ENGINEERING CHANGE NOTICE

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Proj. ECN

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Supplemental [] Direct Revision [X] Change ECN [] Temporary [] Standby [] Supersedure [] Cancel/Void []	Dan A. Reynolds, Process Control, R2-11, 373-3115	[] Yes [X] No	03/20/97
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13a. Description of Change

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14a. Justification (mark one)

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19. Change Impact Review: Indicate the related documents (other than the engineering documents identified on Side 1) that will be affected by the change described in Block 13. Enter the affected document number in Block 20.

SDD/DD	[]	Seismic/Stress Analysis	[]	Tank Calibration Manual	[]
Functional Design Criteria	[]	Stress/Design Report	[]	Health Physics Procedure	[]
Operating Specification	[]	Interface Control Drawing	[]	Spares Multiple Unit Listing	[]
Criticality Specification	[]	Calibration Procedure	[]	Test Procedures/Specification	[]
Conceptual Design Report	[]	Installation Procedure	[]	Component Index	[]
Equipment Spec.	[]	Maintenance Procedure	[]	ASME Coded Item	[]
Const. Spec.	[]	Engineering Procedure	[]	Human Factor Consideration	[]
Procurement Spec.	[]	Operating Instruction	[]	Computer Software	[]
Vendor Information	[]	Operating Procedure	[]	Electric Circuit Schedule	[]
OM Manual	[]	Operational Safety Requirement	[]	ICRS Procedure	[]
FSAR/SAR	[]	IEFD Drawing	[]	Process Control Manual/Plan	[]
Safety Equipment List	[]	Cell Arrangement Drawing	[]	Process Flow Chart	[]
Radiation Work Permit	[]	Essential Material Specification	[]	Purchase Requisition	[]
Environmental Impact Statement	[]	Fac. Proc. Samp. Schedule	[]	Tickler File	[]
Environmental Report	[]	Inspection Plan	[]		[]
Environmental Permit	[]	Inventory Adjustment Request	[]		[]

20. Other Affected Documents: (NOTE: Documents listed below will not be revised by this ECN.) Signatures below indicate that the signing organization has been notified of other affected documents listed below.

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21. Approvals

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Design Authority			Design Agent		
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Cog. Mgr. N.W. Kirch	NW Kirch	4/03/97	QA		
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Other	Frank D. Stoh Jr	4/07/97	Other		

DEPARTMENT OF ENERGY

Signature or a Control Number that tracks the Approval Signature

ADDITIONAL

Chemical and Chemically-Related Considerations Associated with Sluicing Tank C-106 Waste to Tank AY-102

Dan A. Reynolds
Lockheed Martin Hanford Corp., Richland, WA 99352
U.S. Department of Energy Contract DE-AC06-87RL10930

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Abstract: New data on tank 241-C-106 were obtained from grab sampling and from compatibility testing of tank C-106 and tank AY-102 wastes. All chemistry-associated and other compatibility information compiled in this report strongly suggests that the sluicing of the contents of tank C-106, in accord with appropriate controls, will pose no unacceptable risk to workers, public safety, or the environment. In addition, it is expected that the sluicing operation will successfully resolve the High-Heat Safety Issue for tank C-106.

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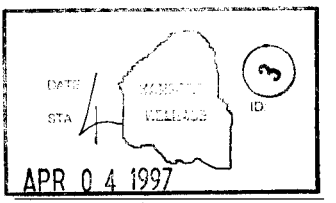

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LIST OF TERMS

AR	PUREX sludge waste from 244-AR Vault
AY-102	tank 241-AY-102
BL	B Plant low-level complexant waste
BNL	Brookhaven National Laboratory
Btu/hr	British thermal units per hour
C-103	tank 241-C-103
C-106	tank 241-C-106
CI	chemical ionization (mass spectrometry)
cm	centimeters
cm/min	centimeters per minute
Cp	heat capacity
CRS	Chemical Reactions Sub-Panel
CWP1	PUREX coating waste
DOE-RL	U.S. Department of Energy - Richland Operations Office
DQO	data quality objective
DSC	differential scanning calorimetry
DTA	differential thermal analysis
EI	electron ionization (mass spectrometry)
FID	flame ionization detector
FTIR	Fourier transform infrared
g/g	grams per gram
g/kg	grams per kilogram
g/L	grams per milliliter
g/mol	gram-moles
GC/MS	gas chromatography/mass spectrometry
GRE	gas release event
HDW	Hanford defense waste
in.	inches
IR	infrared
J/g	joules per gram
K	kelvin
kcal/mol	kilocalories per mole
kgal	kilogallons
kJ	kilojoule
kL	kiloliters
mg	milligrams
mg C/g	milligrams carbon per gram
mg/g	milligrams per gram
mg/L	milligrams per liter
mg/mL	milligrams per milliliter
mL/min	milliliters per minute

LIST OF TERMS (Continued)

mL	milliliter
mol/kg	moles per kilogram
mol/L	moles per liter
mrem	millirem
nCi	nanocuries
nCi/g	nanocuries per gram
PNNL	Pacific Northwest National Laboratory
PUREX	plutonium-uranium extraction
RCR	review comment record
SpG	specific gravity
TAP	Tanks Advisory Panel
TBP	tributyl phosphate (low-level non-TRU liquid waste)
TGA	thermogravimetric analysis
TIC	total inorganic carbon
TOC	total organic carbon
TRU	transuranic
UR	Uranium Recovery
vol%	volume percent
WHC	Westinghouse Hanford Company
wt%	weight percent
XRF	X-ray fluorescence
μCi/g	microcuries per gram
μCi/mL	microcuries per milliliter
μg C/g	micrograms carbon per gram
μg/g	micrograms per gram
μg/kg	micrograms per kilogram
μg/mL	micrograms per milliliter
μL	microliters

CHEMICAL AND CHEMICALLY RELATED ISSUES ASSOCIATED WITH SLUICING TANK C-106 WASTE TO TANK AY-102[1]

1.0 INTRODUCTION

The purpose of this document is to provide additional information to Westinghouse Hanford Company (WHC) staff and to members of the Chemical Reactions Sub-Panel (CRS) of the Tanks Advisory Panel (TAP) for use in evaluating the transfer of high-heat solids from tank 241-C-106 (C-106) to tank 241-AY-102 (AY-102). This report supplements *Safety Assessment for Tank 241-C-106 Waste Retrieval, Project W-320* (WHC 1996). Much of the information contained herein was obtained by running assays and compatibility tests on soft sludges recovered using a large-mouth bottle (on a string) sampler.

During its visits to the Hanford Site in November 1995 and in January, February, and April 1996, the CRS reviewed various safety aspects related to the retrieval of the waste contents of tank C-106, by past practices sluicing of the softer sludges contained in the tank, and transfer to double-shell tank AY-102. That review generated extensive comments (Hudson 1995), captured by WHC in review comment record (RCR) form, that addressed a variety of the CRS concerns, many of which related to the chemical aspects of the waste. This report was written in response to the chemistry-oriented RCRs generated by the CRS, and also addresses a number of chemical concerns, generated by reviewers from the Brookhaven National Laboratory, that were appended with the CRS comments.

No attempt was made in this report to untangle the various RCR comments, some of which dealt with a variety of subjects; rather, the principal author has chosen to identify the underlying issues of concern to both the CRS and the Brookhaven staff and to deal with them in an integrated fashion. Concordance of the information in this report to the RCR comments is provided in Section 2.0, as is the subset of RCRs associated with items assigned for resolution by the principal author (see Appendix A.1).

Section 2.0 of this report contains a discussion that summarizes oversight committee concerns. Section 3.0 provides the reader with a limited amount of relevant background information on tank C-106 and on the analytical tests employed on the waste samples retrieved from the tank in the spring of 1996. Section 4.0 discusses concerns related to the presence of fuel-rich organic chemicals in tank C-106, including an evaluation of the newly identified "sludge oil." Section 5.0 describes experimental tests with actual AY-102 and C-106 samples -- testing that was aimed at assisting an engineering evaluation of waste compatibility concerns. Section 6.0 provides, as input to C-106 thermal characterization modeling, added waste specific information on the observed radio-strontium and cesium

[1]For further information on these subjects, contact Dr. Harry Babad at (509) 373-2897, Ms. Ruth Schreiber at (509) 373-5589, or Dr. Bob Cash at (509) 373-3132.

distribution. Section 7.0 provides information on the observed plutonium distribution in the recent sludge samples. This information will provide some depth-related input on plutonium concentrations for nuclear criticality analysis of tanks C-106 and AY-102. Section 10.0 provides a brief summary/conclusions section, and document references are found in Section 11.0. Further information regarding tank C-106 may be found in *Tank Characterization Report for Single-Shell Tank 241-C-106* (Schreiber et al. 1996).

Appendices included in this report contain: a listing of chemistry-oriented RCRs resulting from the CRS review of retrieval of tank C-106 (Appendix A.1); a tabulation of available draft LABCORE data on the recent wide-mouth bottle-based grab samples obtained from tank C-106 in the spring of 1996 (Appendix A.2); a summary of dose measurements taken during the April 19, 1986 core sampling of tank C-106 that supports thermal modeling (Appendix A.3); a brief discussion of inconsistent total organic carbon (TOC) data and the worst-case total organic carbon measurements in tanks AY-102 and C-106 as reported by Castaing (1995) (Appendix A.4). Finally, a brief discussion of the presence of 2-ethylhexyl phosphate-related materials in tank 241-C-103 (C-103) is provided (Appendix A.5).

2.0 A SUMMARY OF OVERSIGHT COMMITTEE CONCERNS

2.1 SPECIFIC CHEMICAL ISSUES (RCR Comments 8, 9, 21, 28, and 34)

The CRS was concerned with the following specific areas associated with the organic chemistry of tank C-106. Where appropriate, in the body of this document, cross references will be provided to CRS comments and to the data-containing sections of this document.

Potential for a propagating reaction of the residual organics in tank C-106 after dryout. One item of CRS concern was the "evaluation of hazard (e.g., waste dryout and overheating) consequences resulting after sluicing is completed in tank C-106". Appendix A.1, RCR 8 discusses possible consequences and behavior of waste remaining in tank C-106 after sluicing is completed; e.g., waste dryout and overheating (see Appendix A.1, RCRs 8 and 9). A related concern is the possibility of exceeding tank temperature limits (in the absence of water additions) from heat generation in the hardpan left in tank C-106 after sluicing (see Appendix A.1, RCR 34)." Questions that result from this concern include:

Is tank C-106 an organic complexant-rich tank?

- Will any {significant} organic present transfer to AY-102 during sluicing?

  The organics present in tank C-106 are low in energy and therefore will provide neither significant sources of carbon-hydrogen bonds (gas release event issue) nor fuel (organic safety concern) to tank AY-102. (See Section 4.0)

- Will sufficient residual organics remain in the tank to pose a hazard from condensed-phase propagation reactions when ventilation is stopped (and the remaining waste heats and dries out) in tank C-106 after sluicing? (see Appendix A.1, RCR 33)

  The organics present in tank C-106 are low in energy and therefore will not provide significant quantities of fuel (organic safety concern) upon drying out the tank after sluicing is complete. (See Section 4.0)

- Conflicting Chemical Total Organic Carbon (TOC) Data (Part of RCR Comment 28).

  The data provided in Section 4.0 support the information used in the safety analysis for the retrieval process. No high TOC values were observed for the samples obtained from tank C-106. This was one area of concern to the CRS. In addition, the energetics associated with the TOC measurements strongly suggest that any complexants added to tank C-106 have aged to other less-reactive species, such as sodium oxalate.

Strontium Distribution. (Tank Safety-Related Heat Load Concerns) (Related to Appendix A.1, RCRs 8, 9, 32, 33, and 34)

- Where is the heat source? Is there reliable information about its magnitude? What is the evidence that significant heat is not generated in the hardpan? Are temperature records available for the period before the strontium-90 was added to the tank? The CRS suggests examination of existing data for more detailed answers. (RCR 32 and 33)

  The strontium and cesium assays (Section 6.0) reported in this document support the hypothesis that significant quantities of heat-generating materials are found in the soft sludge layer. Although sampling limitations precluded providing a definitive answer to the question of whether significant heat is generated in the hardpan, updated modeling efforts conclude that heat so generated would not pose a safety problem after the sluicing of soft materials from tank C-106 (Bander 1996).

Plutonium Distribution Issues. (RCR Comments 21, 25, and 38)

- Are there any transuranic (TRU)-related waste compatibility issues associated with transfer of wastes from tank C-106 to tank AY-102?

  No criticality-related concerns were identified by the work reported in Section 7.0 of this report. In evaluating the potential for nuclear criticality related to the transfer of the contents of tank C-106 to tank AY-102, the stability constants for plutonium oxyhydroxide precluded significant solubilization of plutonium by the small amounts of complexants in tank AY-102 (Waltar 1996).

The CRS was concerned with whether there is a criticality issue. "We strongly suggest a definitive criticality analysis be performed for this specific project before retrieval begins (RCR 25). What are the consequences with respect to criticality in using a sluicing fluid which contains complexants capable of segregating plutonium?" That task is complete (see Waltar 1996).

Waste Compatibility Concerns. (RCR Comments 21, 22, 23, 35, 36, 37, 39, 40, 41, and 44 deal with some aspect of waste compatibility)

- What is the potential for creation of a gas release event (GRE) in tank AY-102 during or after sluicing of the waste in tank C-106? (RCR Comments 21, 23, and 36)

Although compatibility tests made on combinations of C-106 sludge and AY-102 sludge and supernatant fluids did not suggest any issues associated with GRE formations, data presently available cannot preclude that such an event could occur. Therefore, the project will use a partial sluicing strategy, coupled with a detailed gas evolution and surface and sludge height measurement strategy (Barton 1996), to assure that GRE conditions are not occurring in tank AY-102.

- Are the chemistry and physics of the waste in tank C-106 similar to those known to lead to gas retention and/or potential for GRE events?

  See Barton (1996).

CRS Concerns with Waste Compatibility- and Operability-Related Issues. Concerns were repeatedly voiced by the CRS on the behavior of solids in the C-106 and AY-102 system, resulting in a set of waste compatibility- and operability-related issues. These issues were itemized in the bullets above. The following sections provide more detailed listings of the CRS concerns.

GRE Related Comments. "C-106/AY-102 waste compatibility." The primary concern is creating GRE conditions (RCR 21). Post-transfer "fluffing" of waste and its effect on waste behavior (e.g., gas retention) (RCR 23). Could there be a gas generation (release) problem? Unless safe upper limits for the volume of retained gas can be demonstrated, we suggest continuous monitoring of flammable gas concentration in the dome spaces of both C-106 and AY-102 (consistent with flammable gas controls) before, during, and after retrieval (RCR 36)."

- Are there any other waste compatibility issues associated with transfer of wastes from C-106 to AY-102 (e.g., RCR Comment 41)?

  Compatibility tests made on combinations of C-106 sludge and AY-102 sludge and supernatant fluids did not suggest that any "other" compatibility issues would be associated with the transfer of wastes from tank C-106 to tank AY-102 (See Section 5.0).

- Deagglomeration - RCR Comment 22

  Compatibility tests made on combinations of C-106 sludge and AY-102 sludge and supernatant fluids did not suggest that there would be any deagglomeration-related issues associated with the transfer of wastes from tank C-106 to tank AY-102 (See Sections 5.1 and 5.3).

- Transfer Line Plugging and Waste Compatibility - RCR Comment 39

  Compatibility tests made on combinations of C-106 sludge and AY-102 sludge and supernatant fluids did not suggest that any line plugging-related issues, such as formation of gels, would be associated with the transfer of wastes from tank C-106 to tank AY-102 (See Section 5.3).

- Waste Cooling and Solubility Considerations - RCR Comments 40 and 44

  Consideration of the chemical characteristics of C-106 sludge and AY-102 sludge and supernatant fluids did not suggest that there would be any waste cooling or solubility- related issues associated with the transfer of wastes from tank C-106 to tank AY-102 (See Section 5.4, 5.5).

- Stored Energy (Lattice Energy in Crystals) - RCR Comment 35

  An evaluation of the chemistry and physics of the waste materials in tank C-106 did not suggest any possibility of problems related to stored lattice energy in waste crystals (see Section 5.6).

- Consequences of "Dissolution of Salts" ... Gas Evolution - RCR Comment 37

  Sluicing with dilute liquids will not cause release of water-soluble gases. Although ammonia has been found in the headspaces of most tanks, conditions for its storage and spontaneous release during sluicing in tank C-106 appear unlikely. Furthermore, this document reports that the nature of the solids in tanks C-106 and AY-102 poses no compatibility concerns related to "Dissolution of Salts," because there are no significant amounts of water-soluble salts (the tanks are undersaturated in sodium nitrate and nitrite) present in either of these tanks (See Section 5.4).

Concerns were also voiced by the CRS on the behavior of solids in the C-106 and AY-102 system resulting in a set of waste compatibility- and operability-related issues. This concern was addressed above.

Waste Solubility/Dissolution Effects. "What is the plan to preclude potential precipitation during transfer and getting pipes plugged? Related questions: Will there be a plugging problem during startup or shutdown? How would pipe blockage be addressed? How does the plan to avoid pipe plugging compare with those of past practice (both successful and unsuccessful)? We suggest describing expected gas release, particle size distribution, etc. in the transfer line, together with bounds for flow rate, particle size, and solids loading, entrained or released gas, etc. (to avoid pipe blockage or damage) and associated controls. If pipe blockage cannot be ruled out, we suggest including a description of contingency plans (RCR 39)."

"What are the consequences involved in the dissolution of precipitated salts in the sludge? (RCR 37)"

"What problems will emerge when the saturated sluicing solution, produced in the sluicing operation, drops in temperature in the transfer lines? Answer given at the CRS meeting: "Dilute solutions based on using buffered water should not create saturated sluicing solutions" and "The analysis determined that the temperature change during transfer is less than 2 °C, which is minimum with respect to the unsaturated region of the waste during transfer." We suggest arguments leading to these conclusions be included (RCR 40)."

Specifics Needed On Waste Compatibility Tests. "What tests have been done to demonstrate compatibility between the sluicing fluid and the C-106 waste? (What will be done to ensure compatibility?) While specific actions were not agreed upon, the mixing of actual waste samples would appear to give the most reliable answer. We request presentation of a detailed plan, including important factors and specific steps, to determine waste compatibility. (RCR 41)"

> Compatibility tests were made on C-106 and AY-102 wastes and are reported in Section 5.0.

Solution Concentration Effects. "Is the assumption that dilution can be used to prevent line plugging practical when considered in the light of the mass of soluble precipitated salts in the sludge? Is there a significant amount of potential soluble material than can dissolve and re-precipitate? Whether the answer is yes or no, we believe the answer should be given in the document (RCR 44)."

> As was stated earlier, the wastes were undersaturated with respect to most salts.

Stored Energy (As Superheated Steam). "Is there any stored energy in the waste that may be violently released during sluicing? WHC placed major emphasis during the CRS presentations on the fact that such behavior had not been observed in tanks containing similar high-heat waste. We believe the answer must be based on data from C-106. We therefore suggest re-examination of existing data (including original data references) to attempt reconciliation of inconsistencies and determine whether superheated regions can be ruled out. If superheated regions cannot be ruled out, we suggest considering the potential effects of steam flashing. (RCR 34)"

> Modeling suggests that by keeping the sluicer nozzel level and aimed at the waste liquid level during sluicing, superheated (steam generating) conditions will be avoided. Such controls will become part of operating conditions for sluicing C-106. The waste will also be cooled with a chiller prior to sluicing to ensure the saturation zone no longer exists (Bander 1996).

Waste Settling/Deagglomeration Related Concerns. "Possible de-agglomeration of waste particles and its effect on settling. This concerns both clarification of sluicing fluid and the potential for gas retention (RCR 22)."

Compatibility testing demonstrated little deagglomeration.

Toxic Gas Concerns. "How much and what kinds of toxic gas will be released? We suggest inclusion of a detailed description of the potential source term and corresponding health and safety controls (Part of RCR 37)."

This document provides detailed discussions of many, but not all, of the aspects of chemistry that were of concern to the CRS and provides information for use by the process engineers and/or modelers to evaluate the remaining concerns.

No sampling of the riser exhaust line for ammonia was possible in the time available for this study. However, plans are being implemented to get baseline headspace concentration data for tanks C-106 and AY-102 prior to starting sluicing. These data, coupled with gas monitoring and establishment of gas concentration controls during sluicing (with cool dilute waste solution), should ensure safety with respect to toxic gases.

3.0 RELEVANT BACKGROUND INFORMATION

3.1 THE CHEMISTRY AND STRATIGRAPHY OF TANK C-106

Tank C-106 is a 2,000-kL (530-kgal) tank, and contains four identifiable major waste layers. The bottom layer consists of 102 kL (27 kgal) of uranium recovery (UR) waste (note that 47 kL [12.5 kgal] is needed to fill the tank's dished bottom, leaving only 13 cm [5 in.] of UR waste at the risers at the edge of the tank). The remaining 640 kL (170 kgal) of solid waste is high-heat, higher-plutonium and strontium-containing, soft sludge. NOTE: The observed plutonium concentration is still well below concentrations of criticality concern.

The numbers proposed in the Hanford defined waste (HDW) documentation differ somewhat from those reported in WHC sources. Although other values are used in a number of supporting documents, based on alternate interpretations of historic data (i.e., 91 kL [24 kgal] of hardpan, and 655 kL [173 kgal] of soft sludge for 12%/88% split volumes, respectively, rather than the 25%/75% given in the Agnew [1995] evaluation), this difference has no effect on the outcome of the studies reported in this document.

The waste contents are described in Table 3-1.

Table 3-1. Tank C-106 Solids Waste Type, Volume, and Depth.[1] (Agnew 1995) (2 Sheets)

Waste Type[2] (Tank Bottom to Top)	Waste Volume	Depth at Tank Wall Edge Riser[2]
UR (from treated $BiPO_4$ metal waste)	27 kgal	17 in. [Σ 27 kgal]
CWP1 (PUREX coating waste)	34 kgal	17 in. to 29 in. [Σ 61 kgal]
AR (PUREX sludge from 244-AR Vault - PUREX sludge wash waste)	64 kgal	29 in. to 52 in. [Σ 125 kgal]
BL (B-Plant low-level complexant waste)	20 kgal	52 in. to 59 in. [Σ 145 kgal]
Unknown	52 kgal	59 in. to 78 in.; Assigned to 26 AR and 26 BL [Σ 197 kgal]

Table 3-1. Tank C-106 Solids Waste Type, Volume, and Depth.[1] (Agnew 1995) (2 Sheets)

Notes:

The unknown layer is assigned to reflect a solids level adjustment from 540 kL (142 kgal) in 1978 (4th quarter) to 745 kL (197 kgal) in 1979 (1st quarter). Because there were no further solids-containing waste additions to explain this increase in solids, Agnew (1995) assumed that these solids actually derive from a combination of AR and BL, and assigned the unknown layer contents accordingly.

PUREX = plutonium-uranium extraction

[1]The methods used to get the estimates found in Tables 3-1 and 3-2 are found in Agnew (1995).

[2]The four main waste types (UR, CWP1, AR, and BL) are listed in the order that they entered the tank. However, the unknown waste cannot be assumed to be a layer on the top of the waste; rather, it is the missing volume associated with the HDW transaction record for tank C-106.

[3]Measured from the tank bottom centerline.

The UR layer in Table 3-1 consists of additions of uranium recovery wastes (formally called tributyl phosphate [TBP] waste). However, it undoubtedly contains some unsluiced metal waste heel ("hardpan") as well.

The CWP1 layer consists of cladding waste additions from early PUREX operations accumulated through 1960 (2nd quarter).

The AR layer consists of solids that were transferred from AR Vault from 1967 to 1971. During this operation, PUREX sludge solids that were sluiced from A and AX farms were fed to AR Vault and allowed to sediment. The supernatant was transferred to tank C-106, allowed to clarify, and then transferred to tank C-105 for feed to cesium recovery. Low-Cs supernatants from tank C-105 were cycled to the AR Vault for caustic washing of sludges to leach as much Cs out as possible. These washings were cycled back to tank C-105 through tank C-106.

The AR solids were then acid digested and the supernatant from that digestion was sent to B Plant for Sr removal. Any remnant solids were reneutralized and recycled through the strontium recovery process steps. The AR solids that accumulated in tank C-106 and other tanks were derived from peptized (non-sedimented) solids from all of these processing activities.

In 1974, as a result of an attempt to move some of the AR solids to other C Farm tanks by pumping, some AR solids from tank C-106 were moved to tank C-103. At that point, C-106 began receiving BL waste from B Plant, and the upper layers of the tank are due to these latter additions. The tank was declared inactive in early 1979.

Once again, the unknown 200-kL (52-kgal) layer is most likely simply unaccounted AR and BL solids; Agnew (1995) has assigned them as such in his inventory prediction. His Hanford Defined Waste layer compositions for these waste types are listed in Table 3-2.

The volume of the supernatant liquids in the tank varies according to the level of evaporation of that fluid. The volume has been estimated at about 120 kL (32 kgal).

3.2 SAMPLING ANALYSIS PLAN AND COMPATIBILITY TEST PLAN SUMMARY

The *Tank 241-C-106 Grab Sampling and Analysis Plan* (Schreiber 1996) identifies the overall characterization objectives for sample collection, laboratory analytical evaluation, and reporting requirements for the tank C-106 grab sample event. These requirements are consistent with the *Data Quality Objectives for Tank Farms Waste Compatibility Program* (Fowler 1995), the *Tank Safety Screening Data Quality Objective* (Dukelow et al. 1995), and *Tank 241-C-106 Grab Sample - Technical Letter of Instruction* (Cash and Babad 1996). The specific needs of this sampling event identified in the Sampling and Analysis Plan include:

- Verification that tank C-106 contains little or no TOC or has low energetics
- Spot checking of the radiocesium content in solution to verify dose estimates during retrieval
- Determination of ^{90}Sr and TRU content to demonstrate whether these chemical constituents are well represented in the tank's topmost solids layer.

The WHC 222-S Laboratory test plan, *Sample Preparation of Tank 241-C-106 Samples and Testing for Compatibility with Tank 241-AY-102 Supernate* (Crawford 1996), provides sample preparation methods for the non-routine analyses required by Schreiber (1996). The non-routine analysis guidance specified in Crawford (1996) includes the separation of the tank C-106 solid and liquid fractions, a solvent extraction test to remove organic material from the solids, centrifugation tests to evaluate ease of oil release from C-106 sludges, and compatibility mixing studies of tank C-106 sludge with tank AY-102 supernatant and sludge.

Figure 3-1 contains a cross sectional view of tank C-106 that provides a visual indication of the location of the samples that form the primary focus of this report. A total of 15 grab samples were taken from tank C-106 in February and March 1996. Samples 6C-96-1 to 6C-96-4 were taken through riser 1 on February 8, samples 6C-96-5 to 6C-96-10 were taken

through riser 1 on February 23, and samples 6C-96-11 to 6C-96-16 were taken through riser 7 on March 1. Sample 6C-96-9 was not recovered from the tank because the sample bottle broke during the sampling process.

Table 3-2. Predicted C-106 Waste Chemistry Composition from HDW Estimate.[1] (2 sheets)

Estimated Concentration mol/L	Uranium Recovery UR	CWP1	PUREX AR	B-Plant BL
Na	3.5720	1.98	5.64	6.70
Al		5.15	0.07	6.07
Fe (total)	1.5734	0.16	1.30	2.21
Cr	0.0029	0.00	0.01	0.00
Bi	--	--	0.00	--
La	--	--	0.00	0.00
Hg	--	--	0.00	0.00
$ZrO(OH)_2$	--	--	0.00	--
Pb		0.12	0.00	--
Ni	0.0015	0.00	0.14	1.21
Sr	--	--	--	--
Mn	--	0.00	--	--
Ca	0.3450	0.12	0.11	0.20
K	0.0158	0.00	0.03	0.01
Balance	0.0000	0.00	0.00	0.00
Density	1.3154	1.41	1.30	1.99
Vol.% solids feed	2.8000	8.10	3.10	0.68
Void fraction	0.9142	0.83	0.83	0.57
wt% H_2O	60.0521	57.86	68.82	33.61
TOC wt% C (wet basis)	0.0003	--	--	0.17
OH^{-1} Free	0.0238	0.01	0.06	0.11
OH^{-1}	5.5549	17.49	4.46	30.99
NO_3^{-1}	2.1904	0.56	0.00	0.00
NO_2^{-1}	0.3693	0.67	0.74	0.99
CO_3^{-2}	0.5114	0.12	0.20	0.35
PO_4^{-3}	0.1191	0.02	0.01	--

Table 3-2. Predicted C-106 Waste Chemistry Composition from HDW Estimate.[1] (2 sheets)

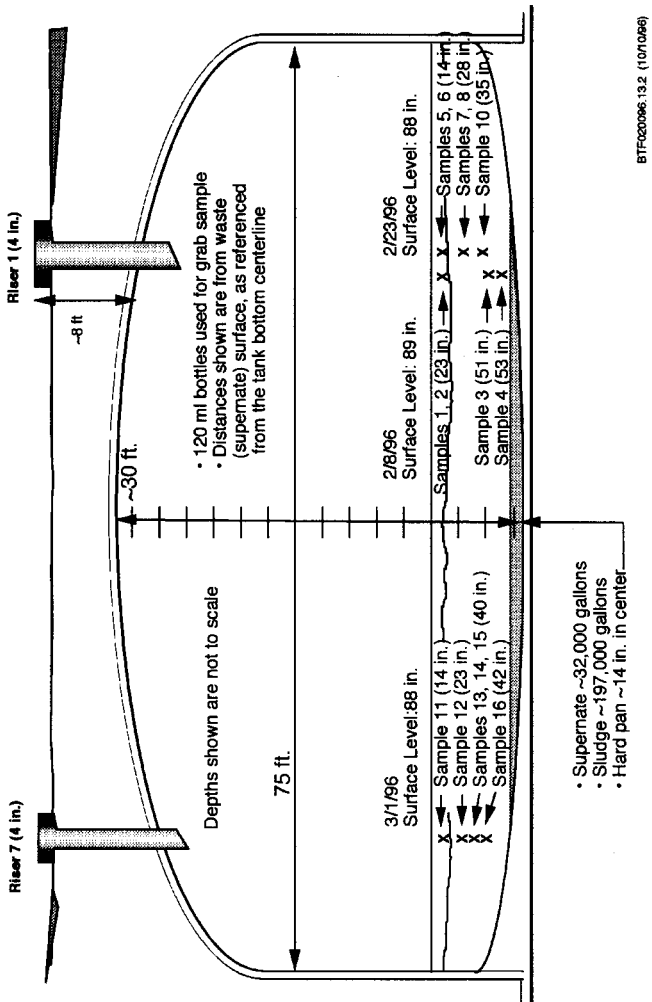
Estimated Concentration mol/L	Uranium Recovery UR	CWP1	PUREX AR	B-Plant BL
Na	3.5720	1.98	5.64	6.70
SO_4^{-2}	0.1298	0.01	0.07	0.03
SiO_3^{-2}	0.0000	0.02	2.27	2.39
F^{-1}	--	--	0.00	--
Cl^{-1}	0.0938	0.01	0.00	--
Citrate [$C_6H_5O_7^{-3}$]	--	--	--	0.01
$EDTA^{-4}$	--	--	--	--
$HEDTA^{-3}$	--	--	--	--
Glycolate	--	--	--	0.012
Acetate	--	--	--	--
Oxalate	--	--	--	--
DBP	--	--	--	--
Butanol	--	--	--	--
NH^3	0.0009	0.00	0.22	0.09
$Fe(CN)_6^{-4}$	--	--	--	--
Pu-239 (nCi/g)	0.0032	0.58	7.27	2.61
U-238 (mol/L)	0.1397	0.10	0.00	0.56
Cs-137 (Ci/L)	0.0013	0.00	0.23	--
Sr-90 (Ci/L) decayed to 1-1-94	0.0220	0.00	11.83	4.70

Notes:

[1]The methods used to get the estimates found in Tables 3-1 and 3-2 are found in Agnew (1995).

-- = No information provided by Agnew (1995).

Figure 3-1. Tank C-106 Grab Sample Activity.



4.0 ORGANIC CHEMICAL CONCENTRATION CONCERNS

The CR-SubTAP expressed concern whether tank C-106 contained sufficient organics to pose a risk for propagation after retrieval of the soft suspendable solids, if the tank contents were allowed to dry out. The primary purpose of retrieving the waste from tank C-106 is to allow WHC to stop adding cooling water, with its concomitant requirement for active ventilation, to the tank. Cooling water addition poses the potential, in these single-shell tanks, that a loss of tank integrity could result in the fluid contents of the tank leaking to the surrounding soils. The addition of water does not in itself pose a potential for a loss of integrity. Although the potential is there whether or not water is added, the required continued addition of water can obviously result in greater consequences if a leak occurs. Such a leak is not unlikely, considering that 63 single-shell tanks have required saltwell pumping to reduce the drainable liquid inventory that could be leaked to the soil.

The organic safety program considers a tank at risk from a propagating reaction if that tank contains 3% or more TOC with an energy value of at least 480 J/g (dry weight basis). The presence of water mitigates these conditions somewhat, but cannot be relied upon relative to high-heat tank C-106. In addition, it is well documented that tanks containing significantly less organic (0.8 to 3% TOC), where the organic is associated with species that contain carbon-hydrogen and nitrogen-hydrogen bonds, generate hydrogen gas at rates considerably more rapid than the rate of radiolysis of water. This production of hydrogen, coupled with inopportune physics, is the cause of a potential Flammable Gas safety issue. This safety issue is a subject of CR-SubTAP concern, and is dealt with in Section 5.2 of this report.

The Safety Screening data quality objective (DQO) (Dukelow et al. 1995) requires testing of tank samples for energetics as well as moisture content. If energetics of 480 J/g (dry weight basis) are found, TOC analysis is required. Because of the interest in the risk from organics, TOC analysis was made part of the sampling and analysis plan (Schreiber 1996). A further modification to standard characterization practices was the addition to the sampling and analysis plan of a dewatering step to minimize analytical ambiguities and identify species-specific effects between the tank solids and the aqueous solutions that are part of the waste. Such a dewatering step would allow one to determine whether energetics in a waste sample were due to fuel-rich soluble organic complexants (which could be easily removed by sluicing), or whether they were associated with the solids. This question focuses on the broader issue of how completely the soft materials in tank C-106 could be sluiced, an issue dealt with in the Project W-320 Safety Assessment (WHC 1996).

Table 4-1 contains the results of differential scanning calorimetry (DSC), thermogravimetric analysis (TGA) and TOC analysis of the sludges obtained from C-106. Interpretation of the data is made a bit more complex than usual by the fact that the dewatering step required in the sampling and analysis plan added another unexpected complication to the analysis and interpretation process.

Table 4-1. Organic Related Analysis: Average DSC, TGA, and TOC Sludge Sample Results by Waste Depth.[7] (2 sheets)

Riser 1					Riser 7		
DSC Dry (J/g)	TGA (wt%)	TOC Dry (wt%)	Depth[1] (in.)	Sample Type	DSC Dry (J/g)	TGA (wt%)	TOC Dry (wt%)
ns	ns	ns	14	Centrifuged sludge	71	9.03	nr
ns	ns	ns		Control sample	235	39.8	nr
ns	ns	ns		Filtered, centrifuged sludge	0	31.9	2.7
110	8.28	nr	28	Centrifuged sludge	ns	ns	ns
0	31.1	nr		Control sample	ns	ns	ns
325	12.8	3.1		Filtered, centrifuged sludge	ns	ns	ns
142[2] 0[3]	52.9[2] 57.9[3]	2.4[5] 2.7[6]		Raw sludge	ns	ns	ns
0	12.9	nr	35	Centrifuged sludge	ns	ns	ns
0	13.5	nr		Control sample	ns	ns	ns
111	25.7	3.0		Filtered, centrifuged sludge	ns	ns	ns
ns	ns	ns	40	Centrifuged sludge	243	9.36	nr
ns	ns	ns		Control sample	112	31.1	nr
ns	ns	ns	40	Filtered, centrifuged sludge	0	23.7	1.9
ns	ns	ns		Raw sludge	127[2] 446[3]	64.2[2] 55.3[3]	8.1[5] 6.5[6]

Table 4-1. Organic Related Analysis: Average DSC, TGA, and TOC Sludge Sample Results by Waste Depth.[7] (2 sheets)

Riser 1					Riser 7		
DSC Dry (J/g)	TGA (wt%)	TOC Dry (wt%)	Depth[1] (in.)	Sample Type	DSC Dry (J/g)	TGA (wt%)	TOC Dry (wt%)
0	3.18	5.7	51	Raw sludge	ns	ns	ns
216[4]	3.59	nr	53	Centrifuged sludge	ns	ns	ns
0	33.5	nr		Control sample	ns	ns	ns
0	24.1	2.1		Filtered, centrifuged sludge	ns	ns	ns

Notes:

nr = not requested
ns = no sample

[1]Measured from waste surface
[2]Run under nitrogen
[3]Run under air
[4]This result is an average of the following: 0 J/g, 1,037 J/g, 0 J/g, 14 J/g, 26.5 J/g. Because this material showed no energetics when tested by PNNL (see Section 4.2.8), 1,037 J/g is clearly due to an analytical or sample handling error.
[5]Dry TOC result calculated using the TGA result run under nitrogen.
[6]Dry TOC result calculated using the TGA result run under air.
[7]DSC results are rounded to the nearest J/g, and TOC results are rounded to the nearest 0.1 wt% to better reflect analytical precision.

The laboratory staff were asked to dewater the sludge by centrifugation using a filter cone to maximize separation of water-soluble from water-insoluble waste components. The liquid that was obtained from the filtering of the sludge was designated "interstitial liquid," and the solids were designated "filtered centrifuged solids." In addition to the filtering, a "control sample" of sludge was processed to compare simple centrifuged material with that which had undergone filtration. A third sludge portion underwent a simple centrifugation in a tapered cone to perform density determinations. The liquid portion obtained from the simple centrifugation was designated "decanted supernate," and the solids were designated "centrifuged solids." Any analyses performed on sludge material that had not been processed to remove liquid ("raw" wet sludge) was designated as "sludge (from liquid grab sample)."

The centrifugation that was performed in the tapered cone resulted in the separation of a hitherto unencountered, sludge-associated organic oil that floated on the aqueous layer. This material was designated as "potential organic layer." When this material was observed, the process for dewatering the bulk of the sludge materials was altered. A simple centrifugation step was added to remove most of the liquid as well as the organic oil before the sludge was centrifuged through the filter cones. This "pre-centrifugation" step produced approximately 0.2 to 0.5 mL of a floating material from an approximately 50-mL sample of "raw" wet sludge. The results of DSC, TGA and TOC analyses on the variety of subsamples of sludge produced by these oil separations and subsequent filtering steps are described below. Information on the nature of the sludge oils so produced are described in Section 4.2.

