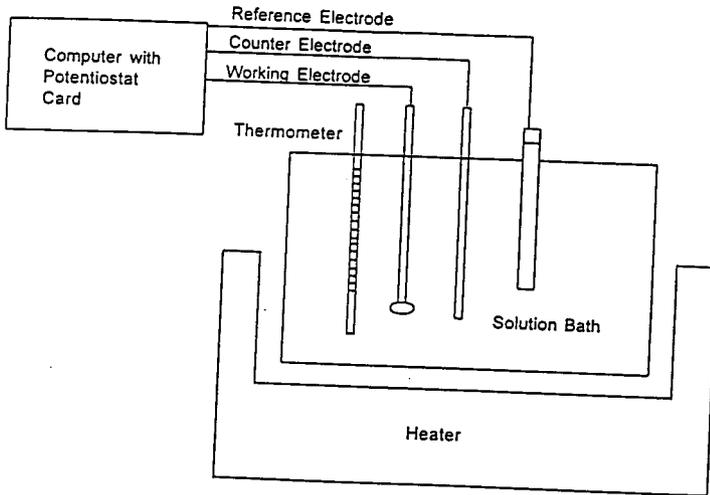


Figure 4. Schematic Showing Test Set-up for the Potentiodynamic Polarization Tests.

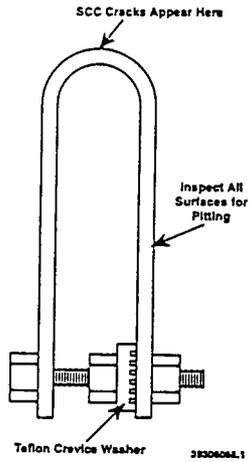


Figure 5. Configuration of the U-bend Specimen Used for Static Corrosion Testing.

4.0 EXPERIMENTAL RESULTS

4.1 SCC TESTING BY SLOW STRAIN RATE

Ondrejcin (1984) used the slow strain rate method to explore the SCC behavior of carbon steels in nuclear waste environments. His data was used to define the safe/unsafe compositional operating regime for carbon steel waste tanks. Ondrejcin's test criterion for susceptibility to SCC was an elongation $\leq 13\%$. SCC was intergranular in the slow strain rate tests. Table 5 shows the slow strain rate data in each of the 24 solutions and the air test for comparison. The elongation values were calculated from the load/displacement data. None of this elongation data meets the Ondrejcin (1984) criterion for susceptibility to SCC. In general, the elongation values were large, close to the value for the air test, implying that there was no SCC taking place in any of these test solutions. The lowest elongation value using the FY 95 test specimens was 17.4% in solution 12. Solution 20 was a replicate of solution 12, and the elongation value in that solution was 18.6%. Solutions 12 and 20 were identical to a solution (0.10 M nitrite, 1.00 M nitrate, and 0.10 M hydroxide) used in the FY 94 slow strain rate test that clearly showed SCC by the Ondrejcin criterion (11.4% elongation). In order to investigate this discrepancy in elongation values between the FY 94 and FY 95 testing, an archival specimen from the FY 94 tests was tested in solution 12 at the usual strain rate of 1.3E-6/sec. This time the elongation value for the FY 94 test specimen was 17.0%, showing good agreement with the 17.4% elongation value found for the FY 95 specimen tested in solution 12. In order to ascertain whether the difference in elongation was due to the strain rate, a test was performed in solution 12 with a FY 95 test specimen at one-fourth the strain rate (3.25E-7/sec) normally used for the testing. The elongation from the test performed with the reduced strain rate was 15.2%, a reduction in elongation but still above the Ondrejcin criterion for SCC. Carbon steel is not known to be strain rate sensitive, so the change in elongation would not be attributed to mechanical effects. The difference in elongation would suggest that additional time in the environment due to the reduced strain rate would lead to enhanced degradation in mechanical properties. The differences between the FY 94 and 95 SCC results raise a serious question about the usefulness of the slow strain rate test method for evaluating the propensity for SCC.

Table 5. Slow Strain Rate Data.

Solution	Ultimate Load, kN	Elongation, %	Relative to air Elongation, %	Reduction in Area, %	Relative to air, % Reduction in
Air	24.9	20.8	100	34.8	100
1	25.1	18.2	77	28.2	81
2	23.6	21.8	92	35.6	102
3	24.6	22.7	105	26.1	75
4	22.2	19.2	101	27.9	80
5	24.9	22.2	119	35.1	101
6	24.9	22.7	121	28.6	82
7	23.7	24.0	108	38.2	110
8	25.4	24.5	104	31.8	91
9	22.9	22.5	101	32.2	93
10	26.2	23.5	95	30.8	89
11	22.8	21.7	97	35.9	103
12	24.5	17.4	93	18.5	53
13	21.4	21.9	104	35.9	103
14	24.8	21.0	95	33.2	95
15	23.5	22.6	99	33.1	95
16	23.6	22.8	99	30.7	88
17	21.2	21.2	112	29.3	84
18	20.9	22.8	111	30.8	89
19	22.4	20.9	97	35.9	103
20	22.6	18.6	90	20.7	59
21	21.3	21.0	112	42.7	123
22	24.2	20.1	90	24.8	71
23	24.8	22.0	109	34.1	98
24	23.9	20.8	119	28.8	83
12*	20.1	17.0	83	10.4	30
12**	23.3	15.2	71	15.5	45

* Test performed with FY 94 specimen in solution 12

** Test performed with a FY 95 specimen at a strain rate of 3.25E-7/sec

SEM photographs of the fracture surfaces at magnifications of 12X and 100X of the slow strain rate specimens are shown in Appendix A. A classic intergranular fracture appearance is not apparent for any of the specimens tested. The fracture surface appearance is not always consistent with complete ductile tearing, however. For example, there is a quasi-cleavage appearance to the fracture surface of the specimen tested a slower strain rate in solution 12, shown in Figure A.27b. Some specimens exhibited a reddish-brown corrosion product on the interior of the fracture surface that was not evident on the edges of the fracture surface. It is hypothesized that during the testing a small amount of the solution had siphoned into the interior of the fracture surface through a small crack in the gage section (implying that a crack opened early in the testing), leading to a fracture appearance as shown in Figure A.11a. Additionally, the FY 95 and FY 94 specimens tested in solution 20 (solution 12), including the specimen tested at the lower strain rate, showed evidence of secondary cracking readily observable at a magnification of 10X. This secondary cracking can be seen in the gage section shown in Figures A.7a, A.9a, A.10a, A.15a, A.21a, A.24a, and A.26a. All except for Figure A.10a represent fracture surfaces of specimens tested in low nitrite/nitrate ratio solutions or the presence of high chloride in the solution. Sludge-washing compositions that lead to secondary cracking are identified in the 1995 Test Matrix, Figure 6. The presence of secondary cracking perpendicular to the applied stress during slow strain rate tests has been used as a criteria for SCC in some environments. This presents a dilemma in how to adequately characterize SCC for slow strain rate tests.

4.2 POTENTIODYNAMIC PITTING TESTING

The current-potential data from the pitting experiments are presented in Appendix B, Figures B.1 through B.24, for each of the twenty-four solutions. The solution composition, open circuit potential (E_{corr}), pitting potential (E_{pit}), and protection potential (E_{prot}) are reported in Table 6. Briefly, a potentiodynamic pitting test is conducted in the following manner:

Starting at the open circuit corrosion potential, the electrochemical potential on the metal specimen is increased in the anodic direction at a constant rate (0.2 mV/s). The potential at the abrupt current increase is known as the pitting potential. In the case of the present tests, the potential scan is reversed at 1.0 V anodic to the open circuit potential, and the voltage is returned to the open circuit value at a rate of 0.2mV/s. When a metal starts to pit, the current increases abruptly, giving a characteristic signature. Once pits initiate and grow, they tend to persist so that the current remains high, causing the formation of a current hysteresis loop. During the reverse scan, the point at which the current decreases and becomes equal or less than the forward scan current is called the protection potential because the growth of the propagating pits is halted. The protection potential is thought to be the lowest potential that permits pitting to initiate; consequently, it has the greatest relevance for predicting pitting propensity for actual service. Figure B.19 illustrates how the pitting and protection potential are defined. At the low current ranges ($\leq 0.1\mu A/cm^2$), the logarithmic current amplifier in the potentiostat becomes noisy and creates the current spikes observed in the current-potential data.

On the basis of E_{prot} , six solutions were found to be capable of leading to pit initiation and propagation, as shown in Table 6. However, these solutions are unlikely to cause pitting under actual field conditions because the E_{prot} was at least 0.5 V anodic (more positive) than the open circuit potential. It would be unlikely that some condition in the tanks would ever result in the electrochemical potential of the tank wall becoming polarized into that regime.

The results from the static tests will be used to confirm the electrochemical results, but this data suggests that the tank waste can be diluted without generating pitting in the immersed tank steel. The other 18 solutions either appear benign to this carbon steel for pitting, or are susceptible to preferential general attack as the potential was increased, as in the case of the four high chloride solutions. Curiously, a small amount of crevice corrosion was observed in almost all cases underneath the polytetrafluorethylene gasket used to protect the electrical contact of the test electrodes.

Table 6. Pitting Experimental Data.

Solutio	Nitrite,	Nitrate,	Hydroxide, M	E_{corr}	E_{pit}	E_{prot}
1	0.03	0.10	0.03	-0.018	NF	NF
2	0.01	0.10	0.03	-0.032	NF	NF
3	0.10	1.00	1.00	-0.095	+0.58	+0.53
4	0.30	1.00	0.10	-0.025	NF	NF
5	0.03	0.30	0.03	-0.044	NF	NF
6	0.03	0.10	0.01	-0.093	NF	NF
7	0.01	0.10	0.10	-0.028	NF	NF
8	0.30	1.00	0.30	-0.039	+0.57	+0.36
9	0.10	0.30	0.03	-0.018	NF	NF
10	0.01	0.10	0.01	-0.054	NF	NF
11	0.10	0.10	0.01	-0.022	NF	NF
12	0.10	1.00	0.10	-0.109	NF	NF
13	0.30	0.30	0.03	-0.038	NF	NF
14	0.10	1.00	0.30	-0.092	NF	NF
15	0.03	0.30	0.30	-0.040	+0.68	+0.58
16	0.03	0.30	0.10	-0.030	+0.74	+0.71
17	0.10	0.30	0.30	-0.041	+0.66	+0.54
18	0.10	0.30	0.10	-0.110	NF	NF
19	0.01	0.10	0.10	-0.049	+0.52	+0.34
20	0.10	1.00	0.10	-0.038	NF	NF
21*	0.025	0.025	0.389	-0.292	NF	NF
22*	0.025	0.393	0.026	-0.121	NF	NF
23*	0.393	0.025	0.026	-0.039	NF	NF
24*	0.393	0.393	0.389	-0.118	NF	NF

NF = Not Found
 * These solutions also contain 0.5 M Chloride

4.3 STATIC TESTS

The static tests were started in March 1995 and terminated in September 1995 after a six month exposure. The specimens were then cleaned, weighed, and the data analyzed. The results are presented in Appendices C, D, E, and F.

Photographs shown in Appendix C were taken of representative specimens from each test solution prior to cleaning. The U-bends and coupons from solutions 1, 9, 11, 13, and 18 exhibited shiny, post-test surfaces in the immersed phase, similar to the pre-test condition of the surface. One solution, solution 11, exhibited a shiny post-test surface in the vapor phase.

Specimens exhibiting this surface condition also had the lowest average corrosion rates, as shown in the weight loss data of Appendix D. Specimens in solutions 1 and 13 exhibited a very thin, blue film in the post-test condition prior to cleaning. The composition of the film was not identified, but appears to be a thin, protective film easily removed with CP-9 (10% HCl with formaldehyde as the inhibitor) cleaning solution. Except for specimens immersed in solution 8 and the specimens in the high chloride solutions, the average uniform corrosion rate was highest for the solutions that had a 10:1 ratio of nitrate to nitrite. The specimens in the solutions that had a 10:1 ratio of nitrate to hydroxide and a 3.3:1 to 1:1 ratio of nitrate to nitrite had the lowest average corrosion rates measured.

The specimens were analyzed and photographed after cleaning in CP-9. Photographs of representative specimens, shown in Appendix E, were added as a visual aid to the interpretation. Measured values for the pitting density, size, and maximum depth, as well as the maximum depth of the crevice attack and waterline attack are listed in tabular form in Appendix F. Weight loss coupons that were immersed in solutions 2, 5, 6, 10, and 22 are shown in Figures E.1, E.3, E.5, E.9, and E.12 because they showed unusual amounts of attack. For example, pronounced crevice attack is visible around the bolt hole in the specimens subjected to solutions 2, 5, 6, 10, and 22. Weight loss specimens from the air/solution interface region from solutions 2, 5, 6, 7, and 10 are shown in Figures E.2, E.4, E.6, E.8, and E.10. These specimens exhibit either moderate pitting or a moderate to heavy amount of waterline attack, or a combination of the two. For comparison, a weight loss specimen immersed in solution 7 with a fairly pristine surface appearance is shown in Figure E.7. This specimen only exhibited light amounts of pitting and crevice attack, and is included for a visual reference point with respect to the specimens that exhibit moderate to heavy attack.

Photographs in Figures E.11 to E.18 were taken of representative specimens exposed to the high chloride solutions. Figure E.11 contains a photograph of a weight loss specimen that was immersed in solution 21 which exhibits a pristine appearance, and was included as a visual reference point. A photograph of a totally immersed weight loss specimen from solution 22 was included in Figure E.12 to show the extent of pitting in the high chloride solution. The pitting in solution 22 was far more extensive, both in area covered and in depth, than for solutions 21, 23, and 24. All of the air/solution interface region specimens (weight loss and U-bend specimens) exhibited catastrophic levels of attack in the vapor phase region at and above the waterline. This can be very clearly seen in Figures E.13, E.14, E.16, E.17, and E.18. The specimen shown in Figure E.13 was accidentally dropped during the cleaning process, and a large chunk of brittle material broke away.

It appears that the corrosion process converted that entire region of metal to oxide. It is interesting to note the vast difference in appearance between totally immersed U-bend specimens, as shown in Figure E.15, and those exposed to the air/solution interface, as shown in Figure E.16. The totally immersed specimen exhibited light amounts of pitting and crevice corrosion, whereas the partially immersed specimen exhibited massive attack at and above the waterline. The attack appears to be focused on the "wicking region" in the vapor phase where the liquid phase is transported upwards by wetting the metal and oxide surface but at the same time is being diluted by downwards movement of condensation.

A tabular summary of the coupon tests observations was combined with the secondary cracking observations (from the slow strain rate tests) in Table 7. Also included is the pH measured for each solution at the conclusion of the static tests. The test solution pH values ranged from 11.52 for solution 11, one of the low hydroxide solutions, to 13.13 for solution 3, which was the only solution with 1.0 M hydroxide. Secondary cracking was observed in slow strain rate specimens tested in solutions 6, 8, 9, 12, 14, 20, and 23 (the specimen in solution 12 was a FY 94 test specimen, but solutions 12 and 20 are replicate solutions). Pitting was described in the table as light, moderate, or heavy, which corresponded to the pit density on the specimen (Light = $2.5E3/m^2$ - $1E4/m^2$, Moderate = $5E4/m^2$, Heavy = $1E5/m^2$). Crevice attack was, in a similar manner, described in the table as light, moderate, or heavy corresponding to the crevice attack area around the bolt hole. It was difficult to identify and measure the contributions to the massive attack on the specimens attributable to pitting and crevice corrosion, as the waterline attack had covered a large area of the specimen. Consequently, the pitting and crevice attack were not described, as above, for chloride-containing solutions 21 through 24 in the table, and the letters "Gr" were substituted to describe the gross general attack found on the specimens. Heavy pitting and crevice attack were noted for the immersed specimens in solution 22, which was a high chloride solution that contained a high concentration ratio of nitrate to nitrite as well as a high concentration ratio of nitrate to hydroxide. The other high chloride solutions contained levels of nitrite and hydroxide comparable to or higher than the nitrate concentration, and light pitting and crevice attack were observed for specimens immersed in these solutions.

A moderate amount of pitting and heavy crevice attack was observed for specimens immersed in solution 6. Additionally, specimens immersed in solutions 1, 2, 5, and 10 also exhibited heavy crevice attack. These solutions all have nitrate concentration levels between 0.1 to 0.3 M, and nitrite and hydroxide concentration levels between 0.01 to 0.03 M. Specimens immersed in the rest of the solutions exhibited only light amounts of pitting and crevice attack, or none at all. The pit density increased moderately for the specimens exposed to the vapor phase of solutions 7, 10, and 17, and remained at a moderate amount for the specimens exposed to the vapor phase of solution 6. Crevice attack was moderate for specimens exposed to the vapor phase of solutions 2, 5, 7, and 12. Waterline attack was heavy for the specimens exposed to solutions 5 and 10, and moderate for the specimens exposed to solutions 1, 2, 6, and 12. With the exception of solutions 7, 12, and 17, the solutions again all have nitrate concentration levels between 0.1 to 0.3 M, and nitrite and hydroxide concentration levels between 0.01 to 0.03 M. Specimens exposed to the vapor phase in the rest of the solutions exhibited only light amounts of pitting and crevice attack, or none at all.

The maximum depth of pitting, crevice attack, and waterline attack is shown in bar charts for the twenty-four solutions in Figures 7 through 11. Sludge-washing compositions that lead to pitting, crevice, or waterline attack depth ≥ 0.05 mm were identified in the 1995 Test Matrix, Figure 12. Pitting depths, in general, were <0.5 mm for specimens tested in both the immersed condition as well as the vapor phase of most of the solutions. This was not true for solutions 1, 5, 6, and 10, as well as for the high chloride solutions. The depth of the crevice attack was greater than for the pits in all solutions where both were present. The occurrence and density of pitting was greater for specimens in the vapor phase as compared to the immersed specimens, but the pits were often very shallow. Waterline attack was present on the specimens in the vapor phase for most of the solutions, with depths comparable to the depths of the crevice attack. A comparison of the corrosion coverage (pitting density, crevice attack area, or waterline attack area) versus the depth of the attack is given in Table 8. There appears to be little correlation between the density of the attack and the depth of the attack for these solutions.

Table 7. Visual Observations From Static Tests and Slow Strain Rate Tests.

Solution	pH	Immersed Specimen, Average Corrosion Rate, mm/y	Secondary Cracking	Pitting - Immersed	Crevice - Immersed	Pitting - Vapor	Crevice - Vapor	Waterline Attack - Vapor
1	12.10	1.5E-3		L	H	L	L	M
2	12.13	2.5E-3		L	H	L	M	M
3	13.13	5.0E-3						
4	12.46	1.4E-3				L	L	L
5	12.09	2.2E-3		L	H	L	M	H
6	11.70	1.6E-3	X	M	H	M	L	M
7	12.64	2.0E-3		L	L	M	M	L
8	12.85	2.7E-3	X					
9	12.02	2.2E-4	X	L	L	L	L	L
10	11.85	7.7E-3		L	H	M	L	H
11	11.52	1.1E-5			L	L	L	L
12	12.46	1.6E-3	X*	L	L	L	M	M
13	12.02	2.0E-4				L		
14	12.88	2.6E-3	X			L	L	L
15	13.00	4.6E-3				L	L	L
16	12.63	3.3E-3			L	L	L	L
17	12.99	1.1E-3				M	L	
18	12.54	1.7E-4				L	L	
19	12.67	2.2E-3		L	L	L	L	L
20	12.50	2.1E-3	X	L		L	L	L
21	13.08	6.4E-3			L	Gr	Gr	Gr
22	12.61	2.4E-2		H	H	Gr	Gr	Gr
23	12.75	3.8E-3	X	L	L	Gr	Gr	Gr
24	12.93	4.6E-3		L	L	Gr	Gr	Gr

shaded cells highlight areas of concern in the data set
 * secondary cracking was found in the FY 94 specimen tested in solution 12
 X = identified on slow strain rate specimens tested in this solution
 L = light, M = moderate, H = heavy, (indicates pit density or crevice attack area)
 Gr = not identified due to gross general attack in this region

Table 8. Comparison of Density of Attack With Depth of Attack.

Solution	Pitting - Immersed	Crevice - Immersed	Pitting - Vapor	Crevice - Vapor	Waterline Attack - Vapor
1	L	H	L	L	M
2	L	H	L	M	M
3					
4			L	L	L
5	L	H	L	M	H
6	M	H	M	L	M
7	L	L	M	M	L
8					
9	L	L	L	L	L
10	L	H	M	L	H
11		L	L	L	L
12	L	L	L	M	M
13			L		
14			L	L	L
15			L	L	L
16		L	L	L	L
17			M	L	
18			L	L	
19	L	L	L	L	L
20	L		L	L	L
21		L	Gr	Gr	Gr
22	H	H	Gr	Gr	Gr
23	L	L	Gr	Gr	Gr
24	L	L	Gr	Gr	Gr

Cell shaded represent pitting, crevice, or waterline depth ≥ 0.05 mm
 L = light, M = moderate, H = heavy, (indicates pit density or crevice attack area)
 Gr = not identified due to gross general attack in this region

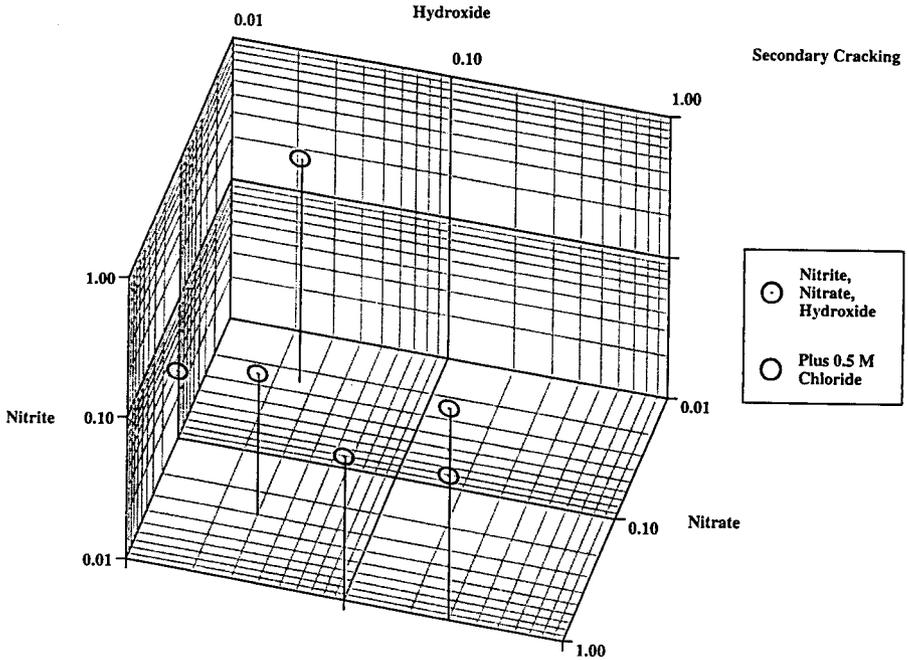


Figure 6. Sludge-Washing Compositions That Led to Secondary Cracking in 1995 Test Matrix.

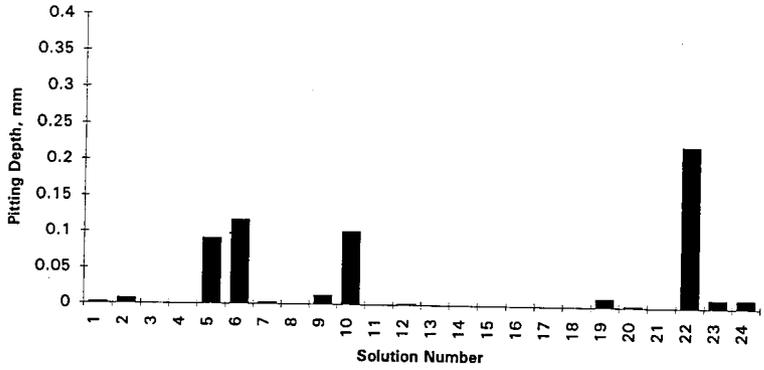


Figure 7. Maximum Pit Depth for Specimens Immersed in Solutions.

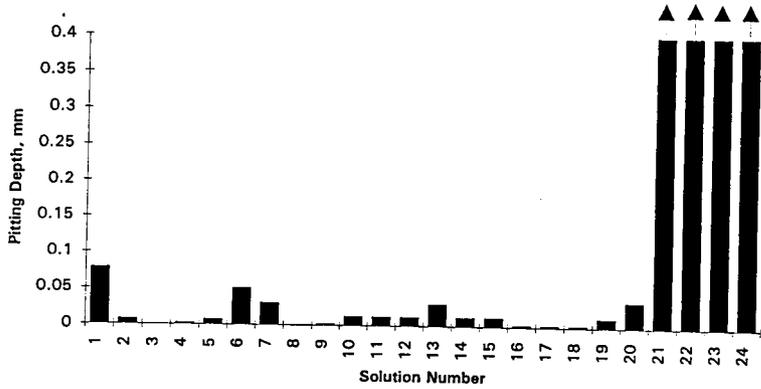


Figure 8. Maximum Pit Depth for Specimens in Vapor Phase.

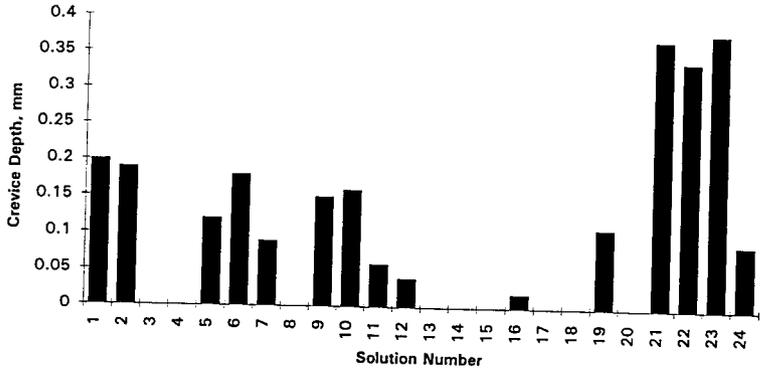


Figure 9. Maximum Depth of Crevice Attack in Immersed Specimens.

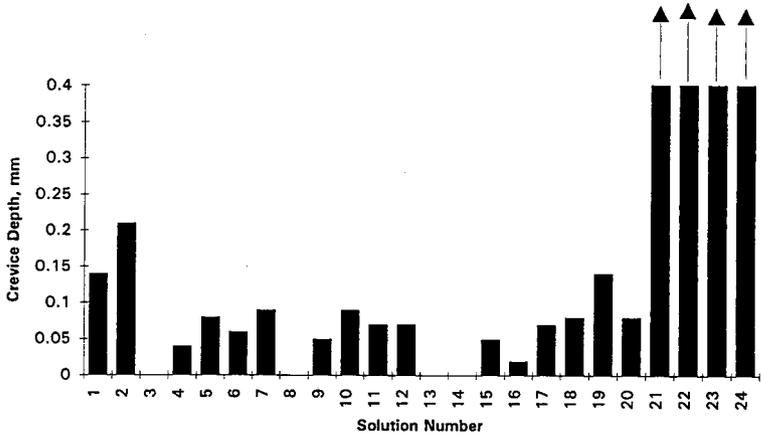


Figure 10. Maximum Depth of Crevice Attack in Vapor Phase Specimens.

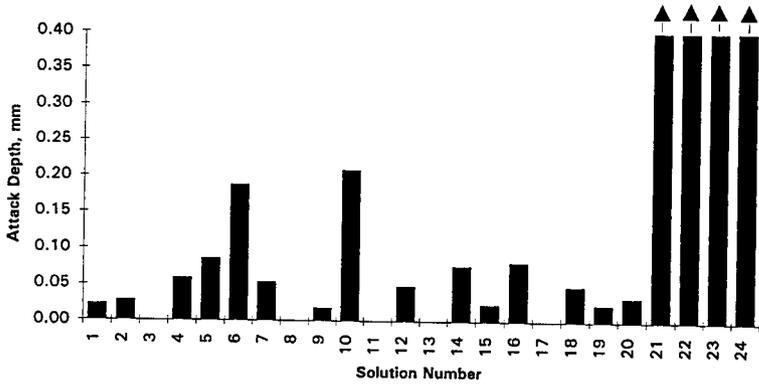


Figure 11. Maximum Depth of Waterline Attack in Vapor Phase Specimens.

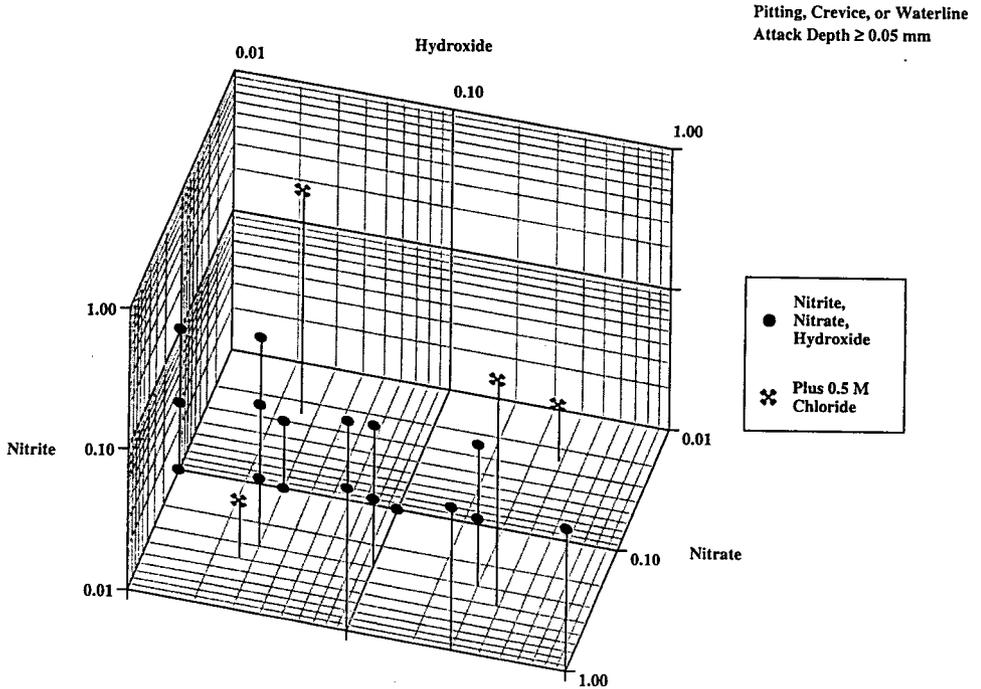


Figure 12. Sludge-Washing Compositions That Led to Pitting, Crevice, or Waterline Attack ≥ 0.05 mm in the 1995 Test Matrix.

5.0 DISCUSSION

As in FY 94, three types of corrosion tests (static coupon tests, slow strain rate tests, and electrochemical tests) were performed in FY 95 to assess the susceptibility of ASTM A-515 Grade 60 carbon steel to failure by corrosion mechanisms. Whereas, the FY 94 testing was focused on scoping studies on the effects of dilute solutions containing hydroxide, nitrate and nitrite, the FY 95 testing was more tightly focused on (1) better parametrizing a troublesome FY 94 compositional regime, (2) enlarging the compositional regime to higher values of nitrate and nitrite, and (3) include the effects of chlorides which exist in several Hanford waste tanks. The specimens were tested in a statistically designed test matrix of twenty-four solutions at 93C in order to more completely evaluate the dilute waste regime. Following a six month exposure, the specimens were examined to determine their susceptibility to uniform corrosion, stress corrosion cracking, pitting, crevice corrosion, and waterline attack.

5.1 EFFECTS OF CHLORIDES

ASTM A-515 was very susceptible to various forms of localized corrosion (pitting, crevice, and waterline attack) in the high chloride solutions. Attack at and above the waterline was so pronounced (complete penetration of the specimen) that it was difficult to uniquely identify the contributions made by pitting, crevice, and uniform corrosion. This behavior is identified in Table 7 by the shaded cells for the vapor phase observations and the letter "Gr" indicating gross general attack. The greatest attack is above the waterline in a "wicking region" where the solution wicked upward by the porous oxide film is diluted by condensation. Thus, the attacked region is probably exposed to a diluted solution composition compared to what exists in the liquid phase. As the attack progresses and the oxide thickens, the attacked region will advance higher above the liquid level. The key insight to this phenomenon is that the totally immersed specimens had very little attack. Operation of the tanks within this range of process chemistry is not recommended due to the severe attack observed in this experimental series. Because the tests performed with high chloride concentrations were intended as scoping tests to look at the behavior of carbon steel tank material in simulated tank chemistries, information is only available for low chloride solutions (solutions 1 - 20) and high chloride solutions (21 - 24). The behavior of the carbon steel at intermediate chloride concentrations or whether there exists a threshold concentration for this chloride effect cannot be deduced from this study. Chlorides appeared to have no effect on SCC.

5.2 PITTING AND CREVICE CORROSION

Pitting was observed on the specimens from many of the solutions, but as shown in Table 8 and in the tables in Appendix F, many of the pits were shallow and small in area. Crevice corrosion and waterline attack presented more of a problem as far as depth of attack and area of attack for many of the specimens, especially in the vapor phase. This corresponded to penetration rates from crevice attack of up to 0.38 mm/y (0.19 mm over 6 mo) for specimens immersed in solution 2 and 0.42 mm/y (0.21 mm over 6 mo) for specimens in the vapor phase of solution 2. Similar penetration rates were found for waterline attack, with up to 0.42mm/y (0.21 mm over 6 mo) measured for specimens in solution 10. At these rates, a 12.7 mm (1/2-in.) steel tank wall would be penetrated in 30 years. Sludge washing operations should only expose the tank to these chemistries for under a year, so penetration due to localized corrosion processes is not expected to cause failure under these circumstances. Operation of the tanks under these chemistries for long periods of time, >30 years, would not be advisable due to the risk of through-wall penetration.

The potentiostatic polarization curves suggest that there is a propensity for pitting for certain potential ranges for immersed specimens in the dilute tank waste chemistry. The electrochemical potential at which pitting could occur, however, is too anodic for pitting to be found in the field, and this was confirmed by the static tests discussed in this report. Although there was a pitting potential identified for solutions 3, 8, 15, 16, 17, and 19, pitting was only observed on specimens tested in solution 19 and only light pitting was observed in that solution chemistry. The experimental results follow the same trend as the pitting tests in a dilute waste chemistry regime carried out at the Savannah River Laboratory (Zapp 1988a, 1988b, 1989a, 1989b). Both studies indicate pitting is associated with a low nitrite/nitrate ratio, although pitting was not observed for all solutions containing the low nitrite/nitrate ratio.

5.3 UNIFORM CORROSION

The uniform attack data for the totally immersed specimens is shown in Table 7. Except for the chloride-containing solutions, all the uniform attack rates are below $5.1E-3$ mm/y (0.2 mpy), making this mode of degradation unimportant. Two of the chloride solutions resulted in higher rates, but the localized attack associated with the chloride solutions dwarfs any uniform attack problems.

5.4 STRESS CORROSION CRACKING

All of the FY 95 slow strain rate (SSR) tests had elongations greater than Ondrejcin's criterion of $\leq 13\%$ elongation for SCC. In other words, none of the 24 solutions demonstrated an ability to cause SCC of ASTM A-515 carbon steel. Examination of the fracture surfaces of the slow strain rate specimens did not definitively indicate SCC for any of the solution chemistries, but areas exist on the surfaces of some specimens that differ from the appearance of ductile failure. However, there were some disturbing observations in the test data that leads one to believe that the SSR technique is not adequately conservative for predicting SCC behavior:

1. Secondary cracking was noted on the gage lengths perpendicular to the applied stress for specimens that were tested in seven solutions: 6, 8, 9, 12, 14, 20, and 23.
2. Solutions 12 and 20 indicated no SCC by the Ondrejcin criterion, but these were duplicates of a solution (#2) that indicated SCC (11% elongation) in the FY 94 testing. When the strain rate was decreased by 1/4, the elongation decreased but was still above the Ondrejcin criterion.

Secondary cracking on the slow strain rate specimens also occurred, with one exception, for solutions with either a 10:1 ratio of nitrate to nitrite or a 10:1 ratio of both nitrate to nitrite and nitrate to hydroxide. The exception was solution 6, which has a low concentration of nitrate with a 3.3:1 ratio of nitrate to nitrite and 10:1 ratio of nitrate to hydroxide. The specimens in the solutions that had a 10:1 ratio of nitrate to hydroxide and a 3.3:1 to 1:1 ratio of nitrate to nitrite had the lowest average corrosion rates measured.

Determination of SCC susceptibility is not always straightforward, and often shallow SCC penetrations are difficult to interpret in SEM photographs. Shallow penetrations are associated with borderline SCC conditions between those that cause severe SCC and those that cause no SCC (Payer et al. 1977). In addition, other factors that measure the ductility of the specimen, such as elongation and reduction of area, are considered in conjunction with the fracture surface appearance to determine SCC susceptibility. Another feature that contributes to the confirmation of SCC susceptibility is the presence of secondary cracking perpendicular to the applied stress along the gage length. Additionally, the severity of SCC is a function of the strain rate. Payer et al. (1975) suggested that there exists a critical range of strain rate for which the severity of SCC is at a maximum. Too high a strain rate will result in a ductile failure of the specimen from mechanical overload, even without the effect of environmental effects. Too slow of a strain rate will allow repassivation of the crack tip, and will suppress the SCC (Payer et al. 1975). The incidence of secondary cracking was noted as a suspicious finding, and it would be recommended to avoid such chemistries during the sludge washing operation as a conservative measure.

Variations in test data from FY 94 when compared to data in the current year's tests may also result from minor changes in the material chemistry of the specimens. Corrosion susceptibility has been found to differ for minor variations of the levels of constituents (such as sulfur and phosphorus), even within the same ASTM specification and grade of a material. It is not entirely clear how much variation in corrosion susceptibility can be expected from slight changes in the minor constituents of the carbon steel. In the absence of a such a correlation, the best results can be obtained by procuring material for corrosion testing that is as close to the tank steel chemistry specifications as is reasonably possible. Waste tanks at Hanford were constructed with older steels that are "dirty" compared to modern steels (modern steels were used in this testing program). Older steels probably contained sulfur levels of about 0.02 wt% and phosphorus levels of about 0.013 wt% (Schwenk and Scott 1996). Steels used for specimens in FY 94 and FY 95 testing contained 0.013 wt% and 0.015 wt% sulfur, respectively, and 0.023 wt% and 0.008 wt% phosphorus, respectively. Yield stress values for the tank steel were reported to average 303 MPa compared to values of 405 MPa and 341 MPa reported for the FY 94 and FY 95 specimens respectively. Repeated attempts to procure representative "dirty" steels from steel mills did not meet with success and no archival tank material was located, so the available steel lots with the highest levels of sulfur and phosphorus were purchased for each year's testing. Tests performed with the "cleaner" steels may not be adequately conservative to assess the corrosion susceptibility due to the enhanced susceptibility of the "dirty" steels to environmental degradation. Therefore, some error is introduced into the testing by using "cleaner" steels, but solution chemistries that indicate corrosion problems for the "cleaner" steels should certainly be avoided in the tank waste environment that contains the "dirtier" steels.

6.0 RECOMMENDATIONS FOR FUTURE WORK

Corrosion testing that has been performed in FY 94 and FY 95 to support sludge washing operations has identified compositional regimes that should be avoided during tank dilution. An important question remains, however, about how well the "cleaner" steels model the corrosion susceptibility of the "dirtier" steels that the tanks were fabricated from. In addition, a scoping study on the effects of chloride on the susceptibility of the tank steel to corrosion has produced unexpectedly high levels of corrosive attack on the test specimens. The chloride level that was chosen for the tests was considered an upper bound for the chloride levels in the Hanford waste tanks (Certa et al. 1993), and a more likely concentration of chloride in the tanks would fall somewhere between the 0.5 M and the 30 mg/L extremes used in this round of testing. The following recommendations are made for future work:

1. Additional testing should be performed to assess the levels of chloride that lead to pronounced levels of attack, and identify a threshold level, if one exists, to operate the process chemistry below.

2. It is the opinion of the authors that every attempt should be made to procure "dirty" steels that are more representative of the actual tank steel chemistry. Procurement of sufficiently "dirty" steels for future tests may require a custom mill run to specifically alloy the steel, procurement of archival materials used in tank fabrication, or an exhaustive search by a materials vendor. The first suggestion may be prohibitively expensive, the second suggestion has been attempted with little success, and the third suggestion seems like the reasonable option at this time.
3. The experimental results should be evaluated by a statistician.

7.0 CONCLUSIONS

Specimens of A515 steel were tested in solutions representative of anticipated sludge-wash chemistries using the slow strain rate method, electrochemical testing, and static testing using U-bends and corrosion test coupons. The following conclusions were obtained from the experimental results:

1. The ductility of many of the specimens, as measured by reduction of area, was slightly lower in aqueous tank chemistries, on average, than in air. The effect of environment of elongation varied from +3.7% to -3.4%. The elongations for the high chloride specimens were uniformly high.
2. The observed small decrease in ductility could not be unambiguously associated with SCC, as there was no definitive change in fracture morphology from microvoid coalescence to inter- or transgranular fracture. For this reason, the decrease in ductility may be associated with another, more benign, embrittlement mechanism. Secondary cracks were found in the gage lengths of some specimens, however, which would indicate a propensity towards SCC.
3. The mechanical behavior of the tank steel was affected by the strain rate, with those specimens tested at the lowest strain rate exhibiting the lowest ductility. This strain-rate dependence indicates that the mechanism responsible for the observed embrittlement is environmental, rather than mechanical. There may exist a critical strain rate for this material for which this material is highly susceptible to SCC that has not been evaluated.
4. Although a propensity for pitting was indicated in six test solutions, the electrochemical potential at which pitting could occur was too anodic for pitting to be expected to occur in the field. This was, for five of the six solutions, confirmed by the pitting observed in the static tests. Pitting was observed for many of the solution chemistries, but pit depth was <0.05 mm for most of the observed pits.

5. Crevice corrosion was observed on the specimens for many of the solution chemistries in the immersed phase and most of the solution chemistries in the vapor phase, with a crevice depth of up to 0.21 mm established over a six month period. Waterline attack was also observed for most solution chemistries, and with measured depths comparable to the crevice attack.
6. Severe corrosion attack was observed for the air/solution interface specimens tested in the high chloride solutions, solutions 21 through 24. There was a significant amount of metal loss associated with the corrosion processes, and the area of greatest attack was at and just above the waterline. The severe corrosion left the specimens in a brittle state, as was evidenced by the fracture of a specimen that was inadvertently dropped during the cleaning operations.
7. Recommendations are made to avoid the solution chemistries during sludge washing that produce secondary cracking during slow strain rate testing or gross general attack as that observed in the high chloride solutions. Heavy crevice, pitting, or waterline attack has been observed for some of the solution chemistries, but through-wall penetration for the deepest attack is calculated at 30 years. Although the depth of attack can be considered significant, sludge washing operations are only expected to keep the tanks in the modified chemistry for less than one year, so failure due to these corrosion processes is not expected.
8. A discrepancy was noted between this and earlier work (Danielson and Bunnell 1994) with regard to the SSR results. It is suspected that the lower ductility observed in the earlier work is due to higher sulfur and phosphorus contents of the material used previously. If this theory is correct, it would indicate that the current tests may be nonconservative in evaluating the performance of the double-shell tank steels, which were made using production techniques that are no longer used. On the other hand, the stress-relieving heat treatment used in the current work would tend to make the material more susceptible to SCC, resulting in more conservative test results.

8.0 REFERENCES

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APPENDIX A: SEM PHOTOGRAPHS OF SLOW STRAIN RATE SPECIMEN FRACTURE SURFACES