As can be seen from Table 4-1, the "dewatered" sludge samples obtained from tank C-106 were moderately high in organics (samples >3% TOC), but were relatively energy poor. Such a result is in keeping with the aging of B Plant organics to sodium oxalate, which is insoluble in the tank wastes. Speciation of sludge samples (see Table 4-2) indeed demonstrated the presence of a significant concentration of sodium oxalate.

Table 4-2. Average C-106 Sludge TOC and Oxalate Results by Waste Depth.

Riser 1				Riser 7	
TOC Dry[5]	Oxalate	Depth[1] (in.)	Sample Type	TOC Dry[5]	Oxalate
μg C/g	μg/g (μg C/g)[2]			μg C/g	μg/g (μg C/g)[2]
ns	ns	14	Filtered, centrifuged sludge[4]	27,000	152,000 (41,400) (Note 3)
31,000	77,500 (21,100)	28	Filtered, centrifuged sludge[4]	ns	ns
30,000	68,600 (18,700)	35	Filtered, centrifuged sludge[4]	ns	ns
ns	ns	40	Filtered, centrifuged sludge[4]	19,000	53,700 (14,600) (Note 3)
21,000	80,200 (21,800)	53	Filtered, centrifuged sludge[4]	ns	ns

Notes:

ns = no sample

[1]Measured from the waste surface.

[2]Carbon equivalent of oxalate is provided in parentheses below the oxalate result.

[3]The observation that on occasion, that oxalate results by liquid chromatography, expressed as carbon, are higher in concentration than the TOC measured on the same sample, is not understood. The results are to be taken only as a semiquantitative indication that sodium oxalate is a significant contributor to the organics in the C-106 sludge solids. The carbon results are in general agreement with the oxalate carbon equivalents results.

[4]These samples contained 13 to 32% water for which the oxalate values were not corrected.

[5]TOC results are rounded to the nearest 1,000 μg C/g on a dry-weight basis.

Analysis of the various aqueous liquid phases produced during sludge oil separation and dewatering confirmed that the waste contains little of the waste soluble complexant added in B Plant (BL waste). These results are tabulated in Table 4-3.

Table 4-3. Organic Related Analysis: Average DSC, TGA, and TOC Liquid Sample Results by Waste Depth.[4]

Riser 1					Riser 7		
DSC Dry (J/g)	TGA (wt%)	TOC (%)[7]	Depth[1] (in.)	Sample type	DSC Dry (J/g)	TGA (wt%)	TOC(%)[7]
0	80.9	1.0[2] 1.5[3]	14	Supernatant	ns	ns	ns
ns	ns	ns	14	Interstitial liquid	10	46.4	0.3[2] 0.3[3]
ns	ns	ns	23	Supernatant	0	79.3	0.8[2] 1.0[3]
0	35.4	0.3[2] 0.3[3,5]	28	Interstitial liquid	ns	ns	ns
0	60.3	0.5[2] 0.5[3]	35	Interstitial liquid	ns	ns	ns
ns	ns	ns	40	Interstitial liquid	445	75.8	0.7[2,6] 0.7[3,5,6]
0	58	0.3[2,6] 0.5[3,6]	53	Interstitial liquid	ns	ns	ns

Notes:

ns = no sample

[1]Measured from waste surface.
[2]TOC performed by direct persulfate oxidation.
[3]TOC performed by furnace oxidation.
[4]DSC results are rounded to the nearest J/g, and TOC results are rounded to the nearest 0.1 wt%.
[5]Measurement performed on decanted supernatant sample.
[6]Assumes a density of 1.15 g/mL.
[7]Dry-weight basis.

Speciation of the aqueous fraction also confirmed that these layers contain only small amounts of sodium oxalate as compared to their carbon content (Table 4-4).

Table 4-4. Average TOC and Oxalate Results for C-106 Liquid Samples Analysis.

Riser 1				Riser 7	
TOC Dry[6] [µg C/g]	Oxalate [µg/mL] (µg C/mL)[3]	Depth[5] (in.)	Sample type	TOC Dry[6] [µg C/g]	Oxalate [µg/mL] (µg C/mL)[3]
10,000[1] 15,000[2]	3,680 (1,000)	14	Supernatant[4]	ns	ns
ns	ns	14	Interstitial liquid[4]	3,000[1] 3,000[2]	3,310[7] (903)
ns	ns	23	Supernatant[4]	8,000[1] 10,000[2]	2,980 (813)
3,000[1] 3,000[2]	I.S.	28	Interstitial liquid[4]	ns	ns
5,000[1] 5,000[2]	3,090 (843)	35	Interstitial liquid[4]	ns	ns
ns	ns	40	Interstitial liquid[4]	7,000[1] 7,000[2]	3,290[7] (897)
3,000[1] 4,000[2]	2,210 (603)	53	Interstitial liquid[4]	ns	ns

Notes:

ns = no sample available
I.S. = insufficient sample to run analysis.

[1]TOC performed by direct persulfate oxidation.
[2]TOC performed by furnace oxidation.
[3]Carbon equivalent of oxalate is provided in parentheses below the oxalate result.
[4]These samples were not corrected for their moisture content.
[5]Measured from waste surface.
[6]TOC results are rounded to the nearest 1,000 µg C/mL.
[7]Measurement performed on decanted supernate sample.

One anomaly observed in comparing TOC and oxalate analysis results was the fact that the 222-S oxalate analysis procedure sometimes resulted in a higher apparent "yield" of sodium oxalate than is bounded by TOC analysis. Because sodium oxalate is quantitatively degraded to carbonate by persulfate oxidation, this anomalous result suggests a matrix interference in the oxalate assay, perhaps another analyte eluting under the oxalate peak.

4.1 POTENTIAL FOR A PROPAGATING REACTION OF THE RESIDUAL ORGANICS IN TANK C-106 AFTER DRYOUT

As was noted in Section 3.1, the waste in tank C-106 consists of:

- BL (B-plant low-level complexant waste) from B Plant after the removal of Sr and Cs (Pu would not have been removed from this waste type during B Plant Sr and Cs removal operations)
- AR-002 (PUREX sludge) high Sr-Cs-Pu from PUREX (via A-106)
- CWP1 coating waste from PUREX
- UR (Uranium Recovery Wastes) on the tank bottom (so called hardpan).

Only BL wastes should contain organic complexants. Agnew (1995) estimated in his model that much of the organic added to the tank was citrate. However, the B Plant flowsheet indicated that most of the citrate in the waste stream was destroyed by the B Plant evaporator, so the actual carbon-containing species would be citrate degradation products (e.g., oxalate).

This historic information, coupled with the data reported in Section 4.0, suggests that the organics in tank C-106 are both well aged (with large oxalate concentrations) and energetically benign. Therefore, leaving some or all of the organics in tank C-106 in the absence of evaporative cooling will not pose a risk of a propagating organic reaction.

The next section describes the result of speciation of the sludge oil obtained by centrifugation of the C-106 solids.

4.2 THE COMPOSITION OF THE OIL RELEASED BY SLUDGE CENTRIFUGATION

As was stated in an earlier section, in order to maximize information obtained from the samples recovered from tank C-106, an extensive dewatering step was built into the laboratory test plans (Schreiber 1996). The 222-S laboratory staff was asked to dewater the sludge in a centrifuge using a fritted disk or filter cone to maximize separation of water-soluble from water-insoluble waste components. This "separation" step was designed to avoid the anomalies sometimes observed when samples containing significant amounts of "water" (e.g., >40%) are analyzed. Errors in analysis results were of particular concern when a waste sample contained species (analytes) that partitioned in both the aqueous and solid phases. Standard centrifugation in a tapered cone was also performed on the sludge samples. Standard centrifugation resulted in the separation of a hitherto-unencountered, sludge-associated organic oil that floated on the aqueous waste layer. The results of speciation and other tests with C-106-derived "sludge" oil are described below.

4.2.1 Summary of Findings

Two of the oil samples centrifuged from tank C-106 sludge were submitted to Pacific Northwest National Laboratory (PNNL) for organic speciation. The oil samples were 7-SA and 13-3 from sludge samples 6C-96-7 and 6C-96-13, respectively. PNNL identified, using a combination of infrared (IR), gas chromatograph/mass spectrometry (GC/MS) and liquid chromatography as the various constituents of the oil, achieving a carbon accountability (TOC) of nearly 80% for the process. The principal constituent of the oil was the compound bis (2-ethylhexyl) phosphoric acid, existing as the sodium salt in the waste. Minor amounts of tributyl phosphate (TBP), normal paraffin hydrocarbon, and the transesterification products of TBP and 2-ethylhexyl alcohol, or of di(2-ethylhexyl) phosphate and butyl alcohol.

This phosphate ester salt was used as a complexing agent in B Plant during the Sr recovery campaigns. The material likely coprecipitated with the sludge when wastes from B Plant were made alkaline before their transfer to the tanks. The absence of a strongly alkaline environment in tank C-106 likely protected this species from hydrolysis. Alternatively, the sodium salt, by analogy with sodium bis-dibutyl phosphate, may be resistant to alkaline hydrolysis.

4.2.2 Infrared Analysis of the Tank C-106 Oils

An aliquot of the tank C-106 sample was weighed and carbon tetrachloride was added. The mixture was slurried and anhydrous sodium sulfate was added to remove the water. The carbon tetrachloride extract was analyzed by Fourier transform infrared (FTIR). The FTIR spectrometer was equipped with a zinc selenide attenuated total reflectance solution sample cell that had a transparent optical window in the mid-IR region of interest. Carbon tetrachloride was used as the reference spectrum to subtract the infrared absorbance of the solvent from the sample spectra. All spectra were collected at 4 reciprocal centimeter resolution.

Comparison of the tank C-106 sample and the reference bis(2-ethylhexyl)phosphate salt materials shows a close match between the two spectra, indicating that the infrared active ingredients in both the tank C-106 sample and the reference material sample are basically the same compounds. The peak locations of each major band in both spectra (reference and sample) match within the resolution of the sample spectrum. In summary, the major infrared active compound in the tank C-106 sample is bis(2-ethylhexyl)phosphate.

4.2.3 Tank C-106 Species Identification and Quantitation

Separable oil samples centrifuged from two of the sludge samples from tank C-106 (7-SA and 13-3) were prepared in the 325 West hot cell by dilution with methylene chloride, drying

the liquid with sodium sulfate, and filtering out solids using a Pasteur pipette plugged with clean cotton.

These samples were dried to constant weight in the 329 labs (Mettler PB303[2] balance sensitivity ±1 mg) and were found to be: sample identity 7-SA = 15 mg, sample identity 13-3 = 22 mg. The samples were taken to known volume and aliquotted for analysis (7-SA = 3.75 mg aliquot, 13-3 = 5.5 mg aliquot).

Each sample aliquot was dissolved in 2 mL methylene chloride and treated with an additional 2 mL diethyl ether that had been saturated with hydrochloric acid. The treatment appears to quantitatively transform the sodium bis (2-ethylhexyl) phosphate in the sample into the free acid form, as evidenced by copious amounts of white precipitate (NaCl) forming in the vessel. The aliquots were then reduced in volume to 100 μL, cooled, and 3 mL of an uncalibrated solution of ethereal diazomethane added. Diazomethane is produced by stirring an ethereal slurry of N-methyl-N-nitrosourea over a 40% KOH solution (Fieser and Fieser 1967). The esterification is essentially complete immediately; the colored diazomethane is used to visually confirm the presence of excess diazomethane. To ensure complete conversion, the samples were left for one hour in the presence of excess diazomethane before analysis to ensure complete conversion.

Prior GC/MS analysis had tentatively identified other materials related to bis(2-ethylhexyl) phosphate in these samples. The mass spectral signature ions (both EI and CI modes) for this group of organic analytes makes identification of these moieties relatively straightforward. Evidence exists that the following molecules are also present in the sample: butyl bis(2-ethylhexyl) phosphate; tris(2-ethylhexyl) phosphate; and butyl (2-ethylhexyl) phosphate. The presence of butylated species is highly indicative of trans-esterification from TBP or capture of butanol in the sample matrix over the life of the sample. These materials do not appear to be artifacts of sample preparation or analysis.

GC analysis of the major phosphoric ester components versus two independently prepared standards of methyl bis(2-ethylhexyl) phosphate (prepared in the same fashion as detailed above) using sodium bis(2-ethylhexyl) phosphate (supplied by Chem. Services, Westchester, Pennsylvania) was done using an HP 5890[3] GC flame ionization detector (FID) equipped with a low polarity, thin phase capillary column (HP-5, 30m x 0.32 mm x 0.25 mm). A single dilution of TBP (supplied by Aldrich Chemical Company, Milwaukee, Wisconsin) was also prepared. Quantitation of the major components (> 5% of the total peak area) is detailed below.

[2]Mettler PB303 is a registered trademark of Mettler Electronics, Anaheim, California.

[3]HP 5890 is a trademark of the Hewlett-Packard Corporation, Avondale, Pennsylvania.

As shown in Tables 4-5 and 4-6, sodium bis(2-ethylhexyl) phosphate is the dominant organic chemical in the oil that separated on centrifugation of tank C-106 sludge. Reasons for this chemical's survival in tank C-106 are not known, but are perhaps related to its lack of solubility in the waste.

Table 4-5. Analysis of Sample 7-SA.

Component	g/g amt.	g Carbon/g amt.
D2EHP	0.66	0.37
BuD2EHP	0.07	0.043
T2EHP	0.01	0.005
TBP	0.05	0.027
Bu2EHP	0.03	0.0215
Total	0.82 g/g amt.	0.46 g C/g amt.

Notes:

D2EHP	=	bis(2-ethylhexyl) phosphate
BuD2EHP	=	butyl bis(2-ethylhexyl) phosphate
T2EHP	=	tris (2-ethylhexyl) phosphate
TBP	=	tributyl phosphate
Bu2EHP	=	butyl (2-ethylhexyl) phosphate

Table 4-6. Analysis of Sample 13-3.

Component	g/g amt.	g Carbon/g amt.
D2EHP	0.54	0.30
BuD2EHP	0.08	0.047
T2EHP	0.005	0.003
TBP	0.06	0.03
Bu2EHP	0.02	0.011
Total	0.70 g/g amt.	0.39 g C/g amt.

Notes:

D2EHP	=	bis(2-ethylhexyl) phosphate
BuD2EHP	=	butyl bis(2-ethylhexyl) phosphate
T2EHP	=	tris (2-ethylhexyl) phosphate
TBP	=	tributyl phosphate
Bu2EHP	=	butyl (2-ethylhexyl) phosphate

4.2.4 PNNL Analysis of Oil Extracted from C-106 Sludge

The results of preliminary organic speciation analysis of methylene chloride extracts sent to PNNL by the WHC 222-S Laboratory are reported in this section. (See Section 4.2.9 for a description of the 222-S extraction process.)

Two samples of a methylene chloride extract of sludge oil were provided by WHC. The were identified as sample 3133 and Sample 3132. Samples 3133 and 3132 were extracted from oil from sludge samples 6C-96-14 and 6C-96-8, respectively. The major constituent in sample 3133 was D2EHP.

These samples are very similar in composition to the oils centrifuged from the C-106 sludges described in the previous samples. However methylene chloride extraction samples were contaminated with bis(2-ethylhexyl) phthalate a material (e.g., phthalates) usually associated with plasticizers. Sample 3132 contained approximately the same amount of D2EHP as sample 3133, but about 3 times as much bis(2-ethylhexyl) phthalate. This may simply be due to contamination from plasticizers in the plastic centrifuge tubes used in the 222-S Laboratory. Quantitation and carbon balance is in progress.

4.2.5 Comparison of Persulfate Quantitation to TOC Furnace Results

In terms of gram amount, the organic quantitation represents 82 and 70% of the total observed mass of the samples. The numbers represent the sodium salt forms present in the sample and standard before acidification or methylation. Unfortunately, standard materials are not available for BuD2EHP, T2EHP, or Bu2EHP at this time; the response observed for the major component (D2EHP) was used to calculated these minor components. Both samples contain small quantities of hydrocarbon materials that were not individually quantitated. The sum total of these hydrocarbons may constitute a maximum of 5% of the total mass of material in the sample.

Carbon analysis is somewhat more suspect in these analyses. Carbon furnace oxidation (PNL ALO 381[4]) of the samples (corrected for inorganic carbon using the acidification step of persulfate oxidation [PNL ALO 380[4]]) gave values of 61.7% carbon and 55.7% carbon for sample GSA (duplicate analysis). Sample 13-3 was done in quadruplicate by persulfate oxidation, yielding values of 27.7, 33.4, 31.3 and 34.4% carbon. Furnace oxidation afforded values of 68.7% carbon, and 62.8% carbon from D2EHP acid form; this material should exhibit a theoretical maximum TOC of 59.6% carbon (the values are 15% and 5% high, respectively.)

[4]Internal procedure of Pacific Northwest National Laboratory, Richland, Washington.

Using the TOC furnace analysis as a benchmark, we have accounted for 78% of the carbon in sample 7-SA by GC; for sample 13-3, GC analysis accounts for 123% of the total measured by TOC. If sample 13-3 was not entirely dried when TOC analysis was performed, this error might account for some of the discrepancy.

The check of the carbon balance verification of the speciation results for C-106 centrifuge oil demonstrates that a reasonable carbon balance using furnace oxidation (in these screening experiments) was obtained. The persulfate method does not account for all of the carbon in the C-106 centrifuged oil samples.

4.2.6 Other Analyses of Tank C-106 Centrifuged Sludge Oil (222-S Laboratory)

Table 4-7 shows results of DSC, TGA, and TOC analyses performed on the oil samples recovered from the centrifuging of sludge samples. There is no obvious explanation for the variability in the results. The oil layers were difficult to separate from the centrifuged sample and may contain both aqueous materials and solids. However, an examination of the results for the aqueous liquids and solids (Appendix A.2) does not appear to explain the results observed in the oil samples.

Table 4-7. Oil Sample Average DSC, TGA, and TOC Results by Waste Depth (222-S Laboratory).

Riser 1				Riser 7		
DSC Dry (J/g)	TGA (%H_2O)	TOC Dry[2,3] (%)	Depth[1] (in.)	DSC Dry (J/g)	TGA (%)	TOC Dry[2,3] (%)
ns	ns	ns	14	0	29.9	3.3
0	35.4	nr	28	ns	ns	ns
587	69.6	10.8	35	ns	ns	ns
ns	ns	ns	40	681	51.3	nr

Notes:

nr = not requested
ns = not sampled
[1]Measured from waste surface.
[2]TOC results are rounded to the nearest 0.1 wt%.
[3]Assumes a density of 1.0 g/mL.

4.2.7 Plutonium Analysis of Tank C-106 Centrifuge Oil

An ongoing concern related to criticality is that organic chemicals might lead to concentration of plutonium under tank conditions. Such a concentration has never been known to happen,

but the concern has led to a portion of the limited amount of isolated C-106 sludge oil being analyzed for plutonium. These results are reported in Table 4-8. The results indicate no concern for increased plutonium concentrations in the oil samples.

Table 4-8. Oil Sample Average Pu Concentration.[1]

Riser 1		Riser 7
Pu-239/240 (g/L)	Depth (in.)[2]	Pu-239/240 (g/L)
ns	14	0.0058
0.0103	35	ns
0.0012	53	ns

Notes:

ns = no sample available

[1]Results were converted from μCi/mL to g/L assuming all alpha decay originates from Pu-239

[2]Measured from waste surface.

4.2.8 Thermal Behavior of Concentrated Extracted C-106 Centrifuge Oil

A sample of material obtained from Hanford Site underground storage tank C-106 was received from the 325B Shielded Facility located in the 325 Building in the 300 Area. Aliquots of the sample contained in platinum sample pans were characterized using DSC, simultaneous differential thermal analysis, and TGA at 5 °C/min (9 °F/min). Because the amount of material was limited, two DSC and one differential thermal (DTA)/TGA analyses were performed in a flowing argon atmosphere and one DSC analysis was performed in a flowing air atmosphere. The sample sizes ranged from 3 to nearly 8 mg. The material was dark and tarry in appearance.

The combined results of the DSC and the DTA/TGA analyses of the C-106 material in argon, respectively, indicate that no exothermic reactions occurred between the waste constituents up to 480 °C (896 °F). (Figures showing the results of the DSC/TGA-DTA analyses are available from PNNL). The DSC results for both analyses indicate that several endothermic reactions occur, though not reproducibly. The TGA and the DTA, which should be less sensitive than the DSC, indicate that three different principal reactions occur as the material is heated. These reactions appear to start near 100 °C (212 °F), 160 °C (320 °F), and 240 °C (464 °F). The endothermic reaction heats, as measured by the DSC using the temperature ranges indicated by the TGA for these three reactions, are provided in Table 4-9; due to the difficulties associated with assigning the correct baseline in these two runs, it is recommended that the values reported be considered more qualitative than

quantitative. In the absence of chemical information on the nature of the evolved gases, any conjecture about the nature of the reactions that are observed would be speculation. Infrared and/or mass spectrographic analysis of the evolved gases could provide some insight into the nature of the reactions that occur.

Table 4-9. DSC-Measured Enthalpies for the Tank C-106 Organic Sample.

	Change in Enthalpy (ΔH) (J/g)		
	Sample		
Temperature Range °C	Run #1 2.9 mg (Ar)	Run #2 6.6 mg (Ar)	Run #3 7.9 mg (Air)
100-160	55	145	140
160-210	Not detected	2	Not observed
240-360	220	145	
250-450	Not observed	Not observed	-890

An 8-mg aliquot of the material was analyzed using DSC in an air atmosphere to determine the susceptibility of the material to reaction with oxygen in the air. The results of that characterization are provided in Table 4-9. As Table 4-9 shows, the material experiences an endothermic reaction between 100 and 160 °C (212 and 320 °F) that requires 140 J/g. Between 250 and 450 °C (482 and 842 °F), the material reacts exothermically with the air, producing 890 J/g. The shape of this exothermic peak suggests that multiple reactions are occurring either due to a stepwise series of reactions or due to the reaction of multiple components in the waste residues with oxygen in the air.

4.2.9 Organic Extraction Study

These were the materials, discussed in Section 4.2.4, provided to PNNL for organic speciation studies.

In order to determine the approximate amount of sludge oil coating the sludge in tank C-106, an experiment extracting the oil from uncentrifuged sludge was performed. Because there was limited sample in parent containers and associated archive containers for 6C-96-8 and 6C-96-14, both samples were used. Organic extraction was performed on each sample as opposed to duplicates on one sample. The sample was weighed into beakers and gently stirred when methylene chloride was added. No foaming or bubbling were apparent upon addition of methylene chloride or stirring of the resulting mixture. Once the mixture had been stirred for at least 10 minutes, the methylene chloride extract was collected in a 60-mL capped jar (see Table 4-10 for details).

Table 4-10. Organic Sludge Washing.

Sample ID	Wet sludge mass (g)	Methylene chloride added 1st wash (g)	Methylene chloride added 2nd wash (g)	Methylene chloride added 3rd wash (g)	Dry sludge remaining after wash (g)	g oil/g wet sludge
6C-96-8, raw sludge, Riser 1 (28 in. waste depth)	9.70	20.11	14.94	16.36	5.28	0.066
6C-96-14, raw sludge, Riser 7 (40 in. waste depth)	12.26	11.59	14.59	22.06	7.19	0.020

Two samples were removed from the extractant mixture for GC/MS analysis. These samples (LABCORE sample number S96T003134), a sample and duplicate, weighed 6.04 g and 7.72 g, respectively. The remaining sample was then subjected to evaporation by nitrogen sparge to less than 40 mL of total volume. The solvent was not completely removed within the time frame to release the samples from the hot cell for shipping to PNNL. Evaporation of the remaining solvent was performed at PNNL.

The amount of oil in the sludge was determined to be 0.066 g oil/g sludge for the 6C-96-8 sample and 0.020 g oil/g sludge for the 6C-96-14 sample. The lower oil concentration of the 6C-96-14 sample may have resulted from a 3.11-g sample slurry loss in processing. The sample container was tipped during the first wash and sludge was lost but rinsed with solvent before proceeding with washing the remaining sample. The sludge mass was adjusted for this loss of material to the collection jar after subsequent washings.

4.3 SAFETY IMPLICATIONS OF OIL RELEASED BY CENTRIFUGATION

Upon identification of the principal constituent of tank C-106 sludge oil as the sodium salt of bis (2-ethylhexyl) phosphate, samples of this material were purchased by Fauske and Associates for reactive system screening tool and tube propagation tests. Results obtained by Fauske for a 12% by weight loading of the phosphate in sodium nitrate (Fauske 1996a and 1996b) indicated that like other simple phosphate ester derived materials found in the tanks, the sodium salt of bis(2-ethylhexyl) phosphoric acid does not show propagating behavior as tested. This finding augments a considerable body of data on butyl esters of phosphoric acid (e.g., TBP and Na and Ca dibutyl phosphate) that are considerably less energetic than either their structures or calculation of their theoretical heats of reactions would suggest. Although

DSC data obtained in the laboratory on impure portions of oil gave a single ambiguous energetics value, resulting in a large scatter between duplicate runs (Table 4-7), the oil is present in such small amounts (see Section 4.2.9) that it poses no threat from propagating reactions. DSC values reported by PNNL (Section 4.2.8) provide further evidence of the lack of reactivity of the oil.

4.4 ACCIDENTAL OVERHEATING OF INITIAL C-106 SAMPLES (6C-96-1 Through 6C-96-4)

On February 8, 1996, four samples (two supernatant and two sludge) were obtained from tank C-106 and sent to the WHC 222-S Laboratory. When the samples were loaded into the hot cell for breakdown and subsampling, the four sample bottles were placed into a water bath to bring the samples to tank temperature. Due to a miscommunication of instructions, the water bath was allowed to heat to dryness, resulting in the loss of the two supernate samples (6C-96-1 and 6C-96-2) and the drying out of sludge sample 6C-96-3, whose sample bottle broke. The second sludge sample (6C-96-4) was overheated to approximately 200 °C (392 °F), but the jar remained intact with no apparent drying of the sample. A full suite of analyses was performed on sample 6C-96-4, while a partial suite of analyses (DSC, TGA, TOC, and anions) was performed on sample 6C-96-3. Comparison of the DSC and TOC results for samples 6C-96-3 and 6C-96-4 with the remaining sludge samples shows no significant differences between the two sets of data.

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5.0 A PARTIAL REEXAMINATION OF WASTE COMPATIBILITY CONCERNS

5.1 COMPATIBILITY TESTING AND ORGANIC EXTRACTION

The following sections report the results of centrifuge tests and mixing tests on tank C-106 sludge and combined C-106 and AY-102 sludge with AY-102 supernate. During these tests, no adverse effects (changes in physical properties) were identified that negatively affect the proposed retrieval of C-106 to AY-102 by past practices sluicing.

5.1.1 Pretesting of Tank AY-102 Sludges for Organic and Tank C-106 Sludges for Organic Separation

An aliquot of tank AY-102 sludge, identified as 102-AY-9, was collected from riser 15H at 1,715 cm (675 in.) prior to addition of caustic to the tank. The sludge was centrifuged at 1,215 G for 10 minutes at approximately 55° C (131 °F). After centrifuging, the interstitial liquid volume was 3.0 mL in 6.5 mL of bulk sludge material. No organic, which could have separated from the sludge, was evident.

Under similar conditions as those stated above, tank C-106 material was centrifuged at 10 G to mimic pumping conditions. The centrifugation conditions are at least an order of magnitude less than those used for oil recovery. No noticeable separation of organic from the sludge sample or interstitial liquid occurred at these lower centrifuge speeds.

5.1.2 Supernate Characteristics

In addition to supernate from sludge sample 102-AY-9, six other supernate samples were checked for foaming. The 102-AY-9 sample was vortexed with no foaming evident. By shaking the supernate, foaming occurred with subsequent breakup in less than 5 seconds. This supernate was not used for compatibility mixing, because it was later learned that the sample was taken from tank AY-102 prior to addition of caustic to the tank. Therefore, six other samples: 2AY-96-1, 2AY-96-2, 2AY-96-3, 2AY-96-4, 2AY-96-5, and 2AY-96-6, which were collected from the tank after the caustic addition (and which are more representative of current conditions), were used. Each of the supernate samples was agitated with variable results.

In all cases where foaming occurred, the dissipation of foam was nearly immediate. Samples 2AY-96-1, 2AY-96-2 and 2AY-96-6 foamed with foam dissipation in less than 20 seconds. Samples 2AY-96-3, 2AY-96-4 and 2AY-96-5 either foamed with immediate dissipation or exhibited no sign of foaming. Because a large amount of supernate was

required for the tests, three samples (2AY-96-5, 2AY-96-2 and 2AY-96-6) were used to perform the compatibility studies. In each case, key characteristics (i.e., pH and specific gravity [SpG]) of the supernate were checked before and after mixing with the sludge.

Supernate samples from tank C-106 were also checked for foaming. Supernate samples from the parent samples that correspond to the sludges being tested were observed after agitating. Sample S96T000536 (parent sample 6C-96-8) and sample S96T001547 (parent sample 6C-96-14) showed foaming with immediate breakup of the foam (within 5 seconds).

In addition, the slurry will not be dropped from the top of the tank in AY-102 but rather will be introduced beneath the surface of the waste through a slurry distributor. This precludes entraining air into the liquid slurry. Foaming is not expected to be an issue due to no observed foaming from chemical reactions on mixing the waste, rapid breaking of froth when a deliberate attempt was made to cause foaming, and equipment design which introduces the slurry beneath the surface.

5.1.3 Tank C-106 Sludge Mixed with Neat AY-102 Supernate

Sludge from tank C-106 parent samples 6C-96-8 and 6C-96-14 were mixed individually with supernate from tank AY-102 (parent sample 2AY-96-5) (see Table 5-1 for details).

Table 5-1. Sludge Mixed with AY-102 (2AY-96-5).[1]

Sludge ID	Grad. Cylinder	Weight of Supernate	Weight of Sludge Added	Weight Percent Sludge
6C-96-8 (S96T000575)	A	53.31	9.98	11.4
6C-96-14 (S96T001550)	E	37.98	3.93	6.5 (10.3 wet sludge basis)

Note:

[1]All mixing for the C-106/AY-102 compatibility study was done with a vibrating mixer that induces a vortex in the sample.

The weight percent sludge value for total slurry was approximated for 10 weight % sludge. The exact concentration of sludge in the mixture was calculated as follows:

$$Wt.\ \%\ sludge = \frac{W_1 - W_2}{W_3 + W_1} * 100$$

where W_1 = mass of wet sludge
W_2 = mass of water in sludge = total sludge weight x % water content x .001
W_3 = mass of supernate.

The test plan for compatibility (Crawford 1996) study targets testing mixtures of C-106 sludge with AY-102 sludge and supernate at 10 wt% slurry using dry weight estimates as a basis for dilution factors. The 6C-96-8 sample was actually 11.4 wt% solids after calculating. The actual concentration of the 6C-96-14 sample was 6.5 wt%. This discrepancy was due to incorrectly accounting for the interstitial liquid content of the sample. The weight percent sludge content in the mixture based on wet sludge, however, is 10.3.

5.1.4 Settling Behavior of C-106 Sludges with AY-102 Supernates

After sludge samples 6C-96-8 and 6C-96-14 were combined with tank AY-102 supernate, the supernate was light yellow and clear and the sludge was red-brown with fine, sand-like particles.

Upon mixing, all solids were suspended in the supernate. Separation of solids from the supernate occurred within 10 minutes for both samples of pure (uncentrifuged) sludge from samples 6C-96-8 and 6C-96-14. The sludge from sample 6C-96-14 appeared to be settling out faster than the sludge from the 6C-96-8 sample. The supernate appeared to be clear of suspended solids after 165 minutes (2 hours and 45 minutes).

The resultant small pH changes and changes in physical properties resulting from mixing tank AY-102 supernate and pure tank C-106 sludge are summarized in Table 5-2. Sample 6C-96-8 shows a slight increase in pH in the suspended slurry and a small decrease in the resultant supernate. Sample 6C-96-14 shows a pH decrease in the slurry with a slightly larger increase in the resultant supernate. The most obvious difference is observed in the pH increase in the supernate that was mixed with 6C-96-14 sludge. An increase in the specific gravity is also observed in both samples after mixing the supernate with the C-106 tank sludge. This SpG increase is observed in the supernate, as well as the resultant sludge layers.

Of greater importance, no exotherm was noted for the combined solution, indicating that the energetics of the mixture are not reactive. Interestingly, the water content of the sludges

remains fairly high after settling. The sample from 6C-96-14 appears to be particularly high with respect to the 6C-96-8 sample. However, both samples, 6C-96-8 and 6C-96-14 also show increases in solid mass and volume after settling (see Table 5-8).

Sludge from parent sample 102-AY-9 was added to each of two graduated cylinders as described in Table 5-3. With the exception of mixing the sludges in 4 parts tank C-106 sludge to 1 part tank AY-102 sludge proportions, the sludges were combined with supernate from tank AY-102 in similar fashion to those previously described sludges.

When the sludge was mixed with tank AY-102 supernate, no foaming, frothing, or bubble formation occurred. The sludge remained brown and mixed quite well in the supernate.

Table 5-2. Characteristics of Sludge Components Before and After Addition of Supernate.

Fraction of Mixture	pH[2]	SpG[1] (g/ml)	Percent water by TGA	DSC (J/g)	Bulk Density (g/mL)	Vol. % settled solids
Sample 6C-96-8: C-106 Sludge with AY-102 Supernate						
Original supernate (S96T002765)	11.2	0.98	---	---	1.06	---
Slurry (S96T002766)	11.2	---	96.24	0	---	17.85
Resultant supernate (S96T002768)	11.1	1.01	---	---	---	---
Resultant sludge (S96T002769)	---	1.27 (sludge)	73.78	---	1.23	---
Sample 6C-96-14: C-106 Sludge with AY-102 Supernate						
Original supernate (S96T002765)	11.2	0.98	---	---	1.03	---
Slurry (S96T002825)	11.1	---	95.78	0	---	7.69
Resulting supernate (S96T002826)	11.5	0.99	---	---	---	---
Resulting sludge (S96T002827)	---	1.52 (sludge)	95.08	---	1.32	---

Note:

[1]No explanation has been found for the observation that the specific gravity of the supernates approaches that of water.

[2]pH results rounded to nearest 0.1.

Table 5-3. Mixed Sludge Composition.[1]

Sample ID	Grad. cylinder	AY-102 sludge added (g)	C-106 sludge added (g)	Portion AY-102: C-106	AY-102 supernate added	Wt% sludge (dry weight basis)
6C-96-8 (S96T000575)	B	1.77	7.13	1:4.03	61.70	9.8
6C-96-14 (S96T001549)	D	1.79	7.32	1:4.09	54.47	10.2

Note:

[1]All mixing for the C-106/AY-102 compatibility study was done on a vibratory mixer that induces a vortex in the sample.

Samples were vortexed until they were thoroughly mixed, and were then allowed to settle. Solids began to separate from the supernate within the first 10 minutes. After 205 minutes (3 hours and 25 minutes) had elapsed, the supernate was still cloudy and clearing. The pure sludge samples cleared in less than 2 hours and 45 minutes, and the mixed sludge samples settled over a longer time than the pure tank C-106 sludges. At the next reading (1,200 minutes [20 hours]), the supernate was clear and yellow. A more exact time for appearance of clear supernate was not available. The 6C-96-14 mixed sludge dropped out of solution faster than the 6C-96-8 mixed sludge. This behavior is similar to that observed in the previous study, which seems to indicate that some difference in settling behavior may occur as a result of tank location, as well as sludge content, when sluicing occurs, although the settling times are relatively rapid compared to the sluicing operations cycle.

The 6C-96-14 sample settled 52 mL of suspended sludge within the first 10 minutes (which corresponds to a linear settling velocity of 0.84 cm/min.), with an initial volume settling rate of 5.2 mL/min, which is more rapid than the previous run of 6C-96-14 material alone. The mixed sludge 6C-96-8 sample behaved similarly to the analogous tank C-106 sludge sample in all respects. The 6C-96-14 mixed sludge sample may have been more rapid in settling due to its higher concentration of large particles than the other samples. While no particle size analysis was performed to verify it, the tank C-106 sample sludge contained a larger amount of chunks of material than previous samples. The settling rate is reported in Table 5-4 by time elapsed from initiation of settling.

Table 5-4. Settling Rate by Time Elapsed from Mixing.

Sample ID	Time Elapsed	Settling Rate	Linear Settling Velocity
6C-96-8	0 - 10 minutes	2.0 mL/min	3.2E-1 cm/min
	10 - 20 minutes	1.8 mL/min	2.9E-1 cm/min
	20 - 30 minutes	0.3 mL/min	4.8E-2 cm/min
	30-105 minutes	0.067 mL/min	1.1E-1 cm/min
6C-96-8 with AY-102 sludge	0 - 10 minutes	1.9 mL/min	3.1E-1 cm/min
	10 - 20 minutes	2.0 mL/min	3.2E-1 cm/min
	20 - 30 minutes	0.70 mL/min	1.1E-1 cm/min
	30 - 40 minutes	0.25 mL/min	4.1E-2 cm/min
	40 - 60 minutes	0.15 mL/min	2.4E-2 cm/min
	60 - 205 minutes	0.043 mL/min	6.7E-3 cm/min
6C-96-14	0 - 10 minutes	2.0 mL/min	3.2E-1 cm/min
	10 - 20 minutes	1.2 mL/min	1.9E-1 cm/min
	20 - 30 minutes	0.15 mL/min	2.4E-2 cm/min
	30 - 105 minutes	0.027 mL/min	4.4E-3 cm/min
6C-96-14 with AY-102 sludge	0 - 10 minutes	5.2 mL/min	8.4E-1 cm/min
	10 - 20 minutes	1.0 mL/min	1.6E-1 cm/min
	20 - 30 minutes	0.05 mL/min	8.1E-3 cm/min
	30 - 40 minutes	nd	nd
	40 - 60 minutes	0.05 mL/min	8.6E-3 cm/min

Note:

nd = No difference between volume observations.

Rate constants based on a logarithmic decay of settling over time were calculated according to first order kinetics dependent on volume in mL (see Figures 5-1 and 5-2). The rate constants for 6C-96-8, 6C-96-8 with AY-102 sludge, 6C-96-14 and 6C-96-14 with AY-102 sludge are: 7.73×10^{-3} min^{-1}, 9.22×10^{-3} min^{-1}, 1.00×10^{-2} min^{-1}, and 1.03×10^{-2} min^{-1}, respectively, for 215 minutes. While converting the measured settling times to information more suitable for engineering analysis, the laboratory found these "derived" constants are not as intuitive for understanding settling behavior as noting the settling progress depicted in Figures 5-1 and 5-2.

Figure 5-1. Settling Rate: C-106 in AY-102 Supernate.

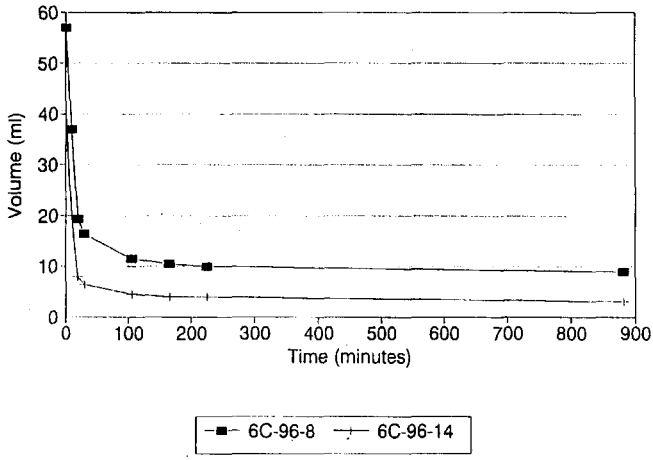

Figure 5-2. Settling Rate: Mixed C-106/AY-102 in AY-102 Supernate.

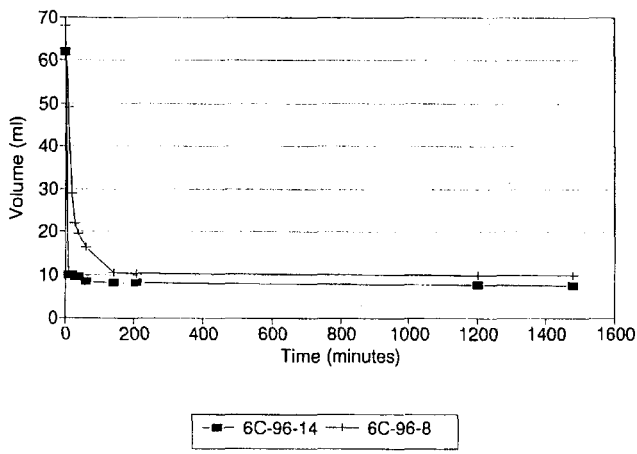

Table 5-5 provides a comparison of supernate and sludge before and after mixing. The pH decreases when the supernate is mixed with the sludge. This pH decrease appears to be larger than that observed for C-106 tank sludge alone and undoubtedly is due to the presence of AY-102 sludge. The sludge used for the C-106/AY-102 mixture includes sludge from tank AY-102 which was taken before caustic was added to the tank.

The amount of solids by volume appears to increase once the mixtures have settled. This is illustrated in Table 5-6, where in all cases both the mass and volume of the sludges after settling are significantly greater than the mass and volume of the sludge in the starting material (see Section 9.1).

Table 5-5. Characteristics of Mixed Sludge Components Before and After Supernate Addition.

Fraction of Mixture	pH[2]	SpG[1] (g/mL)	Percent water by TGA	DSC (Joules)	Bulk Density (g/mL)	Vol. % settled solids
Sample 6C-96-8 with 102-AY-9: Sludge with AY-102 Supernate						
Original Supernate (S96T002833)	12.5	0.98	---	---	1.05	---
Slurry (S96T002770)	11.7	---	96.86	0	---	14.7
Resultant Supernate (S96T002771)	11.8	1.00	---	---	---	---
Resultant Sludge (S96T002772)	---	1.40 (sludge)	79.49	---	1.29	---
Sample 6C-96-14 with 102-AY-9: Sludge with AY-102 Supernate						
Original Supernate (S96T002833)	12.5	1.00	---	---	1.07	---
Slurry (S96T002829)	11.8	---	95.67	0	---	12.1
Resulting Supernate (S96T002830)	11.9	1.00	---	---	---	---
Resulting Sludge (S96T002831)	---	1.42 (sludge)	83.85	---	1.26	---

Note:

[1]No explanation has been found for the observation that the specific gravity of the supernates approaches that of water.

[2]pH results are rounded to nearest 0.1.

Table 5-6. Solids Before and After Settling.

Characteristic	6C-96-8	6C-96-14	6C-96-8 with AY-102	6C-96-14 with AY-102
initial mass (g)	9.98	3.93	8.9	9.11
initial volume (mL)	9.0	3.0	10.0	7.5
final mass (g)	22.84	14.46	60.24	32.66
final volume (mL)	18	9.5	43.0	23

5.1.5 Sedimentation Studies

Sedimentation studies were performed via centrifugation at various speeds to mimic hydrostatic forces within the tank and the relation of G forces on sludge oil separation. No oil separation was observed at either low G forces (e.g., low centrifuge revolutions per minute) or short centrifuge times using full power of the laboratory hot cell centrifuge (estimate to be 1,200 G).

5.2 EFFECTS OF DEAGGLOMERATION (TRANSFER LINE PLUGGING)

The compatibility studies reported in Section 5.1 identified no problem areas resulting from mixing AY-102 supernate with either C-106 and/or combined C-106/AY-102 solids. The compatibility tests described in Section 5.1 were designed explicitly to address CR-SubTAP concerns related to waste compatibility (see Section 2.1). Effects looked for but not found included:

- Ease of sludge oil separation resulting from brief contact with G forces similar to that found in the sluicing pump (Section 5.1.1)
- Foaming (Sections 5.1.2)
- Slow settling (Section 5.1.4)
- Significant changes in waste viscosity (waste thickening)
- Creation of significant quantities of new solid phases as a result of pH changes (Sections 5.1.3, 5.1.4, and 5.1.5)
- Gas evolution (Sections 5.1.3, 5.1.4 and 5.1.5).

Considering the apparent ease with which the soft sludges were transferred to tank C-106, such results are not surprising.

Line plugging does not seem to be a compatibility issue associated with the proposed transfer (10% solids by weight loading) of waste from tank C-106 to tank AY-102. Small but measurable changes in both solution pH and the density of the settled solids, after mixing, did occur, but these appear to pose no threat to retrieval operations.

5.3 CONSEQUENCES OF "DISSOLUTION OF SALTS"

A concern was raised whether a significant amount of potential soluble material was present in tank C-106 and/or tank AY-102 that can dissolve and re-precipitate during retrieval operations (RCR comment 44). The absence from these tanks of significant concentrated evaporator bottoms (or in-tank solidification)-based waste, combined with low sodium and nitrate concentrations, preclude dissolution-solution changes of significance during the proposed retrieval. The only constituent other than soluble sodium nitrate and nitrite salts that pose a potential "solubility problem" would be aluminum.

Changes in alkalinity of the wastes resulting from ongoing caustic consumption in tank AY-102 (the hydroxide concentration may truly be dropping at ~0.005M per month) will require the addition of more caustic to tank AY-102 to protect the tank from corrosion. However, despite the need for additional caustic to raise the pH to meet DST corrosion specifications, the wastes in the C-106/AY-102 system should not undergo significant long-term swings in alkalinity. The alkalinity range of concern is 0.05 M "free" sodium hydroxide. No significantly enhanced aluminum solubility is expected to result from such tank AY-102 caustic adjustments.

5.4 WASTE COOLING AND SOLUBILITY CONSIDERATIONS

Neither tank contains evaporator or in-tank solidification-based waste (see also Section 5.3). The tank C-106 waste is not saturated with sodium salts and contains little nitrate (0.6 mol/L) and nitrite. It is only mildly alkaline. The solution chemistry is dominated by sodium, and carbonate, nitrate, and nitrite anions. It is predominantly an aluminum-iron-calcium, lead, and nickel mixture with hydroxides (as part of metal oxyhydroxide precipitates), carbonate, phosphate and silicate being the dominant anions.

Because the dominant wastes have precipitated, and the aqueous layers are unsaturated with respect to both sodium and nitrate, and cooling associated with retrieval of tank C-106 should have little effect on the amount of solids in the C-106/AY-102 system.

5.5 STORED ENERGY (Lattice Energy in Crystals)

A concern was raised by Brookhaven scientists (Appendix A.1, RCR comment 35) that actinides trapped in a crystal matrix can store energy (e.g., Wigner energy) in the waste as a result of lattice disruptions in crystalline particles larger then 1 nanometer in size.

Specifically the issue raised was "Do the precipitated (in)soluble materials contain trapped electrons, lattice defects, etc. that will liberate heat on dissolution?"

An example of lattice energy storage provided by the Brookhaven staff describes crystal-stored alpha lattice energy strain from decay of 96 kg of Pu (graphite was referenced as the storage material, but no specific literature reference was provided by Brookhaven National Laboratory [BNL] staff). The BNL staff, however, suggested 10^9 joules may be stored over a 10-year period in a graphite plutonium matrix.

When one calculates the effect, assuming, for conservatism, that the waste behaves similarly to graphite, one can calculate how many J/g might be stored.

Assume 746,000 L of waste: general laydown considerations suggest that there is in tank C-106 about 91,000 L of hardpan residues (13%) from UR and CWP1 heels in 1954 and 655,000 (87%) L of other sludge (BL and AR Solids). Further assume a conservative waste density = 1.4 g/mL.

Calculation: 746,000 L x 1.4 g/mL = 1,044,000 kg of waste or 1.044 x 10^9 grams of waste ---> or about 1.044 J/g wet basis. Assuming sludge is at least 55% solids by weight, this becomes 1.9 J/g dry weight basis. If one uses the BNL estimate that all the energy is stored in the bottom 13% of the waste (hardpan), then the result would be 14.6 J/g.

Because the criteria for waste energy concerns, by analogy with the organic and ferrocyanide issues, is 1,200 J/g dry weight basis, such modest amounts of stored energy should not be of concern.

A literature report on stored energy in sodium chloride (Jenks et al. 1975), obtained from D. Powers of Sandia National Laboratories, describes the effects of dissolving sodium chloride that had been previously irradiated, under dry conditions, with gamma energy. The magnitude of these effects was approximately equal to the heat of formation of crystalline sodium chloride, which is 98 kcal/mol (~ 1.7 kcal/mol). However, there is no indication that sodium chloride can store energy when irradiated in solution or with crystals in contact with aqueous media. According to Dr. Powers, in crystalline salts in contact with water (e.g., sodium nitrate and nitrite), phenomena such as Ostwald ripening would interfere with energy accumulation.

Ongoing evaluation of DSCs for waste samples that do not contain significant quantities of either ferrocyanide or TOC does not show identifiable excess energy on heating, which would be the case if lattice energy storage were a significant waste energy factor in Hanford Site waste.

More interestingly, data from PNNL (G. J. Lumetta and coworkers) and Los Alamos National Laboratory sludge washing wastes with 23 waste solids from different tanks (but not specifically C-106 waste) indicate that although sludge compositions vary widely in different tanks, these insoluble wastes are amorphous or microcrystalline and are predominantly between 0.1 and 20 microns in size. Larger size particles, when present, at times appear to deaggregate when stirred and washed (e.g., condition in effect in sluicing), forming materials that settle more slowly than the original sampled materials, perhaps due to fluffing phenomena.

The principal author can find no credible risk associated with storage of crystal lattice energy in the C-106/AY-102 system.

5.6 TOXIC GAS CONCERNS

The CR-SubTAP raised the question of "How much and what kinds of toxic gas will be released (during retrieval)? (Part of RCR 37)"

No sampling of the riser exhaust line for ammonia was possible in the time available for this study. However, plans are being implemented to get baseline headspace concentration data for tanks C-106 and AY-102 prior to starting sluicing. This data, coupled with gas monitoring and establishing gas concentration controls during sluicing (with cool dilute waste solution), should assure safety with respect to toxic gases.

All Hanford Site tanks contain appreciable amounts of ammonia and can contain a myriad of other trace constituents with varying toxicological concerns, as evidenced by gas sampling in the dome space. Air Permit requirements with Washington State Department Ecology assure that the retrieval of C-106 to AY-102 will be protective of both the environment and the health and safety of on and off site workers. As long a gas monitoring related controls are in place and are being implemented (WHC 1996), no special concerns about toxic gas exist.

5.7 A SELECTIVE COMPARISON OF RECENT AY-102 RESULTS FROM PAST SAMPLING EVENTS

The most recent compatibility sampling and analysis results from tank 241-AY-102 are from November 1995. Comparison of these results with the results summarized in Sederburg (1994) show that most constituents appear to be comparable. However, a detailed evaluation of the complete data sets was not possible due to time constraints. It should be noted that

caustic was added in January 1996 to tank AY-102 to bring it back to corrosion control specifications. Because of this addition, the composition of the tank AY-102 waste and future analysis results may differ from the 1995 compatibility results. These minor differences in alkalinity do not affect the conclusions reached in this document.

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6.0 OBSERVED RADIOCESIUM AND STRONTIUM DISTRIBUTION

Concerns were expressed by the CR-SubTAP about "whether C-106 waste can be adequately understood (especially with regard to distribution of heat-generating materials) without the use of additional core samples. Without an understanding of high-heat materials distribution, any basis for estimating heat source removal rate or proportion is questionable (Appendix A.1, RCR 12).

Two parallel approaches were used to support the case that an adequate understanding of high-heat materials distribution in tank C-106 existed. First, modeling of a variety of scenarios associated with different heat distribution cases (Ogden et al. 1996a and Ogden and Crea 1996) demonstrated that even if all of the heat load was confined to the hardpan layer (a bounding case), dryout of tank C-106 would pose no risk with respect to thermally related tank failure concerns after soft sludge retrieval. This bounding case assumed a hardpan layer 45 cm (1.5 ft) thick at the center of the tank and a best estimate of thermal conductivity for dry waste.

Second, the sludge samples retrieved from tank C-106 were analyzed for radiocesium and strontium, as reported in Tables 6-1 and 6-2. This information has been provided the modelers as a means of allowing them to determine that the cases studied did indeed encompass the actual conditions in the tank. Although the quantities of heat-generating materials found in the upper portions of the sludge were lower than that found in the 1986 core composite (Sederburg 1994), the modeling efforts have factored in the recent findings and indicate that these pose no threat to the proposed retrieval operation and outcome.

6.1 C-106 SLUDGE GRAB SAMPLING RESULTS

Tables 6-1 and 6-2 contain data on the radiocesium and radiostrontium concentrations found from the most recent sampling of tank C-106.

In addition, information on dose measurements taken during the April 19, 1986 core sampling of tank C-106 was identified (see Appendix A.3) and the assay information passed on to the WHC modelers as an added source of information on the heat distribution in tank C-106. The recent assays appear bounded by recent modeling results.

Table 6-1. Average Radio Sr and Cs Concentration Sludge Solids Results From C-106 Sludge Grab Samples.

Average Sr and Cs Results by Waste Depth: Sludge Samples[1]					
Riser 1				Riser 7	
Sr-90 (g/L)	Cs-137 (g/L)	Depth[2] (in.)	Sample Type	Sr-90 (g/L)	Cs-137 (g/L)
ns	ns	14	Control sample	3.99E-03	7.18E-03
ns	ns		Filtered, centrifuged sludge	5.27E-03	8.31E-03
4.15E-03	8.11E-03	28	Control sample	ns	ns
6.41E-03	1.20E-02		Filtered, centrifuged sludge	ns	ns
2.07E-03	3.74E-03	35	Control sample	ns	ns
7.79E-03	1.23E-02		Filtered, centrifuged sludge	ns	ns
ns	ns	40	Control sample	9.43E-03	1.42E-02
ns	ns		Filtered, centrifuged sludge	7.23E-03	1.56E-02
6.43E-03	1.12E-02	53	Control sample	ns	ns
7.48E-03	1.12E-02		Filtered, centrifuged sludge	ns	ns

Notes:

ns = no sample

[1]Results were converted from μCi/g to g/L using the density of the centrifuged sludge for each sample.

[2]Measured from waste surface.

Table 6-2. Average Radio Sr and Cs Concentration Results From C-106 Liquid Grab Samples.

Average Sr and Cs Results by Waste Depth: Liquid Samples					
Riser 1		Depth[1] (in.)	Sample Type	Riser 7	
Sr-90 (g/L)	Cs-137 (g/L)			Sr-90 (g/L)	Cs-137 (g/L)
2.63E-06	1.24E-03	14	Supernatant	ns	ns
ns	ns	14	Interstitial liquid	4.82E-06	1.40E-03
		23	Supernatant	3.48E-06	1.26E-03
6.70E-06	1.02E-03	28	Interstitial liquid	ns	ns
6.71E-06	1.77E-03	35	Interstitial liquid	ns	ns
ns	ns	40	Interstitial liquid	5.49E-07	1.76E-03
5.84E-06	1.83E-03	53	Interstitial liquid	ns	ns

Notes:

ns = no sample

[1]Measured from waste surface.

6.2 A SUMMARY OF STRONTIUM ANALYSIS RESULTS FROM THE 1986 CORE SAMPLE

In 1986, a full-depth core sample was obtained from tank C-106. Analyses were performed on the drainable liquid from the core, as well as on a solid composite sample. The solid core composite was made by combining weight fractions of each core segment (Weiss 1987). The strontium results found during this analysis are shown in Table 6-3.

Table 6-3. Sr-90 Results from 1986 Core Sampling of Tank C-106.[1]

Waste Phase	Result (μCi/g or μCi/L)	Result (g/L)
Solid Core Composite	1980	0.0204 [2]
Drainable Liquid	1650	1.19E-05

Notes:

[1]Weiss (1987)

[2]Result converted from μCi/g to g/L using the density result of 1.43 g/mL.

6.3 COMPARISON OF RECENT GRAB SAMPLES IN TANK C-106 WITH 1986 CORE SAMPLE AND THERMAL MODELING

The 1996 grab samples from tank 241-C-106 have been analyzed for ^{90}Sr and ^{137}Cs content. A comparison of the total heat source estimates based on these samples, the sample taken in 1986, and the value used in the thermal modeling has been done. This comparison is shown in the tables below.

The grab samples of the sludge were taken primarily from depths above 104 cm. (41 in.) below the surface of the waste. This region is part of the top layer of sludge used in the thermal modeling which was formed from the noncomplexed waste added to the tank between 1977 and 1979. This layer consists of relatively low amounts of heat generation materials compared to the amounts in the two layers below it, as used in the thermal models.

Since there is some uncertainty in the representativeness of the grab samples, three possible cases were assumed for determining the total heat load in tank 241-C-106. The three cases were assessed separately for the two risers from which the grab samples were taken. The concentrations of ^{137}Cs and ^{90}Sr were assumed to have the following distributions in the three layers used in the thermal models. Calculations are presented for both the maximum and average measured values in all cases.

Case 1: Both radionuclides are uniformly distributed in the three layers of sludge using the measured values.

Case 2: The ^{137}Cs is uniformly distributed in the three layers of sludge using the measured values. The ^{90}Sr is uniformly distributed using the measured values in the top layer and 4.2 times the measured values in the bottom two layers ("homogenized" values for ^{90}Sr in Tables 6-4 and 6-5).

Case 3: Both radionuclides are uniformly distributed using the measured values in the top layer and 4.2 times the measured values in the bottom two layers ("homogenized" values for ^{137}Cs and ^{90}Sr in Tables 6-4 and 6-5).

Case 2 was considered because ^{137}Cs is more soluble in liquid than ^{90}Sr. Case 3 is the distribution determined from the thermal modeling (Bander 1993b).

The core sample taken in 1986 from riser #1 was analyzed after homogenizing the entire sample. Therefore in order to compare the 1996 samples and the 1986 homogenized sample an estimate of the strontium and cesium concentrations for a homogenized sample of the 1996 samples was done. The calculations of homogenized concentrations for the 1996 samples assume that the ratio of the radionuclide concentrations between the bottom two layers and the top layer is the same as that used in the thermal modeling (a ratio of 4.2). The volumes of the sludge layers assumed in calculating homogenized 1996 concentrations are those used in the thermal model (400 kL [105 kgal] in the bottom two layers and 350 kL [92 kgal] in the top layer).

Table 6-4 shows concentrations of ^{90}Sr and ^{137}Cs for the three cases described above using the maximum measured values of the 1996 samples and the 1986 "homogenized" values. The concentration of ^{90}Sr in the 1986 sample compared to the 1996 samples is higher for case 1 and lower for cases 2 and 3. The ^{137}Cs comparison indicates much higher concentrations in the 1996 samples compared to the 1986 sample.

Table 6-5 shows concentrations of ^{90}Sr and ^{137}Cs for the three cases described above using the average of the measured values of the 1996 samples and the 1986 "homogenized" values. The concentration of ^{90}Sr in the 1986 sample compared to the 1996 samples is higher for case 1 and about equal for cases 2 and 3. The ^{137}Cs comparison again indicates much higher concentrations in the 1996 samples compared to the 1986 sample.

Table 6-4. Maximum Value of Strontium and Cesium for 1996 Samples (1986 sample decayed to 1996).

	1996 samples				**1986 sample**	
	Riser #1		**Riser #7**		**Riser #1**	
	^{90}Sr	**^{137}Cs**	**^{90}Sr**	**^{137}Cs**	**^{90}Sr**	**^{137}Cs**
case 1						
sludge (μCi/g)	693	644	862	890	1611	269
liquid (μCi/mL)	0.932	158	0.669	128.5	1.34	22.6
case 2						
sludge (μCi/g)	1878	644	2336	890	1611	269
liquid (μCi/mL)	2.53	158	1.81	128.5	1.34	22.6
case 3						
sludge (μCi/g)	1878	1745	2336	2412	1611	269
liquid (μCi/mL)	2.53	428	1.81	348	1.34	22.6

Notes:

case 1: Uniform concentration of ^{137}Cs and ^{90}Sr throughout waste.
case 2: Uniform concentration of ^{137}Cs throughout waste and "homogenized" concentration of ^{90}Sr.
case 3: "Homogenized" concentration of ^{137}Cs and ^{90}Sr throughout waste.

Table 6-5. Average Value of Strontium and Cesium for 1996 Samples (1986 sample decayed to 1996).

	1996 samples				1986 sample	
	Riser #1 [1]		Riser #7		Riser #1	
	^{90}Sr	^{137}Cs	^{90}Sr	^{137}Cs	^{90}Sr	^{137}Cs
case 1						
sludge (μCi/g)	488	516	603	656	1610	269
liquid (μCi/mL)	0.760	127	0.413	121	1.34	22.6
case 2						
sludge (μCi/g)	1320	516	1630	656	1610	269
liquid (μCi/mL)	2.06	127	1.12	121	1.34	22.6
case 3						
sludge (μCi/g)	1320	1400	1630	1780	1610	269
liquid (μCi/mL)	2.060	344	1.12	328	1.34	22.6

Note:

[1]Riser 1 data included one sample at a depth of 53 inches. This sample was included in the top layer for purposes of comparison with the thermal model.

6.4 HEAD LOAD IN C-106

The heat load for tank C-106 is relatively well known from thermal modeling and evaporation of water from the surface. Current estimates are 110,000 Btu/hr (Bander 1993a) to 132,000 Btu/hr (Fryer 1995). The various analytical results and how those results translate into energy are shown in Table 6-6. The assumptions are that 197,000 gallons of sludge are in tank C-106 with a density of 1.5 g/mL. The decay rates and heat rates are from Wilkins (1984).

Table 6-6. Strontium and Cesium Heat Load in C-106 Sludge

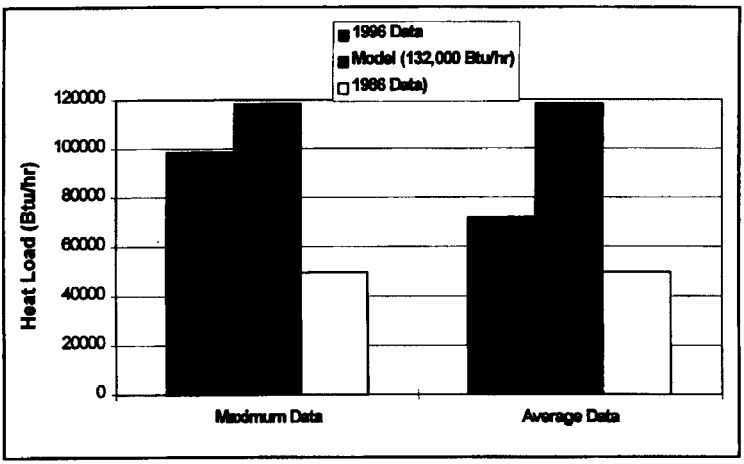
	1996 Grab Sample (Sludge Mean) (Schreiber 1996, Table ES-2)	1986 Core Sample Composite (Schreiber 1996 Page D-12)	1980 Core Sample Composite (Schreiber 1996 Page D-14)
^{137}Cs	654 μCi/mL	330 μCi/g	213 μCi/g
^{90}Sr	546 μCi/mL	1,980 μCi/g	6470 μCi/g
^{137}Cs Btu/hr	7,850	5,940	3,840
^{90}Sr Btu/hr	9340	50,700	165,700
Total Btu/hr	17,190	56,700	169,500
Decayed to 1997	16,790	44,000	115,000

Notice that the cesium-137 values never contribute over 10,000 Btu/hr which is a small percentage of total heat load. Clearly, the bulk of the heat must come from the insoluble strontium-90 and therefore the heat load resides in the non-convective layer.

Lumetta (Lumetta 1996) reports that with weak leaching solution, 38% of the cesium-137 was soluble. With strong caustic leach, this increased to 60% of the cesium-137. This is supported by the 1980 core sample which showed 97.8 μCi/g water soluble cesium-137 versus 213 μCi/g water insoluble cesium-137 (Schreiber 1996). The data does not support the theory that dissolving the cesium-137 from C-106 will remediate the tank. The data does support the thermal modeling which does not consider cesium-137 soluble. The portion of the heat that could be attributed to the supernate in AY-102 is insignificant.

The thermal model best estimate heat load is significantly greater than that derived from the radionuclide data. Because the thermal model heat load estimate is based upon actual waste temperature measurements and evaporation rates, which are more extensive and of higher quality than the sample data, it is considered to be a more reliable heat load estimate.

Figure 6.1. Comparison of Tank C-106 Heat Loads for Case 3.



Best Estimate Heat Load

The best estimate of the heat load currently in C-106 is 123,000 Btu/hr. This is based on a heat load of 132,000 Btu/hr estimated from thermomodeling and evaporation rates in 1994. This estimate was then decayed to 123,000 Btu/hr for 1996 based on a 30 year half life. The calculation for the decay is shown in Appendix A.8. The standard deviation was assigned as 6,000 Btu/hr.

Best Estimate of Heat Profile

There has been some speculation on the distribution of the heat load in the tank. Section 6.1 has tables representing the 1996 grab samples. The information does not show much gradient. The 1986 core sample was composited and only the average values for the radionuclide are available. However, each segment was measured for the radiation through the drill string. This does give some insight. Table 6-7 presents the data.

Table 6-7. Radiation Readings Through Drill String (Weiss 1988).

Segment	Radiation reading, mrad
1	1500
2	2100
3	2800
4	2000

The radiation readings were taken on contact with the drill string. Segment 1 is on top and segment 4 was on the bottom. All segments were a full 19 inches with an estimated 100% recovery. Segment 1 had drainable liquor which represents the liquid above the solid sludge. Segment 3 had the highest radiation readings.

This best estimate is based on several different considerations. The data indicates that the top 2 feet of waste in C-106 has a lower radiolytic heat generation rate when compared to the bottom 4 feet. This is based on temperature profiles, modeling, the radiation readings above and process history.

The best estimate for the top 2 ft of waste is 2 Btu/hr ft^3 with a standard deviation of 0.5 Btu/hr ft^3. The lower 4 ft of waste is assigned a higher volumetric heat rate such that the total heat in the tank is 123,000 Btu/hr.

The radial head load distribution is assumed to be uniform.

6.5 HEAT LOAD IN AY-102

Best Estimate Heat Load

The best estimate heat load in AY-102 is 33,000 Btu/hr with a standard deviation of 5,000 Btu/hr. This value is based on the thermal model of that tank (Sathyanarayana 1996). The heat is assumed to be genarated entirely within the sludge layer that is presently in AY-102. Modeling the present sludge as a separate layer is prudent.

The current sludge layer in AY-102 is assumed by the thermal modeling to remain in place. The rather gentle flows from the slurry distributor which is located approximately 4 m above the sludge is not expected to dislodge the existing sludge.

The sludge layer from C-106 is expected to have a thermal conductivity which may be summarized by the following equation:

$$K = (fs*Ks + (1-fs)*Kl)$$

where

fs	=	fraction of solids
Ks	=	conductivity of the solids
Kl	=	conductivity of liquid

This equation states that the thermal conductivity is the weighted average of the conductivity of the solids and the liquid decreased by the void fraction of gas in the sludge. This is more conservative than the more conventional parallel conductor type model.

Water has a conductivity of 0.35 Btu/hr ft °F. Adding dissolved salts to water decreases the conductivity slightly. The best estimate for the conductivity of the liquid, Kl, is 0.28 Btu/hr ft °F with a standard deviation of 0.03.

Solid conductivities have a larger range. Metals may range up to 35 Btu/hr ft °F while dry sand is about 0.25 Btu/hr ft °F. The best estimate of solid conductivity is 5 Btu/hr ft °F which has been used successfully for thermal modeling at the Hanford Site. The assigned standard deviation is 1 Btu/hr ft °F.

The presence of gas bubbles in a waste will influence the resulting effective, or composite, thermal conductivity. The special case of diffusion through a porous solid with periodically space spheres of a different material has been solved by Maxwell, and can be adapted to heat transfer (Cussler 1984). This model was used to estimate the influence of gas bubbles. The model does not have sphere size as a parameter, because size is irrelevant, i.e., the results are the same irrespective of bubble diameter, and the only geometrical parameter is void fraction. The true conductivity of gas bubbles is not known, and consists of conduction/convection, plus evaporation/condensation. Three values were used to approximate and bound the problem. First, the gas in the bubbles is considered to be air (non-condensible and non-convecting); next, the bubbles are considered, in the extreme, to have a conductivity = 0; and, finally, with a high-conductivity gas plus evaporation/condensation, the thermal conductivity is assumed to be infinite.

As anticipated (Cussler 1984), the calculations show that the conductivity of the bubbles has only a small influence on overall, composite conductivity. With bubble conductivity at 0, the effective conductivity is nearly the same as for air properties, and with infinite conductivity through the bubbles, the effective thermal conductivity is roughly doubled, at the high void fraction. Real bubbles would have an even narrower range of influence on the effective thermal conductivity. In any case, the bulk waste properties dominate the overall thermal conductivity, and the presence of bubbles in the waste most likely has an effect that is only about equal to the variability in waste thermal conductivity.

7.0 OBSERVED PLUTONIUM DISTRIBUTION

As part of the recent tank C-106 grab sampling event, analysis for fissile materials in the top 76 of 178 cm (30 of 70 in.) of sludge was carried out. These results are reported in Tables 7-1 and 7-2. These results are being evaluated by WHC's nuclear criticality experts and will be reported in the final version of Waltar (1996).

According to the Tank Farm Criticality Safety Representative, the plutonium concentrations reported for the supernatant are comparable to historical plutonium supernatant concentrations in tank C-106. The average plutonium concentrations reported for the supernatant (Table 7-1) are higher than average plutonium concentrations reported for historical samples, but similar to the maximum plutonium concentrations from historical samples (Sederburg 1994).

Sludge samples taken in 1986 and 1987 have a plutonium concentration of 0.069 g/L. A 1980 sample from tank C-106 has a maximum plutonium concentration in the sludge of 0.127 g/L. The average plutonium concentration of the 1980 sludge samples was 0.076 g/L (Sederburg 1994). All of the historical values are higher than the plutonium concentrations reported for the 1996 sludge grab samples (Table 7-2). This finding is not unexpected because the maximum concentration of plutonium-bearing waste might be expected to be found at depths greater than samples could be obtained with the sludge "bottle" sampling device. Alternatively, the present estimates of the inventory in tank C-106 may be too high.

The plutonium concentrations in the interstitial liquid (0.013 g/L and 0.0124 g/L) of the 1996 sludge samples appear to be consistent with historic plutonium concentrations in supernatant and interstitial liquid samples.

The method of sampling used for the historical samples was different from the method used for the 1996 sampling event. Therefore, differences in the plutonium concentrations should be expected.

In conclusion, the criticality staff compared the most recent C-106 grab sample data (Tables 7-1 and 7-2) with the data used in the W-320 Safety Analysis (WHC 1996) and the data from CSER 94-001 (Rogers 1994). The general conclusions reached in the W-320 document are still valid using the new grab C-106 grab sample data. The Pu concentrations from the C-106 grab samples are somewhat different from the concentrations used in CSER 94-001 and the W-320 report. The Pu concentrations in the supernate are comparable to previous supernate samples. The Pu concentrations in the sludge are lower than values reported from previous sampling events (Pu = 0.0434 g/L from the high-value grab samples compared to high Pu = 0.127 g/L from core sample). This is not unusual because the methods of sampling are different.

NOTE: The values used in CSER 94-001 are maximum Pu concentrations. The MAXIMUM concentration is typically used when talking about criticality safety. The values used in the W-320 document and obtained from the C-106 grab samples are AVERAGE values.)

Table 7-1. Average C-106 Liquid Sample Plutonium Assay Results.

Average Pu Results by Waste Depth: Liquid Samples[1]							
Riser 1			Depth[2] (in.)	Sample Type	Riser 7		
Pu-239/240 (g/L)	Al (g/L)	Fe (g/L)			Pu-239/240 (g/L)	Al (g/L)	Fe (g/L)
0.0115	<0.02	<0.02	14	Super.	ns	ns	ns
ns	ns	ns	14	I.L.	0.0135	<0.02	<0.02
ns	ns	ns	23	Super.	0.0125	<0.03	<0.03
0.0123	I.S.	I.S.	28	I.L.	ns	ns	ns
0.0133	<0.02	<0.02	35	I.L.	ns	ns	ns
ns	ns	ns	40	I.L.	0.0124	0.058	0.059
0.0138	<0.02	<0.02	53	I.L.	ns	ns	ns

Notes:

ns = no sample available
Super. = supernatant layer
I.L. = interstitial liquid
I.S. = insufficient sample to run analysis.

[1]Results were converted from μCi/mL to g/L assuming all alpha decay originates from Pu-239.

[2]Measured from waste surface.

Table 7-2. Average C-106 Sludge Samples Plutonium Assay Results. (2 sheets)

Average Pu Results by Waste Depth: Sludge Samples[1]							
Riser 1					Riser 7		
Pu-239/240 (g/L)	Al (g/L)[a, 4]	Fe (g/L)[a, 4]	Depth[3] (in.)	Sample Type	Pu-239/240 (g/L)	Al (g/L)[a, 4]	Fe (g/L)[a, 4]
ns	ns	ns	14	Control sample	0.0180	nr	nr
ns	ns	ns		Filtered, centrif. sludge	0.0214	55.0	74.8
0.0401	nr	nr	28	Control sample	ns	ns	ns
0.0359	82.1	109		Filtered, centrif. sludge	ns	ns	ns
<1.70E-03[2]	nr	nr	35	Control sample	ns	ns	ns
0.0433	99.1	134		Filtered, centrif. sludge	ns	ns	ns
ns	ns	ns	40	Control sample	0.0257	nr	nr
ns	ns	ns		Filtered, centrif. sludge	0.0391	96.2	109
0.0300	nr	nr	53	Control sample	ns	ns	ns
	87.3	116		Filtered, centrif. sludge	ns	ns	ns

Table 7-2. Average C-106 Sludge Samples Plutonium Assay Results. (2 sheets)

Notes:

nr = not requested
ns = no sample available

[1]Results were converted from μCi/g to g/L using the density of the centrifuged sludge for each sample and assuming all alpha decay originates from Pu-239.

[2]Insufficient sample to rerun analysis.

[3]Al and Fe results converted from μg/g to g/L using the density of the centrifuged sludge for each sample.

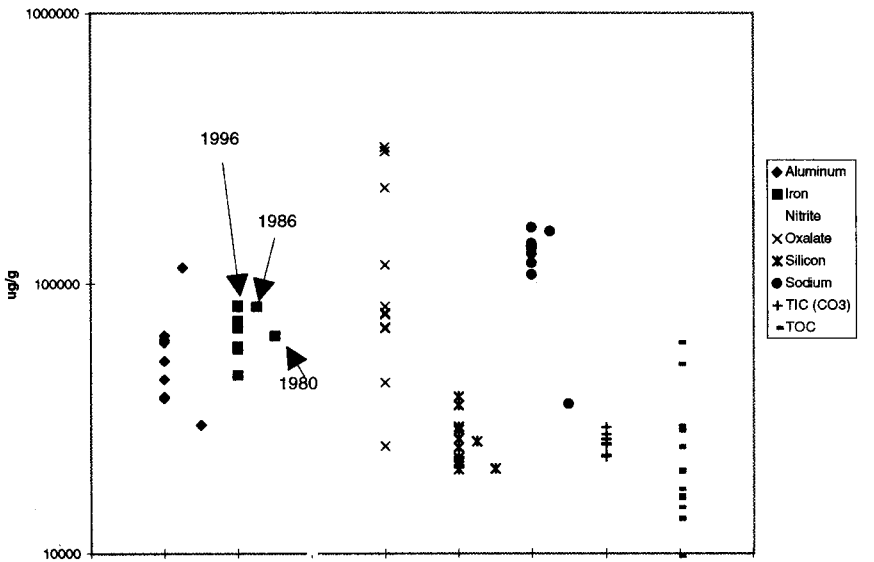
[4]In addition to maintaining Pu concentrations below 2.6 g/L, to assure criticality safety, maintaining the ratio of neutron poisons Al/Pu ratio $\geq$ = 910 and/or Fe/Pu ratio $\geq$ = 160 is an independent means of assuring criticality safety. These criteria are met in the sludges retrieved from C-106.

[5]Measured from waste surface.

8.0 SOLIDS AND DISSOLUTION

The waste in C-106 consists primarily of a solid layer. The solids have been sampled several times in the past decade. Figure 8-1 shows the most prevalent species found in the solid phase of the samples. Those points next to the main sample ranges represent the 1986 and the 1980 core samples. The main sample range represents the 1996 grab samples. Notice that the 1986 and 1980 core sample results fit quite well with the observations from the 1996 grab samples.

Figure 8-1. Major Components in Solids of C-106.



The TOC consists mainly of oxalate. Nitrate is much less prevalent than nitrite and has been left off from this chart.

Samples of the 1996 grab sample was sent to PNNL for settling tests. There samples were examined with an electron microscope. The following species were identified: Fe2O3, FeOOH, Al(OH)3, Si/Al/Fe (i.e., ferro aluminosilicate), and silver oxide (Lumetta 1996).

A thermodynamic equilibrium model (ESP) was used to model the chemistry in C-106. This code identified these species as insoluble compounds:

Table 8-1. ESP Estimation of Solid Species.

Solid Species	Weight Percent of Undissolved Solids*
$NaAlSiO_4$	21.6
$Fe(OH)_3$	21.2
$NaHCO_3$	20.5
$Na_2C_2O_4$	19.8
$Al(OH)_3$	12.5
$CaCO_3$	1.63
$MnCO_3$	0.8
$KAlSiO_4$	0.5
$Pb(OH)_2$	0.5
Ag_2CO_3	0.4
$Cr(OH)_3$	0.2
ZrO_2	0.2
$Ni(OH)_2$	0.1
$SrCO_3$	0.1
$Pu(OH)_4$	0.014

Note:

*The total may not add to 100% due to roundoff.