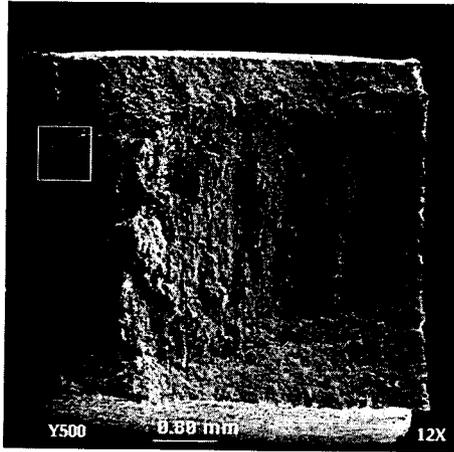


Figure A.1a. Fracture of Specimen from Air

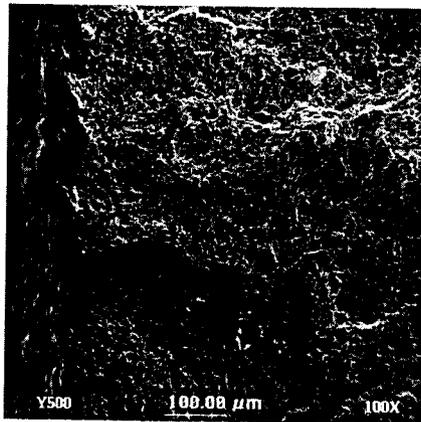


Figure A.1b. Higher Magnification of Fracture Surface

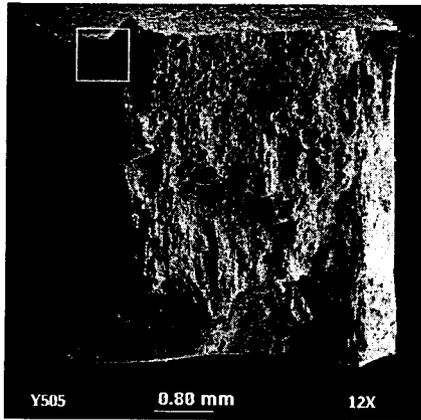


Figure A.2a. Fracture of Specimen from Solution 1

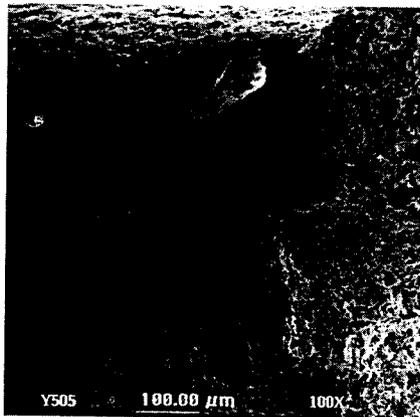


Figure A.2b. Higher Magnification of Fracture Surface

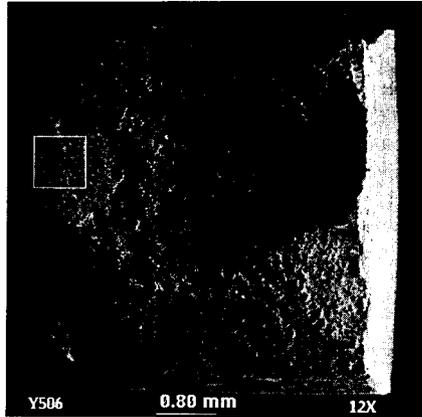


Figure A.3a. Fracture of Specimen from Solution 2

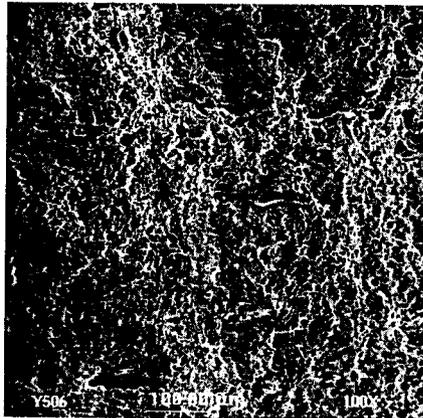


Figure A.3b. Higher Magnification of Fracture Surface

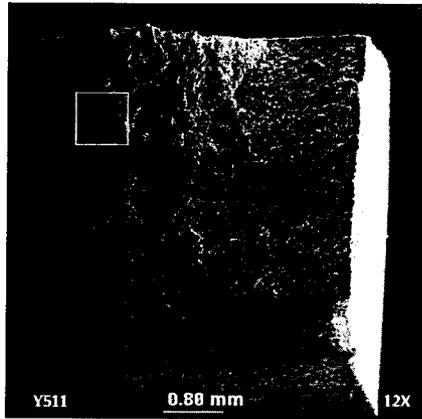


Figure A.4a. Fracture of Specimen from Solution 3

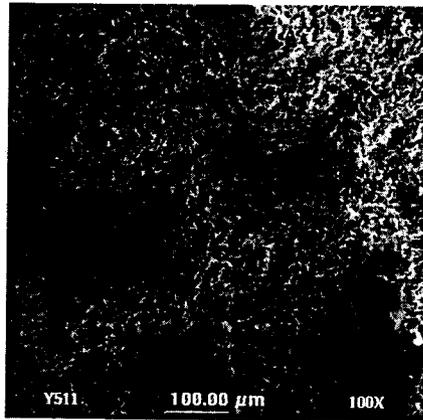


Figure A.4b. Higher Magnification of Fracture Surface

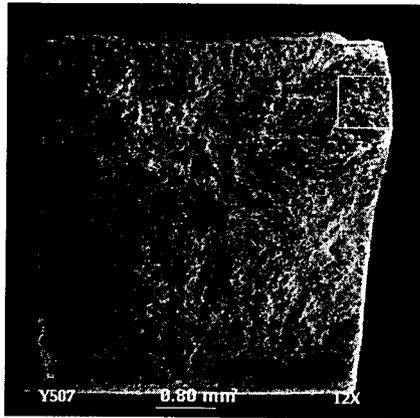


Figure A.5a. Fracture of Specimen from Solution 4

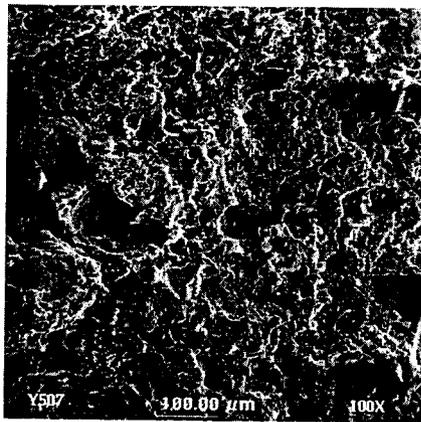


Figure A.5b. Higher Magnification of Fracture Surface

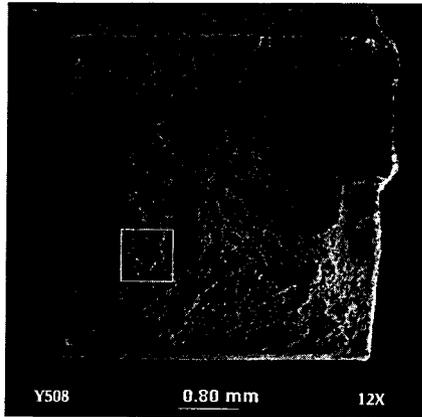


Figure A.6a. Fracture of Specimen from Solution 5

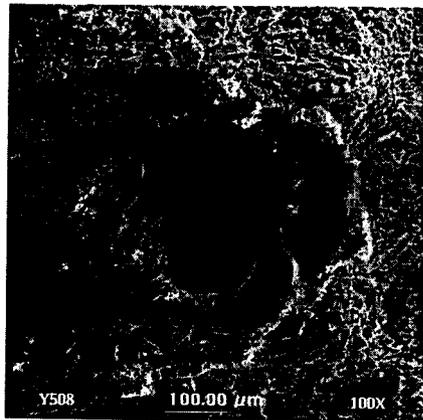


Figure A.6b. Higher Magnification of Fracture Surface

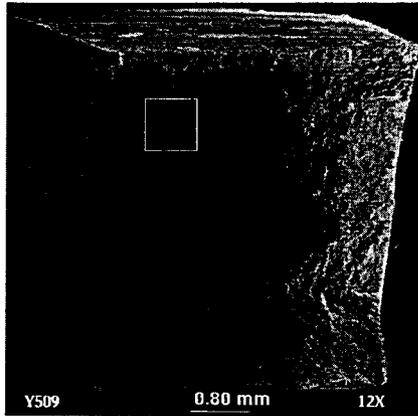


Figure A.7a. Fracture of Specimen from Solution 6

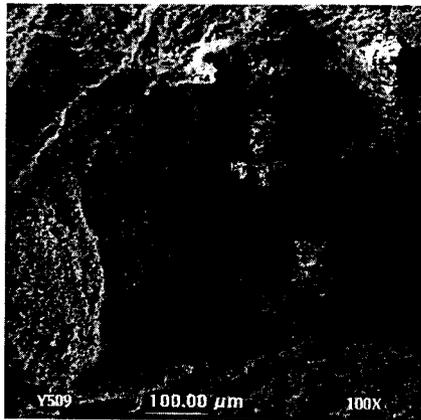


Figure A.7b. Higher Magnification of Fracture Surface

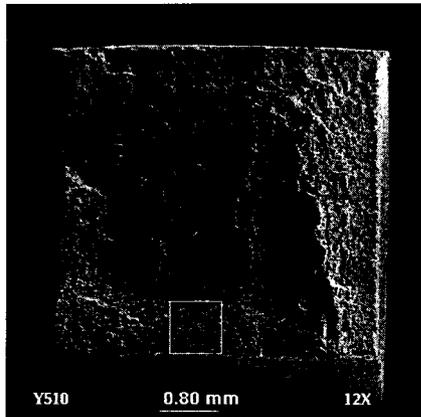


Figure A.8a. Fracture of Specimen from Solution 7

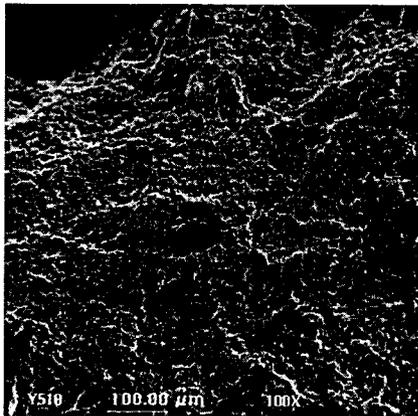


Figure A.8b. Higher Magnification of Fracture Surface

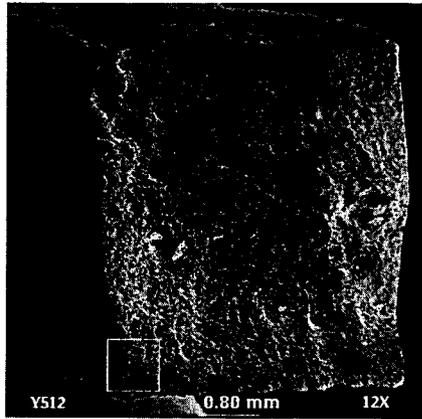


Figure A.9a. Fracture of Specimen from Solution 8

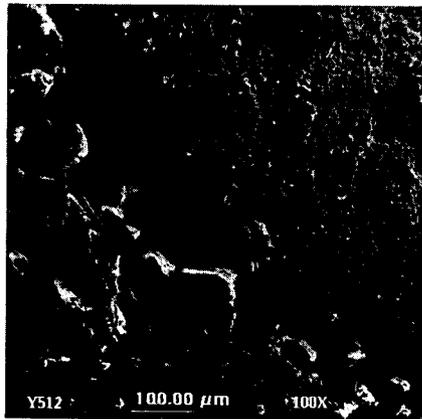


Figure A.9b. Higher Magnification of Fracture Surface

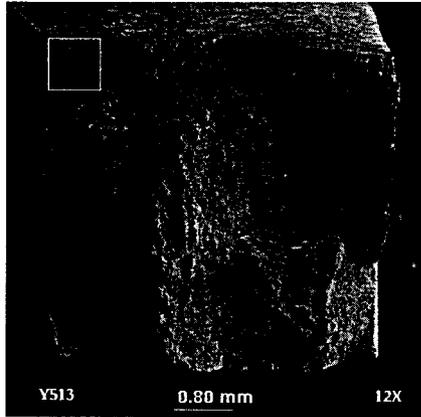


Figure A.10a. Fracture of Specimen from Solution 9

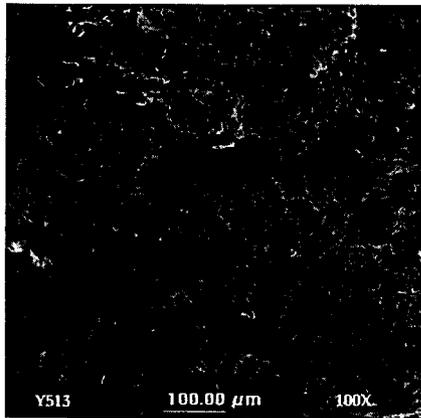


Figure A.10b. Higher Magnification of Fracture Surface

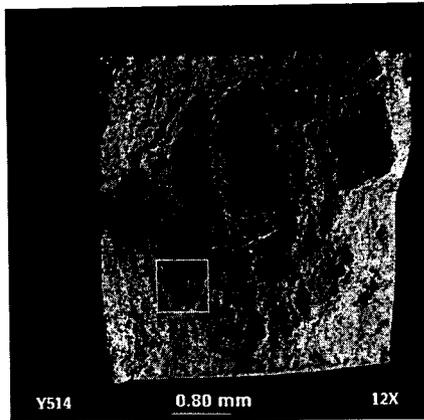


Figure A.11a. Fracture of Specimen from Solution 10



Figure A.11b. Higher Magnification of Fracture Surface

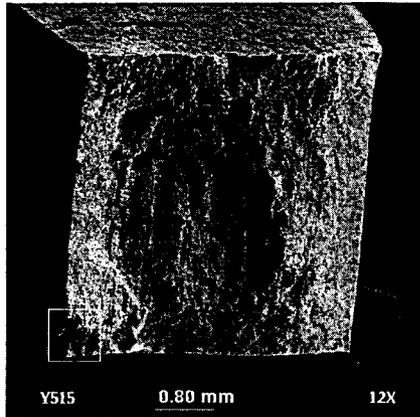


Figure A.12a. Fracture of Specimen from Solution 11

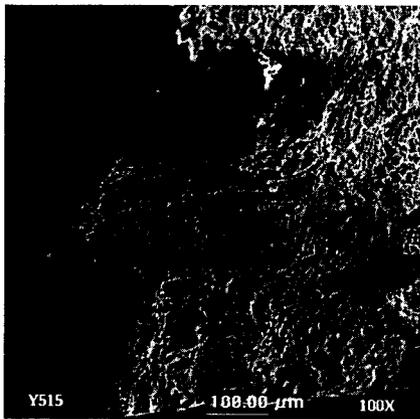


Figure A.12b. Higher Magnification of Fracture Surface

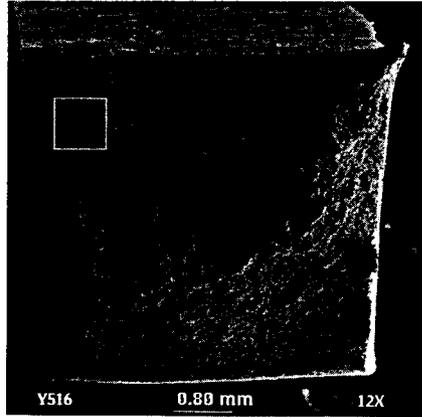


Figure A.13a. Fracture of Specimen from Solution 12

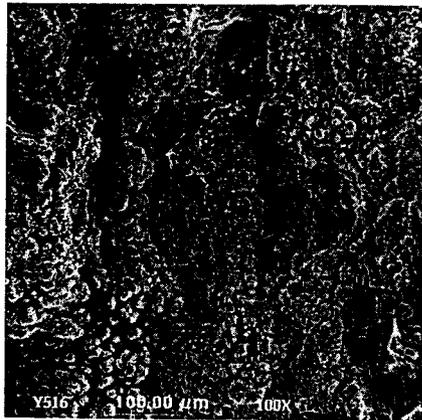


Figure A.13b. Higher Magnification of Fracture Surface

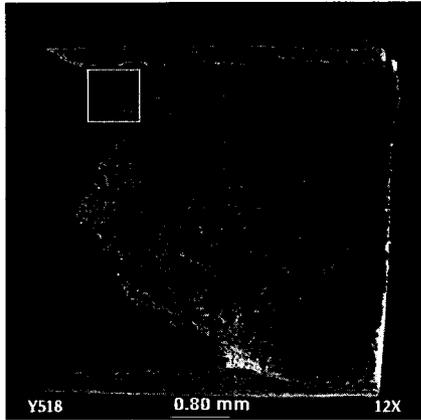


Figure A.14a. Fracture of Specimen from Solution 13

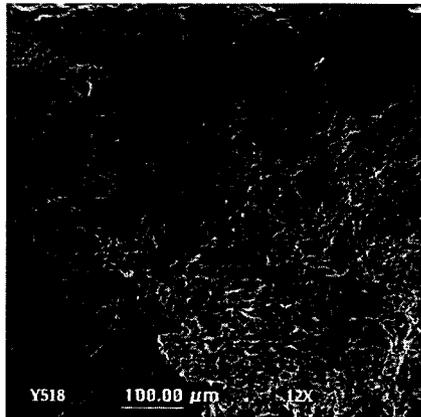


Figure A.14b. Higher Magnification of Fracture Surface

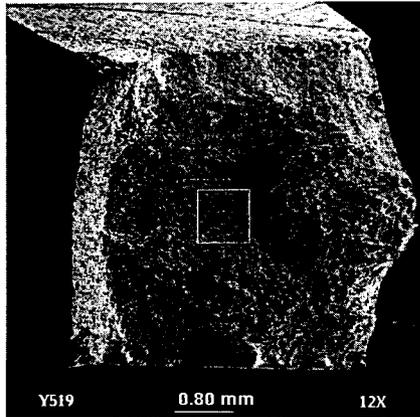


Figure A.15a. Fracture of Specimen from Solution 14

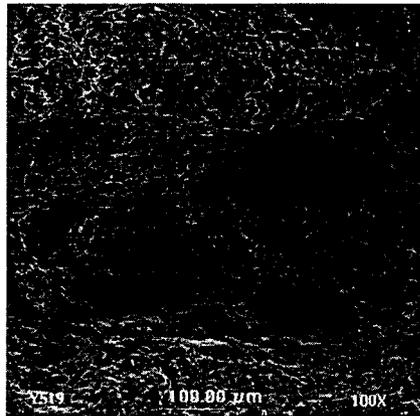


Figure A.15b. Higher Magnification of Fracture Surface

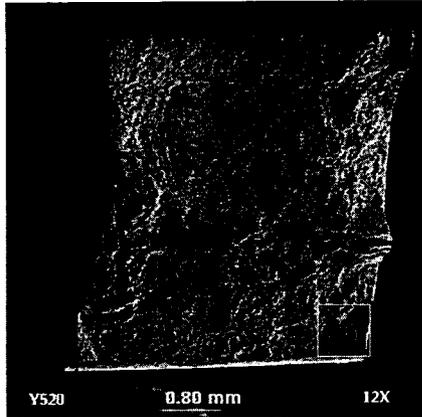


Figure A.16a. Fracture of Specimen from Solution 15

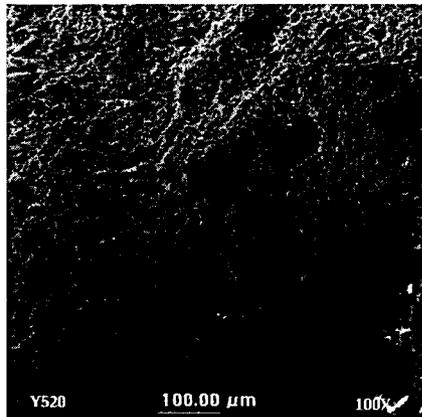


Figure A.16b. Higher Magnification of Fracture Surface

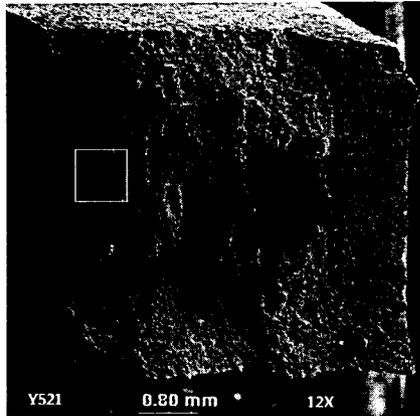


Figure A.17a. Fracture of Specimen from Solution 16

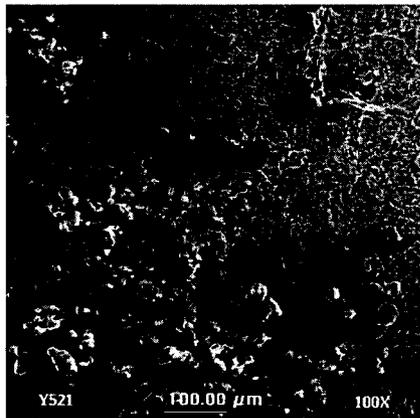


Figure A.17b. Higher Magnification of Fracture Surface

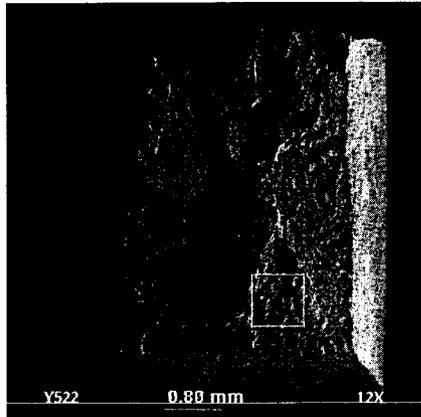


Figure A.18a. Fracture of Specimen from Solution 17

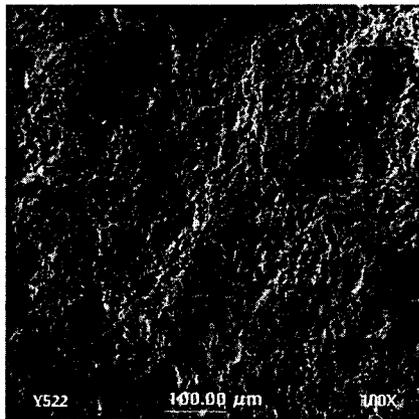


Figure A.18b. Higher Magnification of Fracture Surface

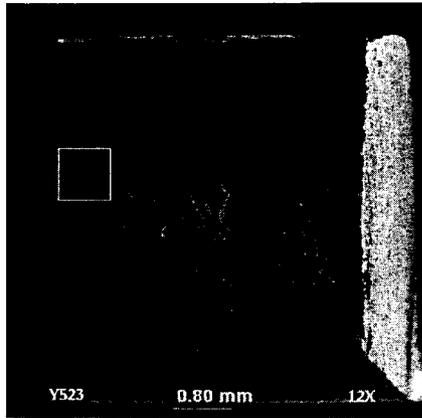


Figure A.19a. Fracture of Specimen from Solution 18

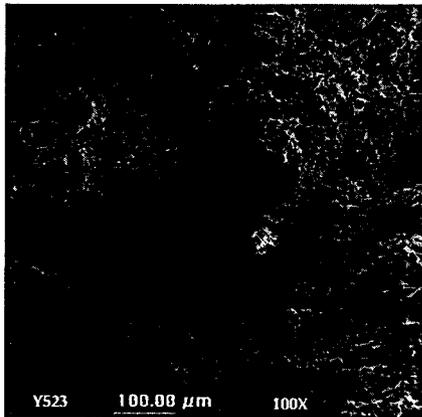


Figure A.19b. Higher Magnification of Fracture Surface

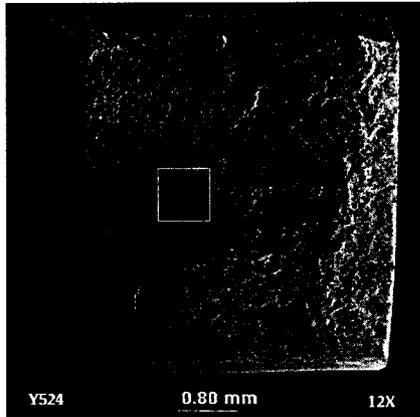


Figure A.20a. Fracture of Specimen from Solution 19

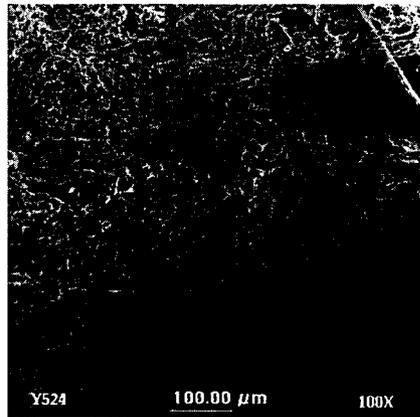


Figure A.20b. Higher Magnification of Fracture Surface

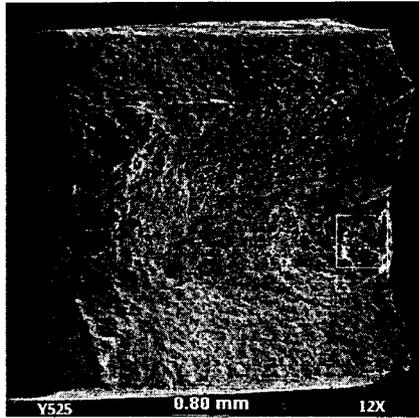


Figure A.21a. Fracture of Specimen from Solution 20

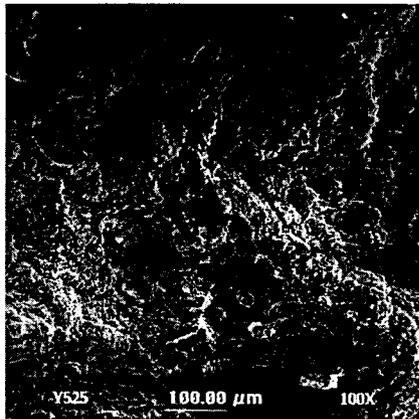


Figure A.21b. Higher Magnification of Fracture Surface

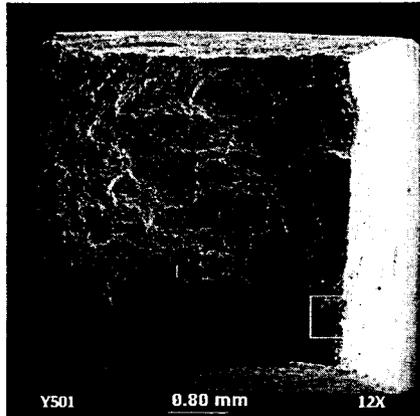


Figure A.22a. Fracture of Specimen from Solution 21

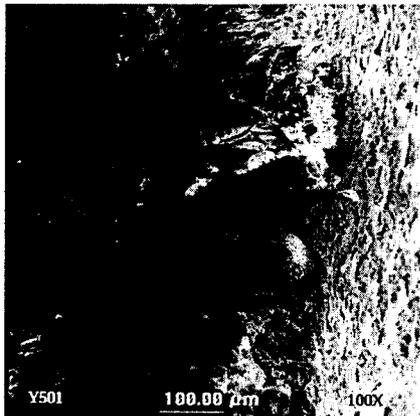


Figure A.22b. Higher Magnification of Fracture Surface

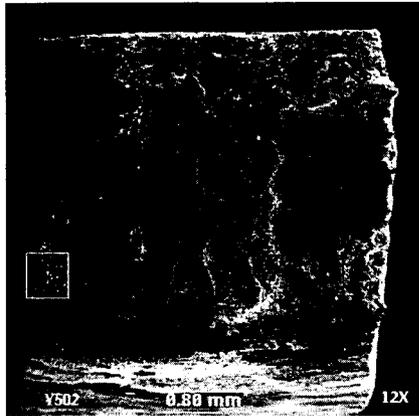


Figure A.23a. Fracture of Specimen from Solution 22

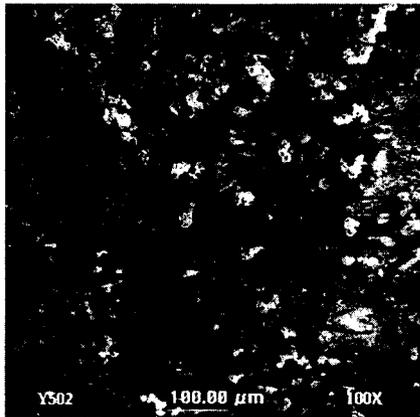


Figure A.23b. Higher Magnification of Fracture Surface

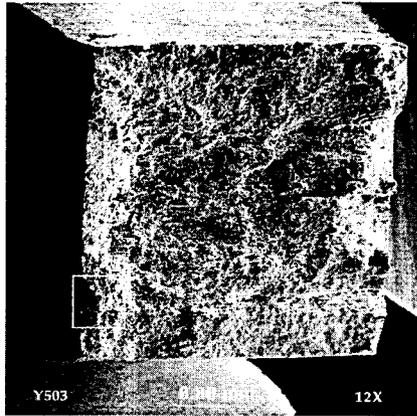


Figure A.24a. Fracture of Specimen from Solution 23

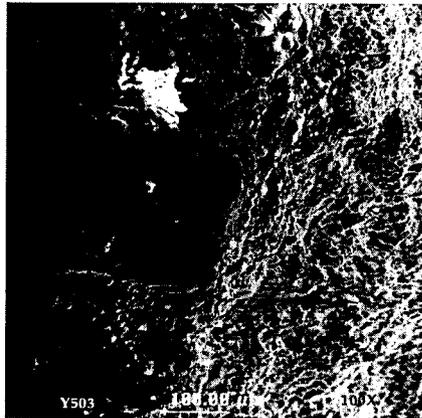


Figure A.24b. Higher Magnification of Fracture Surface

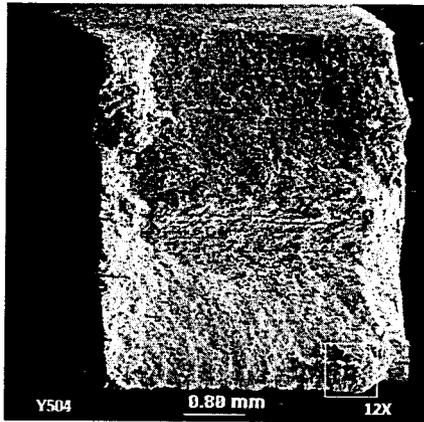


Figure A.25a. Fracture of Specimen from Solution 24

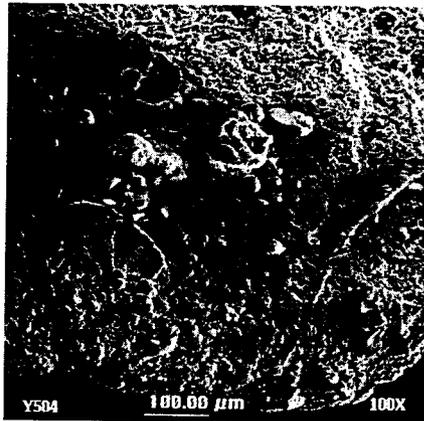


Figure A.25b. Higher Magnification of Fracture Surface

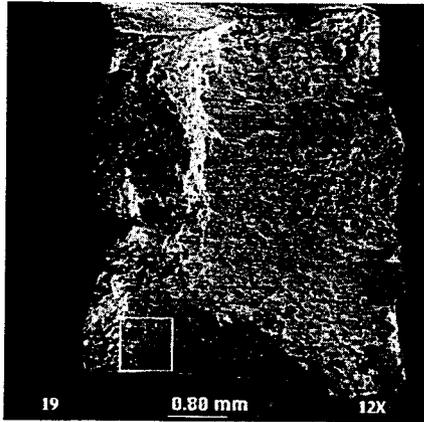


Figure A.26a. Fracture of FY94 Specimen from Solution 12

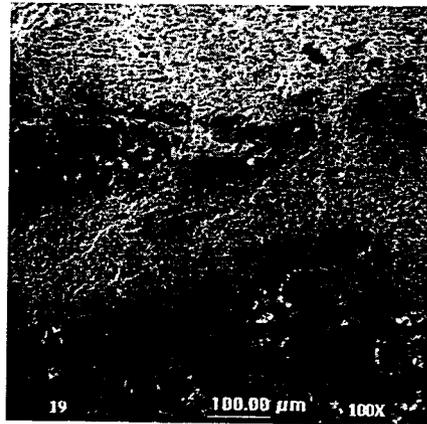


Figure A.26b. Higher Magnification of Fracture Surface

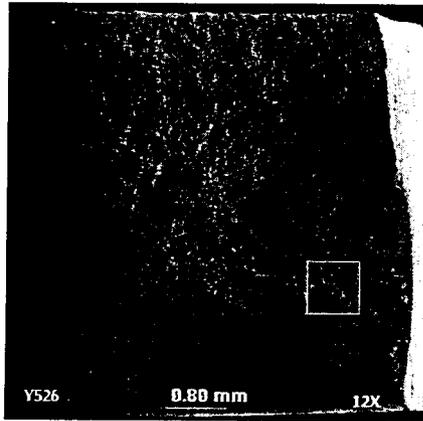


Figure A.27a. Fracture of Specimen from Solution 12, Slower Strain Rate

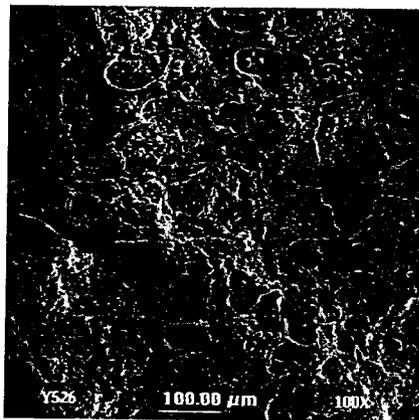


Figure A.27b. Higher Magnification of Fracture Surface

APPENDIX B: POTENTIODYNAMIC SCANS

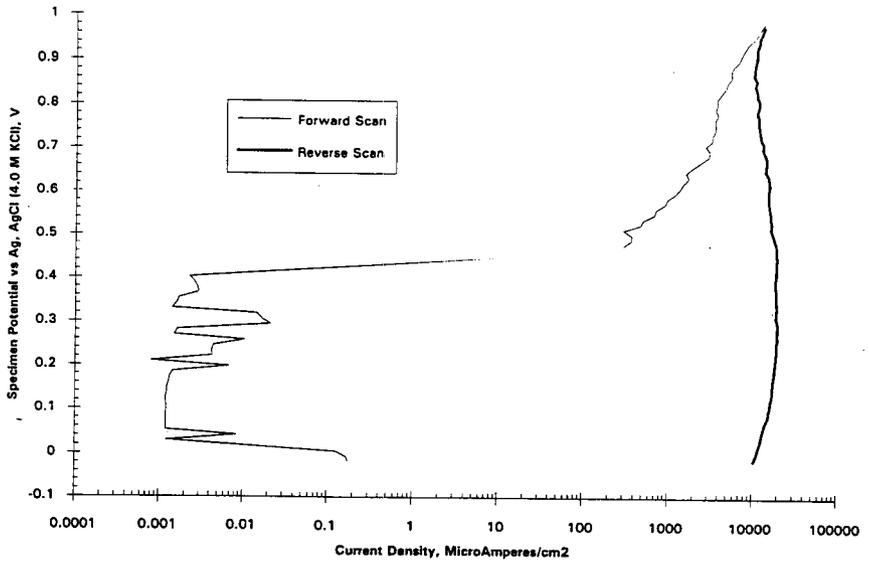


Figure B.1. Potentiodynamic Scan in Solution 1

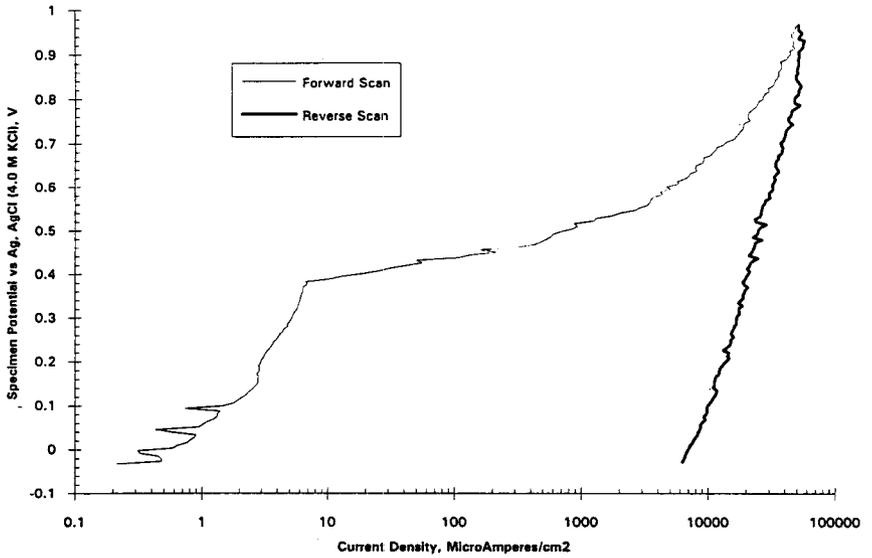


Figure B.2. Potentiodynamic Scan in Solution 2

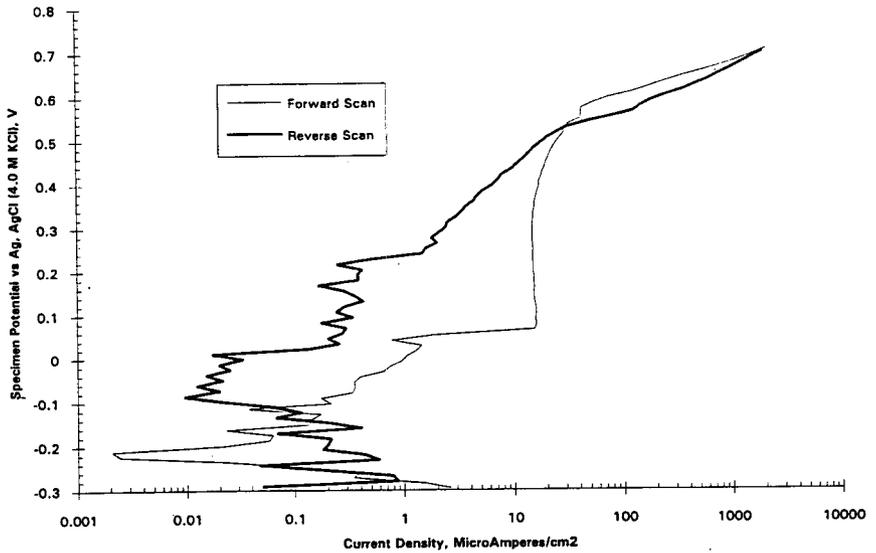


Figure B.3. Potentiodynamic Scan in Solution 3

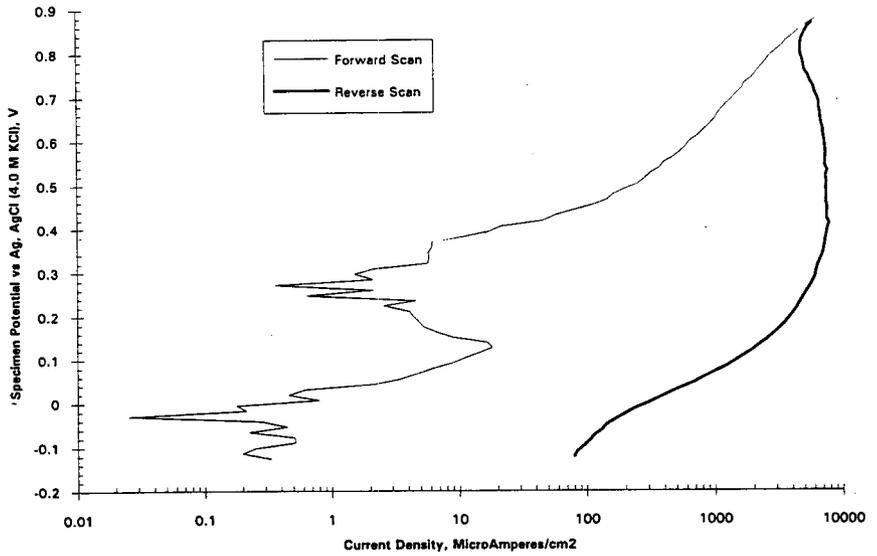


Figure B.4. Potentiodynamic Scan in Solution 4

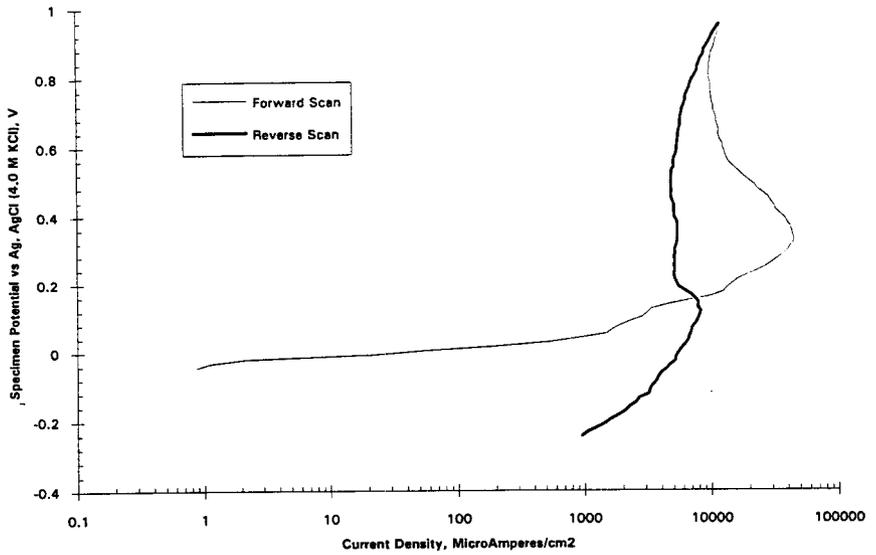


Figure B.5. Potentiodynamic Scan in Solution 5

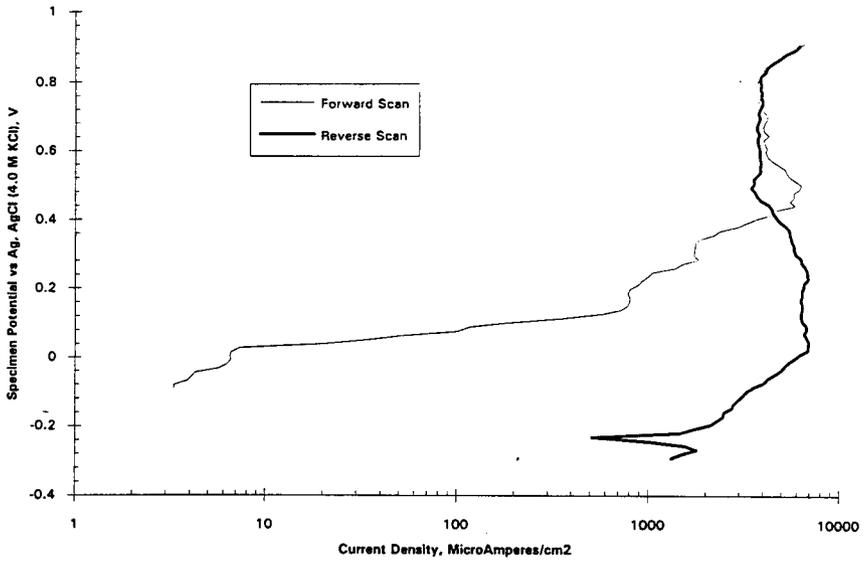


Figure B.6. Potentiodynamic Scan in Solution 6

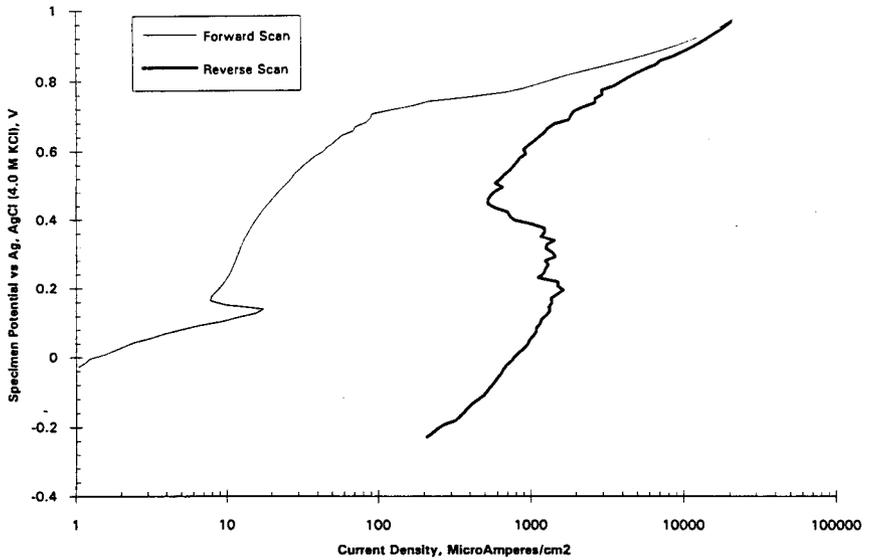