About equal weights of sodium aluminosilicate, iron hydroxide, sodium bicarbonate and sodium oxalate comprise 80% of the solids. There is also a sizeable portion of aluminum hydroxide. Essentially, these are the species which were reported in the electron microscope examination. This also corresponds quite well with those elements that were found in abundance in the solid phase (see Figure 8-1). The sodium bicarbonate, which is 20.5 wt%, is expected to be soluble in the AY-102 supernatant.

8.1 COMPARISON OF SOLIDS CONCENTRATION IN SAMPLES

One measure that can be used to compare the various samples is the percent solids. The percent undissolved solids is a measure of solid packing.

The water content of the grab samples varied widely as are summarized in Table 8-2. Only those samples labeled "Raw sludge" represent the sludge from the tank. Other samples of solids are from a dewatering step. The shaded blocks are calculated using the interstitial liquid dissolved solids (Appendix A.6).

Table 8-2. Comparison of Percent Solids in C-106 Samples.

Sample	%Water	%Total Solids	%Dissolved Solids	%Undissolved Solids	Source
Grab Sample, Raw Sludge 6C-96-8	56.2	43.8	15.4	28.4	Schreiber 1996
Grab composite, Sample B	61.8	38.2	16.9	21.3	Lumetta 1996
1986 Core Composite	52.5	47.5	14.4	33.1	Schreiber 1996
1980 Core, Segment 2	45.5	54.5	12.5	42.	Schreiber 1996
1980 Core, Segment 3	40.8	59.2	11.2	48	Schreiber 1996
1980 Core, Segment 4	38.6	61.4	10.6	50.8	Schreiber 1996
1980 Core, Composite	45.3	54.7	12.4	42.3	Schreiber 1996

The data indicate that there may be more liquid associated with the grab samples than the core samples. The undissolved solids from Table 8-2 indicate 42.3/28.4 = 1.5 ratio. This ratio could be an indication of the difference between grab samples and core samples.

It should be remembered that the grab composite was dried at 105 °C and the 1986 core sample was taken up to 400 °C. This may represent additional mass loss from water of hydration or even carbonate decomposition.

8.2 INTERSTICIAL LIQUID

A full accounting of solid dissolution requires an understanding of the intersticial liquor. Several moisture measurements were made on the interstitial liquor from the 1996 grab samples. Both the centrate and the liquor from the ultrafiltration was measured. Schreiber Table 4-5 reports a value for "supernate." The supernate represents the liquid which covers the solids in C-106 and is somewhat less concentrated than intersticial liquid due to the additions of fresh water from time to time.

The centrate is liquor from a centrifuge step which separated out an aqueous phase (decant supernate), an organic phase, and a solid phase. The water content was measured by a gravimetric method (Table 8-3).

Table 8-3. Decant Supernate % Water by Gravimetric Method (Esch 1996).

Sample	$\%H_2O$
6C-96-4	76.7
	76.8
6C-96-7	78.8
	78.8
6C-96-10	79.3
	79.3
6C-96-11	78.2
	78.3
6C-96-12	79
	79
	79.05
	79.49
Average	78.56
Standard Deviation	0.92

The 1986 core sample liquid composite was 79.7% water which is quite consistent with the grab samples from 1996.

The liquid from the ultrafilter were labeled intersticial liquor in the analysis scheme. The percent water was measured by TGA. The moisture content of this liquid is much more variable. The data is summarized in Table 8-4

Table 8-4. Interstitial Liquid %H_2O by TGA (Schreiber 1996).

Sample	%H_2O
6C-96-4	58.94
	57.09
6C-96-7	34.27
	36.53
6C-96-10	61.32
	59.37
6C-96-11	48.7
	44.37
6C-96-13	74.92
	76.6
Average	55.2
Standard Deviation	14.4

There is greater variability in these measurements. Only one (6C-96-13) seems to be part of the same population as the decant supernate (Table 3). Currently, there is no explanation as to why there is such a difference between these two measurements.

8.3 LEACHING TESTS

Retrieval of C-106 solids will use supernate from AY-102 which has had caustic added to bring it up to about 0.5 M NaOH as the sluicing liquid. The liquid in AY-102 will be a rather dilute solution. It is anticipated that part of the solids in C-106 may be soluble in the dilute solution. There has been some work done with leaching and washing actual waste samples from C-106. These have been reported in two PNNL documents (Lumetta 1996, Brooks 1997). Both studies worked with sludge retrieved from the 1996 grab samples.

A large batch was composited from several of the grab samples. A small portion of the composite went to Lumetta for laboratory tests. The bulk of the sludge went to Brooks for larger scale tests.

Table 8-5 summarizes the information found in Lumetta Figure 2.1. The values in shaded boxes are derived from Lumetta's data.

Table 8-5. Summary of Lumetta's Leaching Study (Lumetta 1996).

Units are in grams	Start	Sample B	Sample B1	Sample C	Sample D	Leaching
Sludge	15.14	0.772	1.529	0.22	0.16	12.45
Mixture	43.94	2.24	4.45	0.65	0.46	36.14
Total Solids	5.79	0.295	0.587	0.086	0.061	4.76
Dissolved Solids	2.56	0.13	0.258	0.037	0.027	2.10
Undissolved Solids	3.23	0.165	.326	.049	.034	2.66
Solids after washing/leaching			0.243			1.651
Percent undissolved Solids which dissolved			25.5%			37.9%

Sample calculations are shown in Appendix A.7. Sample B1 shows that with rather dilute solutions such as AY-102 supernatant, about 25% by weight of the solids dissolve. A more aggressive leaching with 5 M caustic dissolved about 38% of the solids. Solubility models show that the sodium carbonate/bicarbonate will be the solid species most likely to dissolve.

Indications are that perhaps 25% by weight of the undissolved solids will be soluble and dissolve during sluicing. If these solids are carbonate solids as expected, then the resulting sludge will be denser and more compact.

8.4 HEAT OF SOLUTION CONSIDERATIONS

There is a possibility that soluble species may dissolve during sluicing. The most likely is dissolving sodium salts of nitrites and carbonates or bicarbonates. In general, these chemical species dissolve without evolution of heat. The Appendix A.10 shows an estimate of the

temperature effect on dissolving these rather soluble species. The general conclusion is that the dissolution of these salts presents no heating concern. The maximum possible rise in temperature will be much less than 10 Kelvin.

The other possible species to dissolve will be aluminum hydroxide. This is a slow reaction taking days or weeks to reach a new equilibrium. This slow dissolution will not provide significant heat. The heat of solution will not result in a detectable temperature change.

The supernate in AY-102 is anticipated to be about 0.5 M in hydroxide. This is still a dilute solution. The pH of the material in C-106 is about 10.5 to 11.0. There cannot be an acid/base type reaction because both streams are basic. The heat of dilution calculation is shown in Appendix A.11. Temperature change is anticipated to be undectable.

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9.0 FLUFF FACTOR

One of the major concerns for how much waste from C-106 can be safely transferred into AY-102 is the so called "fluff factor." The fluff factor is important because it determines the length over which heat must be conducted to sinks of lower temperatures. The belief is that sluicing will disturb the waste and fluff the waste so that the waste will be at a greater depth in AY-102 than in C-106. This greater depth will inhibit heat transfer and has the potential of limiting the amount of waste retrieved from C-106. This section will look at the various information to examine the fluff factor.

9.1 INTERPRETATION OF SETTLING TEST

Table 5-6 can be misinterperted as a fluff factor. Below is a quote from the principle investigator (B. A. Crawford) explaining in greater detail the results of the tests.

"In response to your concern about volumes of waste after settling, I reviewed my process notes. The discrepancy has occurred due to the way the data was obtained. The settling data and end volumes reflect the amount of material settled in the supernate. The volume of ending material after settling is the best obtainable volume of sludge after the supernate was decanted from it. This means that some of the sludge was suspended in supernate through decanting and the larger volume is what remained in the graduated cylinder after the supernate was removed. The density is probably the most useful value obtained at that point and that may be related back to the ending volume observed in the settling study to provide a better mass value."

It can be seen that the volumes do not really represent a settled solid. Rather, the settled solids have been disturbed during the decanting of the supernate.

9.2 CENTRIFUGATION

Portions of the 1996 grab sample were centrifuged to calculate a vol% solids. Before centrifuging, the samples appeared to be 100% solid. After centrifuging the solids were compressed into a smaller volume and a supernatant layer was formed. This is assumed to represent the compacted state of the sludge in situ. The centrifuge subjected the waste to much more force than gravity.

The fluff factor may be calculated by:

$$\text{Fluff Factor} = 100/\text{vol\% solids}$$

This equation is used in Table 9-1 to calculate the fluff factor.

Table 9-1. Fluff Factor From Volume Percent Solids (Data from Schreiber 1996).

Sample	Volume Percent Solids	Fluff Factor
6C-96-4	59.3	1.68
6C-96-7	69.5	1.44
6C-96-10	85.2	1.17
6C-96-11	59.5	1.68

The largest fluff factor found from this method is 1.68. The lowest is 1.17.

9.3 222-S SETTLING TEST

A sludge from grab sample from the 1996 sampling event was used to measure settling rates when mixed with supernate from AY-102 as reported in Section 5.0. The calculated fluff factor is shown in Table 9-2 below. A sample calculation is shown in Apprendix A.9.

Table 9-2. Fluff Factor From 222-S Settling Tests.

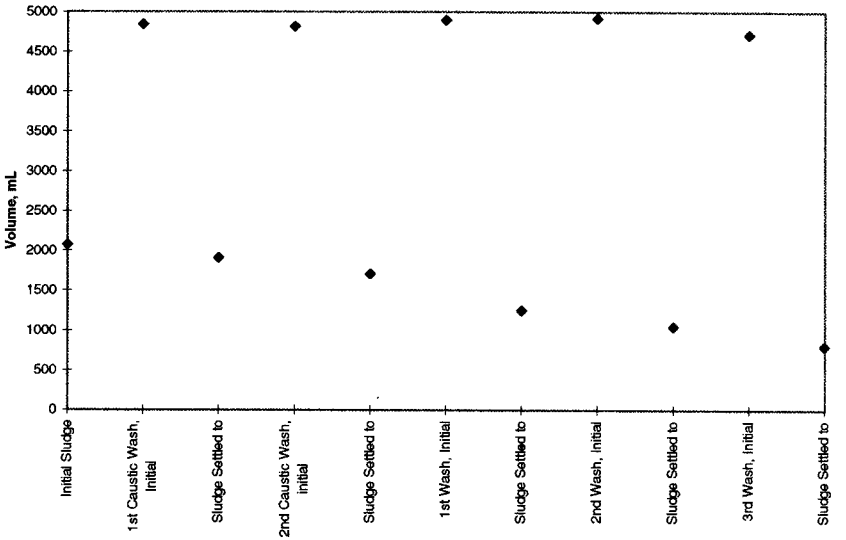
Sample	Weight of Sludge, g (Table 5-6)	Calculated Initial Volume, mL	Final Volume, mL (from Figures 5-1, 5-2)	Calculated Fluff Factor
6C-96-8	9.98	6.65	9	1.35
6C-96-14	3.93	2.62	3	1.15
6C-96-8 & AY-102	8.9	5.9	10	1.69
6C-96-14 & AY-102	9.11	6.1	7.5	1.23

9.4 BROOKS SETTLING TESTS

The settling tests performed by Brooks (Brooks 1997) was similar to the study by Lumetta but on a much larger scale. Whereas Lumetta used approximately 12 g of sludge, Brooks started with about 3000 g. Larger scale equipment was used so that wall effects were reduced.

For fluffing factor, Figure 9-1 shows clearly what happened during the steps of resuspending and settling.

Figure 9-1. Brooks Settling of C-106.



There are two sets of points on this figure. The upper points represent the volume that the sludge from C-106 was fluffed to during suspension. The bottom points represent the volume that the solids settled to after suspension. The solids settled rapidly and all points represent less than three days of settling. Note that the sludge settles to a smaller volume than previously on each step. The final volume of settled solids is 800 mL compared with 2,074 mL initially. This would represent a fluff factor of 800/2074 = 0.38. Overall the Brooks data does not support a fluff factor greater than 1. This data indicates that the settled sludge volume will be less than the starting volume.

9.5 FLUFF FACTOR BEST ESTIMATE

The fluff factor from centrifugation (Table 9-1) range from 1.17 to 1.68. An almost identical range of 1.15 to 1.69 was estimated from the settling tests at 222-S (Table 9-2). The Best Estimate of the fluffing factor is 1.4 with a standard deviation of 0.2. This would give a 95% confidence range from 1.0 to 1.8.

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10.0 SUMMARY OF FINDINGS

The various concerns related to chemistry-associated issues raised (Section 2.0) by the CR-SubTAP were reviewed, and detailed information addressing their concerns is provided in this document or in the reports and letters referenced herein. The reported information has also been provided to those responsible for:

- Modeling tank thermal behavior
- Producing the final safety assessment for retrieval of tank C-106
- Assuring tank C-106's criticality safety
- Assuring efficient operation of the sluicing process (to allow more finely tuned knowledge of tank C-106 and tank AY-102 waste behavior relative to the planned retrieval operation).

Much of the new data resulted from grab sampling tank C-106 and from compatibility testing of C-106 and AY-102 wastes. All of the chemistry-associated and other compatibility information compiled in this report strongly suggests that the sluicing of the contents, in accord with controls required by the Retrieval Safety Analysis (WHC 1996), will pose no unacceptable risk to workers, public safety, or the environment. In addition, it is expected that the sluicing operation will successfully resolve the high-heat safety issue.

The only significant anomaly found during the recent studies, the identification of "sludge oil" associated with C-106 solids (Sections 4.1 through 4.3), also poses no risk to the retrieval operations, but requires attention by the Pretreatment Program relative to unit operations associated with both liquid/solids separation and sludge washing or leaching.

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APPENDIX A.1

CHEMISTRY ORIENTED RCRS RESULTING FROM THE CR-SUBTAP REVIEW OF RETRIEVAL OF TANK C-106

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APPENDIX A.1

CHEMISTRY-ORIENTED RCRS RESULTING FROM THE CR-SUBTAP REVIEW OF RETRIEVAL OF TANK C-106

Excerpts from RCR Forms.

Item	Reviewers Comment	WHC Response
8.	Evaluation of hazard (e.g., waste dry out and overheating) consequences resulting from sluicing shut down, or duration of shut down, on C-106 waste.	Section 2.4.2 includes a discussion of the sluicing process, the consequences of short- and long-term shutdowns, and the measures instituted to prevent waste dryout and overheating, based on *Tank 241-C-106 Parametric Studies in Support of Safety Alternative Process*, included in Appendix E, page E-1216.
9.	Possible consequences and behavior of waste remaining in C-106 after sluicing is completed, e.g., waste dry out and overheating.	Remaining waste and its dryout have no safety consequences, based on Internal Memorandum 74A50-96-BAC-006, included in Appendix E, Page 1139.
12.	Criteria and means for measuring progress of waste transfer, i.e., whether objectives of the project are being met. We question whether C-106 waste can be adequately understood (especially with regard to distribution of heat-generating materials) without the use of additional core samples. Without an understanding of high-heat materials distribution, any basis for estimating heat source removal rate or proportion is questionable. Consequently, we suggest progress determination must be based on measurements of quantities such as transfer waste radiation level, density, flow rate, and/or on-line sampling of transfer waste. We strongly suggest planning and preparation for on-line sampling.	Operational controls and methods to determine the progress (amounts of transferred material) have been provided in Sections 2.4.2 and 2.4.3. This represents a regular but intermittent material balance during routine operations. The distribution of the heat-generating materials is well enough understood (Section 1.2) to allow for a successful retrieval from C-106 without the need for additional core samples and/or in-line monitoring.

Excerpts from RCR Forms.

Item	Reviewers Comment	WHC Response
21.	C-106/AY-102 waste compatibility (including removal of supernate from AY-102 and replacement with treated water). The primary concern is creating GRE conditions. We request a presentation on this topic at a future meeting.	The "Chemical Compatibility of Tank Wastes in 241-C-106, 241-AY-101, and 241-AY-102" WHC-SD-WM-ES-290, Rev. 2, has been included in the SA, in its entirety, in the Appendix E page 931. This study assesses compatibility of four sluicing fluids: 241-AY-101 supernatant, dilute non-complex supernatant (such as 241-AY-102), high caustic (2.5 M NaOH solution), and corrosion inhibited water.
22.	Possible de-agglomeration of waste particles and its effect on settling. This concerns both clarification of sluicing fluid and the potential for gas retention.	The effects of de-agglomeration as it relates to potential for gas retention in tank AY-102 will be discussed by Dr. H. Babad in a letter report centering on several issues at the CRS meeting. Settling as it relates to process control is discussed in Section 2.4.2.1, (requirement to batch transfer material from tank to tank because of failure of material to readily settle in the receipt tank).
23.	Post-transfer "fluffing" of waste and its effect on waste behavior (e.g., gas retention).	The impact of the fluffing factor on the thermal performance is documented in WHC-SD-WM-ER-534 Rev 0, and has been included on page E-1243 of Appendix E. Controls on sludge depth and tank temperature (Section 6.2.3) insure that temperature limits are not exceeded. The impact of fluffing on the GRE remains an open item (Section 6.4) and must be resolved prior to start of Operations.

Excerpts from RCR Forms.

Item	Reviewers Comment	WHC Response
25.	Whether there is a criticality issue. We strongly suggest a definitive criticality analysis be performed for this specific project before retrieval begins.	Section 4.3.1.2 provides the summary of the criticality analysis completed to date. These analyses centered around Pu concentration and poison ratios and showed acceptable double contingency protection against criticalities. Recent concerns about possible Pu separation and concentration mechanisms have resulted in additional limits being placed on all double shell tanks (25 Kg). This remains an open item, Section 6.4 A further evaluation of the analysis is being conducted by a Criticality Safety Review Group made up of WHC, PNNL, and DOE. The outcome of this assessment will also be included in the SA for review, when available.
28.	Justification of data selected for use when conflicting data exist (reconciliation of conflicting data).	All conflicting data have been reconciled, with sufficient justification, and reference material appended to assure the reviewer of adequacy.
29.	Identification and justification of all assumptions used.	All assumptions have been noted, and justifications/background information provided.
32.	Where is the heat source? Do we have reliable information about its magnitude? What is the evidence that significant heat is not generated in the hard pan? Are temperature records available for the period before the addition of Sr? We suggest examination of existing data for more detailed answers. <u>We believe it is important to decide, as soon as possible, whether more core samples are needed to answer these questions.</u>	See responses to item 3 and 6.

Excerpts from RCR Forms.

Item	Reviewers Comment	WHC Response
33.	How can success of the retrieval operation (removing 74% of the heating materials, or all but 40,000 Btu/hr) be measured? The initial answer was that tank C-106 would be monitored after sluicing. Can progress only be determined after completion of the project? Are there no plans for making corrective measures if progress is not satisfactory? We suggest provisions be described (in detail) for monitoring transfer line contents (radiation levels, density, flow volume, etc.) and for sampling of the waste transfer stream. In addition, the best-possible description of the contents of both tanks (before sluicing) is needed. Direct, on-line sampling of transferred waste would appear to be the most satisfactory means for monitoring success.	See response to item 12.
34.	Is there any stored energy in the waste that may be violently released during sluicing? Major emphasis was placed on not observing such behavior in tanks containing similar high heat waste. We believe the answer must be based on data from C-106. We therefore suggest re-examination of existing data (including original data references) to attempt reconciliation of inconsistencies and determine whether superheated regions can be ruled out. If superheated regions cannot be ruled out, we suggest considering the potential effects of steam flashing. A related concern is the possibility of exceeding tank temperature limits (in the absence of water addition) due to hardpan left in C-106 after sluicing.	As described in the responses to items 6, 7 and 9.

Excerpts from RCR Forms.

Item	Reviewers Comment	WHC Response
35.	Do the precipitated soluble materials contain trapped electrons, lattice defects, etc., which will liberate heat on dissolution? We suggest determination of bounding values for possible heat liberation and conferring with BNL to close the issue.	BNL agreed to provide references and a technical basis to support the concern relating to a risk potential in the C-106 system. None has been provided. In addition, WHC/ CRS members have not located any supporting references in the literature for the C-106 case of waste consisting of mostly amorphous, finely divided particles in an aqueous medium. This issue is considered closed.
36.	Could there be a gas generation (release) problem? We suggest developing an upper bound for retained gas. Unless safe upper limits for the volume of retained gas can be demonstrated, we suggest continuous monitoring of flammable gas concentration in the dome spaces of both C-106 and AY-102 (consistent with flammable gas controls) before, during, and after retrieval. Related question: How much gas can be tolerated in the transfer line? We suggest bounding the possible gas content in the transfer line and associated consequences.	Continuous monitoring of flammable gas concentration in the dome of both C-106 and AY-102 before, during, and after retrieval has been required (Section 6.1.1.15 and 6.1.2.15) Relative to gas transfer in the pipeline, refer to the response given for item 18.
37.	What are the consequences involved in the dissolution of precipitated salts in the sludge? How much and what kinds of toxic gas will be released? We suggest inclusion of a detailed description of the potential source term and corresponding health and safety controls.	This discussion will be included in the letter report to be provided by Dr. Babad (WHC) and appended to the SA, when available.

Excerpts from RCR Forms.

Item	Reviewers Comment	WHC Response
38.	What are the consequences with respect to criticality in using a sluicing fluid which contains complexants capable of segregating plutonium? We find the answer given ("The requirements indicate that the occurrence of a criticality accident in the underground waste storage tanks or transfer lines is incredible because of the low concentration of fissile materials present in the waste") not acceptable, and suggest the answer should be based on maximum possible Pu concentration in the specific tanks involved. This would require documenting the Pu content and prediction of maximum possible concentration. Related questions were raised by Kovach: What is the basis for using a different criticality safety criteria for this transfer than the standard site-criticality safety basis? Tank C-106 contains approximately 96 kg of Pu. Is it expected that the proposed volume retrieved (75%) would remove only half of the Pu? <u>We strongly suggest a definitive criticality analysis be performed for this specific project before retrieval begins.</u>	See response to item 25.

Excerpts from RCR Forms.

Item	Reviewers Comment	WHC Response
39.	What is the plan to preclude potential precipitation during transfer and getting pipes plugged? (Related questions: Will there be a plugging problem during start up or shut down? How would pipe blockage be addressed? How does the plan to avoid pipe plugging compare with those of past practice [both successful and unsuccessful?]) We suggest describing expected gas release, particle size distribution, etc. in the transfer line, together with bounds for flow rate, particle size, and solids loading, entrained or released gas, etc. (to avoid pipe blockage or damage) and associated controls. If pipe blockage cannot be ruled out, we suggest including a description of contingency plans.	See responses to items 13, 14, and 18.
40.	What problems will emerge when the saturated sluicing solution, produced in the sluicing operation drops in temperature in the transfer lines? Answer given: "Dilute solutions based on using buffered water should not create saturated sluicing solutions" and "The analysis determined that the temperature change during transfer is less than two degrees Centigrade which is minimum in respect to the unsaturated region of the waste during transfer." We suggest arguments leading to these conclusions be included.	See response to item 17.

Excerpts from RCR Forms.

Item	Reviewers Comment	WHC Response
41.	What tests have been done to demonstrate compatibility between the sluicing fluid and the C-106 waste? (What will be done to ensure compatibility?) While specific actions were not agreed upon, the mixing of actual waste samples would appear to give the most reliable answer. We request presentation of a detailed plan, including important factors and specific steps, to determine waste compatibility.	Laboratory tests involved with mixing samples with AY-102 supernate and C-106 solids are in progress. The results of these tests will be included in the Babad letter report and appended to the SA when available.
44.	Is the assumption that dilution can be used to prevent line plugging practical when considered in the light of the mass of soluble precipitated salts in the sludge? (See answer to "10" above.) Is there a significant amount of potential soluble material than can dissolve and re-precipitate? Whether the answer is yes or no, we believe the answer should be given in the document.	This issue is considered resolved (see Appendix E, page E-1155)

APPENDIX A.2

TABULATION OF AVAILABLE DRAFT LABCORE DATA ON WIDE-MOUTH-BOTTLE-BASED GRAB SAMPLES OBTAINED FROM TANK C-106 IN THE SPRING OF 1996

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APPENDIX A.2

TABULATION OF AVAILABLE DRAFT LABCORE DATA ON WIDE-MOUTH-BOTTLE-BASED GRAB SAMPLES OBTAINED FROM TANK C-106 IN THE SPRING OF 1996

Data Use Caveat:

The data contained in this appendix are preliminary in nature and may be subject to change. This information has not yet undergone the required checks and quality reviews required by WHC laboratory characterization data reporting requirements. It is believed that data review and certification will not result in any changes to the conclusions reported in this document.

Since the original release of this report, the certified data acquired in the recent sludge sampling event was added to the tank characterization database and was reported in Schreiber et al. (1996).

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Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

RISER: 1

SEGMENT #: 6C-96-10

SEGMENT PORTION: Centrifuged Solids (Grab Sample)

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T000558		Bulk Density of Sample	g/mL	n/a	n/a	1.760	n/a	n/a	n/a	n/a	5.00e-01	n/a
S96T000558		DSC Exotherm Dry Calculated	Joules/g Dry	n/a	n/a	0.00e+00	0.00e+00	0.00e+00	0.00	n/a	n/a	n/a
S96T000558		DSC Exotherm on Perkin Elmer	Joules/g	98.45	n/a	0.00e+00	0.00e+00	0.00e+00	0.00	n/a	n/a	n/a
S96T000558		% Water by TGA on Perkin Elmer	%	98.68	n/a	11.71	14.00	12.86	17.8	n/a	n/a	n/a
S96T000558		Volume % Solids	%	n/a	n/a	85.20	n/a	n/a	n/a	n/a	n/a	n/a
S96T000558		% Water by Gravimetric	%	98.14	n/a	17.00	17.20	17.10	0.24	n/a	1.00e-02	n/a

Control Sample: Control Sample

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T000560		DSC Exotherm Dry Calculated	Joules/g Dry	n/a	n/a	0.00e+00	0.00e+00	0.00e+00	0.00	n/a	n/a	n/a
S96T000560		DSC Exotherm on Perkin Elmer	Joules/g	98.45	n/a	0.00e+00	0.00e+00	0.00e+00	0.00	n/a	n/a	n/a
S96T000560		% Water by TGA using Mettler	%	102.2	n/a	13.39	13.59	13.49	1.48	n/a	n/a	n/a
S96T000561	F	Technetium-99 Liq. Scint.	µCi/g	99.47	<3.58e-02	<6.43e-02	<5.53E-2	n/a	n/a	n/a	6.40e-02	6.35E+00
S96T000561	F	Strontium-89/90 High Level	µCi/g	92.68	6.20e-02	1.74e+02	152.0	163.0	13.5	n/a	4.80e-02	6.80E-01
S96T000561	F	Pu-239/240 by TRU-SPEC Resin	µCi/g	94.49	<5.300	<6.20e-02	<4.67E-2	n/a	n/a	n/a	6.20e-02	1.00E+02
S96T000561	F	Cobalt-60 by GEA	µCi/g	98.05	<4.73e-01	<2.05e-01	<1.88e-1	n/a	n/a	n/a	2.05e-01	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
Control Sample: Control Sample (Continued)												
S96T000561	F	Cesium-137 by GEA	µCi/g	98.56	<9.17e-01	1.98e+02	170.0	183.8	15.2	n/a	n/a	1.01
S96T000561	F	Am-241 by Extraction	µCi/g	105.5	<4.43e-02	4.26e-01	3.62e-01	3.94e-01	16.2	n/a	6.80e-02	3.95E+00
S96T000561	F	Alpha of Digested Solid	µCi/g	118.0	<5.57e-02	1.560	1.150	1.355	30.3	107.8	1.32e-01	2.00E+01
Decanted Supernate (Liquid Grab Sludge): Decanted Supernate (Liquid Grab Sludge)												
S96T000559		Specific Gravity	Sp.G.	101.1	n/a	1.156	1.150	1.153	0.52	n/a	1.00e-03	n/a
S96T000559		% Water by Gravimetric	%	98.65	n/a	79.30	79.30	79.30	0.00	n/a	1.00e-02	n/a
Filtered Centrifuged Solids: Filtered Centrifuged Solids												
S96T000567		DSC Exotherm using Mettler	Joules/g	99.82	n/a	69.70	94.70	82.20	30.4	n/a	n/a	n/a
S96T000567		DSC Exotherm Dry Calculated	Joules/g Dry	n/a	n/a	93.87	127.5	110.7	30.4	n/a	n/a	n/a
S96T000567		% Water by TGA using Mettler	%	101.7	n/a	26.22	25.27	25.74	3.69	n/a	n/a	n/a
S96T000568		TIC by Acid/Coulometry	µg/g	97.84	8.00e-01	2.93e+04	2.56e+04	2.74e+04	13.5	100.0	5.000	n/a
S96T000568		TOC by Persulfate/ Coulometry	µg/g	92.03	3.100	2.04e+04	2.49e+04	2.26e+04	19.9	87.90	40.00	n/a
S96T000569		% Water by Gravimetric	%	98.14	n/a	26.30	27.30	26.80	1.37	n/a	1.00e-02	n/a
S96T000570		pH on SST Samples	pH	n/a	n/a	10.56	10.54	10.55	0.19	n/a	1.00e-02	n/a
S96T000571	F	Technetium-99 Liq. Scint.	µCi/g	99.47	<3.58e-02	<2.26e-02	<2.74E-2	n/a	n/a	n/a	2.30e-02	6.16E+00
S96T000571	F	Strontium-89/90 High Level	µCi/g	101.6	1.17e-01	1.86e+02	517.0	351.5	94.2	n/a	4.40e-02	5.50E-01
S96T000571	F	Pu-239/240 by TRU-SPEC Resin	µCi/g	94.49	<5.300	<2.17e-02	<2.79E-2	n/a	n/a	n/a	2.20e-02	1.00E+02
S96T000571	F	Cobalt-60 by GEA	µCi/g	96.66	<1.52e-01	<1.28e-01	3.51e-01	n/a	n/a	n/a	1.28e-01	n/a
S96T000571	F	Cesium-137 by GEA	µCi/g	96.08	<2.04e-01	2.05e+02	531.0	367.8	88.6	n/a	n/a	0.640

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Filtered Centrifuged Solids: Filtered Centrifuged Solids (Continued)												
Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T000571	F	Am-241 by Extraction	µCi/g	103.7	<1.58e-02	5.32e-01	1.560	1.046	98.3	n/a	4.30e-02	2.71E+00
S96T000571	F	Alpha of Digested Solid	µCi/g	118.0	<5.57e-02	1.320	3.570	2.445	92.0	107.2	4.50e-02	1.22E+01
S96T000572	A	Silver-ICP-Acid Digest	µg/g	91.90	<1.00e-02	1.42e+03	1.66e+03	1.54e+03	15.6	72.20	8.430	n/a
S96T000572	A	Boron-ICP-Acid Digest	µg/g	108.8	5.40e-01	71.30	83.00	77.15	15.2	95.54	42.20	n/a
S96T000572	A	Barium-ICP-AcidDigest	µg/g	97.60	<5.00e-02	2.88e+02	340.0	314.0	16.6	97.20	42.20	n/a
S96T000572	A	Beryllium-ICP-Acid Digest	µg/g	103.0	<5.00e-03	<4.220	<4.93e0	n/a	n/a	97.80	4.210	n/a
S96T000572	A	Bismuth-ICP-AcidDigest	µg/g	92.40	<1.00e-01	<84.30	<9.86e1	n/a	n/a	89.00	84.30	n/a
S96T000572	A	Calcium-ICP-AcidDigest	µg/g	100.2	4.59e-01	8.82e+02	1.04e+03	961.0	16.4	101.4	84.30	n/a
S96T000572	A	Cadmium-ICP-Acid Digest	µg/g	94.60	<5.00e-03	39.90	44.50	42.20	10.9	92.26	4.210	n/a
S96T000572	A	Cerium-ICP-AcidDigest	µg/g	100.0	<1.00e-01	2.06e+02	199.0	202.5	3.46	98.92	84.30	n/a
S96T000572	A	Cobalt-ICP-Acid Digest	µg/g	98.40	<2.00e-02	<16.90	<1.97e1	n/a	n/a	96.00	16.90	n/a
S96T000572	A	Chromium-ICP-Acid Digest	µg/g	97.00	1.70e-02	7.69e+02	884.0	826.5	13.9	92.22	8.430	n/a
S96T000572	A	Copper-ICP-AcidDigest	µg/g	92.80	2.60e-02	84.40	96.40	90.40	13.3	92.18	8.430	n/a
S96T000572	A	Iron-ICP-Acid Digest	µg/g	97.60	7.00e-02	7.03e+04	8.25e+04	7.64e+04	16.0	18.42	42.20	n/a
S96T000572	A	Potassium-ICP-Acid Digest	µg/g	98.80	<5.00e-01	6.12e+02	646.0	629.0	5.41	84.88	422.0	n/a
S96T000572	A	Lanthanum-ICP-Acid Digest	µg/g	98.20	<5.00e-02	59.10	72.30	65.70	20.1	96.20	42.20	n/a
S96T000572	A	Lithium-ICP-Acid Digest	µg/g	95.80	<1.00e-02	<8.430	<9.86e0	n/a	n/a	94.60	8.430	n/a
S96T000572	A	Magnesium-ICP-Acid Digest	µg/g	94.60	<1.00e-01	2.25e+02	263.0	244.0	15.6	91.28	84.30	n/a
S96T000572	A	Manganese-ICP-Acid Digest	µg/g	96.60	<1.00e-02	1.75e+03	2.05e+03	1.90e+03	15.8	94.48	8.430	n/a
S96T000572	A	Molybdenum-ICP-Acid Digest	µg/g	97.60	<5.00e-02	<42.20	<4.93e1	n/a	n/a	94.80	42.20	n/a
S96T000572	A	Sodium-ICP-Acid Digest	µg/g	109.0	7.70e-01	1.19e+05	1.41e+05	1.30e+05	16.9	1.84e+03	84.30	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Filtered Centrifuged Solids: Filtered Centrifuged Solids (Continued)												
Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T000572	A	Neodymium-ICP-Acid Digest	µg/g	98.00	<1.00e-01	1.53e+02	170.0	161.5	10.5	96.66	84.30	n/a
S96T000572	A	Nickel-ICP-Acid Digest	µg/g	97.20	<2.00e-02	6.53e+02	755.0	704.0	14.5	88.94	16.90	n/a
S96T000572	A	Phosphorus-ICP-Acid Digest	µg/g	99.80	<2.00e-01	2.22e+03	2.60e+03	2.41e+03	15.8	122.7	169.0	n/a
S96T000572	A	Lead-ICP-Acid Digest	µg/g	91.60	<1.00e-01	2.55e+03	2.97e+03	2.76e+03	15.2	82.02	84.30	n/a
S96T000572	A	Sulfur-ICP-Acid Digest	µg/g	95.60	<1.00e-01	1.13e+03	1.32e+03	1.22e+03	15.5	93.96	84.30	n/a
S96T000572	A	Antimony-ICP-Acid Digest	µg/g	96.60	<6.00e-02	95.40	<5.91e1	n/a	n/a	83.88	50.60	n/a
S96T000572	A	Selenium-ICP-Acid Digest	µg/g	97.80	<1.00e-01	<84.30	<9.86e1	n/a	n/a	98.80	84.30	n/a
S96T000572	A	Silicon-ICP-Acid Digest	µg/g	135.2	2.27e-01	2.27e+04	2.66e+04	2.46e+04	15.8	n/a	42.20	n/a
S96T000572	A	Samarium-ICP-Acid Digest	µg/g	99.80	<1.00e-01	<84.30	<9.86e1	n/a	n/a	99.00	84.30	n/a
S96T000572	A	Strontium-ICP-Acid Digest	µg/g	97.00	<1.00e-02	17.70	20.40	19.05	14.2	95.70	8.430	n/a
S96T000572	A	Titanium-ICP-Acid Digest	µg/g	91.60	<1.00e-02	1.25e+02	147.0	136.0	16.2	89.62	8.430	n/a
S96T000572	A	Thallium-ICP-Acid Digest	µg/g	88.60	<2.00e-01	<1.69e+02	<1.97e2	n/a	n/a	87.60	169.0	n/a
S96T000572	A	Uranium-ICP-AcidDigest	µg/g	94.40	<5.00e-01	7.07e+02	890.0	798.5	22.9	104.1	422.0	n/a
S96T000572	A	Vanadium-ICP-Acid Digest	µg/g	96.40	<5.00e-02	<42.20	<4.93e1	n/a	n/a	95.40	42.20	n/a
S96T000572	A	Zinc-ICP-Acid Digest	µg/g	92.60	2.50e-02	40.30	44.60	42.45	10.1	91.22	8.430	n/a
S96T000572	A	Zirconium-ICP-Acid Digest	µg/g	104.2	<1.00e-02	7.55e+02	890.0	822.5	16.4	180.4	8.430	n/a
S96T000574	W	Fluoride-IC-Dionex 4000i/4500	µg/g	96.10	<1.30e-02	1.94e+02	195.0	194.7	0.51	100.8	55.12	n/a
S96T000574	W	Chloride-IC-Dionex 4000i/4500	µg/g	99.11	3.30e-02	1.47e+02	133.0	140.0	10.0	95.06	72.07	n/a
S96T000574	W	Nitrite-IC-Dionex 4000i/4500	µg/g	97.74	<1.07e-01	1.04e+04	1.03e+04	1.03e+04	0.97	107.5	453.6	n/a
S96T000574	W	Nitrate by IC-Dionex 4000i/4500	µg/g	97.72	<1.40e-01	1.83e+03	978.0	1.41e+03	60.7	93.81	593.2	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
Filtered Centrifuged Solids: Filtered Centrifuged Solids (Continued)												
S96T000574	W	Phosphate-IC-Dionex 4000i/4500	µg/g	100.2	<1.19e-01	3.52e+03	1.01e+03	2.27e+03	111	89.19	504.2	n/a
S96T000574	W	Sulfate by IC-Dionex 4000i/4500	µg/g	97.94	<1.36e-01	3.32e+03	3.31e+03	3.32e+03	0.30	98.26	576.2	n/a
S96T000574	W	Oxalate by IC-Dionex 4000i	µg/g	99.07	<1.05e-01	6.90e+04	6.83e+04	6.86e+04	1.02	116.0	445.2	n/a
S96T002718	F	Technetium-99 Liq. Scint.	µCi/g	104.5	<1.42e-02	<3.52e-02	<3.70E-2	n/a	n/a	n/a	3.50e-02	6.92E+00
S96T002718	F	Strontium-89/90 High Level	µCi/g	110.6	8.13e-01	5.90e+02	639.0	614.5	7.97	n/a	6.41e-01	1.01E+00
S96T002718	F	Pu-239/240 by TRU-SPEC Resin	µCi/g	97.11	<3.90e-02	1.520	1.530	1.525	0.66	n/a	1.02e-01	2.08E+00
S96T002718	F	Cobalt-60 by GEA	µCi/g	98.94	<3.01e-01	<5.33e-01	<4.23e-1	n/a	n/a	n/a	5.33e-01	n/a
S96T002718	F	Cesium-137 by GEA	µCi/g	97.97	<4.49e-01	5.80e+02	633.0	606.3	8.74	n/a	n/a	1.10
S96T002718	F	Am-241 by Extraction	µCi/g	101.3	<2.76e-02	1.870	1.690	1.780	10.1	n/a	1.45e-01	2.69E+00
S96T002718	F	Alpha of Digested Solid	µCi/g	114.1	<5.69e-02	3.500	3.640	3.570	3.92	89.14	9.20e-02	9.86E+00
Interstitial Liquid: Interstitial Liquid												
S96T000563		DSC Exotherm Dry Calculated	Joules/g Dry	n/a	n/a	0.00e+00	0.00e+00	0.00e+00	0.00	n/a	n/a	n/a
S96T000563		DSC Exotherm on Perkin Elmer	Joules/g	95.82	n/a	0.00e+00	0.00e+00	0.00e+00	0.00	n/a	n/a	n/a
S96T000563		% Water by TGA using Mettler	%	100.2	n/a	61.32	59.37	60.34	3.23	n/a	n/a	n/a
S96T000563		Tot. Organic Carbon by Coul.	µg/mL	103.4	2.00e-01	2.44e+03	2.44e+03	2.44e+03	0.00	95.50	55.00	n/a
S96T000563		TOC by Persulfate/ Coulometry	µg/mL	96.00	5.000	2.35e+03	2.28e+03	2.32e+03	3.02	n/a	40.00	n/a
S96T000563		Strontium-89/90 High Level	µCi/mL	99.19	4.00e-03	1.230	6.35e-01	9.32e-01	63.8	n/a	8.00e-03	2.76E+00

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Interstitial Liquid: Interstitial Liquid (Continued)

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T000563		Pu-239/240 by TRU-SPEC Resin	µCi/mL	93.44	<3.56e-03	8.12e-01	8.33e-01	8.23e-01	2.55	n/a	3.80e-02	1.59E+00
S96T000563	D	Silver-ICP-Acid Dil.	µg/mL	97.60	<1.00e-02	<4.010	<4.01e0	n/a	n/a	92.80	4.010	n/a
S96T000563	D	Aluminum-ICP- Acid Dil.	µg/mL	96.60	<5.00e-02	<20.10	<2.01e1	n/a	n/a	92.80	20.10	n/a
S96T000563	D	Arsenic-ICP-Acid Dil.	µg/mL	101.0	<1.00e-01	<40.10	<4.01e1	n/a	n/a	103.8	40.10	n/a
S96T000563	D	Boron-ICP-Acid Dil.	µg/mL	101.8	<5.00e-02	<20.10	<2.01e1	n/a	n/a	102.5	20.10	n/a
S96T000563	D	Barium-ICP-Acid Dil.	µg/mL	99.40	<5.00e-02	<20.10	<2.01e1	n/a	n/a	99.00	20.10	n/a
S96T000563	D	Beryllium-ICP-Acid Dil.	µg/mL	103.8	<5.00e-03	<2.000	<2.00e0	n/a	n/a	101.8	2.000	n/a
S96T000563	D	Bismuth-ICP-Acid Dil.	µg/mL	99.80	<1.00e-01	<40.10	<4.01e1	n/a	n/a	95.50	40.10	n/a
S96T000563	D	Calcium-ICP-Acid Dil.	µg/mL	99.60	<1.00e-01	<40.10	<4.01e1	n/a	n/a	99.00	40.10	n/a
S96T000563	D	Cadmium-ICP-Acid Dil.	µg/mL	100.8	<5.00e-03	<2.000	<2.00e0	n/a	n/a	98.00	2.000	n/a
S96T000563	D	Cerium-ICP-Acid Dil.	µg/mL	100.4	<1.00e-01	<40.10	<4.01e1	n/a	n/a	96.50	40.10	n/a
S96T000563	D	Cobalt-ICP-Acid Dil.	µg/mL	100.2	<2.00e-02	<8.020	<8.02e0	n/a	n/a	97.00	8.020	n/a
S96T000563	D	Chromium-ICP-Acid Dil.	µg/mL	100.2	<1.00e-02	<4.010	<4.01e0	n/a	n/a	98.50	4.010	n/a
S96T000563	D	Copper-ICP-Acid Dil.	µg/mL	100.6	<1.00e-02	<4.010	<4.01e0	n/a	n/a	99.80	4.010	n/a
S96T000563	D	Iron-ICP-Acid Dil.	µg/mL	103.4	<5.00e-02	<20.10	<2.01e1	n/a	n/a	105.2	20.10	n/a
S96T000563	D	Potassium-ICP-Acid Dil.	µg/mL	97.20	<5.00e-01	5.48e+02	564.0	556.0	2.88	96.40	200.0	n/a
S96T000563	D	Lanthanum-ICP-Acid Dil.	µg/mL	100.8	<5.00e-02	<20.10	<2.01e1	n/a	n/a	101.0	20.10	n/a
S96T000563	D	Lithium-ICP-Acid Dil.	µg/mL	97.00	<1.00e-02	<4.010	<4.01e0	n/a	n/a	92.00	4.010	n/a
S96T000563	D	Magnesium-ICP-Acid Dil.	µg/mL	96.80	<1.00e-01	<40.10	<4.01e1	n/a	n/a	93.80	40.10	n/a
S96T000563	D	Manganese-ICP-Acid Dil.	µg/mL	100.2	<1.00e-02	<4.010	<4.01e0	n/a	n/a	99.30	4.010	n/a
S96T000563	D	Molybdenum-ICP-Acid Dil.	µg/mL	99.20	<5.00e-02	21.30	<2.01e1	n/a	n/a	96.70	20.10	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Interstitial Liquid: Interstitial Liquid (Continued)												
Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T000563	D	Sodium-ICP-Acid Dil.	µg/mL	96.60	<1.00e-01	1.03e+05	1.01e+05	1.02e+05	1.96	n/a	40.10	n/a
S96T000563	D	Neodymium-ICP-Acid Dil.	µg/mL	105.8	<1.00e-01	<40.10	<4.01e1	n/a	n/a	105.5	40.10	n/a
S96T000563	D	Nickel-ICP-Acid Dil.	µg/mL	100.4	<2.00e-02	13.70	13.50	13.60	1.47	98.60	8.020	n/a
S96T000563	D	Phosphorus-ICP-Acid Dil.	µg/mL	108.8	<2.00e-01	3.71e+02	375.0	373.0	1.07	115.0	80.20	n/a
S96T000563	D	Lead-ICP-Acid Dil.	µg/mL	100.6	<1.00e-01	<40.10	<4.01e1	n/a	n/a	99.50	40.10	n/a
S96T000563	D	Sulfur-ICP-Acid Dil.	µg/mL	98.20	<1.00e-01	2.48e+03	2.50e+03	2.49e+03	0.80	82.70	40.10	n/a
S96T000563	D	Antimony-ICP-Acid Dil.	µg/mL	94.60	<6.00e-02	<24.10	<2.41e1	n/a	n/a	90.80	24.10	n/a
S96T000563	D	Selenium-ICP-Acid Dil.	µg/mL	102.6	<1.00e-01	<40.10	<4.01e1	n/a	n/a	110.0	40.10	n/a
S96T000563	D	Silicon-ICP-Acid Dil.	µg/mL	95.20	<5.00e-02	25.80	26.90	26.35	4.17	95.10	20.10	n/a
S96T000563	D	Samarium-ICP-Acid Dil.	µg/mL	101.0	<1.00e-01	<40.10	<4.01e1	n/a	n/a	102.0	40.10	n/a
S96T000563	D	Strontium-ICP-Acid Dil.	µg/mL	99.40	<1.00e-02	<4.010	<4.01e0	n/a	n/a	99.30	4.010	n/a
S96T000563	D	Titanium-ICP-Acid Dil.	µg/mL	96.60	<1.00e-02	<4.010	<4.01e0	n/a	n/a	96.00	4.010	n/a
S96T000563	D	Thallium-ICP-Acid Dil.	µg/mL	95.00	<2.00e-01	<80.20	<8.02e1	n/a	n/a	85.80	80.20	n/a
S96T000563	D	Uranium-ICP-Acid Dil.	µg/mL	98.50	<5.00e-01	1.56e+03	1.57e+03	1.56e+03	0.64	102.3	200.0	n/a
S96T000563	D	Vanadium-ICP-Acid Dil.	µg/mL	102.0	<5.00e-02	<20.10	<2.01e1	n/a	n/a	100.0	20.10	n/a
S96T000563	D	Zinc-ICP-Acid Dil.	µg/mL	100.6	<1.00e-02	<4.010	<4.01e0	n/a	n/a	97.50	4.010	n/a
S96T000563	D	Zirconium-ICP-Acid Dil.	µg/mL	99.80	<1.00e-02	3.36e+02	336.0	336.0	0.00	100.6	4.010	n/a
S96T000563		Fluoride-IC-Dionex 4000i/4500	µg/mL	95.42	<1.30e-02	2.36e+02	230.0	232.8	2.58	108.5	27.57	n/a
S96T000563		Chloride-IC-Dionex 4000i/4500	µg/mL	90.38	5.55e-01	3.04e+02	326.0	315.1	6.98	91.65	36.06	n/a
S96T000563		Nitrite-IC-Dionex 4000i/4500	µg/mL	97.95	<1.07e-01	2.91e+04	2.83e+04	2.87e+04	2.79	102.6	226.9	n/a
S96T000563		Nitrate-IC-Dionex4000i/4500	µg/mL	93.97	2.05e-01	1.17e+03	1.14e+03	1.15e+03	2.60	94.46	296.9	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
Interstitial Liquid: Interstitial Liquid (Continued)												
S96T000563		Phosphate-IC-Dionex 4000i/4500	µg/mL	96.89	<1.19e-01	6.49e+02	609.0	629.0	6.36	97.80	252.2	n/a
S96T000563		Sulfate by IC-Dionex 4000i/4500	µg/mL	95.56	<1.36e-01	7.76e+03	7.61e+03	7.69e+03	1.95	98.89	288.2	n/a
S96T000563		Oxalate by IC-Dionex 4000i	µg/mL	95.09	<1.05e-01	3.08e+03	3.09e+03	3.09e+03	0.32	98.43	222.7	n/a
S96T000563		Cobalt-60 by GEA	µCi/mL	96.11	<6.53e-04	<8.45e-03	1.24e-02	n/a	n/a	n/a	8.00e-03	n/a
S96T000563		Cesium-137 by GEA	µCi/mL	95.94	<4.94e-04	1.54e+02	153.0	153.5	0.65	n/a	n/a	0.200
Potential Organic Layer: Potential Organic Layer												
S96T001567		DSC Exotherm using Mettler	Joules/g	113.9	n/a	2.15e+02	142.4	178.8	40.7	n/a	n/a	n/a
S96T001567		DSC Exotherm Dry Calculated	Joules/g Dry	n/a	n/a	7.06e+02	467.7	587.0	40.7	n/a	n/a	n/a
S96T001567		% Water by TGA using Mettler	%	103.7	n/a	71.58	67.52	69.55	5.84	n/a	n/a	n/a
S96T001567		TOC by Persulfate/ Coulometry	µg/mL	94.03	3.000	3.08e+04	3.48e+04	3.28e+04	12.2	n/a	40.00	n/a
S96T002634		Pu-239/240 by TRU-SPEC Resin	µCi/g	99.21	<3.10e-02	6.41e-01	6.31e-01	6.36e-01	1.57	n/a	4.60e-02	2.00E+00
S96T002634		Pu-238 by Ion Exchange	µCi/g	n/a	<3.10e-02	2.00e-01	2.01e-01	2.01e-01	0.50	n/a	4.60e-02	2.78E+00

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

RISER: 1

SEGMENT #: 6C-96-17

SEGMENT PORTION: Field Blank

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T000855		DSC Exotherm using Mettler	Joules/g	94.55	n/a	0.00e+00	0.00e+00	0.00e+00	0.00	n/a	n/a	n/a
S96T000855		Ammonia by ISE-Std Additions	µg/mL	106.8	5.80e-02	<5.000	<5.00	n/a	n/a	104.0	5.000	n/a
S96T000855		pH Direct	pH	n/a	n/a	8.282	8.239	8.261	0.52	n/a	1.00e-02	n/a
S96T000855		Specific Gravity	Sp.G.	102.1	n/a	9.75e-01	9.74e-01	9.74e-01	0.10	n/a	1.00e-03	n/a
S96T000855		% Water by TGA using Mettler	%	101.9	n/a	1.00e+02	99.85	100.2	0.65	n/a	n/a	n/a
S96T000855		Tot. Inorg. Carbon by Coul.	µg/mL	97.17	<5.000	8.000	9.500	8.750	17.1	n/a	5.000	
S96T000855		Tot. Organic Carbon by Coul.	µg/mL	103.0	9.00e-01	17.10	14.30	15.70	17.8	96.70	5.500	n/a
S96T000855		TOC by Persulfate/ Coulometry	µg/mL	93.03	1.600	<40.00	<40	n/a	n/a	n/a	40.00	n/a
S96T000855		% Water by Gravimetric	%	98.82	n/a	1.00e+02	100.0	100.0	0.00	n/a	1.00e-02	n/a
S96T000855		Technetium-99 Liq. Scint.	µCi/mL	102.6	<3.72e-05	<3.56e-05	3.84e-05	n/a	n/a	n/a	3.56e-05	7.04E+00
S96T000855		Strontium-89/90 High Level	µCi/mL	104.1	8.78e-07	1.79e-02	1.79e-02	1.79e-02	0.00	n/a	9.32e-07	2.26E-01
S96T000855		Pu-239/240 by TRU-SPEC Resin	µCi/mL	109.4	<3.66e-05	1.64e-05	1.63e-05	1.63e-05	0.61	n/a	3.66e-06	4.0
S96T000855	D	Silver-ICP-Acid Dil.	µg/mL	99.20	<1.00e-02	<1.00e-02	<1.00e-2	n/a	n/a	81.50	1.00e-02	n/a
S96T000855	D	Aluminum-ICP-Acid Dil.	µg/mL	97.80	<5.00e-02	2.82e-01	2.62e-01	2.72e-01	7.35	98.30	5.00e-02	n/a
S96T000855	D	Arsenic-ICP-Acid Dil.	µg/mL	101.6	<1.00e-01	<1.00e-01	<1.00e-1	n/a	n/a	100.0	1.00e-01	n/a
S96T000855	D	Boron-ICP-Acid Dil.	µg/mL	101.4	<5.00e-02	<5.00e-02	<5.00e-2	n/a	n/a	99.20	5.00e-02	n/a
S96T000855	D	Barium-ICP-Acid Dil.	µg/mL	98.40	<5.00e-02	<5.00e-02	<5.00e-2	n/a	n/a	96.90	5.00e-02	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

SEGMENT PORTION: Field Blank (Continued)

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T000855	D	Beryllium-ICP-Acid Dil.	µg/mL	102.4	<5.00e-03	<5.00e-03	<5.00e-3	n/a	n/a	101.5	5.00e-03	n/a
S96T000855	D	Bismuth-ICP-Acid Dil.	µg/mL	98.80	<1.00e-01	<1.00e-01	<1.00e-1	n/a	n/a	96.20	1.00e-01	n/a
S96T000855	D	Calcium-ICP-Acid Dil.	µg/mL	98.80	<1.00e-01	6.870	6.740	6.805	1.91	98.90	1.00e-01	n/a
S96T000855	D	Cadmium-ICP-Acid Dil.	µg/mL	100.4	<5.00e-03	<5.00e-03	<5.00e-3	n/a	n/a	98.50	5.00e-03	n/a
S96T000855	D	Cerium-ICP-Acid Dil.	µg/mL	99.20	<1.00e-01	<1.00e-01	<1.00e-1	n/a	n/a	94.60	1.00e-01	n/a
S96T000855	D	Cobalt-ICP-Acid Dil.	µg/mL	101.2	<2.00e-02	<2.00e-02	<2.00e-2	n/a	n/a	99.20	2.00e-02	n/a
S96T000855	D	Chromium-ICP-Acid Dil.	µg/mL	101.4	<1.00e-02	<1.00e-02	<1.00e-2	n/a	n/a	98.50	1.00e-02	n/a
S96T000855	D	Copper-ICP-Acid Dil.	µg/mL	99.60	<1.00e-02	<1.00e-02	<1.00e-2	n/a	n/a	99.20	1.00e-02	n/a
S96T000855	D	Iron-ICP-Acid Dil.	µg/mL	101.0	<5.00e-02	5.20e-02	<5.00e-2	n/a	n/a	98.30	5.00e-02	n/a
S96T000855	D	Potassium-ICP-Acid Dil.	µg/mL	101.4	<5.00e-01	<5.00e-01	<5.00e-1	n/a	n/a	123.8	5.00e-01	n/a
S96T000855	D	Lanthanum-ICP-Acid Dil.	µg/mL	99.20	<5.00e-02	<5.00e-02	<5.00e-2	n/a	n/a	97.70	5.00e-02	n/a
S96T000855	D	Lithium-ICP-Acid Dil.	µg/mL	98.40	<1.00e-02	<1.00e-02	<1.00e-2	n/a	n/a	96.90	1.00e-02	n/a
S96T000855	D	Magnesium-ICP-Acid Dil.	µg/mL	97.80	<1.00e-01	1.37e-01	1.20e-01	1.29e-01	13.2	94.10	1.00e-01	n/a
S96T000855	D	Manganese-ICP-Acid Dil.	µg/mL	100.8	<1.00e-02	1.04e-02	1.05e-02	1.05e-02	0.96	98.50	1.00e-02	n/a
S96T000855	D	Molybdenum-ICP-Acid Dil.	µg/mL	101.2	<5.00e-02	<5.00e-02	<5.00e-2	n/a	n/a	98.50	5.00e-02	n/a
S96T000855	D	Sodium-ICP-Acid Dil.	µg/mL	97.40	<1.00e-01	18.50	18.30	18.40	1.09	104.2	1.00e-01	n/a
S96T000855	D	Neodymium-ICP-Acid Dil.	µg/mL	100.0	<1.00e-01	<1.00e-01	<1.00e-1	n/a	n/a	96.90	1.00e-01	n/a
S96T000855	D	Nickel-ICP-Acid Dil.	µg/mL	100.4	<2.00e-02	<2.00e-02	<2.00e-2	n/a	n/a	98.50	2.00e-02	n/a
S96T000855	D	Phosphorus-ICP-Acid Dil.	µg/mL	100.4	<2.00e-01	2.280	2.190	2.235	4.03	101.7	2.00e-01	n/a
S96T000855	D	Lead-ICP-Acid Dil.	µg/mL	101.0	<1.00e-01	<1.00e-01	<1.00e-1	n/a	n/a	101.5	1.00e-01	n/a
S96T000855	D	Sulfur-ICP-Acid Dil.	µg/mL	99.00	<1.00e-01	3.32e-01	3.20e-01	3.26e-01	3.68	95.20	1.00e-01	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

SEGMENT PORTION: Field Blank (Continued)

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T000855	D	Antimony-ICP-Acid Dil.	µg/mL	94.20	<6.00e-02	<6.00e-02	<6.00e-2	n/a	n/a	90.80	6.00e-02	n/a
S96T000855	D	Selenium-ICP-Acid Dil.	µg/mL	98.20	<1.00e-01	<1.00e-01	<1.00e-1	n/a	n/a	97.70	1.00e-01	n/a
S96T000855	D	Silicon-ICP-Acid Dil.	µg/mL	95.00	<5.00e-02	7.36e-01	7.17e-01	7.26e-01	2.62	95.70	5.00e-02	n/a
S96T000855	D	Samarium-ICP-Acid Dil.	µg/mL	99.00	<1.00e-01	<1.00e-01	<1.00e-1	n/a	n/a	95.40	1.00e-01	n/a
S96T000855	D	Strontium-ICP-Acid Dil.	µg/mL	98.20	<1.00e-02	<1.00e-02	<1.00e-2	n/a	n/a	96.90	1.00e-02	n/a
S96T000855	D	Titanium-ICP-Acid Dil.	µg/mL	98.20	<1.00e-02	<1.00e-02	<1.00e-2	n/a	n/a	96.20	1.00e-02	n/a
S96T000855	D	Thallium-ICP-Acid Dil.	µg/mL	97.00	<2.00e-01	<2.00e-01	<2.00e-1	n/a	n/a	86.90	2.00e-01	n/a
S96T000855	D	Uranium-ICP-Acid Dil.	µg/mL	96.70	<5.00e-01	<5.00e-01	<5.00e-1	n/a	n/a	89.60	5.00e-01	n/a
S96T000855	D	Vanadium-ICP-Acid Dil.	µg/mL	101.4	<5.00e-02	<5.00e-02	<5.00e-2	n/a	n/a	98.50	5.00e-02	n/a
S96T000855	D	Zinc-ICP-Acid Dil.	µg/mL	101.8	<1.00e-02	<1.00e-02	<1.00e-2	n/a	n/a	100.8	1.00e-02	n/a
S96T000855	D	Zirconium-ICP-Acid Dil.	µg/mL	98.60	<1.00e-02	<1.00e-02	<1.00e-2	n/a	n/a	95.40	1.00e-02	n/a
S96T000855		Fluoride-IC-Dionex 4000i/4500	µg/mL	101.0	<1.30e-02	9.60e-02	1.08e-01	1.02e-01	11.8	n/a	1.30e-02	n/a
S96T000855		Chloride-IC-Dionex 4000i/4500	µg/mL	97.72	<1.70e-02	14.98	15.00	14.99	0.00	n/a	1.70e-02	n/a
S96T000855		Nitrite-IC-Dionex 4000i/4500	µg/mL	103.0	<1.07e-01	6.32e-01	6.22e-01	6.27e-01	1.59	n/a	1.07e-01	n/a
S96T000855		Nitrate-IC-Dionex4000i/4500	µg/mL	102.8	3.61e-01	1.567	1.600	1.583	1.89	n/a	1.40e-01	n/a
S96T000855		Phosphate-IC-Dionex 4000i/4500	µg/mL	98.53	<1.19e-01	4.59e-01	4.18e-01	4.39e-01	9.35	n/a	1.20e-01	n/a
S96T000855		Sulfate by IC-Dionex 4000i/4500	µg/mL	101.1	<1.36e-01	1.342	1.280	1.311	4.58	n/a	1.36e-01	n/a
S96T000855		Oxalate by IC-Dionex 4000i	µg/mL	104.2	<1.05e-01	<1.05e-01	<1.05e-1	n/a	n/a	n/a	1.05e-01	n/a
S96T000855		Cobalt-60 by GEA	µCi/mL	100.4	<2.62e-05	<3.21e-05	<1.75e-5	n/a	n/a	n/a	3.21e-05	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

SEGMENT PORTION: Field Blank (Continued)

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T000855		Cesium-137 by GEA	µCi/mL	100.0	<7.02e-05	4.41e-02	4.37e-02	4.39e-02	0.91	n/a	n/a	1.15
S96T000855		Am-241 by Extraction	µCi/mL	82.08	<1.16e-05	<1.60e-05	<1.73E-5	n/a	n/a	n/a	1.60e-05	5.27E+00
S96T000855		Alpha in Liquid Samples	µCi/mL	105.9	<1.44e-06	3.34e-05	2.05e-05	2.69e-05	47.9	113.6	3.85e-06	2.10E+01

RISER: 1

SEGMENT #: 6C-96-3

SEGMENT PORTION: Sludge (from Liquid Grab Sample)

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T001526		DSC Exotherm Dry Calculated	Joules/g Dry	n/a	n/a	0.00e+00	0.00e+00	0.00e+00	0.00	n/a	n/a	n/a
S96T001526		DSC Exotherm on Perkin Elmer	Joules/g	99.12	n/a	0.00e+00	0.00e+00	0.00e+00	0.00	n/a	n/a	n/a
S96T001526		% Water by TGA using Mettler	%	99.11	n/a	3.540	2.820	3.180	22.6	n/a	n/a	n/a
S96T001526		TOC by Persulfate/ Coulometry	µg/g	n/a	n/a	6.05e+04	5.03e+04	5.54e+04	18.4	n/a	40.00	n/a
S96T002821	W	Fluoride-IC-Dionex 4000i/4500	µg/g	94.75	<1.30e-02	<1.04e+04	<1.05e4	n/a	n/a	92.03	1.04e+04	n/a
S96T002821	W	Chloride-IC-Dionex 4000i/4500	µg/g	90.89	<1.70e-02	<1.36e+04	<1.37e4	n/a	n/a	86.71	1.36e+04	n/a
S96T002821	W	Nitrite-IC-Dionex 4000i/4500	µg/g	94.71	<1.07e-01	<8.57e+04	<8.63e4	n/a	n/a	90.88	8.57e+04	n/a
S96T002821	W	Nitrate by IC-Dionex 4000i/4500	µg/g	93.48	<1.40e-01	1.71e+07	2.78e+07	2.25e+07	47.7	99.84	1.12e+05	n/a
S96T002821	W	Phosphate-IC-Dionex 4000i/4500	µg/g	98.72	<1.19e-01	<9.52e+04	<9.59e4	n/a	n/a	93.41	9.52e+04	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

SEGMENT PORTION: Sludge (from Liquid Grab Sample) (Continued)

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T002821	W	Sulfate by IC-Dionex 4000i/4500	µg/g	96.20	<1.36e-01	<1.09e+05	<1.10e5	n/a	n/a	92.23	1.09e+05	n/a
S96T002821	W	Oxalate by IC-Dionex 4000i	µg/g	98.06	<1.05e-01	3.40e+05	3.68e+05	3.54e+05	7.91	92.82	8.41e+04	n/a
S96T003178	W	Fluoride-IC-Dionex 4000i/4500	µg/g	106.4	<1.30e-02	2.14e+02	267.0	240.7	22.0	105.9	109.1	n/a
S96T003178	W	Chloride-IC-Dionex 4000i/4500	µg/g	98.23	<1.70e-02	2.92e+02	310.0	300.9	5.98	92.91	142.6	n/a
S96T003178	W	Nitrite-IC-Dionex 4000i/4500	µg/g	93.91	<1.07e-01	1.32e+04	1.43e+04	1.37e+04	8.00	87.64	897.5	n/a
S96T003178	W	Nitrate by IC-Dionex 4000i/4500	µg/g	104.1	5.770	2.96e+03	3.80e+03	3.38e+03	24.9	93.97	1.17e+03	n/a
S96T003178	W	Phosphate-IC-Dionex 4000i/4500	µg/g	103.1	<1.19e-01	1.66e+03	<1.40e3	n/a	n/a	94.69	997.5	n/a
S96T003178	W	Sulfate by IC-Dionex 4000i/4500	µg/g	106.5	<1.36e-01	5.34e+03	5.23e+03	5.29e+03	2.08	97.78	1.14e+03	n/a
S96T003178	W	Oxalate by IC-Dionex 4000i	µg/g	107.5	<1.05e-01	3.08e+05	3.19e+05	3.13e+05	3.51	34.25	881.1	n/a

RISER: 1

SEGMENT #: 6C-96-4

SEGMENT PORTION: Centrifuged Solids (Grab Sample)

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T001527		Bulk Density of Sample	g/mL	n/a	n/a	1.500	n/a	n/a	n/a	n/a	5.00e-01	n/a
S96T001527		DSC Exotherm using Mettler	Joules/g	111.4	n/a	0.00e+00	1.00e+03	500.0	200	n/a	n/a	n/a
S96T0015271		DSC Exotherm using Mettler	Joules/g	112.8	n/a	13.50	25.50	19.50	61.5	n/a	n/a	n/a
S96T001527		DSC Exotherm Dry Calculated	Joules/g Dry	n/a	n/a	0.00e+00	1.04e+03	520.0	200	n/a	n/a	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

SEGMENT PORTION: Centrifuged Solids (Grab Sample) (Continued)												
Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T0015271		DSC Exotherm Dry Calculated	Joules/g Dry	n/a	n/a	14.00	26.45	20.23	61.6	n/a	n/a	n/a
S96T001527		% Water by TGA using Mettler	%	99.31	n/a	3.630	3.540	3.585	2.51	n/a	n/a	n/a
S96T001527		Volume % Solids	%	n/a	n/a	59.30	n/a	n/a	n/a	n/a	n/a	n/a
S96T001527		%Water by Gravimetric	%	98.99	n/a	5.900	5.600	5.750	5.22	n/a	1.00e-01	n/a
Control Sample: Control Sample												
S96T001530		DSC Exotherm Dry Calculated	Joules/g Dry	n/a	n/a	0.00e+00	0.00e+00	0.00e+00	0.00	n/a	n/a	n/a
S96T001530		DSC Exotherm on Perkin Elmer	Joules/g	101.6	n/a	0.00e+00	0.00e+00	0.00e+00	0.00	n/a	n/a	n/a
S96T001530		% Water by TGA on Perkin Elmer	%	99.24	n/a	32.71	34.32	33.52	4.80	n/a	n/a	n/a
S96T001531	F	Technetium-99 Liq. Scint.	µCi/g	104.5	<1.42e-02	<1.43e-02	1.74e-02	n/a	n/a	n/a	1.40e-02	7.09E+00
S96T001531	F	Strontium-89/90 High Level	µCi/g	104.1	<1.20e-01	6.03e+02	589.0	596.0	2.35	n/a	2.83e-01	6.65E-01
S96T001531	F	Pu-239/240 by TRU-SPEC Resin	µCi/g	103.7	<1.55e-02	1.270	1.210	1.240	4.84	n/a	7.60e-02	1.37E+00
S96T001531	F	Cobalt-60 by GEA	µCi/g	101.4	<2.87e-01	<4.96e-01	<4.35e-1	n/a	n/a	n/a	4.96e-01	n/a
S96T001531	F	Cesium-137 by GEA	µCi/g	99.11	<8.64e-01	6.61e+02	625.0	643.0	5.60	n/a	n/a	0.940
S96T001531	F	Am-241 by Extraction	µCi/g	90.60	<1.73e-02	8.84e-01	1.100	9.92e-01	21.8	n/a	6.10e-02	2.24E+00
S96T001531	F	Alpha of Digested Solid	µCi/g	102.3	<4.91e-02	2.630	2.570	2.600	2.31	93.59	4.30e-02	9.54E+00
S96T001528		Specific Gravity	Sp.G.	97.74	n/a	1.230	1.246	1.238	1.29	n/a	1.00e-03	n/a
S96T001528		%Water by Gravimetric	%	98.14	n/a	76.70	76.80	76.75	0.13	n/a	1.00e-01	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Decanted Supernate (Liquid Grab Sludge): Decanted Supernate (Liquid Grab Sludge)												
Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T001537		DSC Exotherm Dry Calculated	Joules/g Dry	n/a	n/a	0.00e+00	0.00e+00	0.00e+00	0.00	n/a	n/a	n/a
S96T001537		DSC Exotherm on Perkin Elmer	Joules/g	101.6	n/a	0.00e+00	0.00e+00	0.00e+00	0.00	n/a	n/a	n/a
S96T001537		% Water by TGA on Perkin Elmer	%	99.24	n/a	22.14	26.07	24.11	16.3	n/a	n/a	n/a
S96T001538		TIC by Acid/Coulometry	µg/g	99.83	5.00e-01	2.54e+04	2.53e+04	2.54e+04	0.39	102.1	5.000	n/a
S96T001538		TOC by Persulfate/ Coulometry	µg/g	92.36	1.600	1.48e+04	1.64e+04	1.56e+04	10.3	84.80	40.00	n/a
S96T001539		% Water by Gravimetric	%	99.32	n/a	27.10	23.10	25.10	15.9	n/a	1.00e-02	n/a
S96T001540		pH on SST Samples	pH	n/a	n/a	10.21	10.18	10.20	0.29	n/a	1.00e-02	n/a
S96T001541	F	Technetium-99 Liq. Scint.	µCi/g	104.5	<1.42e-02	<1.54e-02	1.75e-02	n/a	n/a	n/a	1.50e-02	7.12E+00
S96T001541	F	Strontium-89/90 High Level	µCi/g	104.1	<1.20e-01	6.65e+02	721.0	693.0	8.08	n/a	2.86e-01	6.36E-01
S96T001541	F	Pu-239/240 by TRU-SPEC Resin	µCi/g	103.7	<1.55e-02	1.420	1.480	1.450	4.14	n/a	8.10e-02	1.42E+00
S96T001541	F	Cobalt-60 by GEA	µCi/g	101.4	<2.87e-01	<5.48e-01	<5.72e-1	n/a	n/a	n/a	5.48e-01	n/a
S96T001541	F	Cesium-137 by GEA	µCi/g	99.11	<8.64e-01	6.16e+02	671.0	643.6	8.55	n/a	n/a	1.02
S96T001541	F	Am-241 by Extraction	µCi/g	90.60	<1.73e-02	1.150	1.560	1.355	30.3	n/a	7.40e-02	1.69E+00
S96T001541	F	Alpha of Digested Solid	µCi/g	102.3	<4.91e-02	3.120	3.310	3.215	5.91	94.43	4.80e-02	9.29E+00
S96T001542	A	Silver-ICP-Acid Digest	µg/g	89.40	<1.00e-02	2.50e+03	1.51e+03	2.00e+03	49.4	n/a	6.140	n/a
S96T001542	A	Aluminum-ICP-Acid Digest	µg/g	91.00	1.17e-01	6.20e+04	5.44e+04	5.82e+04	13.1	n/a	30.70	n/a
S96T001542	A	Arsenic-ICP-Acid Digest	µg/g	94.00	<1.00e-01	<61.40	<5.91e1	n/a	n/a	84.70	61.40	n/a
S96T001542	A	Boron-ICP-Acid Digest	µg/g	97.40	5.88e-01	59.20	72.10	65.65	19.6	87.82	30.70	n/a
S96T001542	A	Barium-ICP-Acid Digest	µg/g	94.00	<5.00e-02	3.79e+02	330.0	354.5	13.8	85.52	30.70	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Decanted Supernate (Liquid Grab Sludge): Decanted Supernate (Liquid Grab Sludge) (Continued)

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T001542	A	Beryllium-ICP-Acid Digest	µg/g	103.6	<5.00e-03	<3.070	<2.95e0	n/a	n/a	91.70	3.070	n/a
S96T001542	A	Bismuth-ICP-AcidDigest	µg/g	89.60	<1.00e-01	<61.40	<5.91e1	n/a	n/a	86.10	61.40	n/a
S96T001542	A	Calcium-ICP-AcidDigest	µg/g	91.20	<1.00e-01	1.17e+03	1.18e+03	1.18e+03	0.85	80.76	61.40	n/a
S96T001542	A	Cadmium-ICP-Acid Digest	µg/g	89.20	<5.00e-03	37.90	33.00	35.45	13.8	86.06	3.070	n/a
S96T001542	A	Cerium-ICP-Acid Digest	µg/g	96.60	<1.00e-01	2.42e+02	233.0	237.5	3.79	91.20	61.40	n/a
S96T001542	A	Cobalt-ICP-Acid Digest	µg/g	91.80	<2.00e-02	12.30	<1.18e1	n/a	n/a	88.10	12.30	n/a
S96T001542	A	Chromium-ICP-Acid Digest	µg/g	90.80	<1.00e-02	7.30e+02	660.0	695.0	10.1	84.36	6.140	n/a
S96T001542	A	Copper-ICP-Acid Digest	µg/g	91.60	1.10e-02	93.70	80.40	87.05	15.3	84.82	6.140	n/a
S96T001542	A	Iron-ICP-Acid Digest	µg/g	91.60	<5.00e-02	8.31e+04	7.15e+04	7.73e+04	15.0	n/a	30.70	n/a
S96T001542	A	Potassium-ICP-Acid Digest	µg/g	94.00	<5.00e-01	9.05e+02	644.0	774.5	33.7	77.82	307.0	n/a
S96T001542	A	Lanthanum-ICP-Acid Digest	µg/g	93.80	<5.00e-02	80.30	72.00	76.15	10.9	88.08	30.70	n/a
S96T001542	A	Lithium-ICP-Acid Digest	µg/g	94.20	<1.00e-02	<6.140	<5.91e0	n/a	n/a	86.90	6.140	n/a
S96T001542	A	Magnesium-ICP-Acid Digest	µg/g	86.00	<1.00e-01	3.21e+02	283.0	302.0	12.6	79.10	61.40	n/a
S96T001542	A	Manganese-ICP-Acid Digest	µg/g	90.20	<1.00e-02	2.28e+03	2.00e+03	2.14e+03	13.1	78.58	6.140	n/a
S96T001542	A	Molybdenum-ICP-Acid Digest	µg/g	90.80	<5.00e-02	<30.70	<2.95e1	n/a	n/a	86.80	30.70	n/a
S96T001542	A	Sodium-ICP-Acid Digest	µg/g	103.2	8.79e-01	1.40e+05	1.29e+05	1.34e+05	8.18	n/a	61.40	n/a
S96T001542	A	Neodymium-ICP-Acid Digest	µg/g	93.40	<1.00e-01	1.92e+02	176.0	184.0	8.70	87.22	61.40	n/a
S96T001542	A	Nickel-ICP-Acid Digest	µg/g	92.00	<2.00e-02	7.70e+02	694.0	732.0	10.4	86.38	12.30	n/a
S96T001542	A	Phosphorus-ICP-Acid Digest	µg/g	94.00	<2.00e-01	2.75e+03	2.50e+03	2.62e+03	9.52	57.92	123.0	n/a
S96T001542	A	Lead-ICP-Acid Digest	µg/g	86.20	<1.00e-01	2.90e+03	2.54e+03	2.72e+03	13.2	74.32	61.40	n/a
S96T001542	A	Sulfur-ICP-Acid Digest	µg/g	89.20	<1.00e-01	1.40e+03	1.14e+03	1.27e+03	20.5	74.82	61.40	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Decanted Supernate (Liquid Grab Sludge): Decanted Supernate (Liquid Grab Sludge)