Figure B.7. Potentiodynamic Scan in Solution 7

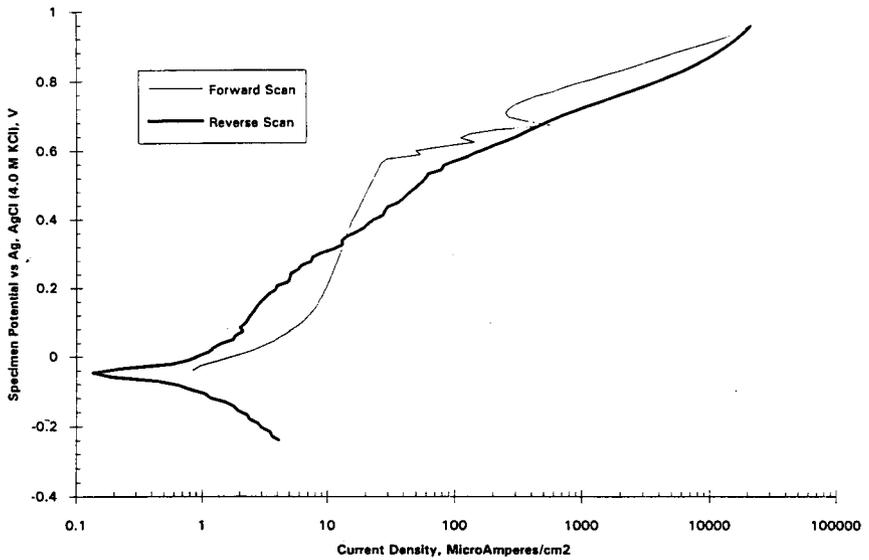


Figure B.8. Potentiodynamic Scan in Solution 8

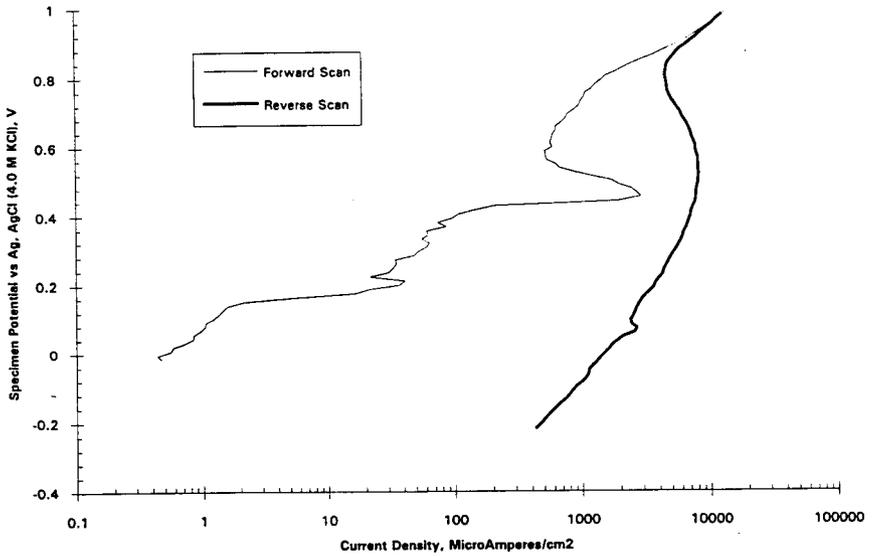


Figure B.9. Potentiodynamic Scan in Solution 9

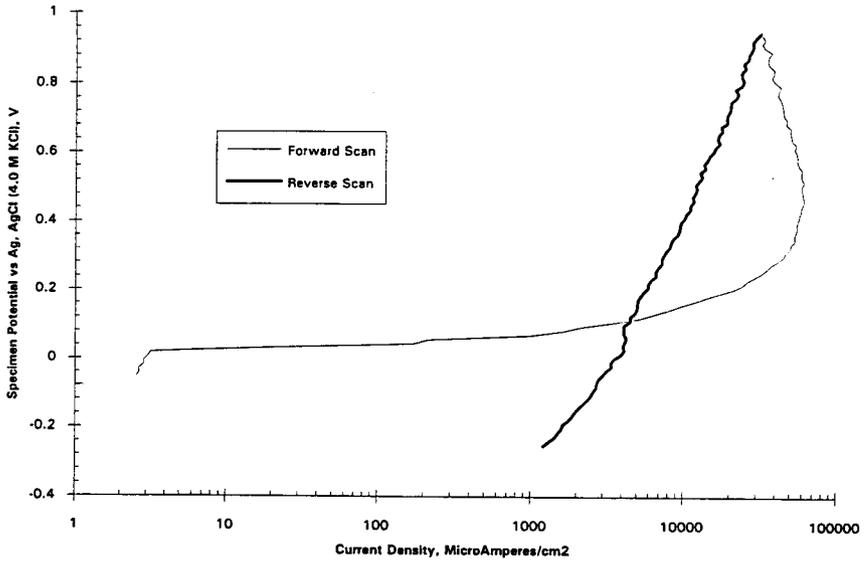


Figure B.10. Potentiodynamic Scan in Solution 10

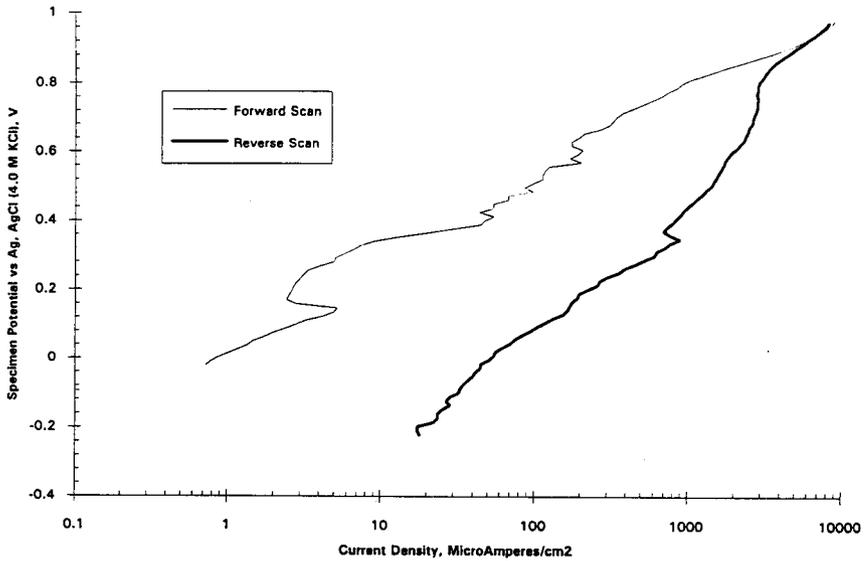


Figure B.11. Potentiodynamic Scan in Solution 11

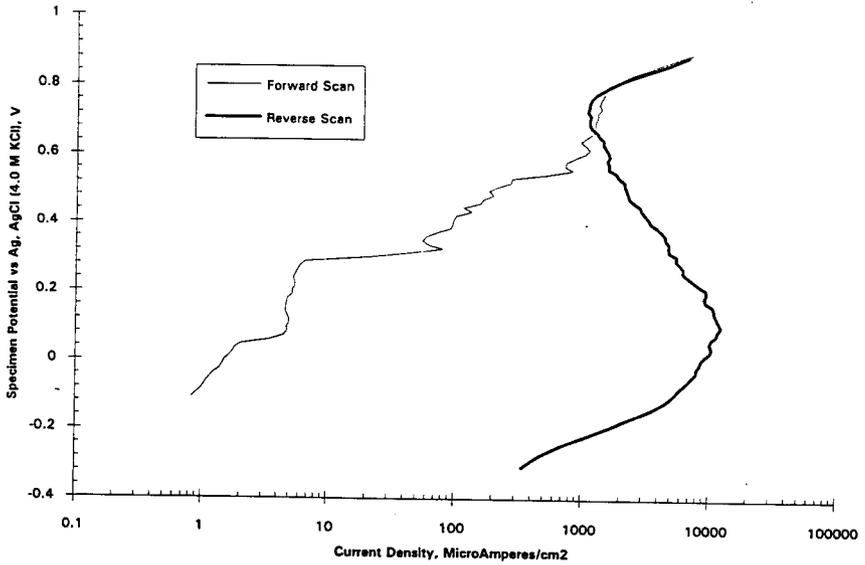


Figure B.12. Potentiodynamic Scan in Solution 12

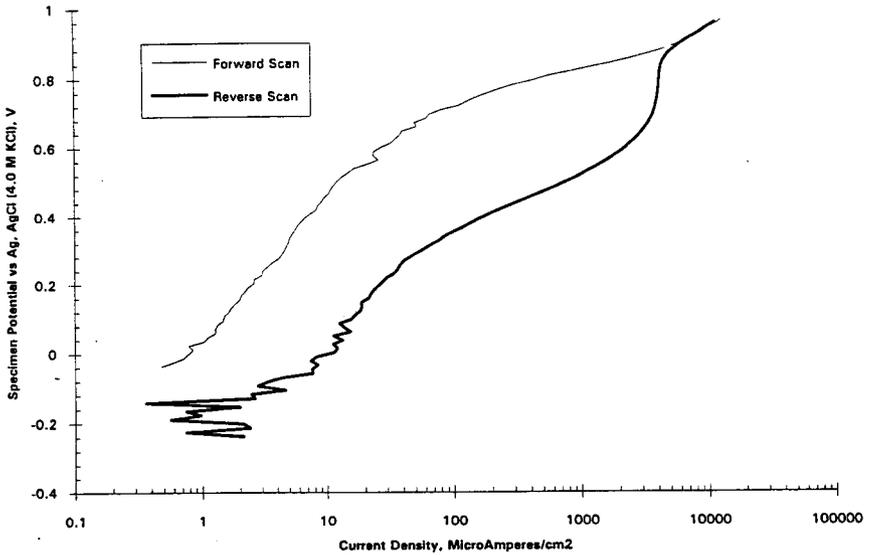


Figure B.13. Potentiodynamic Scan in Solution 13

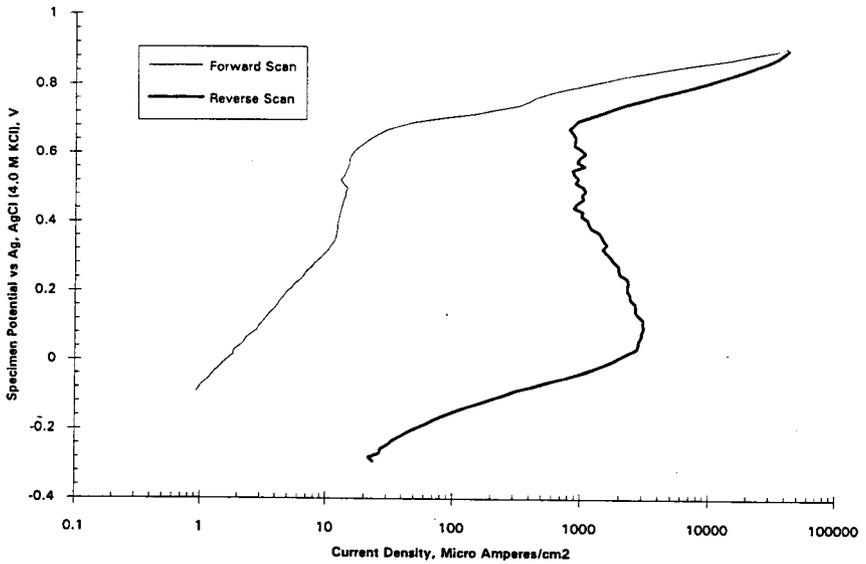


Figure B.14. Potentiodynamic Scan in Solution 14

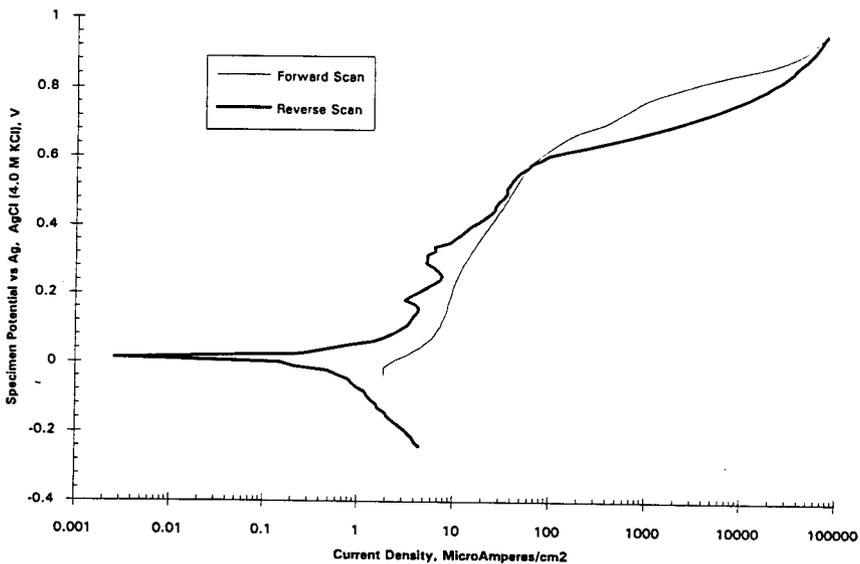


Figure B.15. Potentiodynamic Scan in Solution 15

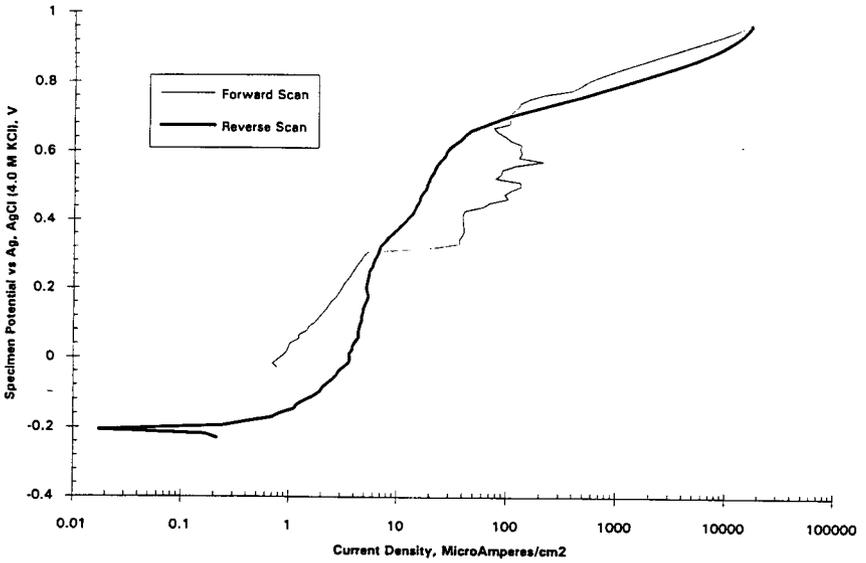


Figure B.16. Potentiodynamic Scan in Solution 16

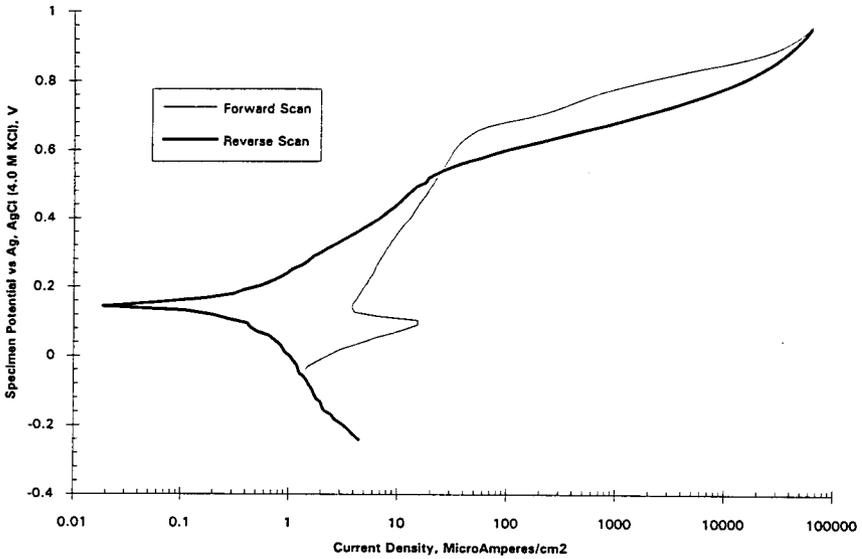


Figure B.17. Potentiodynamic Scan in Solution 17

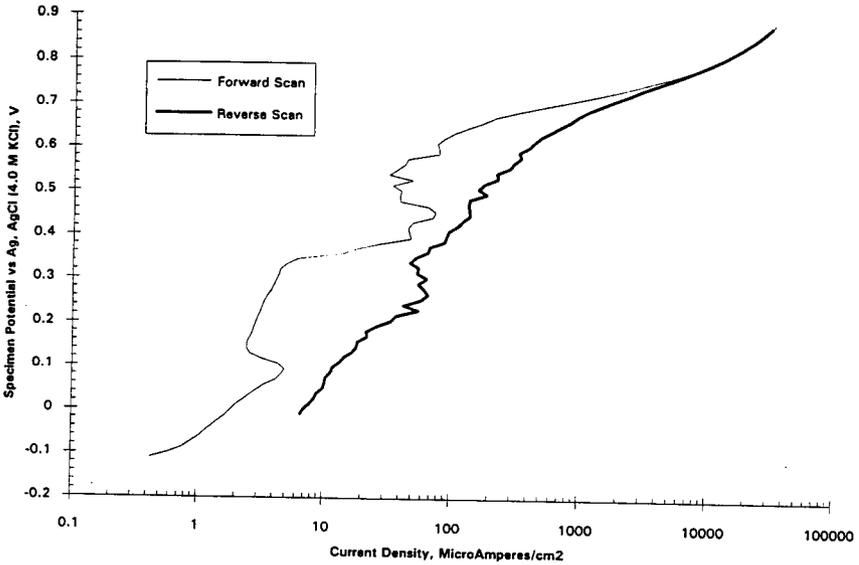


Figure B.18. Potentiodynamic Scan in Solution 18

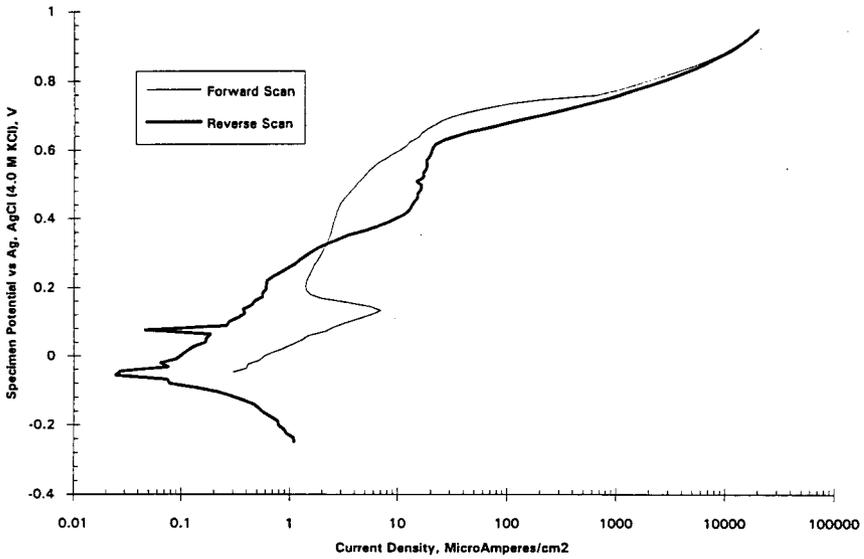


Figure B.19. Potentiodynamic Scan in Solution 19

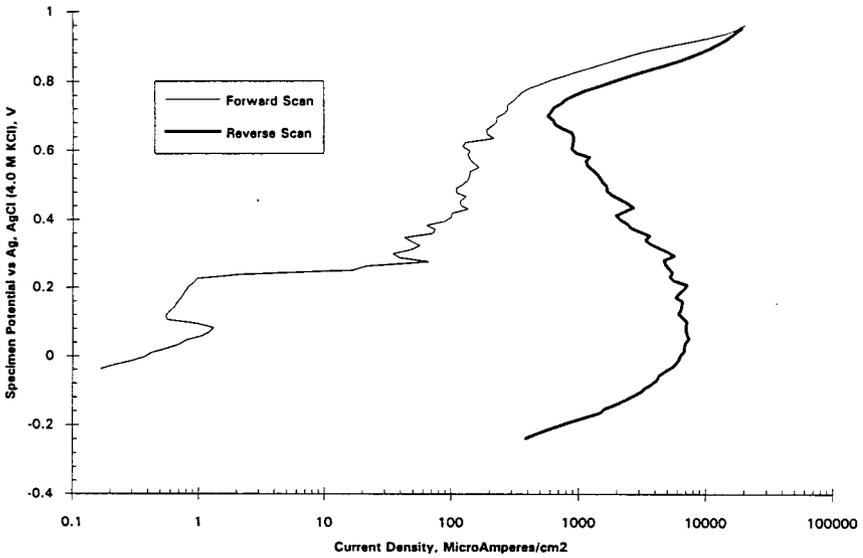


Figure B.20. Potentiodynamic Scan in Solution 20

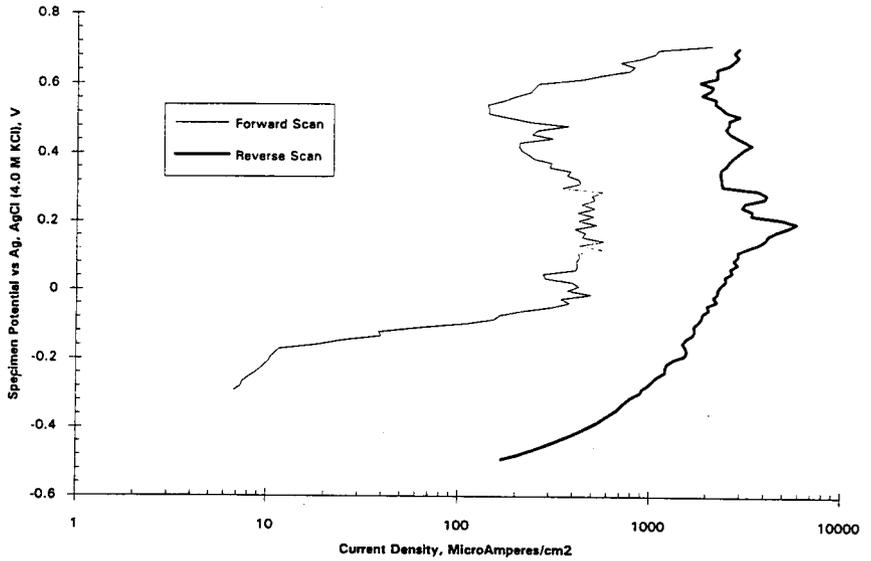


Figure B.21. Potentiodynamic Scan in Solution 21

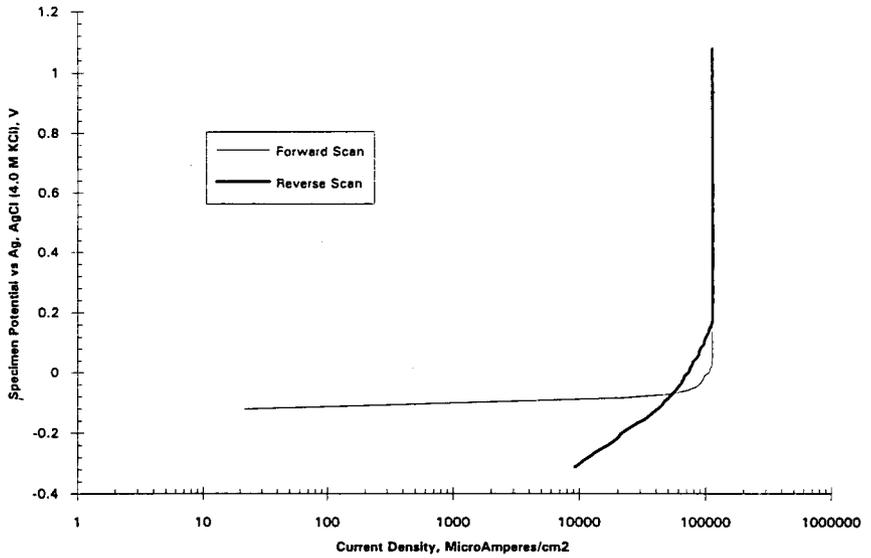


Figure B.22. Potentiodynamic Scan in Solution 22

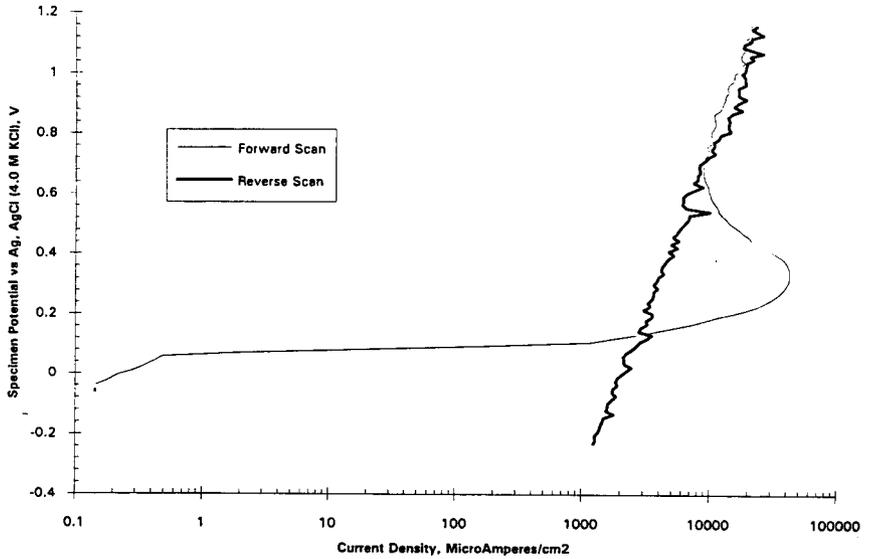


Figure B.23. Potentiodynamic Scan in Solution 23

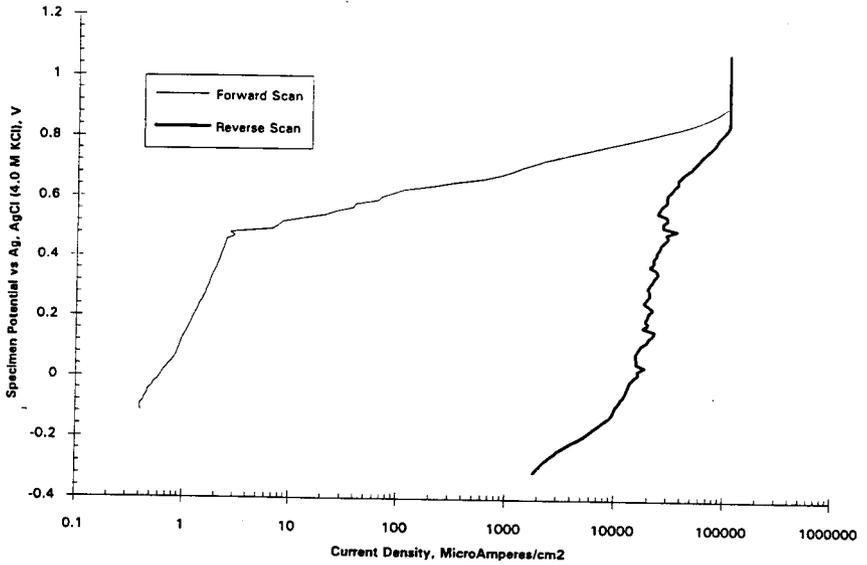


Figure B.24. Potentiodynamic Scan in Solution 24

APPENDIX C: PHOTOGRAPHS OF REPRESENTATIVE SPECIMENS PRIOR TO CLEANING

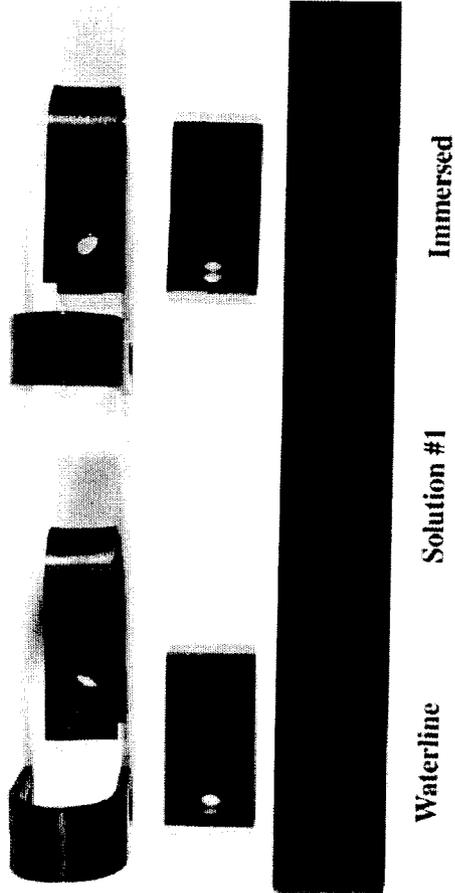


Figure C.1 Solution 1: Representative Specimens After Removal from Test Solution (no cleaning)

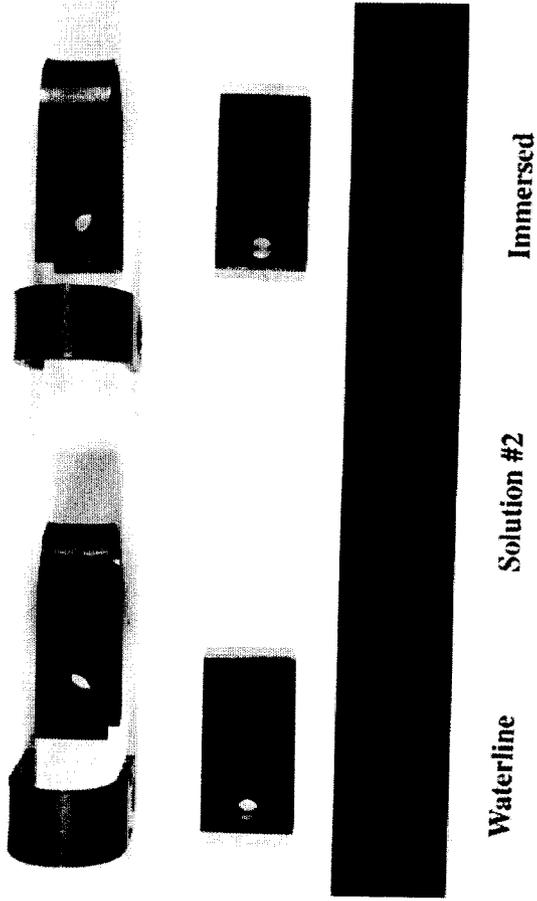


Figure C.2 Solution 2: Representative Specimens After Removal from Test Solution (no cleaning)

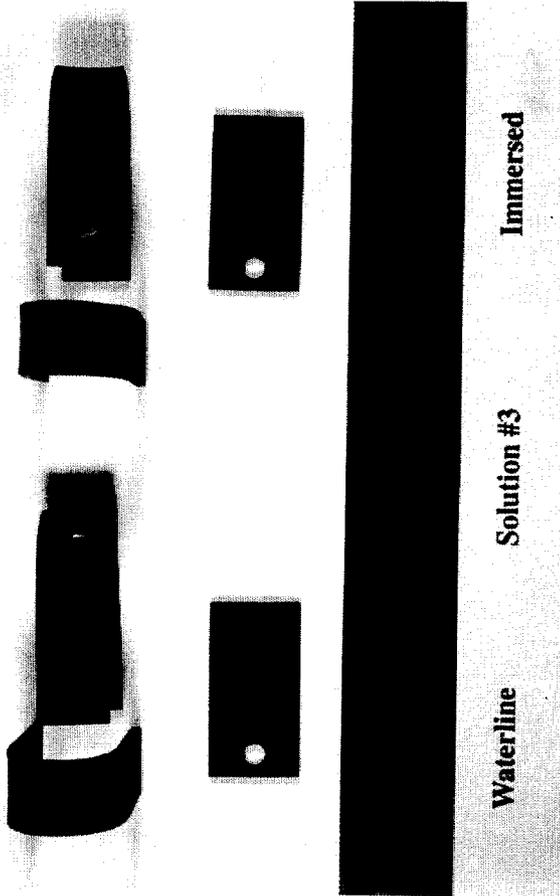


Figure C.3 Solution 3: Representative Specimens After Removal from Test Solution (no cleaning)

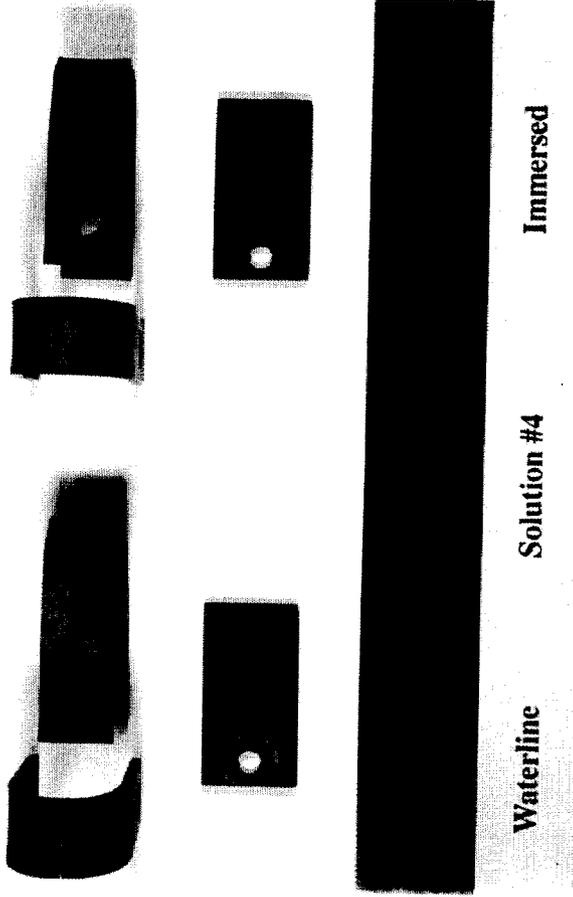


Figure C.4 Solution 4: Representative Specimens After Removal from Test Solution (no cleaning)

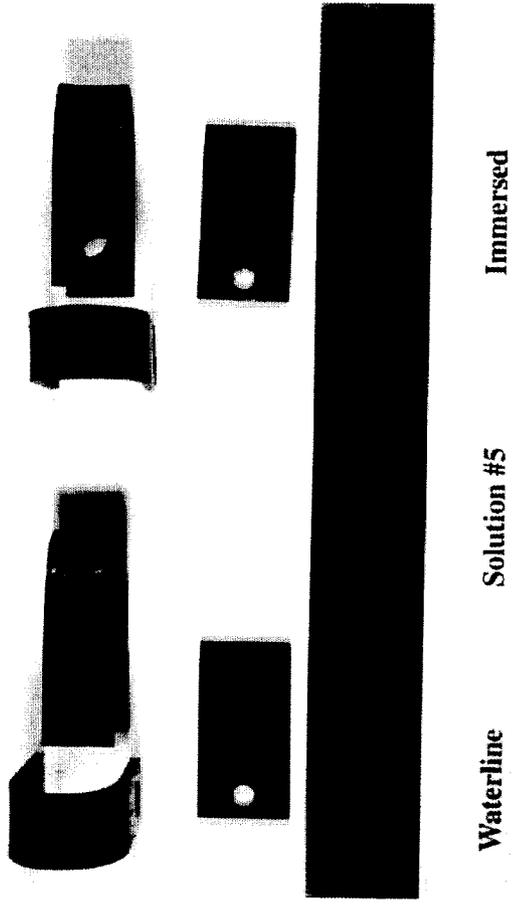


Figure C.5 Solution 5: Representative Specimens After Removal from Test Solution (no cleaning)

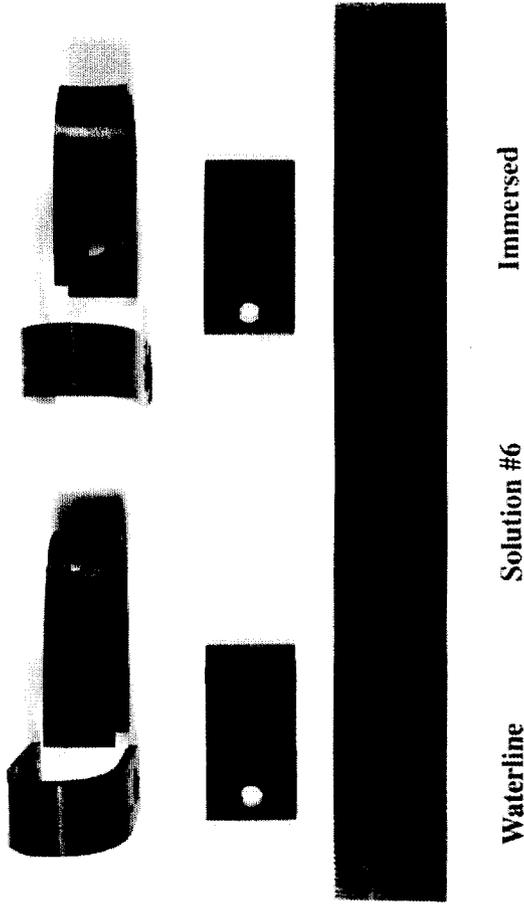


Figure C.6 Solution 6: Representative Specimens After Removal from Test Solution (no cleaning)

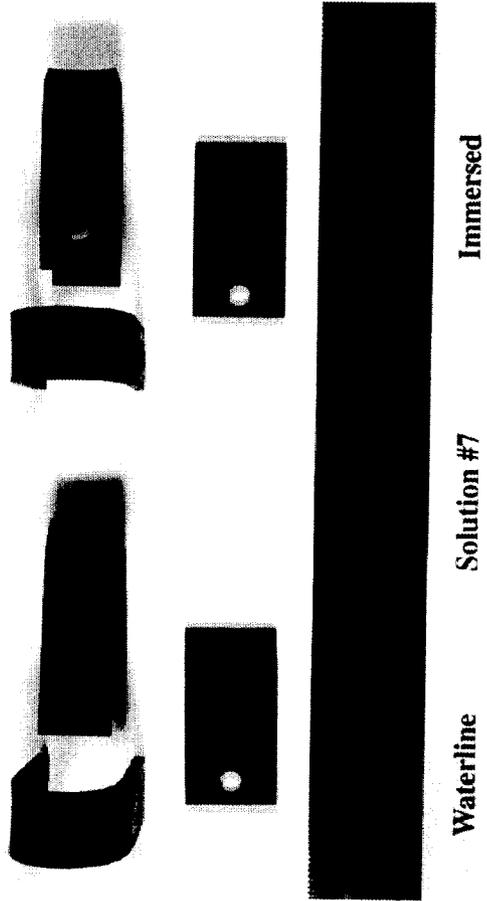


Figure C.7 Solution 7: Representative Specimens After Removal from Test Solution (no cleaning)

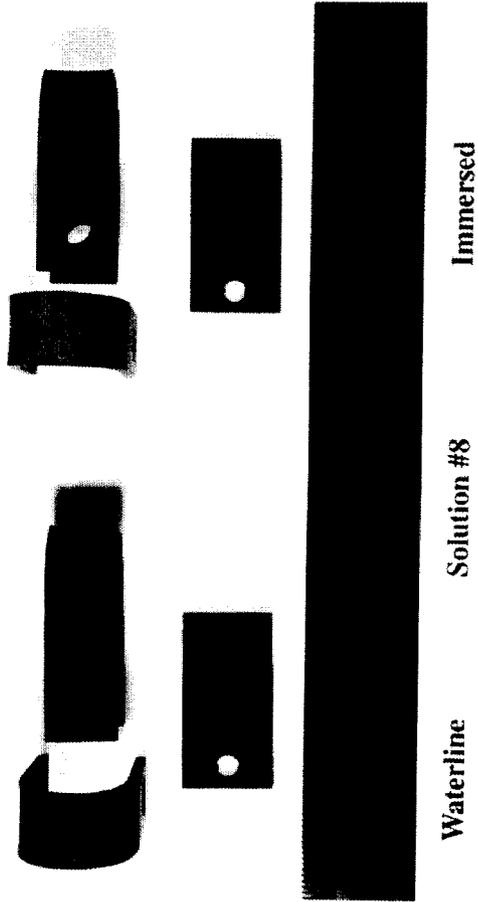


Figure C.8 Solution 8: Representative Specimens After Removal from Test Solution (no cleaning)

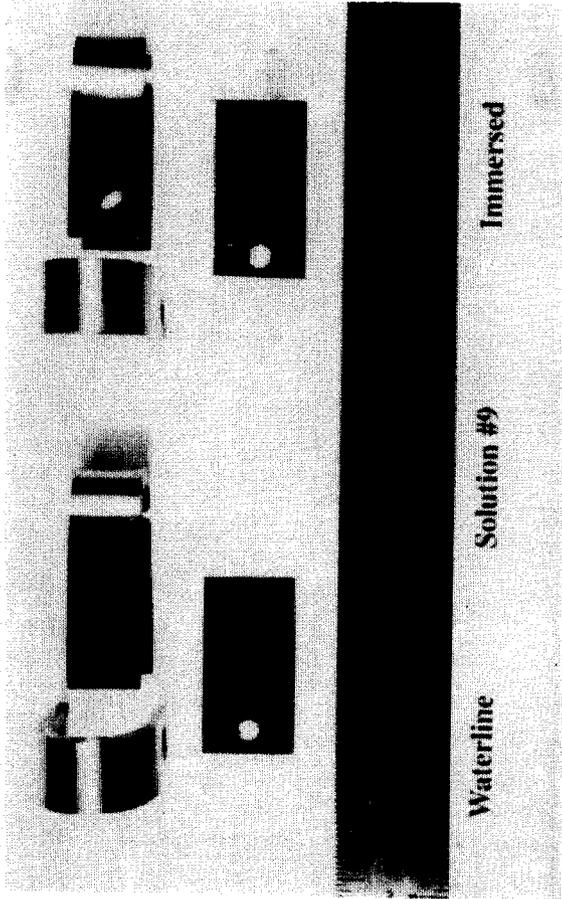


Figure C.9 Solution 9: Representative Specimens After Removal from Test Solution (no cleaning)