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T001542	A	Antimony-ICP-Acid Digest	µg/g	93.00	<6.00e-02	<36.90	<3.54e1	n/a	n/a	89.70	36.90	n/a
S96T001542	A	Selenium-ICP-Acid Digest	µg/g	88.00	<1.00e-01	<61.40	<5.91e1	n/a	n/a	84.70	61.40	n/a
S96T001542	A	Silicon-ICP-Acid Digest	µg/g	129.4	8.36e-01	3.81e+04	2.19e+04	3.00e+04	54.0	n/a	30.70	n/a
S96T001542	A	Samarium-ICP-Acid Digest	µg/g	91.80	<1.00e-01	<61.40	<5.91e1	n/a	n/a	87.90	61.40	n/a
S96T001542	A	Strontium-ICP-Acid Digest	µg/g	92.20	<1.00e-02	25.60	22.90	24.25	11.1	86.16	6.140	n/a
S96T001542	A	Titanium-ICP-Acid Digest	µg/g	86.00	<1.00e-02	1.39e+02	122.0	130.5	13.0	80.10	6.140	n/a
S96T001542	A	Thallium-ICP-Acid Digest	µg/g	86.60	<2.00e-01	<1.23e+02	<1.18e2	n/a	n/a	82.10	123.0	n/a
S96T001542	A	Uranium-ICP-AcidDigest	µg/g	90.50	<5.00e-01	8.56e+02	1.14e+03	998.0	28.5	80.09	307.0	n/a
S96T001542	A	Vanadium-ICP-Acid Digest	µg/g	90.60	<5.00e-02	<30.70	<2.95e1	n/a	n/a	86.50	30.70	n/a
S96T001542	A	Zinc-ICP-Acid Digest	µg/g	87.00	1.20e-02	60.60	49.80	55.20	19.6	84.44	6.140	n/a
S96T001542	A	Zirconium-ICP-Acid Digest	µg/g	98.80	<1.00e-02	9.42e+02	1.38e+03	1.16e+03	37.7	76.00	6.140	n/a
S96T001543	W	Fluoride-IC-Dionex 4000i/4500	µg/g	100.7	<1.30e-02	1.98e+04	<1.09e4	n/a	n/a	89.32	1.09e+04	n/a
S96T001543	W	Chloride-IC-Dionex 4000i/4500	µg/g	92.41	<1.70e-02	2.89e+05	<1.42e4	n/a	n/a	99.37	1.42e+04	n/a
S96T001543	W	Nitrite-IC-Dionex 4000i/4500	µg/g	93.43	<1.07e-01	<8.96e+04	<8.96e4	n/a	n/a	94.71	8.96e+04	n/a
S96T001543	W	Nitrate by IC-Dionex 4000i/4500	µg/g	93.48	<1.40e-01	2.90e+07	2.76e+07	2.83e+07	4.95	88.76	1.17e+05	n/a
S96T001543	W	Phosphate-IC-Dionex 4000i/4500	µg/g	95.24	<1.19e-01	<9.96e+04	<9.96e4	n/a	n/a	98.17	9.96e+04	n/a
S96T001543	W	Sulfate by IC-Dionex 4000i/4500	µg/g	96.20	<1.36e-01	1.38e+05	<1.14e5	n/a	n/a	95.88	1.14e+05	n/a
S96T001543	W	Oxalate by IC-Dionex 4000i	µg/g	97.09	<1.05e-01	5.36e+04	5.21e+04	5.29e+04	2.84	99.03	4.50e+04	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Interstitial Liquid: Interstitial Liquid

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T001544		DSC Exotherm Dry Calculated	Joules/g Dry	n/a	n/a	0.00e+00	0.00e+00	0.00e+00	0.00	n/a	n/a	n/a
S96T001544		DSC Exotherm on Perkin Elmer	Joules/g	99.12	n/a	0.00e+00	0.00e+00	0.00e+00	0.00	n/a	n/a	n/a
S96T001544		pH Direct	pH	n/a	n/a	10.10	n/a	n/a	n/a	n/a	1.00e-02	n/a
S96T001544		% Water by TGA using Mettler	%	100.1	n/a	58.94	57.09	58.02	3.19	n/a	n/a	n/a
S96T001544		Tot. Organic Carbon by Coul.	µg/mL	100.0	1.00e-01	2.32e+03	2.31e+03	2.32e+03	0.43	95.10	55.00	n/a
S96T001544		TOC by Persulfate/ Coulometry	µg/mL	92.36	1.600	1.87e+03	1.50e+03	1.68e+03	22.0	n/a	40.00	n/a
S96T001544		Strontium-89/90 High Level	µCi/mL	97.56	1.20e-02	8.40e-01	7.82e-01	8.11e-01	7.15	n/a	1.70e-02	5.37E+00
S96T001544		Pu-239/240 by TRU-SPEC Resin	µCi/mL	99.47	<2.61e-02	8.67e-01	8.39e-01	8.53e-01	3.28	n/a	6.50e-02	2.18E+00
S96T001544	D	Silver-ICP-Acid Dil.	µg/mL	97.80	<1.00e-02	<4.010	<4.01e0	n/a	n/a	90.30	4.010	n/a
S96T001544	D	Aluminum-ICP-Acid Dil.	µg/mL	100.0	<5.00e-02	<20.10	<2.01e1	n/a	n/a	95.30	20.10	n/a
S96T001544	D	Arsenic-ICP-Acid Dil.	µg/mL	103.0	<1.00e-01	<40.10	<4.01e1	n/a	n/a	104.2	40.10	n/a
S96T001544	D	Boron-ICP-Acid Dil.	µg/mL	103.2	<5.00e-02	<20.10	<2.01e1	n/a	n/a	100.3	20.10	n/a
S96T001544	D	Barium-ICP-Acid Dil.	µg/mL	104.0	<5.00e-02	<20.10	<2.01e1	n/a	n/a	102.0	20.10	n/a
S96T001544	D	Beryllium-ICP-Acid Dil.	µg/mL	105.6	<5.00e-03	<2.000	<2.00e0	n/a	n/a	102.0	2.000	n/a
S96T001544	D	Bismuth-ICP-Acid Dil.	µg/mL	101.4	<1.00e-01	<40.10	<4.01e1	n/a	n/a	89.00	40.10	n/a
S96T001544	D	Calcium-ICP-Acid Dil.	µg/mL	103.2	<1.00e-01	<40.10	<4.01e1	n/a	n/a	107.5	40.10	n/a
S96T001544	D	Cadmium-ICP-Acid Dil.	µg/mL	99.60	<5.00e-03	<2.000	<2.00e0	n/a	n/a	94.00	2.000	n/a
S96T001544	D	Cerium-ICP-Acid Dil.	µg/mL	105.0	<1.00e-01	<40.10	<4.01e1	n/a	n/a	102.0	40.10	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Interstitial Liquid: Interstitial Liquid (Continued)

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T001544	D	Cobalt-ICP-Acid Dil.	µg/mL	100.0	<2.00e-02	<8.020	<8.02e0	n/a	n/a	93.30	8.020	n/a
S96T001544	D	Chromium-ICP-Acid Dil.	µg/mL	98.80	<1.00e-02	<4.010	<4.01e0	n/a	n/a	93.50	4.010	n/a
S96T001544	D	Copper-ICP-Acid Dil.	µg/mL	105.0	<1.00e-02	<4.010	<4.01e0	n/a	n/a	102.3	4.010	n/a
S96T001544	D	Iron-ICP-Acid Dil.	µg/mL	102.0	<5.00e-02	<20.10	<2.01e1	n/a	n/a	103.3	20.10	n/a
S96T001544	D	Potassium-ICP-Acid Dil.	µg/mL	101.4	<5.00e-01	5.92e+02	566.0	579.0	4.49	89.90	200.0	n/a
S96T001544	D	Lanthanum-ICP-Acid Dil.	µg/mL	102.6	<5.00e-02	<20.10	<2.01e1	n/a	n/a	100.5	20.10	n/a
S96T001544	D	Manganese-ICP-Acid Dil.	µg/mL	99.40	<1.00e-02	<4.010	<4.01e0	n/a	n/a	95.80	4.010	n/a
S96T001544	D	Molybdenum-ICP-Acid Dil.	µg/mL	100.2	<5.00e-02	22.30	21.60	21.95	3.19	94.00	20.10	n/a
S96T001544	D	Sodium-ICP-Acid Dil.	µg/mL	105.0	<1.00e-01	1.10e+05	1.10e+05	1.10e+05	0.00	130.9	40.10	n/a
S96T001544	D	Neodymium-ICP-Acid Dil.	µg/mL	108.4	<1.00e-01	<40.10	<4.01e1	n/a	n/a	112.5	40.10	n/a
S96T001544	D	Nickel-ICP-Acid Dil.	µg/mL	99.40	<2.00e-02	14.80	15.60	15.20	5.26	93.30	8.020	n/a
S96T001544	D	Phosphorus-ICP-Acid Dil.	µg/mL	102.0	<2.00e-01	3.52e+02	372.0	362.0	5.52	102.0	80.20	n/a
S96T001544	D	Lead-ICP-Acid Dil.	µg/mL	99.40	<1.00e-01	<40.10	<4.01e1	n/a	n/a	96.50	40.10	n/a
S96T001544	D	Sulfur-ICP-Acid Dil.	µg/mL	99.40	<1.00e-01	2.37e+03	2.28e+03	2.32e+03	3.87	70.50	40.10	n/a
S96T001544	D	Antimony-ICP-Acid Dil.	µg/mL	96.80	<6.00e-02	<24.10	<2.41e1	n/a	n/a	91.80	24.10	n/a
S96T001544	D	Selenium-ICP-Acid Dil.	µg/mL	106.0	<1.00e-01	<40.10	<4.01e1	n/a	n/a	113.7	40.10	n/a
S96T001544	D	Silicon-ICP-Acid Dil.	µg/mL	95.60	<5.00e-02	<20.10	<2.01e1	n/a	n/a	94.00	20.10	n/a
S96T001544	D	Samarium-ICP-Acid Dil.	µg/mL	105.8	<1.00e-01	<40.10	<4.01e1	n/a	n/a	107.5	40.10	n/a
S96T001544	D	Strontium-ICP-Acid Dil.	µg/mL	103.4	<1.00e-02	<4.010	<4.01e0	n/a	n/a	101.3	4.010	n/a
S96T001544	D	Titanium-ICP-Acid Dil.	µg/mL	99.00	<1.00e-02	<4.010	<4.01e0	n/a	n/a	95.50	4.010	n/a
S96T001544	D	Thallium-ICP-Acid Dil.	µg/mL	97.20	<2.00e-01	<80.20	<8.02e1	n/a	n/a	89.80	80.20	n/a
S96T001544	D	Uranium-ICP-Acid Dil.	µg/mL	100.0	<5.00e-01	1.54e+03	1.64e+03	1.59e+03	6.29	108.4	200.0	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
Interstitial Liquid: Interstitial Liquid (Continued)												
S96T001544	D	Vanadium-ICP-Acid Dil.	µg/mL	102.0	<5.00e-02	<20.10	<2.01e1	n/a	n/a	97.50	20.10	n/a
S96T001544	D	Zinc-ICP-Acid Dil.	µg/mL	100.0	<1.00e-02	5.250	5.980	5.615	13.0	92.70	4.010	n/a
S96T001544	D	Zirconium-ICP-Acid Dil.	µg/mL	101.4	<1.00e-02	3.72e+02	378.0	375.0	1.60	101.1	4.010	n/a
S96T001544		Fluoride-IC-Dionex 4000i/4500	µg/mL	98.81	<1.30e-02	1.97e+02	199.0	198.2	1.01	n/a	14.44	n/a
S96T001544		Chloride-IC-Dionex 4000i/4500	µg/mL	93.17	<1.70e-02	5.84e+02	588.0	586.1	0.68	n/a	18.89	n/a
S96T001544		Nitrite-IC-Dionex 4000i/4500	µg/mL	98.61	<1.07e-01	2.59e+04	2.62e+04	2.60e+04	1.15	n/a	118.9	n/a
S96T001544		Nitrate-IC-Dionex4000i/4500	µg/mL	99.67	2.38e-01	9.43e+02	954.0	948.5	1.16	n/a	155.5	n/a
S96T001544		Phosphate-IC-Dionex 4000i/4500	µg/mL	100.7	<1.19e-01	5.85e+02	547.0	565.9	6.71	n/a	132.1	n/a
S96T001544		Sulfate by IC-Dionex 4000i/4500	µg/mL	99.53	<1.36e-01	6.83e+03	6.86e+03	6.85e+03	0.44	n/a	151.0	n/a
S96T001544		Oxalate by IC-Dionex 4000i	µg/mL	100.2	<1.05e-01	2.19e+03	2.23e+03	2.21e+03	1.81	n/a	116.7	n/a
S96T001544		Cobalt-60 by GEA	µCi/mL	98.94	<2.16e-02	<3.38e-02	<2.27e-2	n/a	n/a	n/a	3.40e-02	n/a
S96T001544		Cesium-137 by GEA	µCi/mL	100.4	<6.06e-02	1.59e+02	157.0	158.0	1.27	n/a	n/a	0.550
Potential Organic Layer: Potential Organic Layer												
S96T001545		Pu-239/240 by TRU-SPEC Resin	µCi/mL	96.33	<3.03e-05	4.26e-03	4.21e-03	4.24e-03	1.18	n/a	3.06e-04	2.23E+00
Sludge (from Liquid Grab Sample): Sludge (from Liquid Grab Sample)												
S96T003179	W	Fluoride-IC-Dionex 4000i/4500	µg/g	106.4	<1.30e-02	4.95e+02	142.0	318.3	111	n/a	56.77	n/a
S96T003179	W	Chloride-IC-Dionex 4000i/4500	µg/g	98.23	<1.70e-02	6.36e+02	261.0	448.7	83.6	n/a	74.24	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Sludge (from Liquid Grab Sample): Sludge (from Liquid Grab Sample) (Continued)

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T003179	W	Nitrite-IC-Dionex 4000i/4500	µg/g	93.91	<1.07e-01	1.19e+04	1.23e+04	1.21e+04	3.31	n/a	467.3	n/a
S96T003179	W	Nitrate by IC-Dionex 4000i/4500	µg/g	104.1	5.770	3.08e+03	4.31e+03	3.69e+03	33.3	n/a	610.9	n/a
S96T003179	W	Phosphate-IC-Dionex 4000i/4500	µg/g	103.1	<1.19e-01	1.60e+03	1.98e+03	1.79e+03	21.2	n/a	519.2	n/a
S96T003179	W	Sulfate by IC-Dionex 4000i/4500	µg/g	106.5	<1.36e-01	4.06e+03	3.85e+03	3.96e+03	5.31	n/a	593.5	n/a
S96T003179	W	Oxalate by IC-Dionex 4000i	µg/g	107.5	<1.05e-01	1.17e+05	4.30e+04	8.02e+04	92.5	n/a	458.5	n/a

RISER: 1

SEGMENT #: 6C-96-5

SEGMENT PORTION: Supernate

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T000538		DSC Exotherm using Mettler	Joules/g	96.66	n/a	0.00e+00	0.00e+00	0.00e+00	0.00	n/a	n/a	n/a
S96T000538		DSC Exotherm Dry Calculated	Joules/g Dry	n/a	n/a	0.00e+00	0.00e+00	0.00e+00	0.00	n/a	n/a	n/a
S96T000538		Ammonia by ISE-Std Additions	µg/mL	96.84	3.100	<5.000	<5	n/a	n/a	n/a	5.000	n/a
S96T000538		pH Direct	pH	n/a	n/a	10.10	10.08	10.09	6.94	n/a	1.00e-02	n/a
S96T000538		Specific Gravity	Sp.G.	98.88	n/a	1.155	1.155	1.155	0.00	n/a	1.00e-02	n/a
S96T000538		% Water by TGA using Mettler	%	103.0	n/a	80.91	80.84	80.88	0.09	n/a	n/a	n/a
S96T000538		Tot. Inorg. Carbon by Coul.	µg/mL	103.0	<5.000	2.00e+04	2.02e+04	2.01e+04	1.00	81.90	105.0	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

SEGMENT PORTION: Supernate (Continued)												
Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T000538		Tot. Organic Carbon by Coul.	µg/mL	97.03	<5.000	3.36e+03	3.24e+03	3.30e+03	3.64	95.40	55.00	n/a
S96T000538		TOC by Persulfate/ Coulometry	µg/mL	96.70	9.900	2.30e+03	2.18e+03	2.24e+03	5.36	n/a	40.00	n/a
S96T000538		% Water by Gravimetric	%	102.0	n/a	81.40	81.40	81.40	0.00	n/a	1.00e-02	n/a
S96T000538	D	Silver-ICP-Acid Dil.	µg/mL	100.8	<1.00e-02	11.20	9.690	10.45	14.5	80.10	4.010	n/a
S96T000538	D	Aluminum-ICP-Acid Dil.	µg/mL	98.40	<5.00e-02	<20.00	<2.00e1	n/a	n/a	97.40	20.10	n/a
S96T000538	D	Arsenic-ICP-Acid Dil.	µg/mL	103.8	<1.00e-01	<40.10	<4.01e1	n/a	n/a	100.8	40.10	n/a
S96T000538	D	Boron-ICP-Acid Dil.	µg/mL	100.4	<5.00e-02	<20.00	<2.00e1	n/a	n/a	101.6	20.10	n/a
S96T000538	D	Barium-ICP-Acid Dil.	µg/mL	102.6	<5.00e-02	<20.00	<2.00e1	n/a	n/a	98.60	20.10	n/a
S96T000538	D	Beryllium-ICP-Acid Dil.	µg/mL	104.0	<5.00e-03	<2.000	<2.00e0	n/a	n/a	101.6	2.000	n/a
S96T000538	D	Bismuth-ICP-Acid Dil.	µg/mL	101.8	<1.00e-01	<40.10	<4.01e1	n/a	n/a	100.8	40.10	n/a
S96T000538	D	Calcium-ICP-Acid Dil.	µg/mL	104.2	<1.00e-01	<40.10	<4.01e1	n/a	n/a	105.3	40.10	n/a
S96T000538	D	Cadmium-ICP-Acid Dil.	µg/mL	102.8	<5.00e-03	<2.000	<2.00e0	n/a	n/a	101.8	2.000	n/a
S96T000538	D	Cerium-ICP-Acid Dil.	µg/mL	105.6	<1.00e-01	<40.10	<4.01e1	n/a	n/a	105.1	40.10	n/a
S96T000538	D	Cobalt-ICP-Acid Dil.	µg/mL	103.4	<2.00e-02	<8.020	<8.02e0	n/a	n/a	101.8	8.020	n/a
S96T000538	D	Chromium-ICP-Acid Dil.	µg/mL	104.0	<1.00e-02	<4.010	<4.01e0	n/a	n/a	102.8	4.010	n/a
S96T000538	D	Copper-ICP-Acid Dil.	µg/mL	104.2	<1.00e-02	<4.010	<4.01e0	n/a	n/a	99.60	4.010	n/a
S96T000538	D	Iron-ICP-Acid Dil.	µg/mL	103.2	<5.00e-02	<20.00	<2.00e1	n/a	n/a	102.3	20.10	n/a
S96T000538	D	Potassium-ICP-Acid Dil.	µg/mL	103.4	<5.00e-01	8.01e+02	658.0	729.5	19.6	67.30	200.0	n/a
S96T000538	D	Lanthanum-ICP-Acid Dil.	µg/mL	103.6	<5.00e-02	<20.00	<2.00e1	n/a	n/a	101.1	20.10	n/a
S96T000538	D	Lithium-ICP-Acid Dil.	µg/mL	99.60	<1.00e-02	<4.010	<4.01e0	n/a	n/a	97.90	4.010	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

SEGMENT PORTION: Supernate (Continued)

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T000538	D	Magnesium-ICP-Acid Dil.	µg/mL	97.60	<1.00e-01	<40.10	<4.01e1	n/a	n/a	94.60	40.10	n/a
S96T000538	D	Manganese-ICP-Acid Dil.	µg/mL	100.6	<1.00e-02	<4.010	<4.01e0	n/a	n/a	98.10	4.010	n/a
S96T000538	D	Molybdenum-ICP-Acid Dil.	µg/mL	103.8	<5.00e-02	29.30	25.00	27.15	15.8	101.5	20.10	n/a
S96T000538	D	Sodium-ICP-Acid Dil.	µg/mL	98.20	<1.00e-01	1.07e+05	9.68e+04	1.02e+05	10.0	n/a	40.10	n/a
S96T000538	D	Neodymium-ICP-Acid Dil.	µg/mL	105.2	<1.00e-01	<40.10	<4.01e1	n/a	n/a	103.3	40.10	n/a
S96T000538	D	Nickel-ICP-Acid Dil.	µg/mL	101.6	<2.00e-02	18.40	15.70	17.05	15.8	100.0	8.020	n/a
S96T000538	D	Phosphorus-ICP-Acid Dil.	µg/mL	102.2	<2.00e-01	3.24e+02	300.0	312.0	7.69	90.20	80.20	n/a
S96T000538	D	Lead-ICP-Acid Dil.	µg/mL	102.0	<1.00e-01	<40.10	<4.01e1	n/a	n/a	105.1	40.10	n/a
S96T000538	D	Sulfur-ICP-Acid Dil.	µg/mL	98.80	<1.00e-01	3.06e+03	2.71e+03	2.88e+03	12.1	n/a	40.10	n/a
S96T000538	D	Antimony-ICP-Acid Dil.	µg/mL	96.20	<6.00e-02	<24.10	<2.41e1	n/a	n/a	98.10	24.10	n/a
S96T000538	D	Selenium-ICP-Acid Dil.	µg/mL	98.40	<1.00e-01	<40.10	<4.01e1	n/a	n/a	101.6	40.10	n/a
S96T000538	D	Silicon-ICP-Acid Dil.	µg/mL	99.00	<5.00e-02	26.20	23.00	24.60	13.0	98.30	20.10	n/a
S96T000538	D	Samarium-ICP-Acid Dil.	µg/mL	100.4	<1.00e-01	<40.10	<4.01e1	n/a	n/a	98.60	40.10	n/a
S96T000538	D	Strontium-ICP-Acid Dil.	µg/mL	101.8	<1.00e-02	<4.010	<4.01e0	n/a	n/a	99.10	4.010	n/a
S96T000538	D	Titanium-ICP-Acid Dil.	µg/mL	100.4	<1.00e-02	<4.010	<4.01e0	n/a	n/a	98.60	4.010	n/a
S96T000538	D	Thallium-ICP-Acid Dil.	µg/mL	99.00	<2.00e-01	<80.20	<8.02e1	n/a	n/a	97.60	80.20	n/a
S96T000538	D	Uranium-ICP-Acid Dil.	µg/mL	99.20	<5.00e-01	1.87e+03	1.77e+03	1.82e+03	5.49	56.65	200.0	n/a
S96T000538	D	Vanadium-ICP-Acid Dil.	µg/mL	103.4	<5.00e-02	<20.00	<2.00e1	n/a	n/a	102.3	20.10	n/a
S96T000538	D	Zinc-ICP-Acid Dil.	µg/mL	101.6	<1.00e-02	5.090	4.050	4.570	22.8	101.8	4.010	n/a
S96T000538	D	Zirconium-ICP-Acid Dil.	µg/mL	102.0	<1.00e-02	4.45e+02	404.0	424.5	9.66	82.70	4.010	n/a
S96T000538		Fluoride-IC-Dionex 4000i/4500	µg/mL	100.7	<1.30e-02	3.17e+02	347.0	332.0	9.04	96.61	132.6	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

SEGMENT PORTION: Supernate (Continued)												
Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T000538		Chloride-IC-Dionex 4000i/4500	µg/mL	102.5	5.00e-02	2.48e+02	428.0	337.9	53.3	102.0	173.4	n/a
S96T000538		Nitrite-IC-Dionex 4000i/4500	µg/mL	103.5	<1.07e-01	2.91e+04	2.87e+04	2.89e+04	1.38	106.3	1.09e+03	n/a
S96T000538		Nitrate-IC-Dionex4000i/4500	µg/mL	102.1	<1.40e-01	2.04e+03	1.58e+03	1.81e+03	25.4	103.1	1.43e+03	n/a
S96T000538		Phosphate-IC-Dionex 4000i/4500	µg/mL	103.1	<1.19e-01	<1.21e+03	<1.21e3	n/a	n/a	103.7	1.21e+03	n/a
S96T000538		Sulfate by IC-Dionex 4000i/4500	µg/mL	99.53	<1.36e-01	7.46e+03	7.86e+03	7.66e+03	5.22	101.0	1.39e+03	n/a
S96T000538		Oxalate by IC Dionex 4000i	µg/mL	105.3	<1.05e-01	3.65e+03	3.70e+03	3.68e+03	1.36	108.4	1.07e+03	n/a
S96T000539		Technetium-99 Liq. Scint.	µCi/mL	101.8	<3.54e-03	8.52e-02	9.23e-02	8.87e-02	8.00	n/a	4.00e-03	3.03E+00
S96T000539		Strontium-89/90 High Level	µCi/mL	95.12	8.00e-03	3.69e-01	3.62e-01	3.65e-01	1.92	n/a	2.00e-03	3.46E+00
S96T000539		Pu-239/240 by TRU-SPEC Resin	µCi/mL	88.28	<3.12e-03	7.40e-01	6.92e-01	7.16e-01	6.70	n/a	3.10e-02	1.65E+00
S96T000539		Cobalt-60 by GEA	µCi/mL	99.23	<1.99e-05	<5.71e-03	<6.13e-3	n/a	n/a	n/a	6.00e-03	n/a
S96T000539		Cesium-137 by GEA	µCi/mL	101.5	<5.81e-05	1.08e+02	107.0	107.5	0.93	n/a	n/a	0.210
S96T000539		Am-241 by Extraction	µCi/mL	80.13	<1.15e-02	1.50e-02	1.21e-02	1.35e-02	21.4	n/a	1.20e-02	4.65E+00
S96T000539		Alpha in Liquid Samples	µCi/mL	102.6	<3.84e-03	1.150	1.140	1.145	0.87	108.9	1.00e-02	5.03E+00

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

RISER: 1

SEGMENT #: 6C-96-7

SEGMENT PORTION: Centrifuged Solids (Grab Sample)

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T000542		Bulk Density of Sample	g/mL	n/a	n/a	1.710	n/a	n/a	n/a	n/a	5.00e-01	n/a
S96T000542		DSC Exotherm using Mettler	Joules/g	113.5	n/a	1.12e+02	89.10	100.5	22.8	n/a	n/a	n/a
S96T000542		DSC Exotherm Dry Calculated	Joules/g Dry	n/a	n/a	1.22e+02	97.14	109.6	22.8	n/a	n/a	n/a
S96T000542		% Water by TGA on Perkin Elmer	%	98.68	n/a	8.040	8.510	8.275	5.68	n/a	n/a	n/a
S96T000542		Volume % Solids	%	n/a	n/a	69.50	n/a	n/a	n/a	n/a	n/a	n/a
S96T000542		% Water by Gravimetric	%	98.14	n/a	9.800	10.00	9.900	0.22	n/a	1.00e-02	n/a
Control Sample: Control Sample												
S96T000543		DSC Exotherm Dry Calculated	Joules/g Dry	n/a	n/a	0.00e+00	0.00e+00	0.00e+00	0.00	n/a	n/a	n/a
S96T000543		DSC Exotherm on Perkin Elmer	Joules/g	95.82	n/a	0.00e+00	0.00e+00	0.00e+00	0.00	n/a	n/a	n/a
S96T000543		% Water by TGA on Perkin Elmer	%	99.41	n/a	29.76	32.47	31.12	8.71	n/a	n/a	n/a
S96T000546	F	Technetium-99 Liq. Scint.	µCi/g	99.47	<3.58e-02	5.51e-02	4.48e-02	5.00e-02	20.6	n/a	3.50e-02	5.81E+00
S96T000546	F	Strontium-89/90 High Level	µCi/g	92.68	6.20e-02	3.32e+02	342.0	337.0	2.97	n/a	5.30e-02	5.19E-01
S96T000546	F	Pu-239/240 by TRU-SPEC Resin	µCi/g	92.13	<3.43e-02	1.520	1.390	1.455	8.93	n/a	1.13e-01	2.03E+00
S96T000546	F	Cobalt-60 by GEA	µCi/g	96.66	<1.52e-01	<2.33e-01	<2.27e-1	n/a	n/a	n/a	2.33e-01	n/a
S96T000546	F	Cesium-137 by GEA	µCi/g	96.08	<2.04e-01	4.03e+02	417.0	409.9	3.41	n/a	n/a	0.580
S96T000546	F	Am-241 by Extraction	µCi/g	106.1	<2.54e-02	1.010	1.230	1.120	19.6	n/a	8.10e-02	3.4

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
Control Sample: Control Sample (Continued)												
S96T000546	F	Alpha of Digested Solid	µCi/g	118.0	<5.57e-02	2.880	2.570	2.725	11.4	106.4	7.20e-02	1.03E+01
Decanted Supernate (Liquid Grab Sludge): Decanted Supernate (Liquid Grab Sludge)												
S96T000544		pH Direct	pH	n/a	n/a	10.09	n/a	n/a	n/a	n/a	1.00e-02	n/a
S96T000544		Specific Gravity	Sp.G.	101.1	n/a	1.200	1.194	1.197	0.50	n/a	1.00e-03	n/a
S96T000544		Tot. Organic Carbon by Coul.	µg/mL	100.0	1.00e-01	2.07e+03	2.02e+03	2.04e+03	2.44	100.0	55.00	n/a
S96T000544		% Water by Gravimetric	%	98.65	n/a	78.80	78.80	78.80	0.00	n/a	1.00e-02	n/a
S96T000544		Strontium-89/90 High Level	µCi/mL	101.6	<2.06e-03	9.68e-01	8.93e-01	9.30e-01	8.06	n/a	4.00e-03	2.08E+00
S96T000544		Pu-239/240 by TRU-SPEC Resin	µCi/mL	92.39	<3.82e-03	7.69e-01	7.56e-01	7.62e-01	1.70	n/a	3.60e-02	1.96E+00
Filtered Centrifuged Solids: Filtered Centrifuged Solids												
S96T000551		DSC Exotherm using Mettler	Joules/g	113.5	n/a	2.87e+02	279.9	283.4	2.47	n/a	n/a	n/a
S96T000551		DSC Exotherm Dry Calculated	Joules/g Dry	n/a	n/a	3.29e+02	320.9	324.9	2.46	n/a	n/a	n/a
S96T000551		% Water by TGA using Mettler	%	102.2	n/a	9.440	16.11	12.77	52.2	n/a	n/a	n/a
S96T000552		TIC by Acid/Coulometry	µg/g	97.84	8.00e-01	2.56e+04	2.76e+04	2.66e+04	7.52	n/a	5.000	n/a
S96T000552		TOC by Persulfate/ Coulometry	µg/g	92.03	3.100	2.47e+04	2.92e+04	2.70e+04	16.7	n/a	40.00	n/a
S96T000553		% Water by Gravimetric	%	98.14	n/a	18.90	19.20	19.05	0.38	n/a	1.00e-02	n/a
S96T000554		pH on SST Samples	pH	n/a	n/a	10.40	10.50	10.45	0.96	n/a	1.00e-02	n/a
S96T000555	F	Technetium-99 Liq. Scint.	µCi/g	99.47	<3.58e-02	4.09e-02	<3.53E-2	n/a	n/a	n/a	3.70e-02	6.26E+00
S96T000555	F	Strontium-89/90 High Level	µCi/g	92.68	6.20e-02	5.19e+02	523.0	521.0	0.77	n/a	1.14e-01	6.08E-01

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Filtered Centrifuged Solids: Filtered Centrifuged Solids (Continued)

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T000555	F	Pu-239/240 by TRU-SPEC Resin	µCi/g	98.69	<3.56e-02	1.320	1.280	1.300	3.08	n/a	8.90e-02	2.09E+00
S96T000555	F	Cobalt-60 by GEA	µCi/g	98.05	<4.73e-01	0.00e+00	<5.71e-1	n/a	n/a	n/a	n/a	n/a
S96T000555	F	Cesium-137 by GEA	µCi/g	98.56	<9.17e-01	5.96e+02	622.0	609.0	4.27	n/a	n/a	17.0
S96T000555	F	Am-241 by Extraction	µCi/g	106.1	<2.54e-02	1.330	1.220	1.275	8.63	n/a	9.60e-02	2.8
S96T000555	F	Alpha of Digested Solid	µCi/g	118.0	<5.57e-02	3.330	3.060	3.195	8.45	109.7	7.70e-02	9.94E+00
S96T000556	A	Silver-ICP-Acid Digest	µg/g	91.90	<1.00e-02	2.77e+03	2.02e+03	2.40e+03	31.3	n/a	11.00	n/a
S96T000556	A	Aluminum-ICP-Acid Digest	µg/g	96.60	1.18e-01	5.17e+04	4.42e+04	4.80e+04	15.6	1.38e+03	54.80	n/a
S96T000556	A	Arsenic-ICP-Acid Digest	µg/g	97.20	<1.00e-01	<1.10e+02	<9.43e1	n/a	n/a	95.60	110.0	n/a
S96T000556	A	Boron-ICP-Acid Digest	µg/g	108.8	5.40e-01	<54.80	<4.72e1	n/a	n/a	99.40	54.80	n/a
S96T000556	A	Barium-ICP-Acid Digest	µg/g	97.60	<5.00e-02	3.04e+02	260.0	282.0	15.6	102.2	54.80	n/a
S96T000556	A	Beryllium-ICP-Acid Digest	µg/g	103.0	<5.00e-03	<5.480	<4.72e0	n/a	n/a	98.40	5.480	n/a
S96T000556	A	Bismuth-ICP-AcidDigest	µg/g	92.40	<1.00e-01	<1.10e+02	<9.43e1	n/a	n/a	89.80	110.0	n/a
S96T000556	A	Calcium-ICP-AcidDigest	µg/g	100.2	4.59e-01	1.33e+03	1.12e+03	1.22e+03	17.1	91.02	110.0	n/a
S96T000556	A	Cadmium-ICP-Acid Digest	µg/g	94.60	<5.00e-03	33.30	27.10	30.20	20.5	94.16	5.480	n/a
S96T000556	A	Cerium-ICP-Acid Digest	µg/g	100.0	<1.00e-01	1.78e+02	174.0	176.0	2.27	106.1	110.0	n/a
S96T000556	A	Cobalt-ICP-Acid Digest	µg/g	98.40	<2.00e-02	<21.90	<1.89e1	n/a	n/a	97.20	21.90	n/a
S96T000556	A	Chromium-ICP-Acid Digest	µg/g	97.00	1.70e-02	6.45e+02	552.0	598.5	15.5	107.3	11.00	n/a
S96T000556	A	Copper-ICP-Acid Digest	µg/g	92.80	2.60e-02	89.70	76.70	83.20	15.6	94.02	11.00	n/a
S96T000556	A	Iron-ICP-Acid Digest	µg/g	97.60	7.00e-02	6.87e+04	5.86e+04	6.36e+04	15.9	1.65e+03	54.80	n/a
S96T000556	A	Potassium-ICP-Acid Digest	µg/g	98.80	<5.00e-01	6.43e+02	588.0	615.5	8.94	118.1	548.0	n/a
S96T000555	F	Strontium-89/90 High Level	µCi/g	92.68	6.20e-02	5.19e+02	523.0	521.0	0.77	n/a	1.14e-01	6.08E-01

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Filtered Centrifuged Solids: Filtered Centrifuged Solids (Continued)

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T000556	A	Lithium-ICP-Acid Digest	µg/g	95.80	<1.00e-02	<11.00	<9.43e0	n/a	n/a	93.80	11.00	n/a
S96T000556	A	Magnesium-ICP-Acid Digest	µg/g	94.60	<1.00e-01	2.19e+02	187.0	203.0	15.8	95.58	110.0	n/a
S96T000556	A	Manganese-ICP-Acid Digest	µg/g	96.60	<1.00e-02	1.86e+03	1.59e+03	1.72e+03	15.7	136.5	11.00	n/a
S96T000556	A	Molybdenum-ICP-Acid Digest	µg/g	97.60	<5.00e-02	<54.80	<4.72e1	n/a	n/a	96.00	54.80	n/a
S96T000556	A	Sodium-ICP-Acid Digest	µg/g	109.0	7.70e-01	1.61e+05	1.37e+05	1.49e+05	16.1	1.69e+03	110.0	n/a
S96T000556	A	Neodymium-ICP-Acid Digest	µg/g	98.00	<1.00e-01	1.39e+02	127.0	133.0	9.02	102.7	110.0	n/a
S96T000556	A	Nickel-ICP-Acid Digest	µg/g	97.20	<2.00e-02	6.45e+02	550.0	597.5	15.9	109.8	21.90	n/a
S96T000556	A	Phosphorus-ICP-Acid Digest	µg/g	99.80	<2.00e-01	2.58e+03	2.20e+03	2.39e+03	15.9	148.5	219.0	n/a
S96T000556	A	Lead-ICP-Acid Digest	µg/g	91.60	<1.00e-01	2.49e+03	2.15e+03	2.32e+03	14.7	148.3	110.0	n/a
S96T000556	A	Sulfur-ICP-Acid Digest	µg/g	95.60	<1.00e-01	1.39e+03	1.19e+03	1.29e+03	15.5	121.2	110.0	n/a
S96T000556	A	Antimony-ICP-Acid Digest	µg/g	96.60	<6.00e-02	<65.70	<5.66e1	n/a	n/a	97.80	65.70	n/a
S96T000556	A	Selenium-ICP-Acid Digest	µg/g	97.80	<1.00e-01	<1.10e+02	<9.43e1	n/a	n/a	100.0	110.0	n/a
S96T000556	A	Silicon-ICP-Acid Digest	µg/g	135.2	2.27e-01	2.87e+04	2.47e+04	2.67e+04	15.0	736.3	54.80	n/a
S96T000556	A	Samarium-ICP-Acid Digest	µg/g	99.80	<1.00e-01	<1.10e+02	<9.43e1	n/a	n/a	101.4	110.0	n/a
S96T000556	A	Strontium-ICP-Acid Digest	µg/g	97.00	<1.00e-02	21.10	17.90	19.50	16.4	95.68	11.00	n/a
S96T000556	A	Titanium-ICP-Acid Digest	µg/g	91.60	<1.00e-02	1.20e+02	102.0	111.0	16.2	92.06	11.00	n/a
S96T000556	A	Thallium-ICP-Acid Digest	µg/g	88.60	<2.00e-01	<2.19e+02	<1.89e2	n/a	n/a	88.60	219.0	n/a
S96T000556	A	Uranium-ICP-AcidDigest	µg/g	94.40	<5.00e-01	8.30e+02	686.0	758.0	19.0	94.13	548.0	n/a
S96T000556	A	Vanadium-ICP-Acid Digest	µg/g	96.40	<5.00e-02	<54.80	<4.72e1	n/a	n/a	95.80	54.80	n/a
S96T000556	A	Zinc-ICP-Acid Digest	µg/g	92.60	2.50e-02	39.60	35.20	37.40	11.8	93.38	11.00	n/a
S96T000556	A	Zirconium-ICP-Acid Digest	µg/g	104.2	<1.00e-02	49.30	39.40	44.35	22.3	151.7	11.00	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
Filtered Centrifuged Solids: Filtered Centrifuged Solids (Continued)												
S96T000557	W	Fluoride-IC-Dionex 4000i/4500	µg/g	96.10	<1.30e-02	2.09e+02	198.0	203.6	5.41	109.0	50.69	n/a
S96T000557	W	Chloride-IC-Dionex 4000i/4500	µg/g	99.11	3.30e-02	1.72e+02	169.0	170.4	1.76	99.37	66.28	n/a
S96T000557	W	Nitrite-IC-Dionex 4000i/4500	µg/g	97.74	<1.07e-01	1.35e+04	1.34e+04	1.35e+04	0.74	114.6	417.3	n/a
S96T000557	W	Nitrate by IC-Dionex 4000i/4500	µg/g	97.72	<1.40e-01	1.27e+03	1.25e+03	1.26e+03	1.59	103.3	545.4	n/a
S96T000557	W	Phosphate-IC-Dionex 4000i/4500	µg/g	100.2	<1.19e-01	9.29e+02	985.0	957.0	5.85	109.7	463.7	n/a
S96T000557	W	Sulfate by IC-Dionex 4000i/4500	µg/g	97.94	<1.36e-01	4.12e+03	4.11e+03	4.11e+03	0.24	105.1	529.8	n/a
S96T000557	W	Oxalate by IC-Dionex 4000i	µg/g	99.07	<1.05e-01	7.80e+04	7.70e+04	7.75e+04	1.29	110.4	409.3	n/a
Interstitial Liquid: Interstitial Liquid												
S96T000545		DSC Exotherm Dry Calculated	Joules/g Dry	n/a	n/a	0.00e+00	0.00e+00	0.00e+00	0.00	n/a	n/a	n/a
S96T000545		DSC Exotherm on Perkin Elmer	Joules/g	95.82	n/a	0.00e+00	0.00e+00	0.00e+00	0.00	n/a	n/a	n/a
S96T000545		% Water by TGA on Perkin Elmer	%	102.0	n/a	34.27	36.53	35.40	6.38	n/a	n/a	n/a
S96T000545		TOC by Persulfate/ Coulometry	µg/mL	96.00	5.000	2.42e+03	2.43e+03	2.42e+03	0.41	n/a	40.00	n/a
S96T000545		Cobalt-60 by GEA	µCi/mL	96.11	<6.53e-04	<7.50e-03	1.08e-02	n/a	n/a	n/a	8.00e-03	n/a
S96T000545		Cesium-137 by GEA	µCi/mL	95.94	<4.94e-04	76.50	100.0	88.25	26.6	n/a	n/a	0.290