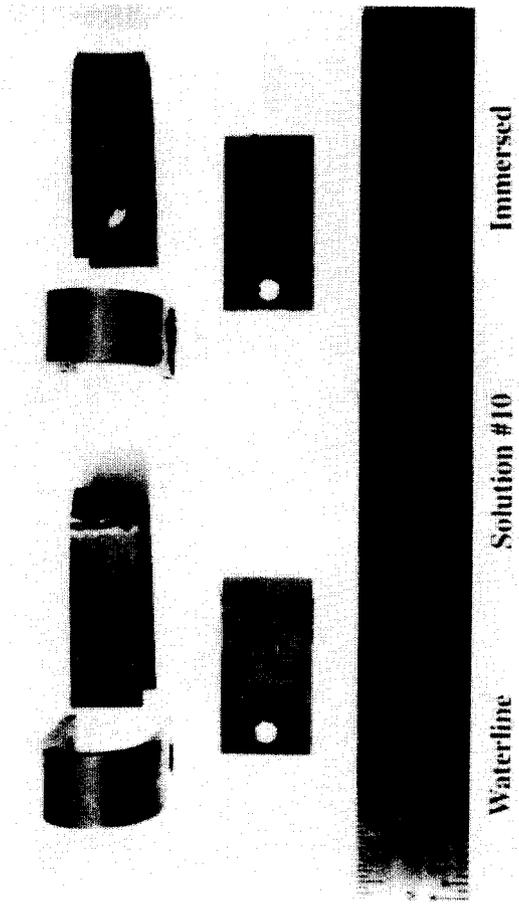


Figure C.10 Solution 10: Representative Specimens After Removal from Test Solution (no cleaning)

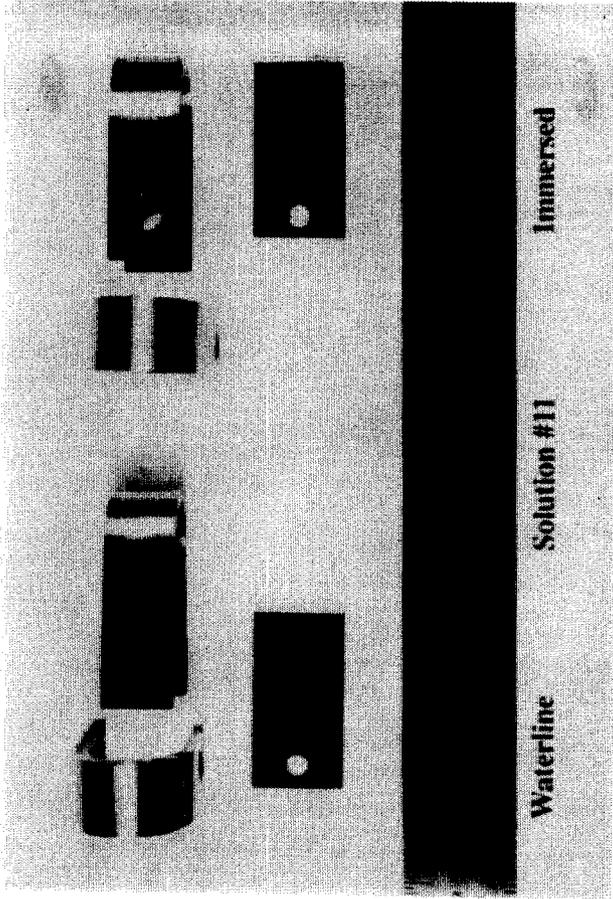


Figure C.11 Solution 11: Representative Specimens After Removal from Test Solution (no cleaning)

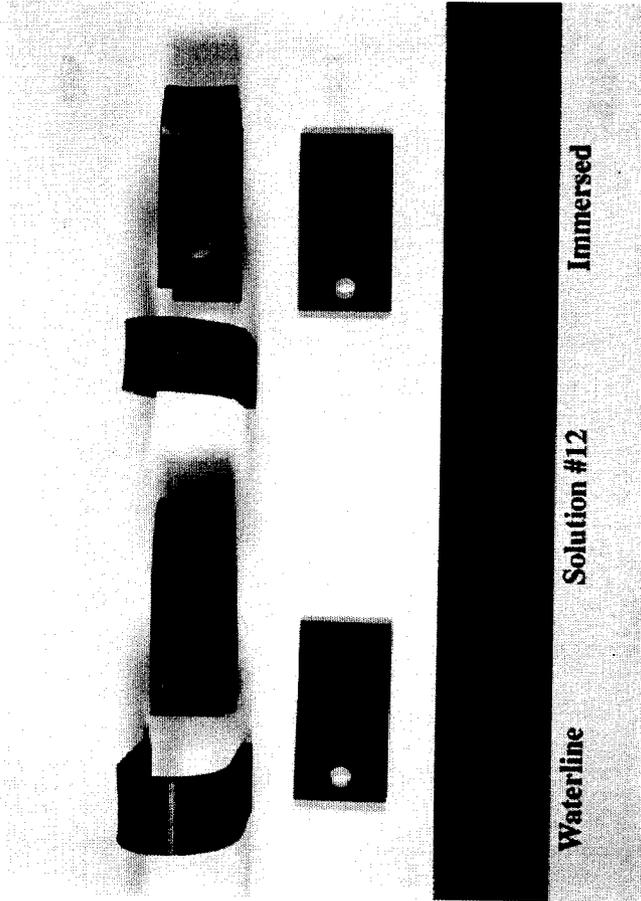


Figure C.12 Solution 12: Representative Specimens After Removal from Test Solution (no cleaning)

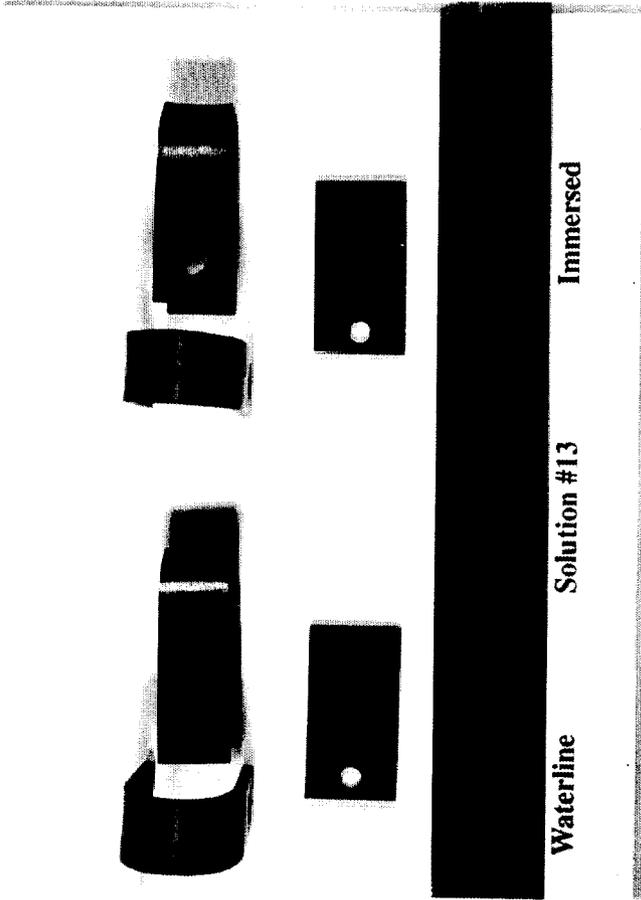


Figure C.13 Solution 13: Representative Specimens After Removal from Test Solution (no cleaning)

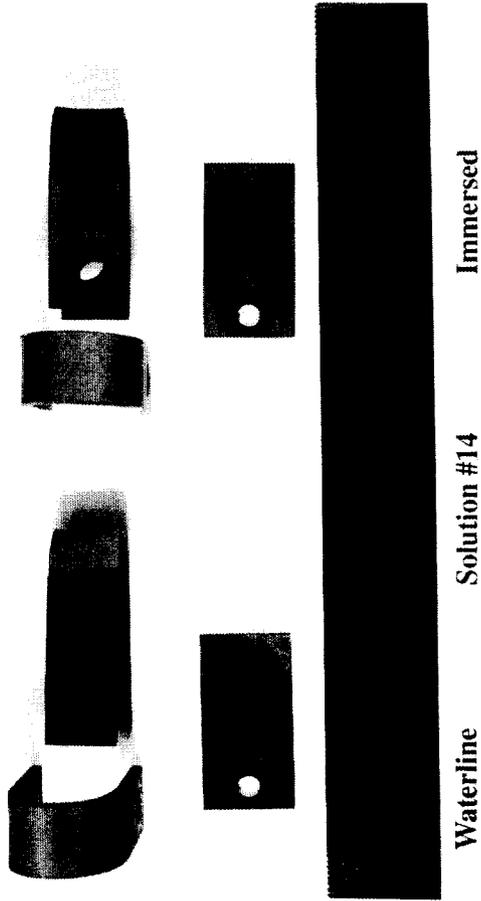


Figure C.14 Solution 14: Representative Specimens After Removal from Test Solution (no cleaning)

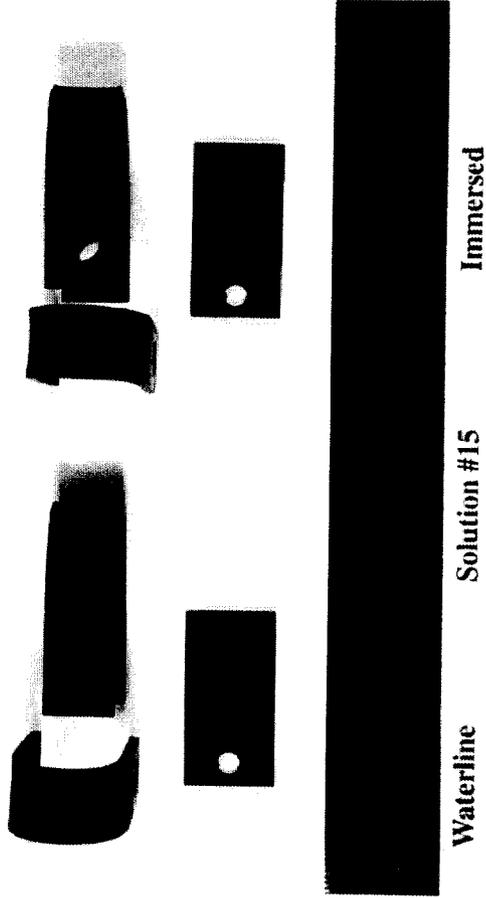


Figure C.15 Solution 15: Representative Specimens After Removal from Test Solution (no cleaning)

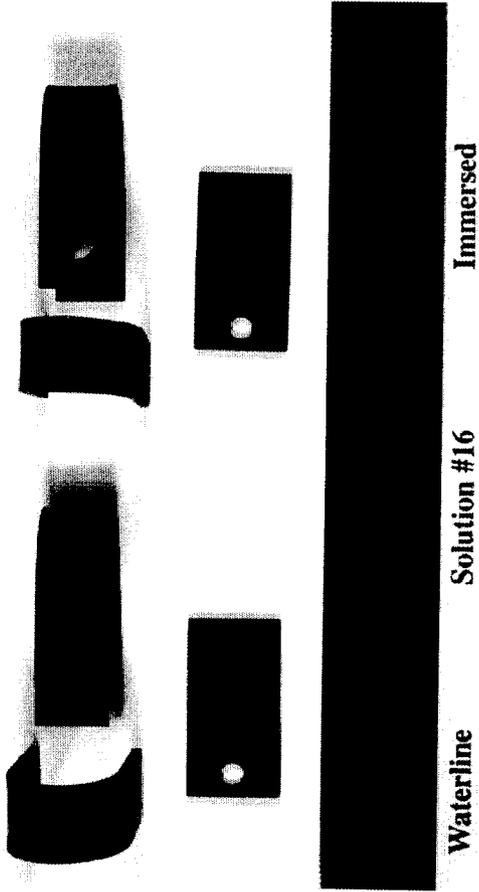


Figure C.16 Solution 16: Representative Specimens After Removal from Test Solution (no cleaning)

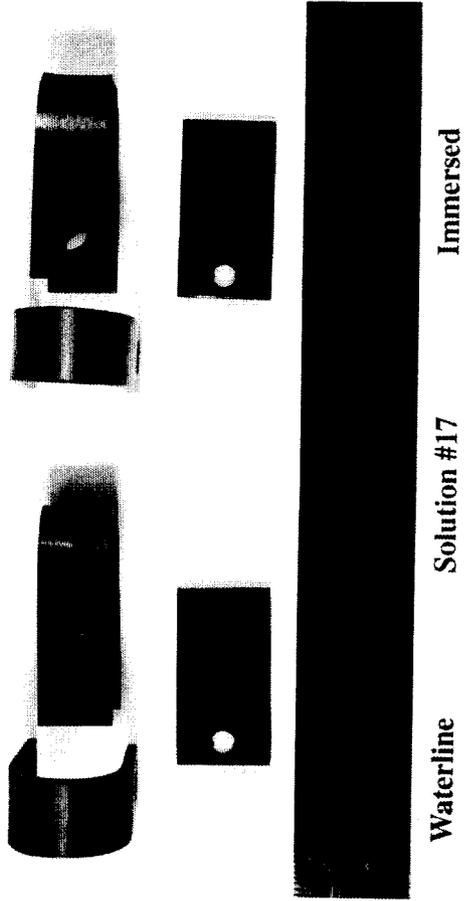


Figure C.17 Solution 17: Representative Specimens After Removal from Test Solution (no cleaning)

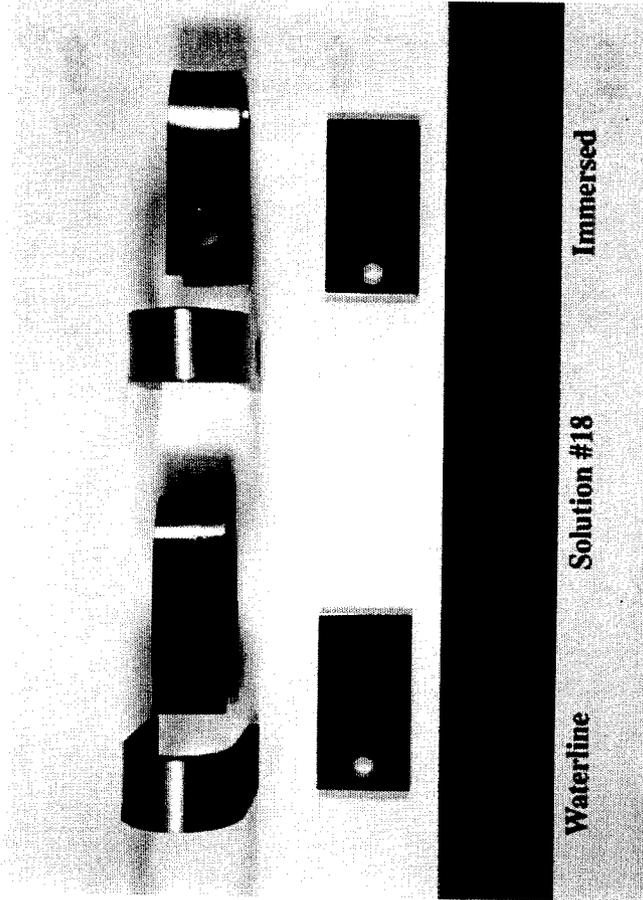


Figure C.18 Solution 15: Representative Specimens After Removal from Test Solution (no cleaning)

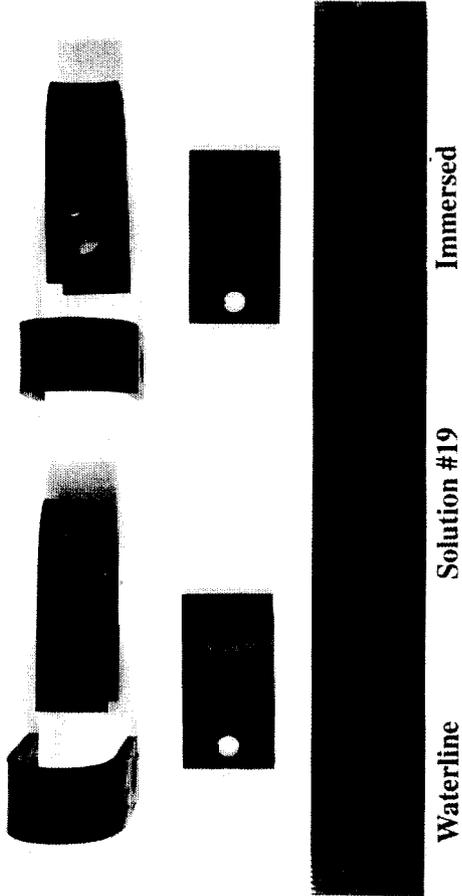


Figure C.19 Solution 19: Representative Specimens After Removal from Test Solution (no cleaning)

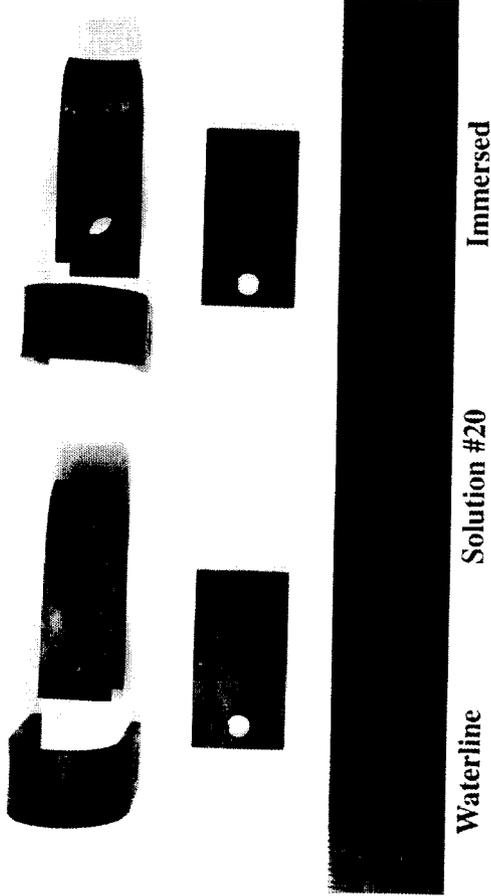


Figure C.20: Representative Specimens After Removal from Test Solution (no cleaning)

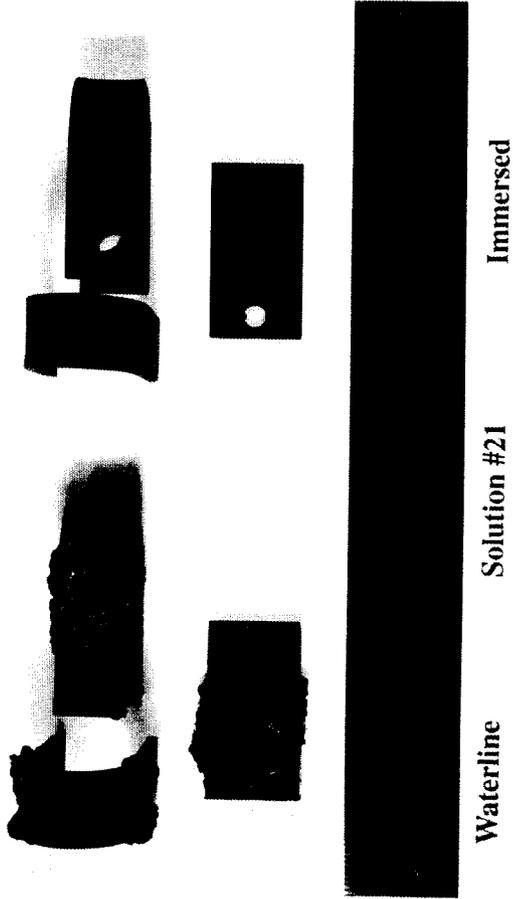


Figure C.21 Solution 21: Representative Specimens After Removal from Test Solution (no cleaning)

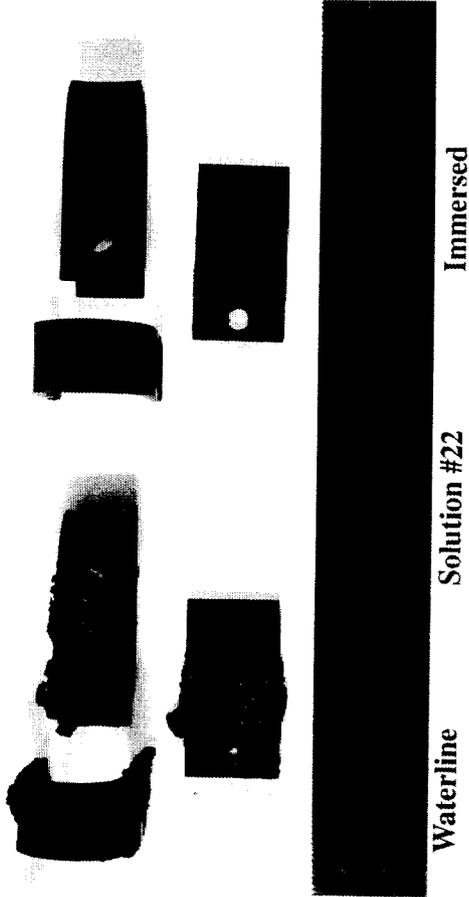


Figure C.22 Solution 22: Representative Specimens After Removal from Test Solution (no cleaning)

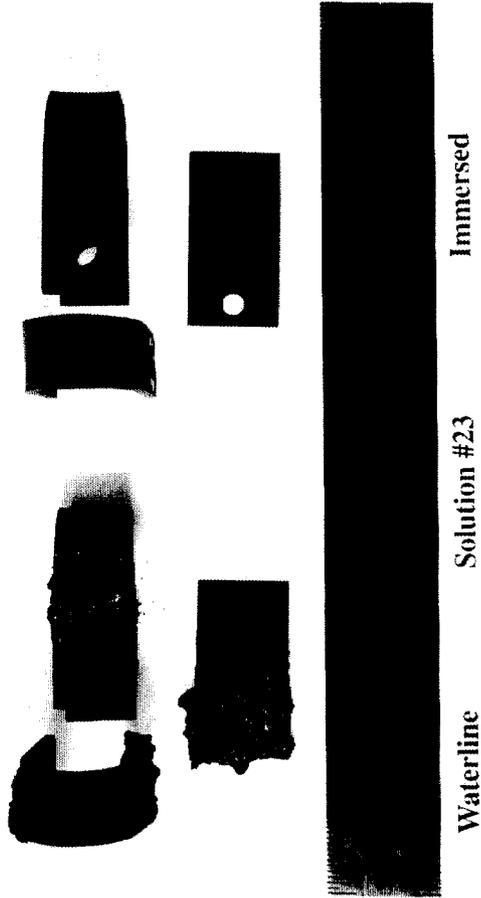


Figure C.23 Solution 23: Representative Specimens After Removal from Test Solution (no cleaning)

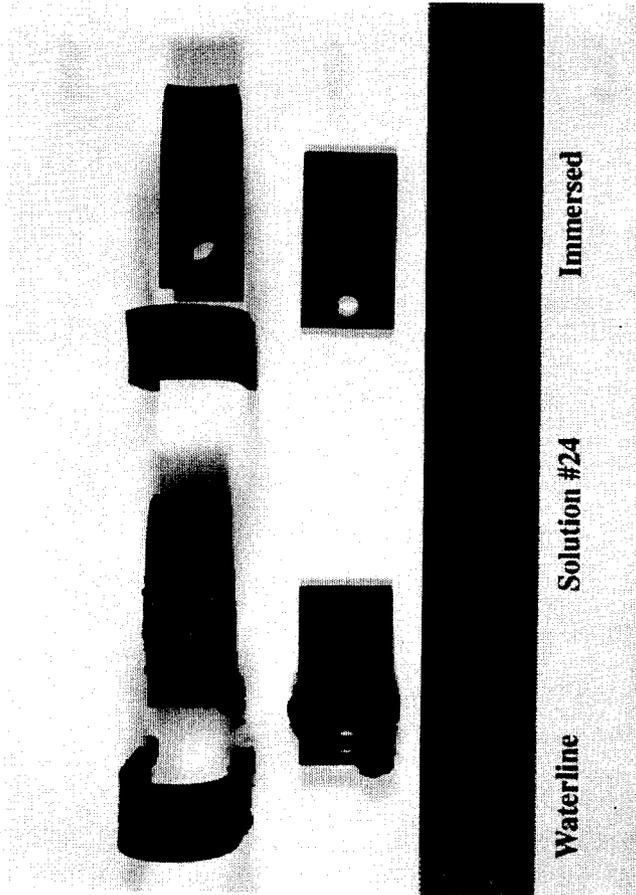


Figure C.24 Solution 24: Representative Specimens After Removal from Test Solution (no cleaning)