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Potential Organic Layer: Potential Organic Layer												
Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T001548		DSC Exotherm using Mettler	Joules/g	112.5	n/a	0.00e+00	0.00e+00	0.00e+00	0.00	n/a	n/a	n/a
S96T001548		DSC Exotherm Dry Calculated	Joules/g Dry	n/a	n/a	0.00e+00	0.00e+00	0.00e+00	0.00	n/a	n/a	n/a
S96T001548		% Water by TGA using Mettler	%	103.9	n/a	34.16	35.78	34.97	4.63	n/a	n/a	n/a
RISER:1												
SEGMENT #: 6C-96-8												
SEGMENT PORTION: Compatibility Study Mixture												
Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T002765		pH Direct	pH	n/a	n/a	11.16	n/a	n/a	n/a	n/a	1.00e-02	n/a
S96T002765		Specific Gravity	Sp.G.	101.2	n/a	9.80e-01	9.77e-01	9.78e-01	0.31	n/a	1.00e-02	n/a
S96T002766		DSC Exotherm on Perkin Elmer	Joules/g	100.6	n/a	0.00e+00	0.00e+00	0.00e+00	0.00	n/a	n/a	n/a
S96T002766		pH Direct	pH	n/a	n/a	11.22	n/a	n/a	n/a	n/a	1.00e-02	n/a
S96T002766		% Water by TGA on Perkin Elmer	%	97.87	n/a	96.24	96.16	96.20	0.08	n/a	n/a	n/a
S96T002769		Bulk Density of Sample	g/mL	n/a	n/a		n/a	n/a	n/a	n/a	5.00e-01	n/a
S96T002769		% Water by TGA using Mettler	%	99.54	n/a	73.78	76.28	75.03	3.33	n/a	n/a	n/a
S96T002770		DSC Exotherm using Mettler	Joules/g	111.8	n/a	0.00e+00	0.00e+00	0.00e+00	0.00	n/a	n/a	n/a
S96T002770		pH Direct	pH	n/a	n/a	11.71	11.69	11.70	0.17	n/a	1.00e-02	n/a
S96T002770		% Water by TGA using Mettler	%	99.54	n/a	96.86	97.03	96.94	0.18	n/a	n/a	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

SEGMENT PORTION: Compatibility Study Mixture (Continued)												
Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T002772		Bulk Density of Sample	g/mL	n/a	n/a		n/a	n/a	n/a	n/a	5.00e-01	n/a
S96T002772		% Water by TGA using Mettler	%	99.54	n/a	79.49	78.63	79.06	1.09	n/a	n/a	n/a
Decanted Supernate (Liquid Grab Sludge): Decanted Supernate (Liquid Grab Sludge)												
S96T002768		pH Direct	pH	n/a	n/a	11.10	n/a	n/a	n/a	n/a	1.00e-02	n/a
S96T002768		Specific Gravity	Sp.G.	101.2	n/a	1.005	9.97e-01	1.001	0.80	n/a	1.00e-02	n/a
S96T002771		pH Direct	pH	n/a	n/a	11.81	11.79	11.80	0.17	n/a	1.00e-02	n/a
S96T002771		Specific Gravity	Sp.G.	97.43	n/a	1.002	9.91e-01	9.96e-01	1.10	n/a	1.00e-02	n/a
Potential Organic Layer: Potential Organic Layer												
S96T003134		2-Butoxyethanol	µg/L	n/a	n/a	SEETICS	NA	n/a	n/a	n/a	n/a	n/a
S96T003134		Nonane (C9)	µg/mL	n/a	n/a	U0.00e+00	n/a	n/a	n/a	n/a	50.00	n/a
S96T003134		Decane (C10)	µg/mL	n/a	n/a	U0.00e+00	n/a	n/a	n/a	n/a	50.00	n/a
S96T003134		Undecane (C11)	µg/mL	n/a	n/a	J1.590	n/a	n/a	n/a	n/a	50.00	n/a
S96T003134		Dodecane (C12)	µg/mL	n/a	n/a	J10.10	n/a	n/a	n/a	n/a	50.00	n/a
S96T003134		Tridecane (C13)	µg/mL	n/a	n/a	J45.60	n/a	n/a	n/a	n/a	50.00	n/a
S96T003134		Tetradecane (C14)	µg/mL	n/a	n/a	J27.60	n/a	n/a	n/a	n/a	50.00	n/a
S96T003134		Pentadecane (C15)	µg/mL	n/a	n/a	J2.370	n/a	n/a	n/a	n/a	50.00	n/a
S96T003134		Tri-n-butylphosphate	µg/mL	n/a	n/a	J31.90	n/a	n/a	n/a	n/a	50.00	n/a
S96T003134		Hexadecane (C16) Surr	µg/mL	n/a	n/a	83.50	n/a	n/a	n/a	n/a	50.00	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
Sludge (from Liquid Grab Sample): Sludge (from Liquid Grab Sample)												
S96T000854		TOC by Persulfate/ Coulometry	µg/g	95.36	8.300	1.34e+04	9.32e+03	1.14e+04	35.9	n/a	40.00	n/a
S96T002021		DSC Exotherm using Mettler	Joules/g	97.72	n/a	33.50	100.6	67.05	100	n/a	n/a	n/a
S96T002021		DSC Exotherm Dry Calculated	Joules/g Dry	n/a	n/a	71.10	213.5	142.3	100	n/a	n/a	n/a
S96T002021		% Water by TGA using Mettler	%	99.93	n/a	59.60	46.16	52.88	25.4	n/a	n/a	n/a
S96T002042		DSC Exotherm Dry Calculated	Joules/g Dry	n/a	n/a	0.00e+00	0.00e+00	0.00e+00	0.00	n/a	n/a	n/a
S96T002042		DSC Exotherm on Perkin Elmer	Joules/g	92.02	n/a	0.00e+00	0.00e+00	0.00e+00	0.00	n/a	n/a	n/a
S96T002042		% Water by TGA using Mettler	%	99.16	n/a	60.45	60.55	60.50	0.17	n/a	n/a	n/a
S96T0020421		% Water by TGA using Mettler	%	99.83	n/a	56.10	54.50	55.30	2.89	n/a	n/a	n/a
RISER: 7												
SEGMENT #: 2AY-96-6												
SEGMENT PORTION: Supernate												
S96T002833		pH Direct	pH	n/a	n/a	12.52	n/a	n/a	n/a	n/a	1.00e-02	n/a
S96T002833		Specific Gravity	Sp.G.	101.2	n/a	9.76e-01	9.87e-01	9.82e-01	1.12	n/a	1.00e-02	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

SEGMENT #: 6C-96-11												
SEGMENT PORTION: Centrifuged Solids (Grab Sample)												
S96T001674		Bulk Density of Sample	g/mL	n/a	n/a	1.450	n/a	n/a	n/a	n/a	5.00e-01	n/a
S96T001674		DSC Exotherm using Mettler	Joules/g	97.72	n/a	19.70	109.6	64.65	139	n/a	n/a	n/a
S96T001674		DSC Exotherm Dry Calculated	Joules/g Dry	n/a	n/a	21.66	120.5	71.08	139	n/a	n/a	n/a
S96T001674		% Water by TGA using Mettler	%	99.93	n/a	9.630	8.430	9.030	13.3	n/a	n/a	n/a
S96T001674		Volume % Solids	%	n/a	n/a	59.50	n/a	n/a	n/a	n/a	n/a	n/a
S96T001674		% Water by Gravimetric	%	100.8	n/a	12.40	10.90	11.65	12.9	n/a	1.00e-02	n/a
Control Sample: Control Sample												
S96T001676		DSC Exotherm using Mettler	Joules/g	112.1	n/a	1.46e+02	137.2	141.6	6.21	n/a	n/a	n/a
S96T001676		DSC Exotherm Dry Calculated	Joules/g Dry	n/a	n/a	2.42e+02	227.8	235.1	6.21	n/a	n/a	n/a
S96T001676		% Water by TGA using Mettler	%	102.3	n/a	40.05	39.47	39.76	1.46	n/a	n/a	n/a
S96T001678	F	Technetium-99 Liq. Scint.	µCi/g	99.21	n/a	1.93e-02	2.75e-02	2.34e-02	35.0	n/a	1.80e-02	6.25E+00
S96T001678	F	Strontium-89/90 High Level	µCi/g	102.4	7.55e-01	3.83e+02	381.0	382.0	0.52	n/a	2.36e-01	7.89E-01
S96T001678	F	Pu-239/240 by TRU-SPEC Resin	µCi/g	100.3	<1.71e-02	7.75e-01	7.65e-01	7.70e-01	1.30	n/a	4.90e-02	2.01E+00
S96T001678	F	Cobalt-60 by GEA	µCi/g	99.96	<1.06e-03	<7.17e-01	<5.87e-1	n/a	n/a	n/a	7.17e-01	n/a
S96T001678	F	Cesium-137 by GEA	µCi/g	100.6	<2.56e-03	4.50e+02	408.0	429.1	9.79	n/a	n/a	1.55
S96T001678	F	Am-241 by Extraction	µCi/g	97.13	<1.31e-02	7.03e-01	7.15e-01	7.09e-01	1.69	n/a	6.10e-02	2.64E+00
S96T001678	F	Alpha of Digested Solid	µCi/g	102.3	<4.10e-02	1.500	1.620	1.560	7.69	91.09	6.10e-02	9.65E+00
S96T001675		Specific Gravity	Sp.G.	102.1	n/a	1.153	1.138	1.145	1.31	n/a	1.00e-03	n/a
S96T001675		% Water by Gravimetric	%	98.82	n/a	78.20	78.30	78.25	0.13	n/a	1.00e-02	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Decanted Supernate (Liquid Grab Sludge): Decanted Supernate (Liquid Grab Sludge) (Continued)

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T002024		pH Direct	pH	n/a	n/a	10.15	n/a	n/a	n/a	n/a	1.00e-02	n/a
S96T002024		Specific Gravity	Sp.G.	97.74	n/a	1.195	1.195	1.195	0.00	n/a	1.00e-03	n/a
S96T002024		Fluoride-IC-Dionex 4000i/4500	µg/mL	98.98	<1.30e-02	2.01e+02	209.0	205.1	3.90	127.5	14.44	n/a
S96T002024		Chloride-IC-Dionex 4000i/4500	µg/mL	99.75	<1.70e-02	2.58e+02	266.0	261.9	3.05	97.85	18.89	n/a
S96T002024		Nitrite-IC-Dionex 4000i/4500	µg/mL	103.5	<1.07e-01	2.59e+04	2.79e+04	2.69e+04	7.43	134.9	118.9	n/a
S96T002024		Nitrate-IC-Dionex4000i/4500	µg/mL	103.1	<1.40e-01	9.81e+02	1.01e+03	995.5	2.91	97.23	155.5	n/a
S96T002024		Phosphate-IC-Dionex 4000i/4500	µg/mL	103.5	<1.19e-01	4.42e+02	480.0	460.9	8.24	101.3	132.1	n/a
S96T002024		Sulfate by IC-Dionex 4000i/4500	µg/mL	101.6	<1.36e-01	6.69e+03	7.20e+03	6.94e+03	7.34	112.2	151.0	n/a
S96T002024		Oxalate by IC-Dionex 4000i	µg/mL	103.2	<1.05e-01	3.18e+03	3.45e+03	3.31e+03	8.14	106.3	116.7	n/a
S96T002024		Cobalt-60 by GEA	µCi/mL	93.30	<8.67e-04	<4.63e-03	<4.49e-3	n/a	n/a	n/a	5.00e-03	n/a
S96T002024		Cesium-137 by GEA	µCi/mL	90.88	<2.68e-03	1.28e+02	127.0	127.5	0.78	n/a	n/a	0.140

Filtered Centrifuged Solids: Filtered Centrifuged Solids

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T001685		DSC Exotherm Dry Calculated	Joules/g Dry	n/a	n/a	0.00e+00	0.00e+00	0.00e+00	0.00	n/a	n/a	n/a
S96T001685		DSC Exotherm on Perkin Elmer	Joules/g	100.3	n/a	0.00e+00	0.00e+00	0.00e+00	0.00	n/a	n/a	n/a
S96T001685		% Water by TGA on Perkin Elmer	%	99.39	n/a	32.54	31.29	31.91	3.92	n/a	n/a	n/a
S96T001686		TIC by Acid/Coulometry	µg/g	93.68	3.00e-01	2.32e+04	2.28e+04	2.30e+04	1.74	n/a	5.000	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Filtered Centrifuged Solids: Filtered Centrifuged Solids (Continued)												
Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T001686		TOC by Persulfate/ Coulometry	µg/g	94.03	3.000	2.00e+04	1.73e+04	1.86e+04	14.5	n/a	40.00	n/a
S96T001687		% Water by Gravimetric	%	98.99	n/a	34.10	34.10	34.10	0.00	n/a	1.00e-02	n/a
S96T001688		pH on SST Samples	pH	n/a	n/a	10.42	n/a	n/a	n/a	n/a	1.00e-02	n/a
S96T001689	F	Technetium-99 Liq. Scint.	µCi/g	99.21	n/a	2.97e-02	5.04e-01	2.67e-01	178	n/a	2.90e-02	6.23E+00
S96T001689	F	Strontium-89/90 High Level	µCi/g	102.4	7.55e-01	4.87e+02	523.0	505.0	7.13	n/a	4.36e-01	9.54E-01
S96T001689	F	Pu-239/240 by TRU-SPEC Resin	µCi/g	100.3	<1.71e-02	9.01e-01	9.26e-01	9.13e-01	2.74	n/a	7.40e-02	2.18E+00
S96T001689	F	Cobalt-60 by GEA	µCi/g	99.72	<2.20e-02	<3.03e-01	<4.13e-1	n/a	n/a	n/a	3.03e-01	n/a
S96T001689	F	Cesium-137 by GEA	µCi/g	100.9	<5.54e-01	4.83e+02	509.0	495.9	5.24	n/a	n/a	0.990
S96T001689	F	Am-241 by Extraction	µCi/g	97.13	<1.31e-02	1.030	9.80e-01	1.005	4.98	n/a	9.80e-02	2.85E+00
S96T001689	F	Alpha of Digested Solid	µCi/g	102.3	<4.10e-02	1.680	1.840	1.760	9.09	93.31	1.13e-01	1.23E+01
S96T001690	A	Silver-ICP-Acid Digest	µg/g	90.20	<1.00e-02	1.96e+03	1.25e+03	1.60e+03	44.2	139.0	3.830	n/a
S96T001690	A	Aluminum-ICP-Acid Digest	µg/g	91.40	1.09e-01	3.81e+04	3.77e+04	3.79e+04	1.06	130.2	19.10	n/a
S96T001690	A	Arsenic-ICP-Acid Digest	µg/g	93.80	<1.00e-01	<38.30	<3.93e1	n/a	n/a	90.50	38.30	n/a
S96T001690	A	Boron-ICP-Acid Digest	µg/g	97.60	6.50e-01	25.80	30.70	28.25	17.3	90.36	19.10	n/a
S96T001690	A	Barium-ICP-Acid Digest	µg/g	94.00	<5.00e-02	2.22e+02	219.0	220.5	1.36	90.42	19.10	n/a
S96T001690	A	Beryllium-ICP-Acid Digest	µg/g	102.6	<5.00e-03	<1.910	<1.97e0	n/a	n/a	97.50	1.910	n/a
S96T001690	A	Bismuth-ICP-AcidDigest	µg/g	91.20	<1.00e-01	<38.30	<3.93e1	n/a	n/a	91.10	38.30	n/a
S96T001690	A	Calcium-ICP-AcidDigest	µg/g	91.60	1.28e-01	2.65e+03	2.50e+03	2.58e+03	5.83	84.64	38.30	n/a
S96T001690	A	Cadmium-ICP-Acid Digest	µg/g	89.60	<5.00e-03	23.90	24.80	24.35	3.70	88.24	1.910	n/a
S96T001690	A	Cerium-ICP-Acid Digest	µg/g	97.00	<1.00e-01	1.41e+02	152.0	146.5	7.51	94.62	38.30	n/a
S96T001690	A	Cobalt-ICP-Acid Digest	µg/g	92.40	<2.00e-02	<7.660	8.350	n/a	n/a	90.60	7.660	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
Filtered Centrifuged Solids: Filtered Centrifuged Solids (Continued)												
S96T001690	A	Chromium-ICP-Acid Digest	µg/g	91.00	<1.00e-02	5.28e+02	538.0	533.0	1.88	90.42	3.830	n/a
S96T001690	A	Copper-ICP-Acid Digest	µg/g	92.00	1.10e-02	95.60	94.20	94.90	1.48	89.50	3.830	n/a
S96T001690	A	Iron-ICP-Acid Digest	µg/g	90.80	5.00e-02	4.59e+04	5.74e+04	5.16e+04	22.3	81.64	19.10	n/a
S96T001690	A	Potassium-ICP-Acid Digest	µg/g	93.00	<5.00e-01	5.53e+02	514.0	533.5	7.31	96.10	191.0	n/a
S96T001690	A	Lanthanum-ICP-Acid Digest	µg/g	94.40	<5.00e-02	49.60	47.80	48.70	3.70	91.60	19.10	n/a
S96T001690	A	Lithium-ICP-Acid Digest	µg/g	95.20	<1.00e-02	<3.830	<3.93e0	n/a	n/a	92.00	3.830	n/a
S96T001690	A	Magnesium-ICP-Acid Digest	µg/g	86.40	<1.00e-01	2.50e+02	264.0	257.0	5.45	85.64	38.30	n/a
S96T001690	A	Manganese-ICP-Acid Digest	µg/g	90.80	<1.00e-02	3.21e+03	3.27e+03	3.24e+03	1.85	102.1	3.830	n/a
S96T001690	A	Molybdenum-ICP-Acid Digest	µg/g	91.40	<5.00e-02	<19.10	<1.97e1	n/a	n/a	89.50	19.10	n/a
S96T001690	A	Sodium-ICP-Acid Digest	µg/g	103.6	8.77e-01	1.08e+05	1.08e+05	1.08e+05	0.00	n/a	38.30	n/a
S96T001690	A	Neodymium-ICP-Acid Digest	µg/g	93.80	<1.00e-01	1.28e+02	125.0	126.5	2.37	91.22	38.30	n/a
Filtered Centrifuged Solids: Filtered Centrifuged Solids												
S96T001690	A	Nickel-ICP-Acid Digest	µg/g	91.80	<2.00e-02	5.15e+02	518.0	516.5	0.58	91.10	7.660	n/a
S96T001690	A	Phosphorus-ICP-Acid Digest	µg/g	96.80	<2.00e-01	1.76e+03	1.81e+03	1.78e+03	2,80	110.1	76.60	n/a
S96T001690	A	Lead-ICP-Acid Digest	µg/g	86.80	<1.00e-01	1.90e+03	1.95e+03	1.92e+03	2.60	89.66	38.30	n/a
S96T001690	A	Sulfur-ICP-Acid Digest	µg/g	90.20	<1.00e-01	9.18e+02	938.0	928.0	2.16	93.06	38.30	n/a
S96T001690	A	Antimony-ICP-Acid Digest	µg/g	93.40	<6.00e-02	<23.00	<2.36e1	n/a	n/a	92.50	23.00	n/a
S96T001690	A	Selenium-ICP-Acid Digest	µg/g	88.60	<1.00e-01	<38.30	<3.93e1	n/a	n/a	89.50	38.30	n/a
S96T001690	A	Silicon-ICP-Acid Digest	µg/g	125.0	7.70e-01	2.16e+04	2.05e+04	2.10e+04	5.23	72.84	19.10	n/a
S96T001690	A	Samarium-ICP-Acid Digest	µg/g	92.60	<1.00e-01	<38.30	<3.93e1	n/a	n/a	91.10	38.30	n/a
S96T001690	A	Strontium-ICP-Acid Digest	µg/g	92.40	<1.00e-02	20.10	20.00	20.05	0.50	89.04	3.830	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
Filtered Centrifuged Solids: Filtered Centrifuged Solids (Continued)												
S96T001690	A	Titanium-ICP-Acid Digest	µg/g	86.20	<1.00e-02	87.40	87.50	87.45	0.11	83.24	3.830	n/a
S96T001690	A	Thallium-ICP-Acid Digest	µg/g	86.00	<2.00e-01	<76.60	<7.87e1	n/a	n/a	85.00	76.60	n/a
S96T001690	A	Uranium-ICP-AcidDigest	µg/g	91.20	<5.00e-01	5.78e+02	588.0	583.0	1.72	87.90	191.0	n/a
S96T001690	A	Vanadium-ICP-Acid Digest	µg/g	111.0	<5.00e-02	<19.10	<1.97e1	n/a	n/a	89.10	19.10	n/a
S96T001690	A	Zinc-ICP-Acid Digest	µg/g	87.40	1.10e-02	62.30	87.40	74.85	33.5	87.56	3.830	n/a
S96T001690	A	Zirconium-ICP-Acid Digest	µg/g	99.20	<1.00e-02	1.62e+02	431.0	296.5	90.7	119.5	3.830	n/a
S96T001691	W	Fluoride-IC-Dionex 4000i/4500	µg/g	95.42	<1.30e-02	<9.51e+03	<9.34e3	n/a	n/a	n/a	9.51e+03	n/a
S96T001691	W	Chloride-IC-Dionex 4000i/4500	µg/g	91.39	<1.70e-02	<1.24e+04	<1.22e4	n/a	n/a	n/a	1.24e+04	n/a
S96T001691	W	Nitrite-IC-Dionex 4000i/4500	µg/g	93.80	<1.07e-01	<7.83e+04	<7.69e4	n/a	n/a	n/a	7.83e+04	n/a
S96T001691	W	Nitrate by IC-Dionex 4000i/4500	µg/g	93.81	<1.40e-01	2.18e+07	2.43e+07	2.30e+07	10.8	n/a	1.02e+05	n/a
S96T001691	W	Phosphate-IC-Dionex 4000i/4500	µg/g	95.79	<1.19e-01	<8.70e+04	<8.54e4	n/a	n/a	n/a	8.70e+04	n/a
S96T001691	W	Sulfate by IC-Dionex 4000i/4500	µg/g	95.09	<1.36e-01	<9.94e+04	<9.76e4	n/a	n/a	n/a	9.94e+04	n/a
S96T001691	W	Oxalate by IC-Dionex 4000i	µg/g	96.12	<1.05e-01	1.40e+05	1.19e+05	1.29e+05	16.2	n/a	7.68e+04	n/a
Interstitial Liquid: Interstitial Liquid												
S96T001681		DSC Exotherm using Mettler	Joules/g	101.6	n/a	5.500	5.500	5.500	0.00	n/a	n/a	n/a
S96T001681		DSC Exotherm Dry Calculated	Joules/g Dry	n/a	n/a	10.27	10.27	10.27	0.00	n/a	n/a	n/a
S96T001681		% Water by TGA on Perkin Elmer	%	99.27	n/a	48.47	44.37	46.42	8.83	n/a	n/a	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Interstitial Liquid: Interstitial Liquid (Continued)												
Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T001681		Tot. Organic Carbon by Coul.	µg/mL	93.36	1.300	2.06e+03	2.08e+03	2.07e+03	0.97	96.30	55.00	n/a
S96T001681		TOC by Persulfate/ Coulometry	µg/mL	93.36	6.500	1.64e+03	1.62e+03	1.63e+03	1.23	n/a	40.00	n/a
S96T001681		Strontium-89/90 High Level	µCi/mL	n/a	n/a	6.71e-01	6.68e-01	6.69e-01	0.45	n/a	8.00e-03	3.75E+00
S96T001681		Pu-239/240 by TRU-SPEC Resin	µCi/mL	98.69	<1.67e-02	8.40e-01	8.34e-01	8.37e-01	0.72	n/a	4.90e-02	1.88E+00
S96T001681	D	Silver-ICP-Acid Dil.	µg/mL	98.20	<1.00e-02	<4.010	<4.01e0	n/a	n/a	93.80	4.010	n/a
S96T001681	D	Aluminum-ICP-Acid Dil.	µg/mL	98.20	<5.00e-02	<20.10	<2.01e1	n/a	n/a	96.00	20.10	n/a
S96T001681	D	Arsenic-ICP-Acid Dil.	µg/mL	102.2	<1.00e-01	<40.10	<4.01e1	n/a	n/a	105.7	40.10	n/a
S96T001681	D	Boron-ICP-Acid Dil.	µg/mL	101.0	<5.00e-02	<20.10	<2.01e1	n/a	n/a	101.3	20.10	n/a
S96T001681	D	Barium-ICP-Acid Dil.	µg/mL	99.20	<5.00e-02	<20.10	<2.01e1	n/a	n/a	99.80	20.10	n/a
S96T001681	D	Beryllium-ICP-Acid Dil.	µg/mL	102.8	<5.00e-03	<2.000	<2.00e0	n/a	n/a	101.5	2.000	n/a
S96T001681	D	Bismuth-ICP-Acid Dil.	µg/mL	99.60	<1.00e-01	<40.10	<4.01e1	n/a	n/a	90.80	40.10	n/a
S96T001681	D	Calcium-ICP-Acid Dil.	µg/mL	97.60	<1.00e-01	<40.10	<4.01e1	n/a	n/a	97.30	40.10	n/a
S96T001681	D	Cadmium-ICP-Acid Dil.	µg/mL	99.80	<5.00e-03	<2.000	<2.00e0	n/a	n/a	96.00	2.000	n/a
S96T001681	D	Cerium-ICP-Acid Dil.	µg/mL	101.6	<1.00e-01	<40.10	<4.01e1	n/a	n/a	99.30	40.10	n/a
S96T001681	D	Cobalt-ICP-Acid Dil.	µg/mL	101.8	<2.00e-02	<8.020	<8.02e0	n/a	n/a	98.00	8.020	n/a
S96T001681	D	Chromium-ICP-Acid Dil.	µg/mL	100.6	<1.00e-02	<4.010	<4.01e0	n/a	n/a	98.30	4.010	n/a
S96T001681	D	Copper-ICP-Acid Dil.	µg/mL	100.6	<1.00e-02	<4.010	<4.01e0	n/a	n/a	99.80	4.010	n/a
S96T001681	D	Iron-ICP-Acid Dil.	µg/mL	100.0	<5.00e-02	<20.10	<2.01e1	n/a	n/a	101.8	20.10	n/a
S96T001681	D	Potassium-ICP-Acid Dil.	µg/mL	101.2	<5.00e-01	5.41e+02	533.0	537.0	1.49	98.30	200.0	n/a
S96T001681	D	Lanthanum-ICP-Acid Dil.	µg/mL	98.60	<5.00e-02	<20.10	<2.01e1	n/a	n/a	98.50	20.10	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Interstitial Liquid: Interstitial Liquid (Continued)

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T001681	D	Lithium-ICP-Acid Dil.	µg/mL	100.4	<1.00e-02	<4.010	<4.01e0	n/a	n/a	95.50	4.010	n/a
S96T001681	D	Magnesium-ICP-Acid Dil.	µg/mL	98.20	<1.00e-01	<40.10	<4.01e1	n/a	n/a	94.80	40.10	n/a
S96T001681	D	Manganese-ICP-Acid Dil.	µg/mL	100.0	<1.00e-02	<4.010	<4.01e0	n/a	n/a	98.00	4.010	n/a
S96T001681	D	Molybdenum-ICP-Acid Dil.	µg/mL	101.8	<5.00e-02	<20.10	<2.01e1	n/a	n/a	104.0	20.10	n/a
S96T001681	D	Sodium-ICP-Acid Dil.	µg/mL	99.40	<1.00e-01	9.91e+04	9.56e+04	9.74e+04	3.60	n/a	40.10	n/a
S96T001681	D	Neodymium-ICP-Acid Dil.	µg/mL	99.80	<1.00e-01	<40.10	<4.01e1	n/a	n/a	104.7	40.10	n/a
S96T001681	D	Nickel-ICP-Acid Dil.	µg/mL	99.80	<2.00e-02	11.50	11.30	11.40	1.75	96.60	8.020	n/a
S96T001681	D	Phosphorus-ICP-Acid Dil.	µg/mL	102.0	<2.00e-01	2.66e+02	275.0	270.5	3.33	103.1	80.20	n/a
S96T001681	D	Lead-ICP-Acid Dil.	µg/mL	99.20	<1.00e-01	<40.10	<4.01e1	n/a	n/a	98.30	40.10	n/a
S96T001681	D	Sulfur-ICP-Acid Dil.	µg/mL	100.2	<1.00e-01	2.24e+03	2.15e+03	2.20e+03	4.10	79.60	40.10	n/a
S96T001681	D	Antimony-ICP-Acid Dil.	µg/mL	95.40	<6.00e-02	<24.10	<2.41e1	n/a	n/a	91.00	24.10	n/a
S96T001681	D	Selenium-ICP-Acid Dil.	µg/mL	103.6	<1.00e-01	<40.10	<4.01e1	n/a	n/a	118.7	40.10	n/a
S96T001681	D	Silicon-ICP-Acid Dil.	µg/mL	95.40	<5.00e-02	27.50	20.40	23.95	29.6	92.90	20.10	n/a
S96T001681	D	Samarium-ICP-Acid Dil.	µg/mL	99.60	<1.00e-01	<40.10	<4.01e1	n/a	n/a	102.5	40.10	n/a
S96T001681	D	Strontium-ICP-Acid Dil.	µg/mL	99.20	<1.00e-02	<4.010	<4.01e0	n/a	n/a	99.50	4.010	n/a
S96T001681	D	Titanium-ICP-Acid Dil.	µg/mL	98.20	<1.00e-02	<4.010	<4.01e0	n/a	n/a	97.50	4.010	n/a
S96T001681	D	Thallium-ICP-Acid Dil.	µg/mL	96.00	<2.00e-01	<80.20	<8.02e1	n/a	n/a	92.00	80.20	n/a
S96T001681	D	Uranium-ICP-Acid Dil.	µg/mL	96.60	<5.00e-01	1.60e+03	1.50e+03	1.55e+03	6.45	98.85	200.0	n/a
S96T001681	D	Vanadium-ICP-Acid Dil.	µg/mL	101.2	<5.00e-02	<20.10	<2.01e1	n/a	n/a	99.30	20.10	n/a
S96T001681	D	Zinc-ICP-Acid Dil.	µg/mL	102.2	<1.00e-02	<4.010	<4.01e0	n/a	n/a	97.50	4.010	n/a
S96T001681	D	Zirconium-ICP-Acid Dil.	µg/mL	98.60	<1.00e-02	3.30e+02	319.0	324.5	3.39	98.70	4.010	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
Interstitial Liquid: Interstitial Liquid (Continued)												
S96T001681		Cobalt-60 by GEA	µCi/mL	97.28	<3.26e-04	<5.05e-03	<4.80e-3	n/a	n/a	n/a	5.00e-03	n/a
S96T001681		Cesium-137 by GEA	µCi/mL	97.05	1.00e-03	1.21e+02	121.0	121.0	0.00	n/a	n/a	0.140
Potential Organic Layer: Potential Organic Layer												
S96T001679		DSC Exotherm using Mettler	Joules/g	93.85	n/a	0.00e+00	0.00e+00	0.00e+00	0.00	n/a	n/a	n/a
S96T001679		DSC Exotherm Dry Calculated	Joules/g Dry	n/a	n/a	0.00e+00	0.00e+00	0.00e+00	0.00	n/a	n/a	n/a
S96T001679		% Water by TGA using Mettler	%	101.2	n/a	28.37	31.34	29.86	9.95	n/a	n/a	n/a
S96T001679		TOC by Persulfate/Coulometry	µg/mL	94.03	3.000	2.48e+04	2.20e+04	2.34e+04	12.0	n/a	40.00	n/a
S96T002635		Pu-239/240 by TRU-SPEC Resin	µCi/g	99.21	<3.10e-02	3.63e-01	3.57e-01	3.60e-01	1.67	n/a	2.80e-02	2.19E+00
S96T002635		Pu-238 by Ion Exchange	µCi/g	n/a	<3.10e-02	1.12e-01	1.00e-01	1.06e-01	11.3	n/a	2.80e-02	3.22E+00
Sludge (from Liquid Grab Sample): Sludge (from Liquid Grab Sample)												
S96T003180	W	Fluoride-IC-Dionex4000i/4500	µg/g	104.2	<1.30e-02	1.12e+02	344.0	228.2	102	n/a	49.60	n/a
S96T003180	W	Chloride-IC-Dionex4000i/4500	µg/g	96.58	<1.70e-02	1.56e+02	153.0	154.3	1.94	n/a	64.87	n/a
S96T003180	W	Nitrite-IC-Dionex4000i/4500	µg/g	93.91	<1.07e-01	8.22e+03	7.20e+03	7.71e+03	13.2	n/a	408.2	n/a
S96T003180	W	Nitrate by IC-Dionex4000i/4500	µg/g	102.8	5.910	2.65e+03	2.35e+03	2.50e+03	12.0	n/a	533.8	n/a
S96T003180	W	Phosphate-IC-Dionex4000i/4500	µg/g	105.3	<1.19e-01	8.29e+02	<4.15e2	n/a	n/a	n/a	453.6	n/a
S96T003180	W	Sulfate by IC-Dionex4000i/4500	µg/g	105.7	<1.36e-01	2.53e+03	2.28e+03	2.41e+03	10.4	n/a	518.5	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
Sludge (from Liquid Grab Sample): Sludge (from Liquid Grab Sample) (Continued)												
S96T003180	W	Oxalate by IC-Dionex4000i	µg/g	105.3	<1.05e-01	7.82e+04	2.26e+05	1.52e+05	97.2	n/a	400.6	n/a
RISER: 7												
SEGMENT #: 6C-96-12												
SEGMENT PORTION: Supernate												
S96T001023		DSC Exotherm using Mettler	Joules/g	108.3	n/a	0.00e+00	0.00e+00	0.00e+00	0.00	n/a	n/a	n/a
S96T001023		DSC Exotherm Dry Calculated	Joules/g Dry	n/a	n/a	0.00e+00	0.00e+00	0.00e+00	0.00	n/a	n/a	n/a
S96T001023		Ammonia by ISE-Std Additions	µg/mL	96.84	3.100	<5.000	<5	n/a	n/a	99.00	5.000	n/a
S96T001023		pH Direct	pH	n/a	n/a	10.24	10.24	10.24	0.06	n/a	1.00e-02	n/a
S96T001023		Specific Gravity	Sp.G.	98.45	n/a	1.173	1.193	1.183	1.69	n/a	1.00e-03	n/a
S96T001023		% Water by TGA using Mettler	%	102.2	n/a	79.05	79.49	79.27	0.52	n/a	n/a	n/a
S96T001023		Tot. Inorg. Carbon by Coul.	µg/mL	103.2	<5.000	2.43e+04	2.46e+04	2.44e+04	1.23	99.00	105.0	n/a
S96T001023		Tot. Organic Carbon by Coul.	µg/mL	99.70	<5.000	2.49e+03	2.54e+03	2.52e+03	1.99	97.30	55.00	n/a
S96T001023		TOC by Persulfate/ Coulometry	µg/mL	91.36	2.800	1.97e+03	2.09e+03	2.03e+03	5.91	n/a	40.00	n/a
S96T001023		% Water by Gravimetric	%	102.2	n/a	79.00	79.00	79.00	0.00	n/a	1.00e-02	n/a
S96T001023	D	Silver-ICP-Acid Dil.	µg/mL	100.8	<1.00e-02	9.210	9.930	9.570	7.52	87.10	6.010	n/a
S96T001023	D	Aluminum-ICP-Acid Dil.	µg/mL	98.40	<5.00e-02	<30.00	<3.00e1	n/a	n/a	95.90	30.10	n/a
S96T001023	D	Barium-ICP-Acid Dil.	µg/mL	102.6	<5.00e-02	<30.00	<3.00e1	n/a	n/a	95.80	30.10	n/a
S96T001023	D	Beryllium-ICP-Acid Dil.	µg/mL	104.0	<5.00e-03	<3.000	<3.00e0	n/a	n/a	99.40	3.000	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

SEGMENT PORTION: Supernate (Continued)