APPENDIX D: WEIGHT LOSS DATA

TABLE.XLS

Type	Location	Spec ID#	Soln #23	Starting Wt., g	Post Wt g	Wt. Loss	Specimen Area, cm2	Corr Rate mm/y	Aver Corr Rate, mm/y
Corrosion	Liquid	482	30.6060	30.5587	0.0458	30.4256	3.81E-03		
Corrosion	Liquid	483	30.7166	30.6738	0.0413	30.3302	3.45E-03	3.84E-03	
Corrosion	Liquid	484	30.7570	30.7038	0.0517	30.7037	4.26E-03		
Corrosion	Vapor	485	31.0223	24.5082	6.4506	30.6268	5.33E-01		
Corrosion	Vapor	486	31.0413	24.5082	6.4696	30.7409	5.33E-01	5.22E-01	
Corrosion	Vapor	487	30.6167	24.5082	6.0450	30.5375	5.01E-01		
U-bend	Liquid	337	56.1089	55.9888	0.1116	56.9999	4.96E-03		
U-bend	Liquid	338	56.6890	56.5763	0.1042	57.5521	4.58E-03	4.76E-03	
U-bend	Liquid	339	56.4222	56.3064	0.1073	57.2981	4.74E-03		
U-bend	Vapor	340	55.8168	not cleaned					
U-bend	Vapor	341	55.4771	not cleaned					
U-bend	Vapor	342	56.0766	not cleaned					
			Soln #24						
Type	Location	Spec ID#	Starting Wt., g	Post Wt g	Wt. Loss	Specimen Area, cm2	Corr Rate mm/y	Aver Corr Rate, mm/y	
Corrosion	Liquid	488	30.8237	30.7653	0.0569	30.5867	4.71E-03		
Corrosion	Liquid	489	30.8381	30.7819	0.0547	30.6750	4.51E-03	4.56E-03	
Corrosion	Liquid	490	30.5760	30.5204	0.0541	30.6673	4.47E-03		
Corrosion	Vapor	491	30.2074	23.9074	6.2365	30.5578	5.17E-01		
Corrosion	Vapor	492	30.8632	28.7767	2.0230	30.7221	1.67E-01	2.69E-01	
Corrosion	Vapor	493	30.4711	28.9194	1.4882	30.5720	1.23E-01		
U-bend	Liquid	343	55.5618	55.4589	0.0944	56.4791	4.23E-03		
U-bend	Liquid	344	55.8338	55.7294	0.0959	56.7381	4.28E-03	4.30E-03	
U-bend	Liquid	345	55.3499	55.2436	0.0978	56.2774	4.40E-03		
U-bend	Vapor	346	55.3808	not cleaned					
U-bend	Vapor	347	55.3628	not cleaned					
U-bend	Vapor	348	55.8844	not cleaned					

TABLE.XLS

Type	Location	Spec ID#	Soln #21		Wt. Loss	Specimen Area, cm2	Corr Rate mm/y	Aver Corr Rate, mm/y
			Starting Wt., g	Post Wt g				
Corrosion	Liquid	470	31.1375	31.0604	0.0756	30.7610	6.22E-03	
Corrosion	Liquid	471	30.4382	30.3624	0.0743	30.4873	6.17E-03	6.37E-03
Corrosion	Liquid	472	31.0324	30.9494	0.0815	30.6602	6.73E-03	
Corrosion	Vapor	473	30.7922	24.1516	6.5771	30.5761	5.45E-01	
Corrosion	Vapor	474	31.0420	25.0842	5.8943	30.6833	4.86E-01	5.27E-01
Corrosion	Vapor	475	31.1561	24.4331	6.6595	30.6262	5.50E-01	
U-bend	Liquid	325	54.5348	54.3699	0.1564	55.5015	7.13E-03	
U-bend	Liquid	326	54.6402	54.4743	0.1574	55.6019	7.17E-03	7.20E-03
U-bend	Liquid	327	54.7315	54.5621	0.1609	55.6888	7.31E-03	
U-bend	Vapor	328	53.9866	not cleaned				
U-bend	Vapor	329	54.2646	not cleaned				
U-bend	Vapor	330	54.2785	not cleaned				
Type	Location	Spec ID#	Soln #22		Wt. Loss	Specimen Area, cm2	Corr Rate mm/y	Aver Corr Rate, mm/y
			Starting Wt., g	Post Wt g				
Corrosion	Liquid	476	30.4253	30.1055	0.3183	30.6067	2.63E-02	
Corrosion	Liquid	477	30.5640	30.3112	0.2513	30.6017	2.08E-02	2.39E-02
Corrosion	Liquid	478	30.7326	30.4350	0.2961	30.4835	2.46E-02	
Corrosion	Vapor	479	30.7388	24.8561	5.8192	30.6282	4.81E-01	
Corrosion	Vapor	480	31.1138	24.7855	6.2648	30.7272	5.16E-01	3.96E-01
Corrosion	Vapor	481	31.0764	28.7130	2.2999	30.7232	1.90E-01	
U-bend	Liquid	331	54.6375	54.2705	0.3585	55.5993	1.63E-02	
U-bend	Liquid	332	55.3933	55.0864	0.2984	56.3187	1.34E-02	1.47E-02
U-bend	Liquid	333	55.6951	55.3623	0.3243	56.6060	1.45E-02	
U-bend	Vapor	334	54.8656	not cleaned				
U-bend	Vapor	335	54.8032	not cleaned				
U-bend	Vapor	336	56.1804	not cleaned				

TABLE XLS

Type	Location	Spec ID#	Soln #19	Starting Wt., g	Post Wt g	Wt. Loss	Specimen Area, cm2	Corr Rate mm/y	Aver Corr Rate, mm/y
Corrosion	Liquid	458	30.6566	30.6275	0.0276	0.0276	30.6441	2.28E-03	
Corrosion	Liquid	459	30.7306	30.7005	0.0286	0.0286	30.5939	2.37E-03	2.25E-03
Corrosion	Liquid	460	30.1905	30.1639	0.0251	0.0251	30.4172	2.09E-03	
Corrosion	Vapor	461	31.0874	31.0644	0.0215	0.0215	30.7437	1.77E-03	
Corrosion	Vapor	462	30.8333	30.8069	0.0249	0.0249	30.6572	2.06E-03	1.92E-03
Corrosion	Vapor	463	30.8541	30.8290	0.0236	0.0236	30.6869	1.95E-03	
U-bend	Liquid	313	54.4216	54.3645	0.0486	0.0486	55.3938	2.22E-03	
U-bend	Liquid	314	54.7925	54.7317	0.0523	0.0523	55.7468	2.38E-03	2.31E-03
U-bend	Liquid	315	54.7721	54.7121	0.0515	0.0515	55.7274	2.34E-03	
U-bend	Vapor	316	54.5736	54.5212	0.0439	0.0439	55.5385	2.00E-03	
U-bend	Vapor	317	54.9822	54.9231	0.0506	0.0506	55.9274	2.29E-03	2.21E-03
U-bend	Vapor	318	55.4440	55.3837	0.0518	0.0518	56.3670	2.33E-03	
			Soln #20						
Type	Location	Spec ID#	Starting Wt., g	Post Wt g	Wt. Loss	Specimen Area, cm2	Corr Rate mm/y	Aver Corr Rate, mm/y	
Corrosion	Liquid	464	30.8514	30.8259	0.0240	0.0240	30.6927	1.98E-03	
Corrosion	Liquid	465	30.9331	30.9058	0.0258	0.0258	30.6851	2.13E-03	2.10E-03
Corrosion	Liquid	466	30.8357	30.8076	0.0266	0.0266	30.5695	2.20E-03	
Corrosion	Vapor	467	31.2313	31.1886	0.0412	0.0412	30.7933	3.39E-03	
Corrosion	Vapor	468	30.3659	30.3273	0.0371	0.0371	30.4859	3.08E-03	3.16E-03
Corrosion	Vapor	469	30.7851	30.7472	0.0364	0.0364	30.6894	3.00E-03	
U-bend	Liquid	319	54.5503	54.4981	0.0437	0.0437	55.5163	1.99E-03	
U-bend	Liquid	320	55.7314	55.6768	0.0461	0.0461	56.6406	2.06E-03	2.02E-03
U-bend	Liquid	321	55.9754	55.9218	0.0451	0.0451	56.8728	2.01E-03	
U-bend	Vapor	322	54.8053	54.7387	0.0581	0.0581	55.7590	2.64E-03	
U-bend	Vapor	323	54.8818	54.8164	0.0569	0.0569	55.8319	2.58E-03	2.55E-03
U-bend	Vapor	324	54.0298	53.9684	0.0529	0.0529	55.0208	2.43E-03	

TABLE.XLS

Type	Location	Spec ID#	Soln #17		Post Wt g	Wt. Loss	Specimen Area, cm ²	Corr Rate mm/y	Aver Corr Rate, mm/y
			Starting Wt., g	Post Wt g					
Corrosion	Liquid	446	30.8866	30.8713	0.0138	30.7225	1.14E-03		
Corrosion	Liquid	447	30.5311	30.5162	0.0134	30.6372	1.11E-03	1.12E-03	
Corrosion	Liquid	448	30.0649	30.0499	0.0135	30.5583	1.12E-03		
Corrosion	Vapor	449	30.3289	30.3041	0.0233	30.5958	1.93E-03		
Corrosion	Vapor	450	30.4025	30.3777	0.0233	30.5613	1.93E-03	1.83E-03	
Corrosion	Vapor	451	30.6479	30.6285	0.0199	30.6199	1.65E-03		
U-bend	Liquid	301	55.1596	55.1277	0.0234	56.0963	1.06E-03		
U-bend	Liquid	302	55.7649	55.7342	0.0222	56.6725	9.92E-04	1.03E-03	
U-bend	Liquid	303	54.9133	54.8818	0.0230	55.8618	1.04E-03		
U-bend	Vapor	304	55.2329	55.1685	0.0559	56.1661	2.52E-03		
U-bend	Vapor	305	55.0327	54.9738	0.0504	55.9755	2.28E-03	2.41E-03	
U-bend	Vapor	306	55.0744	55.0124	0.0535	56.0152	2.42E-03		
Type	Location	Spec ID#	Soln #18		Post Wt g	Wt. Loss	Specimen Area, cm ²	Corr Rate mm/y	Aver Corr Rate, mm/y
			Starting Wt., g	Post Wt g					
Corrosion	Liquid	452	30.1635	30.1589	0.0031	30.5661	2.57E-04		
Corrosion	Liquid	453	30.4010	30.3980	0.0015	30.5392	1.24E-04	1.71E-04	
Corrosion	Liquid	454	30.1610	30.1579	0.0016	30.5226	1.33E-04		
Corrosion	Vapor	455	30.3221	30.2972	0.0234	30.5250	1.94E-03		
Corrosion	Vapor	456	30.4546	30.4311	0.0220	30.5668	1.82E-03	1.98E-03	
Corrosion	Vapor	457	30.5968	30.5688	0.0265	30.6263	2.19E-03		
U-bend	Liquid	307	55.8202	55.8128	-0.0011	56.7251	-4.91E-05		
U-bend	Liquid	308	55.7893	55.7850	-0.0042	56.6957	-1.88E-04	-1.30E-04	
U-bend	Liquid	309	55.7094	55.7043	-0.0034	56.6196	-1.52E-04		
U-bend	Vapor	310	55.7220	55.6698	0.0437	56.6316	1.95E-03		
U-bend	Vapor	311	55.6883	55.6392	0.0406	56.5996	1.82E-03	1.81E-03	
U-bend	Vapor	312	55.8097	55.7643	0.0369	56.7151	1.65E-03		

TABLE XLS

Type	Location	Spec ID#	Soln #15			Wt. Loss	Specimen Area, cm2	Corr Rate mm/y	Aver Corr Rate, mm/y
			Starting Wt., g	Post Wt g	Area, cm2				
Corrosion	Liquid	434	30.4218	30.3646	0.0557	30.6163	4.61E-03		
Corrosion	Liquid	435	30.8250	30.7688	0.0547	30.5744	4.53E-03	4.56E-03	
Corrosion	Liquid	436	30.7128	30.6564	0.0549	30.6366	4.54E-03		
Corrosion	Vapor	437	30.1947	30.1587	0.0345	30.5138	2.86E-03		
Corrosion	Vapor	438	30.6755	30.6424	0.0316	30.5730	2.62E-03	2.74E-03	
Corrosion	Vapor	439	30.3093	30.2748	0.0330	30.4373	2.74E-03		
U-bend	Liquid	289	55.7208	55.6207	0.0916	56.6305	4.09E-03		
U-bend	Liquid	290	55.4953	55.3945	0.0923	56.4158	4.14E-03	4.15E-03	
U-bend	Liquid	291	55.1116	55.0097	0.0934	56.0506	4.22E-03		
U-bend	Vapor	292	56.2337	56.1537	0.0715	57.1187	3.17E-03		
U-bend	Vapor	293	55.3965	55.3251	0.0629	56.3218	2.83E-03	3.00E-03	
U-bend	Vapor	294	53.9479	53.8741	0.0653	54.9429	3.01E-03		
Type	Location	Spec ID#	Soln #16			Wt. Loss	Specimen Area, cm2	Corr Rate mm/y	Aver Corr Rate, mm/y
			Starting Wt., g	Post Wt g	Area, cm2				
Corrosion	Liquid	440	31.1207	31.0793	0.0399	30.8018	3.28E-03		
Corrosion	Liquid	441	30.5607	30.5181	0.0411	30.6228	3.40E-03	3.34E-03	
Corrosion	Liquid	442	30.2506	30.2089	0.0402	30.5421	3.33E-03		
Corrosion	Vapor	443	30.7500	30.7069	0.0416	30.6832	3.43E-03		
Corrosion	Vapor	444	30.5862	30.5434	0.0413	30.6492	3.41E-03	3.21E-03	
Corrosion	Vapor	445	31.0423	31.0070	0.0338	30.7553	2.78E-03		
U-bend	Liquid	295	55.5299	55.4503	0.0711	56.4488	3.19E-03		
U-bend	Liquid	296	56.2014	56.1121	0.0808	57.0880	3.58E-03	3.41E-03	
U-bend	Liquid	297	53.7159	53.6329	0.0745	54.7220	3.45E-03		
U-bend	Vapor	298	55.6669	55.5956	0.0628	56.5792	2.81E-03		
U-bend	Vapor	299	55.7341	55.6635	0.0621	56.6431	2.76E-03	2.93E-03	
U-bend	Vapor	300	55.4482	55.3682	0.0715	56.3710	3.21E-03		

TABLE XLS

Type	Location	Spec ID#	Soln #13		Post Wt g	Wt. Loss	Specimen Area, cm ²	Corr Rate mm/y	Aver Corr Rate, mm/y
			Starting Wt., g	Starting Wt., g					
Corrosion	Liquid	422	30.7559	30.7522	0.0022	30.6350	1.82E-04		
Corrosion	Liquid	423	31.0759	31.0716	0.0028	30.6808	2.31E-04	1.98E-04	
Corrosion	Liquid	424	30.8218	30.8181	0.0022	30.6616	1.82E-04		
Corrosion	Vapor	425	30.4357	30.4265	0.0077	30.6031	6.37E-04		
Corrosion	Vapor	426	30.2006	30.1902	0.0089	30.5172	7.38E-04	6.76E-04	
Corrosion	Vapor	427	30.6881	30.6787	0.0079	30.6678	6.52E-04		
U-bend	Liquid	277	55.4890	55.4788	0.0017	56.4098	7.63E-05		
U-bend	Liquid	278	55.5376	55.5318	-0.0027	56.4561	-1.21E-04	2.18E-07	
U-bend	Liquid	279	54.7657	54.7562	0.0010	55.7213	4.54E-05		
U-bend	Vapor	280	56.4640	56.4474	0.0081	57.3379	3.58E-04		
U-bend	Vapor	281	56.2871	56.2702	0.0084	57.1695	3.72E-04	3.31E-04	
U-bend	Vapor	282	55.0517	55.0374	0.0058	55.9936	2.62E-04		
			Soln #14						
Type	Location	Spec ID#	Starting Wt., g	Post Wt g	Wt. Loss	Specimen Area, cm ²	Corr Rate mm/y	Aver Corr Rate, mm/y	
Corrosion	Liquid	428	30.5013	30.4681	0.0317	30.5873	2.62E-03		
Corrosion	Liquid	429	30.7708	30.7381	0.0312	30.6576	2.58E-03	2.61E-03	
Corrosion	Liquid	430	29.2987	29.2655	0.0317	30.3537	2.64E-03		
Corrosion	Vapor	431	31.0518	31.0067	0.0436	30.6999	3.60E-03		
Corrosion	Vapor	432	30.8186	30.7733	0.0438	30.6420	3.62E-03	3.58E-03	
Corrosion	Vapor	433	30.8478	30.6035	0.0428	30.6233	3.54E-03		
U-bend	Liquid	283	55.0167	54.9542	0.0540	55.9603	2.44E-03		
U-bend	Liquid	284	55.2280	55.1677	0.0518	56.1614	2.33E-03	2.36E-03	
U-bend	Liquid	285	55.6568	55.5971	0.0512	56.5696	2.29E-03		
U-bend	Vapor	286	55.5717	55.4899	0.0733	56.4886	3.28E-03		
U-bend	Vapor	287	55.4961	55.4177	0.0699	56.4166	3.14E-03	3.21E-03	
U-bend	Vapor	288	55.8673	55.7870	0.0718	56.7699	3.20E-03		

TABLE.XLS

Type	Location	Spec ID#	Soln #11		Post Wt g	Wt. Loss	Specimen Area, cm2	Corr Rate mm/y	Aver Corr Rate, mm/y
			Starting Wt., g	Starting Wt., g					
Corrosion	Liquid	410	30.2164	30.2140	0.0009	30.5595	7.46E-05		
Corrosion	Liquid	411	30.5793	30.5792	-0.0014	30.6471	-1.16E-04	1.12E-05	
Corrosion	Liquid	412	30.3008	30.2984	0.0009	30.4822	7.47E-05		
Corrosion	Vapor	413	30.3237	30.3202	0.0020	30.5661	1.66E-04		
Corrosion	Vapor	414	30.5228	30.5197	0.0016	30.7346	1.32E-04	1.38E-04	
Corrosion	Vapor	415	30.4647	30.4618	0.0014	30.5620	1.16E-04		
U-bend	Liquid	265	55.2704	55.2654	-0.0035	56.2018	-1.58E-04		
U-bend	Liquid	266	55.3297	55.3265	-0.0053	56.2582	-2.38E-04	-1.95E-04	
U-bend	Liquid	267	55.1375	55.1332	-0.0042	56.0753	-1.90E-04		
U-bend	Vapor	268	54.7167	54.7093	-0.0011	55.6747	-5.00E-05		
U-bend	Vapor	269	54.7071	54.6906	0.0080	55.6656	3.64E-04	1.99E-04	
U-bend	Vapor	270	55.3870	55.3722	0.0063	56.3127	2.83E-04		
			Soln #12						
Type	Location	Spec ID#	Soln #12		Post Wt g	Wt. Loss	Specimen Area, cm2	Corr Rate mm/y	Aver Corr Rate, mm/y
			Starting Wt., g	Starting Wt., g					
Corrosion	Liquid	416	30.4892	30.4656	0.0221	30.5261	1.83E-03		
Corrosion	Liquid	417	30.6258	30.6038	0.0205	30.6276	1.69E-03	1.65E-03	
Corrosion	Liquid	418	30.2612	30.2424	0.0173	30.6200	1.43E-03		
Corrosion	Vapor	419	30.6865	30.6460	0.0390	30.6162	3.22E-03		
Corrosion	Vapor	420	30.8938	30.8528	0.0395	30.7249	3.25E-03	3.25E-03	
Corrosion	Vapor	421	30.6928	30.6517	0.0396	30.6989	3.27E-03		
U-bend	Liquid	271	54.0163	53.9758	0.0320	55.0080	1.47E-03		
U-bend	Liquid	272	55.8406	55.8018	0.0303	56.7445	1.35E-03	1.44E-03	
U-bend	Liquid	273	55.9816	55.9392	0.0339	56.8787	1.51E-03		
U-bend	Vapor	274	55.5007	55.4257	0.0665	56.4210	2.98E-03		
U-bend	Vapor	275	56.3753	56.3116	0.0552	57.2535	2.44E-03	2.73E-03	
U-bend	Vapor	276	55.8542	55.7836	0.0621	56.7575	2.77E-03		

TABLE.XLS

Type	Location	Spec ID#	Soln #9		Post Wt g	Wt. Loss	Specimen Area, cm2	Corr Rate mm/y	Aver. Corr Rate, mm/y
			Starting Wt., g	Wt., g					
Corrosion	Liquid	398	30.5774	30.5735	0.0024	30.5491	1.99E-04		
Corrosion	Liquid	399	29.2529	29.2482	0.0032	30.2303	2.68E-04	2.19E-04	
Corrosion	Liquid	400	30.9877	30.9839	0.0023	30.5421	1.91E-04		
Corrosion	Vapor	401	30.9160	30.9082	0.0063	30.5775	5.22E-04		
Corrosion	Vapor	402	30.8359	30.8256	0.0088	30.5922	7.28E-04	5.67E-04	
Corrosion	Vapor	403	30.8164	30.8094	0.0085	30.7740	4.52E-04		
U-bend	Liquid	253	54.8698	54.8569	0.0044	55.8204	2.00E-04		
U-bend	Liquid	254	55.1661	55.1567	0.0099	56.1025	4.08E-05	8.61E-05	
U-bend	Liquid	255	55.0807	55.0718	0.0094	56.0212	1.81E-05		
U-bend	Vapor	256	54.9793	54.9672	0.0036	55.9247	1.63E-04		
U-bend	Vapor	257	55.1752	55.1588	0.0079	56.1111	3.56E-04	3.10E-04	
U-bend	Vapor	258	55.1760	55.1584	0.0091	56.1119	4.11E-04		
Soln #10									
Type	Location	Spec ID#	Starting Wt., g	Post Wt g	Wt. Loss	Specimen Area, cm2	Corr Rate mm/y	Aver. Corr Rate, mm/y	
Corrosion	Liquid	404	30.2213	30.1367	0.0831	30.4078	6.92E-03		
Corrosion	Liquid	405	29.7655	29.6789	0.0851	30.2776	7.12E-03	7.73E-03	
Corrosion	Liquid	406	30.8524	30.5404	0.1105	30.5078	9.17E-03		
Corrosion	Vapor	407	30.7620	30.6753	0.0852	30.6797	7.03E-03		
Corrosion	Vapor	408	30.4286	30.2928	0.1343	30.5063	1.11E-02	8.35E-03	
Corrosion	Vapor	409	30.3976	30.3131	0.0830	30.5950	6.87E-03		
U-bend	Liquid	259	55.3036	54.8257	0.4694	56.2334	2.11E-02		
U-bend	Liquid	260	55.8825	55.7028	0.1712	56.7844	7.63E-03	1.27E-02	
U-bend	Liquid	261	54.8422	54.6255	0.2082	55.7942	9.45E-03		
U-bend	Vapor	262	54.7897	54.6128	0.1684	55.7442	7.65E-03		
U-bend	Vapor	263	55.3677	55.2181	0.1411	56.2944	6.35E-03	6.98E-03	
U-bend	Vapor	264	55.6609	55.4969	0.1555	56.5735	6.96E-03		

TABLE.XLS

Type	Location	Spec ID#	Soln #7	Starting Wt., g	Post Wt g	Wt. Loss	Specimen Area, cm2	Corr Rate mm/y	Aver Corr Rate, mm/y
Corrosion	Liquid	386	30.6086	30.5821	0.0250	30.5680	2.07E-03		
Corrosion	Liquid	387	30.4745	30.4480	0.0250	30.6518	2.06E-03	2.03E-03	
Corrosion	Liquid	388	30.4700	30.4448	0.0237	30.5520	1.96E-03		
Corrosion	Vapor	389	30.7372	30.7184	0.0173	30.6233	1.43E-03		
Corrosion	Vapor	390	30.7245	30.7013	0.0217	30.7708	1.79E-03	1.84E-03	
Corrosion	Vapor	391	30.9125	30.8829	0.0281	30.6996	2.32E-03		
U-bend	Liquid	236	53.5607	53.5019	0.0503	54.5743	2.33E-03		
U-bend	Liquid	237	54.9199	54.8637	0.0477	55.8681	2.16E-03	2.19E-03	
U-bend	Liquid	238	55.4923	55.4373	0.0465	56.4130	2.09E-03		
U-bend	Vapor	239	55.3966	55.3409	0.0472	56.3219	2.12E-03		
U-bend	Vapor	245	55.9564	55.8870	0.0609	56.8548	2.71E-03	2.36E-03	
U-bend	Vapor	246	56.2112	56.1518	0.0509	57.0973	2.26E-03		
Type	Location	Spec ID#	Soln #8	Starting Wt., g	Post Wt g	Wt. Loss	Specimen Area, cm2	Corr Rate mm/y	Aver Corr Rate, mm/y
Corrosion	Liquid	392	30.6294	30.5952	0.0327	30.5693	2.71E-03		
Corrosion	Liquid	393	30.4422	30.4105	0.0302	30.4016	2.51E-03	2.71E-03	
Corrosion	Liquid	394	30.7147	30.6783	0.0349	30.5026	2.90E-03		
Corrosion	Vapor	395	30.6588	30.6051	0.0522	30.5066	4.33E-03		
Corrosion	Vapor	396	30.2067	30.1511	0.0541	30.5088	4.49E-03	4.25E-03	
Corrosion	Vapor	397	30.5726	30.5238	0.0473	30.4917	3.93E-03		
U-bend	Liquid	247	55.2813	55.2131	0.0597	56.2121	2.69E-03		
U-bend	Liquid	248	55.4756	55.4044	0.0627	56.3971	2.81E-03	2.71E-03	
U-bend	Liquid	249	55.7819	55.7144	0.0590	56.6886	2.63E-03		
U-bend	Vapor	250	55.8576	55.7674	0.0807	56.7607	3.64E-03		
U-bend	Vapor	251	55.5023	55.4131	0.0807	56.4225	3.62E-03	3.53E-03	
U-bend	Vapor	252	55.6345	55.5518	0.0742	56.5483	3.32E-03		

TABLE XLS

Type	Location	Spec ID#	Soln #5		Post Wt g	Wt. Loss	Specimen Area, cm ²	Corr Rate mm/y	Aver Corr Rate, mm/y
			Starting Wt., g	Starting Wt., g					
Corrosion	Liquid	374	30.1389	30.1090	0.0284	30.3779	2.37E-03		
Corrosion	Liquid	375	30.3651	30.3263	0.0273	30.4862	2.27E-03	2.21E-03	
Corrosion	Liquid	376	30.2543	30.2289	0.0239	30.4443	1.99E-03		
Corrosion	Vapor	377	30.5470	30.5206	0.0249	30.5705	2.06E-03		
Corrosion	Vapor	378	30.2843	30.2493	0.0335	30.4207	2.79E-03	2.20E-03	
Corrosion	Vapor	379	30.0047	29.9825	0.0207	30.1730	1.74E-03		
U-bend	Liquid	224	54.6539	54.5677	0.0777	55.6149	3.94E-03		
U-bend	Liquid	225	54.1479	54.0716	0.0678	55.1333	3.11E-03	3.54E-03	
U-bend	Liquid	226	54.9654	54.8592	0.0877	55.9019	3.97E-03		
U-bend	Vapor	227	53.5802	53.5148	0.0569	54.5929	2.64E-03		
U-bend	Vapor	228	54.9481	54.8933	0.0463	55.8950	2.10E-03	2.18E-03	
U-bend	Vapor	229	54.8020	54.7536	0.0399	55.7559	1.81E-03		
Type	Location	Spec ID#	Soln #6		Post Wt g	Wt. Loss	Specimen Area, cm ²	Corr Rate mm/y	Aver Corr Rate, mm/y
			Starting Wt., g	Starting Wt., g					
Corrosion	Liquid	380	30.4051	30.3852	0.0184	30.4379	1.53E-03		
Corrosion	Liquid	381	30.4626	30.4384	0.0227	30.4510	1.89E-03	1.63E-03	
Corrosion	Liquid	382	30.2885	30.2693	0.0177	30.4784	1.47E-03		
Corrosion	Vapor	383	30.6120	30.5984	0.0121	30.5605	1.00E-03		
Corrosion	Vapor	384	30.5788	30.5676	0.0097	30.6202	8.02E-04	8.94E-04	
Corrosion	Vapor	385	30.2530	30.2409	0.0106	30.5862	8.77E-04		
U-bend	Liquid	230	54.3715	54.2941	0.0689	55.3461	3.15E-03		
U-bend	Liquid	231	54.4233	54.3516	0.0632	55.3954	2.89E-03	3.14E-03	
U-bend	Liquid	232	54.3692	54.2865	0.0742	55.3439	3.39E-03		
U-bend	Vapor	233	53.9403	53.9077	0.0241	54.9357	1.11E-03		
U-bend	Vapor	234	53.6792	53.6370	0.0337	54.6871	1.56E-03	1.16E-03	
U-bend	Vapor	235	52.9751	52.9491	0.0175	54.0169	8.20E-04		

TABLE.XLS

Type	Location	Spec ID#	Soln #3			Post Wt g	Wt. Loss	Specimen Area, cm ²	Corr Rate mm/y	Aver Corr Rate, mm/y
			Starting Wt., g	Starting Wt., g	Post Wt g					
Corrosion	Liquid	362	30.3702	30.3043	0.0644	30.6107	5.33E-03			
Corrosion	Liquid	363	30.1322	30.0710	0.0597	30.4892	4.96E-03	5.02E-03		
Corrosion	Liquid	364	30.4220	30.3626	0.0579	30.5984	4.79E-03			
Corrosion	Vapor	365	29.6343	29.5676	0.0652	30.4178	5.43E-03			
Corrosion	Vapor	366	29.9560	29.8926	0.0619	30.5056	5.14E-03	5.07E-03		
Corrosion	Vapor	367	30.3170	30.2593	0.0562	30.6045	4.65E-03			
U-bend	Liquid	212	53.6176	53.4985	0.1106	54.6285	5.13E-03			
U-bend	Liquid	213	53.7249	53.6058	0.1106	54.7306	5.12E-03	5.13E-03		
U-bend	Liquid	214	56.1640	56.0395	0.1160	57.0524	5.15E-03			
U-bend	Vapor	215	54.2658	54.1646	0.0927	55.2455	4.25E-03			
U-bend	Vapor	216	53.3920	53.2928	0.0907	54.4137	4.22E-03	4.19E-03		
U-bend	Vapor	217	53.1311	53.0351	0.0875	54.1654	4.09E-03			
Soln #4										
Type	Location	Spec ID#	Starting Wt., g	Post Wt g	Wt. Loss	Specimen Area, cm ²	Corr Rate mm/y	Aver Corr Rate, mm/y		
Corrosion	Liquid	368	30.2673	30.2485	0.0173	30.5877	1.43E-03			
Corrosion	Liquid	369	30.3232	30.3046	0.0171	30.6014	1.41E-03	1.38E-03		
Corrosion	Liquid	370	30.4735	30.4563	0.0157	30.4376	1.31E-03			
Corrosion	Vapor	371	30.2833	30.2436	0.0386	30.4501	3.18E-03			
Corrosion	Vapor	372	30.1098	30.0692	0.0391	30.2736	3.27E-03	3.22E-03		
Corrosion	Vapor	373	29.9939	29.9538	0.0386	30.4009	3.21E-03			
U-bend	Liquid	218	53.4561	53.4125	0.0351	54.4747	1.63E-03			
U-bend	Liquid	219	52.3783	52.3417	0.0281	53.4488	1.33E-03	1.55E-03		
U-bend	Liquid	220	51.7632	51.7192	0.0355	52.8633	1.70E-03			
U-bend	Vapor	221	51.5932	51.5303	0.0544	52.7015	2.61E-03			
U-bend	Vapor	222	53.5575	53.4870	0.0520	54.5713	2.88E-03	2.72E-03		
U-bend	Vapor	223	53.5914	53.5252	0.0575	54.6035	2.68E-03			

TABLE.XLS

Type	Location	Spec ID#	Soln #1		Post Wt g	Wt. Loss	Specimen Area, cm ²	Corr Rate mm/y	Aver Corr Rate, mm/y
			Starting Wt., g	Starting Wt., g					
Corrosion	Liquid	350	30.2288	30.2046	0.0227	30.7128	1.87E-03		
Corrosion	Liquid	351	29.8495	29.8318	0.0162	30.5058	1.34E-03	1.47E-03	
Corrosion	Liquid	352	30.0967	30.0808	0.0144	30.5344	1.19E-03		
Corrosion	Vapor	353	30.3633	30.3545	0.0073	30.6617	6.03E-04		
Corrosion	Vapor	354	30.2732	30.2607	0.0110	30.6769	9.08E-04	8.36E-04	
Corrosion	Vapor	355	30.7063	30.6827	0.0121	30.7102	9.97E-04		
U-bend	Liquid	200	53.3953	53.3874	-0.0008	54.4169	-2.79E-05		
U-bend	Liquid	201	52.3876	52.3722	0.0089	53.4577	3.27E-04	4.61E-04	
U-bend	Liquid	202	52.8646	52.8330	0.0231	53.9117	1.08E-03		
U-bend	Vapor	203	53.7554	53.7400	0.0089	54.7596	3.19E-04		
U-bend	Vapor	204	54.3935	54.3734	0.0116	55.3670	5.30E-04	4.96E-04	
U-bend	Vapor	205	54.1686	54.1462	0.0139	55.1530	6.38E-04		
			Soln #2						
Type	Location	Spec ID#	Starting Wt., g	Post Wt g	Wt. Loss	Specimen Area, cm ²	Corr Rate mm/y	Aver Corr Rate, mm/y	
Corrosion	Liquid	356	30.4569	30.4244	0.0310	30.3586	2.59E-03		
Corrosion	Liquid	357	30.8977	30.8535	0.0427	30.8019	3.51E-03	2.51E-03	
Corrosion	Liquid	358	29.9883	29.9696	0.0172	30.4224	1.43E-03		
Corrosion	Vapor	359	30.2041	30.1824	0.0202	30.4835	1.68E-03		
Corrosion	Vapor	360	30.5175	30.4930	0.0230	30.4615	1.91E-03	1.84E-03	
Corrosion	Vapor	361	30.5504	30.5255	0.0234	30.5878	1.94E-03		
U-bend	Liquid	206	53.9672	53.9220	0.0367	54.9613	6.66E-02		
U-bend	Liquid	207	54.3216	54.2751	0.0380	55.2986	6.85E-02	5.90E-02	
U-bend	Liquid	208	54.0249	53.9933	0.0231	55.0162	4.18E-02		
U-bend	Vapor	209	53.7746	53.7459	0.0202	54.7779	3.68E-02		
U-bend	Vapor	210	54.1980	54.1629	0.0266	55.1810	4.80E-02	4.60E-02	
U-bend	Vapor	211	54.2555	54.2175	0.0295	55.2357	5.32E-02		

APPENDIX E: OPTICAL PHOTOGRAPHS OF CLEANED SPECIMENS

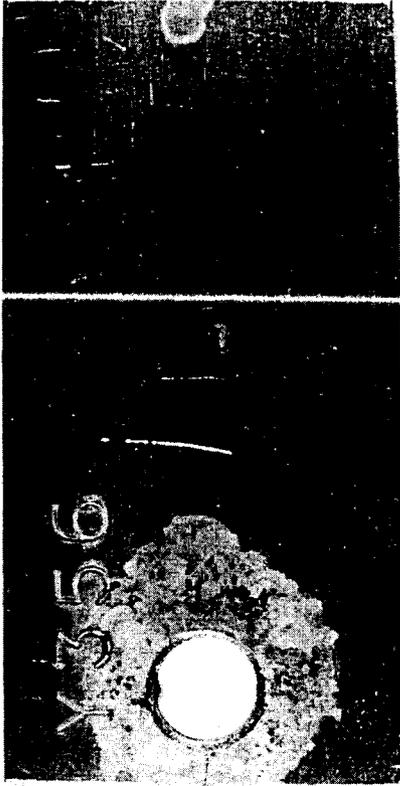


Figure E.1 Totally Immersed Weight Loss Specimen from Solution 2.
Note crevice attack around hole.

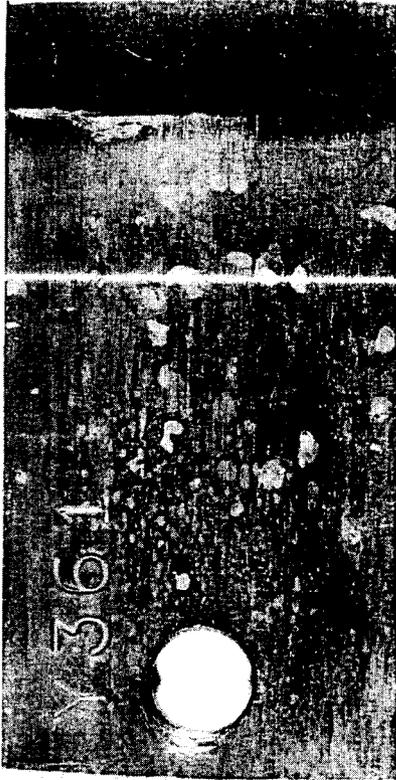


Figure E.2 Air/Solution Weight Loss Specimen from Solution 2.
Note waterline attack and pits in the vapor phase.

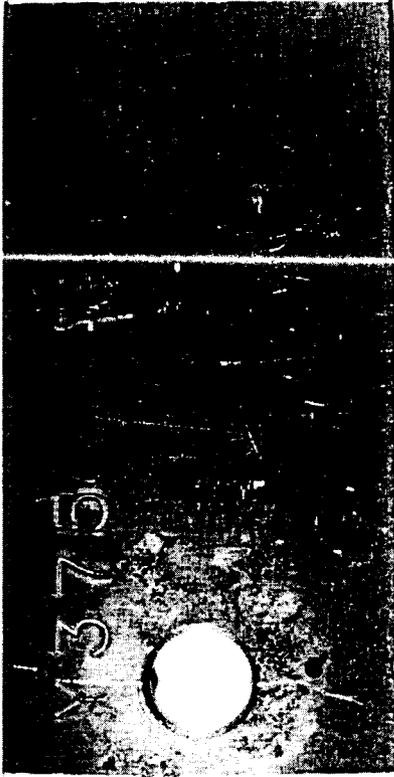


Figure E.3 Totally Immersed Weight Loss Specimen from Solution 5.
Note crevice attack around hole.



Figure E.4 Air/Solution Weight Loss Specimen from Solution 5.
Note waterline attack.

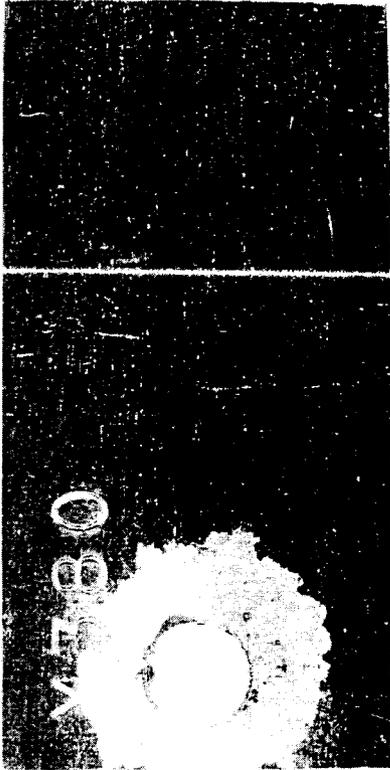


Figure E.5 Totally Immersed Weight Loss Specimen from Solution 6.
Note crevice attack around hole.



Figure E.6 Air/Solution Weight Loss Specimen from Solution 6.
Note waterline attack and pits in the vapor phase.

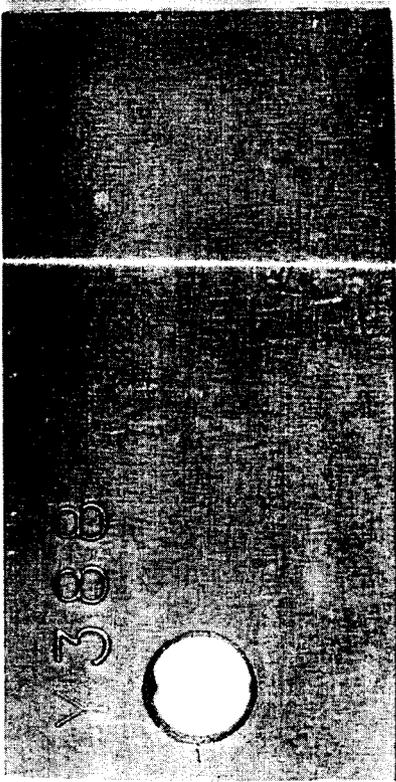


Figure E.7 Totally Immersed Weight Loss Specimen from Solution 7.
Note pristine appearance of surface.

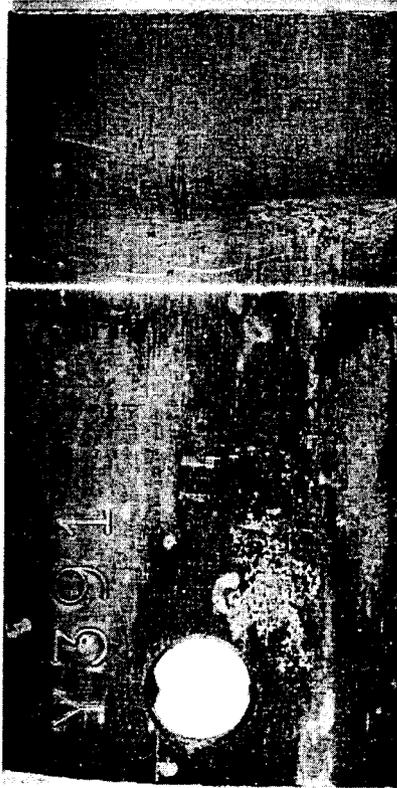


Figure E.8 Air/Solution Weight Loss Specimen from Solution 7.
Note waterline attack and crevice attack near hole.

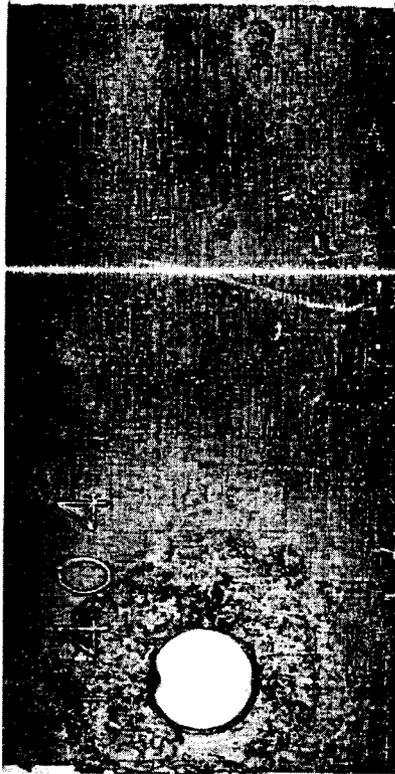


Figure E.9 Totally Immersed Weight Loss Specimen from Solution 10.
Note crevice attack around hole and pits along the length of the specimen.

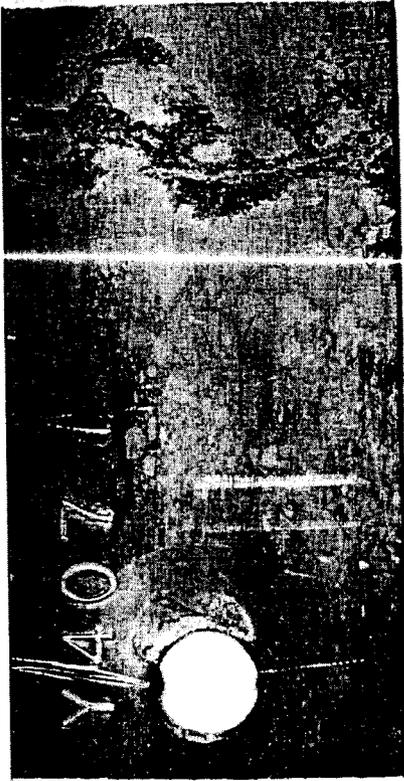


Figure E.10 Air/Solution Weight Loss Specimen from Solution 10.
Note extensive waterline attack, pits in the vapor space
and slight crevice attack at hole.



Figure E.11 Totally Immersed Weight Loss Specimen from Solution 21.
Note pristine appearance of surface.



Figure E.12 Totally Immersed Weight Loss Specimen from Solution 22.
Note deep pits present on the specimen surface and crevice
attack at hole.



Figure E.13 Air/Solution Weight Loss Specimen from Solution 23.
Note extensive removal of metal at and above the
waterline due to massive waterline attack.



Figure E.14 Air/Solution Weight Loss Specimen from Solution 23.
Note extensive removal of metal at and above the
waterline due to massive waterline attack.



Figure E.15 Totally Immersed U-Bend Specimen from Solution 23.
Note small amount of crevice attack around hole.



Figure E.16 Air/Solution U-Bend Specimen from Solution 23.
Note extensive removal of metal at and above the
waterline due to massive waterline attack.



Figure E.17 Air/Solution Weight Loss Specimen from Solution 24.
Note extensive removal of metal at and above the
waterline due to massive waterline attack.



Figure E.18 Air/Solution Weight Loss Specimen from Solution 24.
Note pronounced area of attack with metal removal in
vapor phase.

APPENDIX F: OBSERVATIONS ON CLEANED SPECIMENS

**Observations on Cleaned Specimens:
Pitting (Density, Size, Maximum Depth), Crevice Attack (Maximum Depth), Waterline Attack (Maximum Depth)**

Solution 1

Immersed Specimens	Pitting: incipient pits 2.5E3/m ² , <0.5 mm ² , <0.4 mm Crevice Attack: 0.20 mm deep
Air/Soln Interface Specimens	Pitting: 1E4/m ² , 0.81 mm ² , <0.4 mm Crevice Attack: 0.14 mm deep Waterline attack: 0.02 mm deep

Solution 2

Immersed Specimens	Pitting: 2.5E3/m ² , <0.5 mm ² , <0.4 mm Heavy Crevice Attack: 0.19 mm deep
Air/Soln Interface Specimens	Pitting: 1E4/m ² , 0.81 mm ² , <0.4 mm Moderate Crevice Attack: 0.21 mm deep Waterline attack: 0.03 mm deep

Solution 3

Immersed Specimens	Pitting: none Crevice Attack: none
Air/Soln Interface Specimens	Pitting: none Crevice Attack: none, except incipient crevice on one U-bend specimen

Solution 4

Immersed Specimens	Pitting: none Crevice Attack: none, except incipient crevice on one U-bend specimen
Air/Soln Interface Specimens	Pitting: $2.5E3/m^2$, $<0.5 \text{ mm}^2$, $<0.4 \text{ mm}$ Light Crevice Attack: 0.04 mm deep Waterline attack: 0.06 mm deep

Solution 5

Immersed Specimens	Pitting: $1E4/m^2$, 2.48 mm^2 , $<0.4 \text{ mm}$ Heavy Crevice Attack: 0.12 mm deep
Air/Soln Interface Specimens	Pitting: $1E4/m^2$, $<0.5 \text{ mm}^2$, $<0.4 \text{ mm}$ Moderate Crevice Attack: 0.08 mm deep Waterline attack: 0.09 mm deep

Solution 6

Immersed Specimens	Pitting: $1E4/m^2 - 5E4/m^2$, 1.82 mm^2 , $<0.4 \text{ mm}$ Heavy Crevice Attack: 0.18 mm deep
Air/Soln Interface Specimens	Pitting: $5E4/m^2$, 0.81 mm^2 , $<0.4 \text{ mm}$ Light Crevice Attack: 0.06 mm deep Waterline attack: 0.19 mm deep

Solution 7

Immersed Specimens	Pitting: $2.5E3/m^2$, $<0.5 \text{ mm}^2$, $<0.4 \text{ mm}$ Light Crevice Attack: 0.09 mm deep
Air/Soln Interface Specimens	Pitting: $5E4/m^2$, $<0.5 \text{ mm}^2$, $<0.4 \text{ mm}$ Crevice Attack: 0.14 mm deep Waterline attack: 0.05 mm deep

Solution 8

Immersed Specimens	Pitting: none Crevice Attack: none
Air/Soln Interface Specimens	Pitting: none Crevice Attack: none

Solution 9

Immersed Specimens	Pitting: $2.5E3/m^2$, $<0.5 \text{ mm}^2$, $<0.4 \text{ mm}$ Light Crevice Attack: 0.15 mm deep
Air/Soln Interface Specimens	Pitting: $1E4/m^2$, $<0.5 \text{ mm}^2$, $<0.4 \text{ mm}$ Light Crevice Attack: 0.05 mm deep Waterline attack: 0.02 mm deep

Solution 10

Immersed Specimens	Pitting: $1E4/m^2$, 50.11 mm ² , <0.4 mm Heavy Crevice Attack: 0.16 mm deep
Air/Soln Interface Specimens	Pitting: $5E4/m^2$, 0.62 mm ² , <0.4 mm Light Crevice Attack: 0.09 mm deep Waterline attack: 0.21 mm deep

Solution 11

Immersed Specimens	Pitting: None Light Crevice Attack: 0.06 mm deep
Air/Soln Interface Specimens	Pitting: $1E4/m^2$, <0.5 mm ² , <0.4 mm Light Crevice Attack: 0.07 mm deep Light waterline attack on one U-bend

Solution 12

Immersed Specimens	Pitting: $2.5E3/m^2$, <0.5 mm ² , <0.4 mm Light Crevice Attack: 0.04 mm deep
Air/Soln Interface Specimens	Pitting: $2.5E3/m^2$, <0.5 mm ² , <0.4 mm Moderate Crevice Attack: 0.07 mm deep Waterline attack: 0.05 mm deep

Solution 13

Immersed Specimens	Pitting: none Crevice Attack: none
Air/Soln Interface Specimens	Pitting: $2.5E3/m^2$, <0.5 mm ² , <0.4 mm Crevice Attack: none

Solution 14

Immersed Specimens	Pitting: none Crevice Attack: none
Air/Soln Interface Specimens	Pitting: $1E4/m^2$, $<0.5 \text{ mm}^2$, $<0.4 \text{ mm}$ Crevice Attack: none Light waterline attack: 0.08 mm deep

Solution 15

Immersed Specimens	Pitting: none Crevice Attack: none
Air/Soln Interface Specimens	Pitting: $2.5E3/m^2$, 1.27 mm^2 , $<0.4 \text{ mm}$ Light Crevice Attack: 0.05 mm Light waterline attack: 0.02 mm deep

Solution 16

Immersed Specimens	Pitting: none Light Crevice Attack: 0.02 mm deep
Air/Soln Interface Specimens	Pitting: $1E4/m^2$, 0.81 mm^2 , $<0.4 \text{ mm}$ Very Light Crevice Attack: 0.02 mm deep Light waterline attack: 0.08 mm deep

Solution 17

Immersed Specimens	Pitting: none Crevice Attack: none
Air/Soln Interface Specimens	Pitting: $5E4/m^2$, 1.27 mm^2 , $<0.4 \text{ mm}$ Very Light Crevice Attack: 0.07 mm deep

Solution 18

Immersed Specimens	Pitting: none Crevice Attack: none
Air/Soln Interface Specimens	Pitting: $1E4/m^2$, 0.81 mm^2 , $<0.4 \text{ mm}$ Light Crevice Attack: on one U-bend 0.08 mm deep

Solution 19

Immersed Specimens	Pitting: $2.5E3/m^2$, $<0.5 \text{ mm}^2$, $<0.4 \text{ mm}$ Light Crevice Attack: on U-bend 0.11 mm deep
Air/Soln Interface Specimens	Pitting: $1E4/m^2$, $<0.5 \text{ mm}^2$, $<0.4 \text{ mm}$ Light Crevice Attack: 0.14 mm deep Waterline attack: 0.02 mm deep

Solution 20

Immersed Specimens	Pitting: $2.5E3/m^2$, $<0.5 \text{ mm}^2$, $<0.4 \text{ mm}$ Crevice Attack: none
Air/Soln Interface Specimens	Pitting: $1E4/m^2$, 0.81 mm^2 , $<0.4 \text{ mm}$ Light Crevice Attack: 0.08 mm deep Waterline attack: 0.03 mm deep

Solution 21

Immersed Specimens	Pitting: none, grainy appearance to surface Crevice Attack: 0.37 mm deep
Air/Soln Interface Specimens	gross general attack, especially at and just above waterline

Solution 22

Immersed Specimens	Pitting: pronounced pitting $1E5/m^2$, $<0.5 \text{ mm}^2$, $<0.4 \text{ mm}$ Heavy Crevice Attack: 0.34 mm deep
Air/Soln Interface Specimens	gross general attack, especially at and just above waterline

Solution 23

Immersed Specimens	Pitting: $1E4/m^2$, $<0.5 \text{ mm}^2$, $<0.4 \text{ mm}$ Light Crevice Attack: 0.38 mm deep
Air/Soln Interface Specimens	gross general attack, especially at and just above waterline

Solution 24

Immersed Specimens	Pitting: slight pitting $2.5E3/m^2$, $<0.5 \text{ mm}^2$, $<0.4 \text{ mm}$ Very Light Crevice Attack: 0.09 mm deep
Air/Soln Interface Specimens	gross general attack, especially at and just above waterline

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