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T001023	D	Bismuth-ICP-Acid Dil.	µg/mL	101.8	<1.00e-01	<60.10	<6.01e1	n/a	n/a	102.6	60.10	n/a
S96T001023	D	Calcium-ICP-Acid Dil.	µg/mL	104.2	<1.00e-01	<60.10	<6.01e1	n/a	n/a	102.1	60.10	n/a
S96T001023	D	Cadmium-ICP-Acid Dil.	µg/mL	102.8	<5.00e-03	<3.000	<3.00e0	n/a	n/a	98.80	3.000	n/a
S96T001023	D	Cerium-ICP-Acid Dil.	µg/mL	105.6	<1.00e-01	<60.10	<6.01e1	n/a	n/a	101.9	60.10	n/a
S96T001023	D	Cobalt-ICP-Acid Dil.	µg/mL	103.4	<2.00e-02	<12.00	<1.20e1	n/a	n/a	99.80	12.00	n/a
S96T001023	D	Chromium-ICP-Acid Dil.	µg/mL	104.0	<1.00e-02	<6.010	<6.01e0	n/a	n/a	100.1	6.010	n/a
S96T001023	D	Copper-ICP-Acid Dil.	µg/mL	104.2	<1.00e-02	<6.010	<6.01e0	n/a	n/a	96.30	6.010	n/a
S96T001023	D	Iron-ICP-Acid Dil.	µg/mL	103.2	<5.00e-02	<30.00	<3.00e1	n/a	n/a	99.30	30.10	n/a
S96T001023	D	Potassium-ICP-Acid Dil.	µg/mL	103.4	<5.00e-01	6.94e+02	788.0	741.0	12.7	107.3	300.0	n/a
S96T001023	D	Lanthanum-ICP-Acid Dil.	µg/mL	103.6	<5.00e-02	<30.00	<3.00e1	n/a	n/a	97.80	30.10	n/a
S96T001023	D	Lithium-ICP-Acid Dil.	µg/mL	99.60	<1.00e-02	<6.010	<6.01e0	n/a	n/a	96.80	6.010	n/a
S96T001023	D	Magnesium-ICP-Acid Dil.	µg/mL	97.60	<1.00e-01	<60.10	<6.01e1	n/a	n/a	95.00	60.10	n/a
S96T001023	D	Manganese-ICP-Acid Dil.	µg/mL	100.6	<1.00e-02	<6.010	<6.01e0	n/a	n/a	94.60	6.010	n/a
S96T001023	D	Molybdenum-ICP-Acid Dil.	µg/mL	103.8	<5.00e-02	<30.00	<3.00e1	n/a	n/a	103.8	30.10	n/a
S96T001023	D	Sodium-ICP-Acid Dil.	µg/mL	98.20	<1.00e-01	1.08e+05	1.04e+05	1.06e+05	3.77	n/a	60.10	n/a
S96T001023	D	Neodymium-ICP-Acid Dil.	µg/mL	105.2	<1.00e-01	<60.10	<6.01e1	n/a	n/a	100.1	60.10	n/a
S96T001023	D	Nickel-ICP-Acid Dil.	µg/mL	101.6	<2.00e-02	14.00	14.70	14.35	4.88	98.80	12.00	n/a
S96T001023	D	Phosphorus-ICP-Acid Dil.	µg/mL	102.2	<2.00e-01	2.53e+02	247.0	250.0	2.40	97.30	120.0	n/a
S96T001023	D	Lead-ICP-Acid Dil.	µg/mL	102.0	<1.00e-01	<60.10	<6.01e1	n/a	n/a	102.4	60.10	n/a
S96T001023	D	Sulfur-ICP-Acid Dil.	µg/mL	98.80	<1.00e-01	2.49e+03	2.45e+03	2.47e+03	1.62	69.70	60.10	n/a
S96T001023	D	Antimony-ICP-Acid Dil.	µg/mL	96.20	<6.00e-02	<36.10	<3.61e1	n/a	n/a	96.90	36.10	n/a
S96T001023	D	Selenium-ICP-Acid Dil.	µg/mL	98.40	<1.00e-01	<60.10	<6.01e1	n/a	n/a	99.40	60.10	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

SEGMENT PORTION: Supernate (Continued)

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T001023	D	Silicon-ICP-Acid Dil.	µg/mL	99.00	<5.00e-02	<30.00	<3.00e1	n/a	n/a	99.90	30.10	n/a
S96T001023	D	Samarium-ICP-Acid Dil.	µg/mL	100.4	<1.00e-01	<60.10	<6.01e1	n/a	n/a	95.90	60.10	n/a
S96T001023	D	Strontium-ICP-Acid Dil.	µg/mL	101.8	<1.00e-02	<6.010	<6.01e0	n/a	n/a	96.30	6.010	n/a
S96T001023	D	Titanium-ICP-Acid Dil.	µg/mL	100.4	<1.00e-02	<6.010	<6.01e0	n/a	n/a	96.10	6.010	n/a
S96T001023	D	Thallium-ICP-Acid Dil.	µg/mL	99.00	<2.00e-01	<1.20e+02	<1.20e2	n/a	n/a	96.40	120.0	n/a
S96T001023	D	Uranium-ICP-Acid Dil.	µg/mL	99.20	<5.00e-01	1.48e+03	1.41e+03	1.44e+03	4.84	76.80	300.0	n/a
S96T001023	D	Vanadium-ICP-Acid Dil.	µg/mL	103.4	<5.00e-02	<30.00	<3.00e1	n/a	n/a	99.40	30.10	n/a
S96T001023	D	Zinc-ICP-Acid Dil.	µg/mL	101.6	<1.00e-02	<6.010	<6.01e0	n/a	n/a	100.6	6.010	n/a
S96T001023	D	Zirconium-ICP-Acid Dil.	µg/mL	102.0	<1.00e-02	3.44e+02	333.0	338.5	3.25	92.80	6.010	n/a
S96T001023		Fluoride-IC-Dionex 4000i/4500	µg/mL	91.69	<1.30e-02	1.83e+02	184.0	183.4	0.54	105.1	14.44	n/a
S96T001023		Chloride-IC-Dionex 4000i/4500	µg/mL	99.49	<1.70e-02	3.20e+02	317.0	318.7	0.94	92.15	36.06	n/a
S96T001023		Nitrite-IC-Dionex 4000i/4500	µg/mL	92.18	<1.07e-01	2.42e+04	2.40e+04	2.41e+04	0.83	100.9	118.9	n/a
S96T001023		Nitrate-IC-Dionex4000i/4500	µg/mL	93.16	4.44e-01	1.11e+03	1.12e+03	1.11e+03	0.90	88.27	155.5	n/a
S96T001023		Phosphate-IC-Dionex 4000i/4500	µg/mL	89.74	<1.19e-01	8.63e+02	845.0	854.0	2.11	81.68	132.1	n/a
S96T001023		Sulfate by IC-Dionex 4000i/4500	µg/mL	92.08	<1.36e-01	6.54e+03	6.53e+03	6.54e+03	0.15	93.03	151.0	n/a
S96T001023		Oxalate by IC-Dionex 4000i	µg/mL	97.25	<1.05e-01	2.98e+03	2.98e+03	2.98e+03	0.00	97.25	116.7	n/a
S96T001024		Technetium-99 Liq.Scint.	µCi/mL	103.9	<3.65e-04	1.60e-01	4.79e-01	3.20e-01	99.8	n/a	2.57e-04	6.80E-01
S96T001024		Strontium-89/90 High Level	µCi/mL	95.12	8.00e-03	4.84e-01	4.82e-01	4.83e-01	0.41	n/a	2.00e-03	3.01E+00
S96T001024		Pu-239/240 by TRU-SPEC Resin	µCi/mL	88.28	<3.12e-03	7.38e-01	8.14e-01	7.76e-01	9.79	n/a	3.40e-02	1.67E+00

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
SEGMENT PORTION: Supernate (Continued)												
S96T001024		Cobalt-60 by GEA	µCi/mL	99.23	<1.99e-05	<6.19e-03	<5.55e-3	n/a	n/a	n/a	6.00e-03	n/a
S96T001024		Cesium-137 by GEA	µCi/mL	101.5	<5.81e-05	1.08e+02	110.0	109.0	1.83	n/a	n/a	0.210
S96T001024		Am-241 by Extraction	µCi/mL	80.13	<1.15e-02	<1.13e-02	<1.28E-2	n/a	n/a	n/a	1.10e-02	5.59E+00
S96T001024		Alpha in Liquid Samples	µCi/mL	88.23	<4.98e-03	9.28e-01	8.80e-01	9.04e-01	5.31	92.86	1.20e-02	5.11E+00
RISER: 7												
SEGMENT #: 6C-96-13												
SEGMENT PORTION: Centrifuged Solids (Grab Sample)												
S96T001030		Bulk Density of Sample	g/mL	n/a	n/a	1.520	n/a	n/a	n/a	n/a	5.00e-01	n/a
S96T001030		DSC Exotherm using Mettler	Joules/g	112.1	n/a	1.81e+02	258.9	219.9	35.5	n/a	n/a	n/a
S96T001030		DSC Exotherm Dry Calculated	Joules/g Dry	n/a	n/a	2.00e+02	285.6	242.6	35.4	n/a	n/a	n/a
S96T001030		% Water by TGA on Perkin Elmer	%	99.16	n/a	9.240	9.480	9.360	2.56	n/a	n/a	n/a
S96T001030		Volume % Solids	%	n/a	n/a	67.30	n/a	n/a	n/a	n/a	n/a	n/a
S96T001030		%Water by Gravimetric	%	98.99	n/a	19.30	22.40	20.85	14.9	n/a	1.00e-02	n/a
Control Sample: Control Sample												
S96T001034		DSC Exotherm using Mettler	Joules/g	100.9	n/a	87.40	66.70	77.05	26.9	n/a	n/a	n/a
S96T001034		DSC Exotherm Dry Calculated	Joules/g Dry	n/a	n/a	1.27e+02	96.81	111.9	26.9	n/a	n/a	n/a
S96T001034		% Water by TGA using Mettler	%	99.43	n/a	31.29	30.91	31.10	1.22	n/a	n/a	n/a
S96T001036	F	Technetium-99 Liq.Scint.	µCi/g	102.9	<1.62e-02	3.59e-02	2.41e-02	3.00e-02	39.3	n/a	1.70e-02	6.45E+00
S96T001036	F	Strontium-89/90 High Level	µCi/g	99.19	6.97e-01	1.24e+03	483.0	861.5	87.9	n/a	1.87e-01	4.24E-01

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Control Sample: Control Sample (Continued)												
Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T001036	F	Pu-239/240 by TRU-SPEC Resin	µCi/g	97.90	<1.60e-02	1.200	8.95e-01	1.047	29.1	n/a	6.80e-02	1.82E+00
S96T001036	F	Cobalt-60 by GEA	µCi/g	101.4	<4.12e-01	<5.75e-01	<5.58e-1	n/a	n/a	n/a	5.75e-01	n/a
S96T001036	F	Cesium-137 by GEA	µCi/g	103.2	<4.46e-01	8.99e+02	716.0	807.6	22.7	n/a	n/a	0.810
S96T001036	F	Am-241 by Extraction	µCi/g	101.0	<1.28e-02	1.460	1.210	1.335	18.7	n/a	1.20e-01	2.62E+00
S96T001036	F	Alpha of Digested Solid	µCi/g	114.8	<6.30e-02	6.330	2.420	4.375	89.4	96.66	1.09e-01	6.97E+00
Decanted Supernate (Liquid Grab Sludge): Decanted Supernate (Liquid Grab Sludge)												
S96T001032		Specific Gravity	Sp.G.	n/a	n/a	I.S.	I.S.	n/a	n/a	n/a	1.00e-03	n/a
S96T002025		pH Direct	pH	n/a	n/a	10.09	n/a	n/a	n/a	n/a	1.00e-02	n/a
S96T002025		Tot. Organic Carbon by Coul.	µg/mL	100.0	1.00e-01	1.95e+03	1.95e+03	1.95e+03	0.00	103.0	55.00	n/a
S96T002025		Pu-239/240 by TRU-SPEC Resin	µCi/mL	96.33	<3.33e-03	7.73e-01	7.66e-01	7.70e-01	0.91	n/a	3.80e-02	1.66E+00
S96T002025		Fluoride-IC-Dionex 4000i/4500	µg/mL	98.98	<1.30e-02	1.91e+02	209.0	200.2	9.00	n/a	14.44	n/a
S96T002025		Chloride-IC-Dionex 4000i/4500	µg/mL	99.75	<1.70e-02	2.82e+02	293.0	287.2	3.83	n/a	18.89	n/a
S96T002025		Nitrite-IC-Dionex 4000i/4500	µg/mL	103.5	<1.07e-01	2.74e+04	3.05e+04	2.90e+04	10.7	n/a	118.9	n/a
S96T002025		Nitrate-IC-Dionex 4000i/4500	µg/mL	103.1	<1.40e-01	9.69e+02	1.10e+03	1.03e+03	12.7	n/a	155.5	n/a
S96T002025		Phosphate-IC-Dionex 4000i/4500	µg/mL	103.5	<1.19e-01	4.88e+02	558.0	522.8	13.4	n/a	132.1	n/a
S96T002025		Sulfate by IC-Dionex 4000i/4500	µg/mL	101.6	<1.36e-01	7.19e+03	7.98e+03	7.58e+03	10.4	n/a	151.0	n/a
S96T002025		Oxalate by IC-Dionex 4000i	µg/mL	103.2	<1.05e-01	3.11e+03	3.47e+03	3.29e+03	10.9	n/a	116.7	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Decanted Supernate (Liquid Grab Sludge): Decanted Supernate (Liquid Grab Sludge) (Continued)												
Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T002025		Cobalt-60 by GEA	µCi/mL	93.30	<8.67e-04	<4.03e-03	<4.34e-3	n/a	n/a	n/a	4.00e-03	n/a
S96T002025		Cesium-137 by GEA	µCi/mL	90.88	<2.68e-03	1.04e+02	105.0	104.5	0.96	n/a	n/a	0.160
Filtered Centrifuged Solids: Filtered Centrifuged Solids												
S96T001559		DSC Exotherm Dry Calculated	Joules/g Dry	n/a	n/a	0.00e+00	0.00e+00	0.00e+00	0.00	n/a	n/a	n/a
S96T001559		DSC Exotherm on Perkin Elmer	Joules/g	100.3	n/a	0.00e+00	0.00e+00	0.00e+00	0.00	n/a	n/a	n/a
S96T001559		% Water by TGA on Perkin Elmer	%	99.39	n/a	21.28	26.12	23.70	20.4	n/a	n/a	n/a
S96T001560		TIC by Acid/ Coulometry	µg/g	93.68	3.00e-01	2.64e+04	2.66e+04	2.65e+04	0.75	103.0	5.000	n/a
S96T001560		TOC by Persulfate/ Coulometry	µg/g	94.03	3.000	1.60e+04	1.35e+04	1.48e+04	16.9	77.00	40.00	n/a
S96T001561		% Water by Gravimetric	%	98.65	n/a	25.90	26.70	26.30	3.04	n/a	1.00e-02	n/a
S96T001562		pH on SST Samples	pH	n/a	n/a	10.67	10.62	10.64	0.47	n/a	1.00e-02	n/a
S96T001563	F	Technetium-99 Liq. Scint.	µCi/g	102.9	<1.62e-02	4.11e-02	3.23e-02	3.67e-02	24.0	n/a	1.50e-02	4.90E-01
S96T001563	F	Strontium-89/90 High Level	µCi/g	99.19	6.97e-01	6.38e+02	683.0	660.5	6.81	n/a	1.86e-01	5.91E-01
S96T001563	F	Pu-239/240 by TRU-SPEC Resin	µCi/g	97.90	<1.60e-02	1.650	1.540	1.595	6.90	n/a	8.50e-02	1.76E+00
S96T001563	F	Cobalt-60 by GEA	µCi/g	101.4	<4.12e-01	<6.24e-01	<5.83e-1	n/a	n/a	n/a	6.24e-01	n/a
S96T001563	F	Cesium-137 by GEA	µCi/g	103.2	<4.46e-01	8.88e+02	892.0	890.2	0.45	n/a	n/a	0.810
S96T001563	F	Am-241 by Extraction	µCi/g	101.0	<1.28e-02	1.590	1.630	1.610	2.48	n/a	1.32e-01	2.54E+00
S96T001563	F	Alpha of Digested Solid	µCi/g	114.8	<6.30e-02	3.610	3.670	3.640	1.65	108.4	1.10e-01	9.56E+00
S96T001564	A	Silver-ICP-Acid Digest	µg/g	90.20	<1.00e-02	1.81e+03	3.33e+03	2.57e+03	59.1	n/a	4.220	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Filtered Centrifuged Solids: Filtered Centrifuged Solids (Continued)

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T001564	A	Aluminum-ICP-Acid Digest	µg/g	91.40	1.09e-01	6.21e+04	6.45e+04	6.33e+04	3.79	n/a	21.10	n/a
S96T001564	A	Arsenic-ICP-Acid Digest	µg/g	93.80	<1.00e-01	<42.20	<4.18e1	n/a	n/a	n/a	42.20	n/a
S96T001564	A	Boron-ICP-Acid Digest	µg/g	97.60	6.50e-01	79.30	61.30	70.30	25.6	n/a	21.10	n/a
S96T001564	A	Barium-ICP-Acid Digest	µg/g	94.00	<5.00e-02	3.67e+02	375.0	371.0	2.16	n/a	21.10	n/a
S96T001564	A	Beryllium-ICP- Acid Digest	µg/g	102.6	<5.00e-03	<2.110	<2.09e0	n/a	n/a	n/a	2.110	n/a
S96T001564	A	Bismuth-ICP-Acid Digest	µg/g	91.20	<1.00e-01	<42.20	<4.18e1	n/a	n/a	n/a	42.20	n/a
S96T001564	A	Calcium-ICP-Acid Digest	µg/g	91.60	1.28e-01	1.20e+03	1.27e+03	1.24e+03	5.67	n/a	42.20	n/a
S96T001564	A	Cadmium-ICP-Acid Digest	µg/g	89.60	<5.00e-03	36.50	38.90	37.70	6.37	n/a	2.110	n/a
S96T001564	A	Cerium-ICP-Acid Digest	µg/g	97.00	<1.00e-01	2.13e+02	251.0	232.0	16.4	n/a	42.20	n/a
S96T001564	A	Cobalt-ICP-Acid Digest	µg/g	92.40	<2.00e-02	10.30	11.10	10.70	7.48	n/a	8.450	n/a
S96T001564	A	Chromium-ICP- Acid Digest	µg/g	91.00	<1.00e-02	6.55e+02	682.0	668.5	4.04	n/a	4.220	n/a
S96T001564	A	Copper-ICP-Acid Digest	µg/g	92.00	1.10e-02	1.04e+02	108.0	106.0	3.77	n/a	4.220	n/a
S96T001564	A	Iron-ICP-Acid Digest	µg/g	90.80	5.00e-02	7.00e+04	7.29e+04	7.14e+04	4.06	n/a	21.10	n/a
S96T001564	A	Potassium-ICP- Acid Digest	µg/g	93.00	<5.00e-01	9.42e+02	932.0	937.0	1.07	n/a	211.0	n/a
S96T001564	A	Lanthanum-ICP- Acid Digest	µg/g	94.40	<5.00e-02	70.50	73.50	72.00	4.17	n/a	21.10	n/a
S96T001564	A	Lithium-ICP-Acid Digest	µg/g	95.20	<1.00e-02	4.900	5.090	4.995	3.80	n/a	4.220	n/a
S96T001564	A	Magnesium-ICP- Acid Digest	µg/g	86.40	<1.00e-01	2.79e+02	303.0	291.0	8.25	n/a	42.20	n/a
S96T001564	A	Manganese-ICP- Acid Digest	µg/g	90.80	<1.00e-02	3.01e+03	3.12e+03	3.06e+03	3.59	n/a	4.220	n/a
S96T001564	A	Molybdenum-ICP-Acid Digest	µg/g	91.40	<5.00e-02	<21.10	<2.09e1	n/a	n/a	n/a	21.10	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Filtered Centrifuged Solids: Filtered Centrifuged Solids (Continued)

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T001564	A	Sodium-ICP-Acid Digest	µg/g	103.6	8.77e-01	1.41e+05	1.35e+05	1.38e+05	4.35	n/a	42.20	n/a
S96T001564	A	Neodymium-ICP-Acid Digest	µg/g	93.80	<1.00e-01	1.74e+02	187.0	180.5	7.20	n/a	42.20	n/a
S96T001564	A	Nickel-ICP-Acid Digest	µg/g	91.80	<2.00e-02	7.08e+02	740.0	724.0	4.42	n/a	8.450	n/a
S96T001564	A	Phosphorus-ICP- Acid Digest	µg/g	96.80	<2.00e-01	2.71e+03	2.74e+03	2.72e+03	1.10	n/a	84.50	n/a
S96T001564	A	Lead-ICP-Acid Digest	µg/g	86.80	<1.00e-01	2.81e+03	2.85e+03	2.83e+03	1.41	n/a	42.20	n/a
S96T001564	A	Sulfur-ICP-Acid Digest	µg/g	90.20	<1.00e-01	1.67e+03	1.51e+03	1.59e+03	10.1	n/a	42.20	n/a
S96T001564	A	Antimony-ICP- Acid Digest	µg/g	93.40	<6.00e-02	<25.30	<2.51e1	n/a	n/a	n/a	25.30	n/a
S96T001564	A	Selenium-ICP- Acid Digest	µg/g	88.60	<1.00e-01	<42.20	<4.18e1	n/a	n/a	n/a	42.20	n/a
S96T001564	A	Silicon-ICP-Acid Digest	µg/g	125.0	7.70e-01	3.55e+04	2.95e+04	3.25e+04	18.5	n/a	21.10	n/a
S96T001564	A	Samarium-ICP- Acid Digest	µg/g	92.60	<1.00e-01	<42.20	<4.18e1	n/a	n/a	n/a	42.20	n/a
S96T001564	A	Strontium-ICP- Acid Digest	µg/g	92.40	<1.00e-02	23.50	24.60	24.05	4.57	n/a	4.220	n/a
S96T001564	A	Titanium-ICP- Acid Digest	µg/g	86.20	<1.00e-02	1.15e+02	121.0	118.0	5.08	n/a	4.220	n/a
S96T001564	A	Thallium-ICP- Acid Digest	µg/g	86.00	<2.00e-01	<84.50	<8.36e1	n/a	n/a	n/a	84.50	n/a
S96T001564	A	Uranium-ICP-Acid Digest	µg/g	91.20	<5.00e-01	1.06e+03	927.0	993.5	13.4	n/a	211.0	n/a
S96T001564	A	Vanadium-ICP- Acid Digest	µg/g	111.0	<5.00e-02	<21.10	<2.09e1	n/a	n/a	n/a	21.10	n/a
S96T001564	A	Zinc-ICP-Acid Digest	µg/g	87.40	1.10e-02	53.50	58.00	55.75	8.07	n/a	4.220	n/a
S96T001564	A	Zirconium-ICP- Acid Digest	µg/g	99.20	<1.00e-02	4.52e+02	1.10e+03	776.0	83.5	n/a	4.220	n/a
S96T001565	W	Fluoride-IC-Dionex 4000i/4500	µg/g	95.42	<1.30e-02	<1.06e+04	<1.09e4	n/a	n/a	96.44	1.06e+04	n/a
S96T001565	W	Chloride-IC-Dionex 4000i/4500	µg/g	91.39	<1.70e-02	<1.38e+04	<1.43e4	n/a	n/a	93.80	1.38e+04	n/a
S96T001565	W	Nitrite-IC-Dionex 4000i/4500	µg/g	93.80	<1.07e-01	<8.71e+04	<9.00e4	n/a	n/a	97.26	8.71e+04	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Filtered Centrifuged Solids: Filtered Centrifuged Solids (Continued)												
Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T001565	W	Nitrate by IC-Dionex 4000i/4500	µg/g	93.81	<1.40e-01	2.90e+07	1.80e+07	2.35e+07	46.8	97.07	1.14e+05	n/a
S96T001565	W	Phosphate-IC- Dionex 4000i/4500	µg/g	95.79	<1.19e-01	<9.68e+04	<1.00e5	n/a	n/a	97.99	9.68e+04	n/a
S96T001565	W	Sulfate by IC-Dionex 4000i/4500	µg/g	95.09	<1.36e-01	<1.11e+05	<1.14e5	n/a	n/a	97.62	1.11e+05	n/a
S96T001565	W	Oxalate by IC-Dionex 4000i	µg/g	97.09	<1.05e-01	<4.38e+04	9.23e+04	n/a	n/a	98.64	4.38e+04	n/a
Interstitial Liquid: Interstitial Liquid												
S96T001566		DSC Exotherm using Mettler	Joules/g	93.85	n/a	1.19e+02	96.80	107.8	20.5	n/a	n/a	n/a
S96T001566		DSC Exotherm Dry Calculated	Joules/g Dry	n/a	n/a	4.90e+02	399.3	444.9	20.5	n/a	n/a	n/a
S96T001566		% Water by TGA using Mettler	%	101.2	n/a	74.92	76.60	75.76	2.22	n/a	n/a	n/a
S96T001566		TOC by Persulfate/ Coulometry	µg/mL	93.36	6.500	1.86e+03	1.83e+03	1.84e+03	1.63	n/a	40.00	n/a
S96T001566		Strontium-89/90 High Level	µCi/mL	n/a	n/a	6.39e-02	8.86e-02	7.62e-02	32.4	n/a	2.40e-02	3.65E+01
S96T001566	D	Silver-ICP-Acid Dil.	µg/mL	97.40	<1.00e-02	8.510	9.270	8.890	8.55	92.20	4.010	n/a
S96T001566	D	Aluminum-ICP- Acid Dil.	µg/mL	96.20	<5.00e-02	48.10	66.90	57.50	32.7	90.00	20.10	n/a
S96T001566	D	Arsenic-ICP-Acid Dil.	µg/mL	100.4	<1.00e-01	<40.10	<4.01e1	n/a	n/a	106.2	40.10	n/a
S96T001566	D	Boron-ICP-Acid Dil.	µg/mL	101.0	<5.00e-02	32.10	32.40	32.25	0.93	98.20	20.10	n/a
S96T001566	D	Barium-ICP-Acid Dil.	µg/mL	97.60	<5.00e-02	<20.10	<2.01e1	n/a	n/a	100.0	20.10	n/a
S96T001566	D	Beryllium-ICP- Acid Dil.	µg/mL	102.6	<5.00e-03	<2.000	<2.00e0	n/a	n/a	102.5	2.000	n/a
S96T001566	D	Bismuth-ICP-Acid Dil.	µg/mL	98.60	<1.00e-01	<40.10	<4.01e1	n/a	n/a	90.00	40.10	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Interstitial Liquid: Interstitial Liquid (Continued)

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T001566	D	Calcium-ICP-Acid Dil.	µg/mL	98.20	<1.00e-01	<40.10	<4.01e1	n/a	n/a	100.8	40.10	n/a
S96T001566	D	Cadmium-ICP- Acid Dil.	µg/mL	100.2	<5.00e-03	<2.000	<2.00e0	n/a	n/a	96.80	2.000	n/a
S96T001566	D	Cerium-ICP-Acid Dil.	µg/mL	98.60	<1.00e-01	<40.10	<4.01e1	n/a	n/a	96.80	40.10	n/a
S96T001566	D	Cobalt-ICP-Acid Dil.	µg/mL	99.60	<2.00e-02	<8.020	<8.02e0	n/a	n/a	97.00	8.020	n/a
S96T001566	D	Chromium-ICP- Acid Dil.	µg/mL	100.0	<1.00e-02	<4.010	<4.01e0	n/a	n/a	98.30	4.010	n/a
S96T001566	D	Copper-ICP-Acid Dil.	µg/mL	99.00	<1.00e-02	<4.010	<4.01e0	n/a	n/a	99.30	4.010	n/a
S96T001566	D	Iron-ICP-Acid Dil.	µg/mL	103.2	<5.00e-02	52.80	64.70	58.75	20.3	98.80	20.10	n/a
S96T001566	D	Potassium-ICP- Acid Dil.	µg/mL	97.80	<5.00e-01	6.71e+02	634.0	652.5	5.67	82.10	200.0	n/a
S96T001566	D	Lanthanum-ICP- Acid Dil.	µg/mL	99.60	<5.00e-02	<20.10	<2.01e1	n/a	n/a	100.5	20.10	n/a
S96T001566	D	Lithium-ICP-Acid Dil.	µg/mL	95.00	<1.00e-02	<4.010	<4.01e0	n/a	n/a	91.00	4.010	n/a
S96T001566	D	Magnesium-ICP- Acid Dil.	µg/mL	96.60	<1.00e-01	<40.10	<4.01e1	n/a	n/a	94.30	40.10	n/a
S96T001566	D	Manganese-ICP- Acid Dil.	µg/mL	100.0	<1.00e-02	<4.010	<4.01e0	n/a	n/a	99.00	4.010	n/a
S96T001566	D	Molybdenum-ICP-Acid Dil.	µg/mL	98.20	<5.00e-02	22.40	22.70	22.55	1.33	98.20	20.10	n/a
S96T001566	D	Sodium-ICP-Acid Dil.	µg/mL	95.80	<1.00e-01	1.13e+05	1.10e+05	1.12e+05	2.69	n/a	40.10	n/a
S96T001566	D	Neodymium-ICP-Acid Dil.	µg/mL	104.6	<1.00e-01	<40.10	<4.01e1	n/a	n/a	105.2	40.10	n/a
S96T001566	D	Nickel-ICP-Acid Dil.	µg/mL	99.80	<2.00e-02	15.20	15.00	15.10	1.32	97.70	8.020	n/a
S96T001566	D	Phosphorus-ICP- Acid Dil.	µg/mL	112.2	<2.00e-01	3.68e+02	393.0	380.5	6.57	121.9	80.20	n/a
S96T001566	D	Lead-ICP-Acid Dil.	µg/mL	100.6	<1.00e-01	<40.10	<4.01e1	n/a	n/a	102.8	40.10	n/a
S96T001566	D	Sulfur-ICP-Acid Dil.	µg/mL	99.60	<1.00e-01	2.73e+03	2.71e+03	2.72e+03	0.74	85.10	40.10	n/a
S96T001566	D	Antimony-ICP- Acid Dil.	µg/mL	105.6	<6.00e-02	<24.10	<2.41e1	n/a	n/a	84.30	24.10	n/a
S96T001566	D	Selenium-ICP- Acid Dil.	µg/mL	100.6	<1.00e-01	<40.10	<4.01e1	n/a	n/a	117.0	40.10	n/a
S96T001566	D	Silicon-ICP-Acid Dil.	µg/mL	94.40	<5.00e-02	1.18e+02	124.0	121.0	4.96	90.80	20.10	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
Interstitial Liquid: Interstitial Liquid (Continued)												
S96T001566	D	Samarium-ICP- Acid Dil.	µg/mL	98.80	<1.00e-01	<40.10	<4.01e1	n/a	n/a	102.8	40.10	n/a
S96T001566	D	Strontium-ICP- Acid Dil.	µg/mL	97.80	<1.00e-02	<4.010	<4.01e0	n/a	n/a	100.3	4.010	n/a
S96T001566	D	Titanium-ICP- Acid Dil.	µg/mL	95.60	<1.00e-02	<4.010	<4.01e0	n/a	n/a	96.80	4.010	n/a
S96T001566	D	Thallium-ICP- Acid Dil.	µg/mL	94.60	<2.00e-01	<80.20	<8.02e1	n/a	n/a	86.50	80.20	n/a
S96T001566	D	Uranium-ICP-Acid Dil.	µg/mL	95.60	<5.00e-01	1.87e+03	1.83e+03	1.85e+03	2.16	99.85	200.0	n/a
S96T001566	D	Vanadium-ICP- Acid Dil.	µg/mL	101.4	<5.00e-02	<20.10	<2.01e1	n/a	n/a	100.0	20.10	n/a
S96T001566	D	Zinc-ICP-Acid Dil.	µg/mL	100.8	<1.00e-02	<4.010	<4.01e0	n/a	n/a	96.80	4.010	n/a
S96T001566	D	Zirconium-ICP- Acid Dil.	µg/mL	98.80	<1.00e-02	3.79e+02	375.0	377.0	1.06	99.90	4.010	n/a
S96T001566		Cobalt-60 by GEA	µCi/mL	98.44	<2.89e-03	<6.19e-03	<7.13e-3	n/a	n/a	n/a	6.00e-03	n/a
S96T001566		Cesium-137 by GEA	µCi/mL	96.31	<8.70e-03	1.35e+02	170.0	152.5	23.0	n/a	n/a	0.210
Potential Organic Layer: Potential Organic Layer												
S96T001553		DSC Exotherm using Mettler	Joules/g	113.9	n/a	2.08e+02	167.9	188.0	21.4	n/a	n/a	n/a
S96T001553		DSC Exotherm Dry Calculated	Joules/g Dry	n/a	n/a	7.54e+02	608.3	681.1	21.4	n/a	n/a	n/a
S96T001553		% Water by TGA using Mettler	%	103.7	n/a	72.40	30.11	51.26	82.5	n/a	n/a	n/a
Sludge (from Liquid Grab Sample): Sludge (from Liquid Grab Sample)												
S96T003181	W	Fluoride-IC- Dionex 4000i/4500	µg/g	104.2	<1.30e-02	4.02e+02	119.0	260.3	109	97.63	52.21	n/a
S96T003181	W	Chloride-IC- Dionex 4000i/4500	µg/g	96.58	<1.70e-02	1.56e+02	197.0	176.4	23.2	149.4	68.28	n/a
S96T003181	W	Nitrite-IC-Dionex 4000i/4500	µg/g	93.91	<1.07e-01	1.16e+04	1.09e+04	1.13e+04	6.22	93.54	429.8	n/a
S96T003181	W	Nitrate by IC-Dionex 4000i/4500	µg/g	102.8	5.910	9.89e+02	1.94e+03	1.46e+03	64.9	96.09	561.9	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Sludge (from Liquid Grab Sample): Sludge (from Liquid Grab Sample) (Continued)												
Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T003181	W	Phosphate-IC- Dionex 4000i/4500	µg/g	105.3	<1.19e-01	9.24e+02	1.08e+03	1.00e+03	15.6	97.44	477.5	n/a
S96T003181	W	Sulfate by IC- Dionex 4000i/4500	µg/g	105.7	<1.36e-01	3.52e+03	3.12e+03	3.32e+03	12.0	100.6	545.8	n/a
S96T003181	W	Oxalate by IC- Dionex 4000i	µg/g	105.3	<1.05e-01	2.50e+04	8.25e+04	5.37e+04	107	99.80	421.7	n/a
SEGMENT PORTION: Compatibility Study Mixture												
S96T002825		DSC Exotherm on Perkin Elmer	Joules/g	100.6	n/a	0.00e+00	0.00e+00	0.00e+00	0.00	n/a	n/a	n/a
S96T002825		pH Direct	pH	n/a	n/a	11.12	n/a	n/a	n/a	n/a	1.00e-02	n/a
S96T002825		% Water by TGA on Perkin Elmer	%	97.87	n/a	95.78	90.16	92.97	6.04	n/a	n/a	n/a
S96T002827		Bulk Density of Sample	g/mL	n/a	n/a		n/a	n/a	n/a	n/a	5.00e-01	n/a
S96T002827		% Water by TGA using Mettler	%	103.7	n/a	95.08	93.40	94.24	1.78	n/a	n/a	n/a
S96T002829		DSC Exotherm using Mettler	Joules/g	111.8	n/a	0.00e+00	580.2	290.1	200	n/a	n/a	n/a
S96T0028291		DSC Exotherm using Mettler	Joules/g	114.2	n/a	0.00e+00	77.80	38.90	200	n/a	n/a	n/a
S96T002829		pH Direct	pH	n/a	n/a	11.80	11.79	11.79	0.08	n/a	1.00e-02	n/a
S96T002829		% Water by TGA using Mettler	%	99.54	n/a	95.69	96.02	95.85	0.34	n/a	n/a	n/a
S96T002831		Bulk Density of Sample	g/mL	n/a	n/a		n/a	n/a	n/a	n/a	5.00e-01	n/a
S96T002831		% Water by TGA on Perkin Elmer	%	99.61	n/a	83.85	85.53	84.69	1.98	n/a	n/a	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

SEGMENT PORTION: Compatibility Study Mixture												
Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T002826		pH Direct	pH	n/a	n/a	11.50	n/a	n/a	n/a	n/a	1.00e-02	n/a
S96T002826		Specific Gravity	Sp.G.	101.2	n/a	9.88e-01	9.72e-01	9.80e-01	1.63	n/a	1.00e-02	n/a
S96T002830		pH Direct	pH	n/a	n/a	11.91	11.90	11.91	0.08	n/a	1.00e-02	n/a
S96T002830		Specific Gravity	Sp.G.	97.43	n/a	9.96e-01	9.99e-01	9.98e-01	0.30	n/a	1.00e-02	n/a
Potential Organic Layer: Potential Organic Layer												
S96T003230		2-Butoxyethanol	µg/L	n/a	n/a	SEETICS	NA	n/a	n/a	n/a	n/a	n/a
S96T003230		Nonane (C9)	µg/mL	n/a	n/a	U0.00e+00	n/a	n/a	n/a	n/a	50.00	n/a
S96T003230		Decane (C10)	µg/mL	n/a	n/a	U0.00e+00	n/a	n/a	n/a	n/a	50.00	n/a
S96T003230		Undecane (C11)	µg/mL	n/a	n/a	J4.070	n/a	n/a	n/a	n/a	50.00	n/a
S96T003230		Dodecane (C12)	µg/mL	n/a	n/a	J27.00	n/a	n/a	n/a	n/a	50.00	n/a
S96T003230		Tridecane (C13)	µg/mL	n/a	n/a	1.19e+02	n/a	n/a	n/a	n/a	50.00	n/a
S96T003230		Tetradecane (C14)	µg/mL	n/a	n/a	77.00	n/a	n/a	n/a	n/a	50.00	n/a
S96T003230		Pentadecane (C15)	µg/mL	n/a	n/a	J6.270	n/a	n/a	n/a	n/a	50.00	n/a
S96T003230		Tri-n-butylphosphate	µg/mL	n/a	n/a	J48.80	n/a	n/a	n/a	n/a	50.00	n/a
S96T003230		Hexadecane (C16) Surr	µg/mL	n/a	n/a	83.90	n/a	n/a	n/a	n/a	50.00	n/a
S96T001551		TOC by Persulfate/ Coulometry	µg/g	95.36	8.300	2.97e+04	2.85e+04	2.91e+04	4.12	82.00	40.00	n/a
S96T002350		DSC Exotherm using Mettler	Joules/g	111.4	n/a	29.80	61.10	45.45	68.9	n/a	n/a	n/a
S96T002350		DSC Exotherm Dry Calculated	Joules/g Dry	n/a	n/a	83.15	170.5	126.8	68.9	n/a	n/a	n/a
S96T002350		% Water by TGA using Mettler	%	99.31	n/a	65.05	63.26	64.16	2.79	n/a	n/a	n/a
S96T002351		DSC Exotherm using Mettler	Joules/g	112.8	n/a	1.81e+02	218.1	199.3	18.8	n/a	n/a	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
Potential Organic Layer: Potential Organic Layer (Continued)												
S96T002351		DSC Exotherm Dry Calculated	Joules/g Dry	n/a	n/a	4.04e+02	487.9	445.9	18.8	n/a	n/a	n/a
S96T002351		% Water by TGA on Perkin Elmer	%	97.43	n/a	56.03	54.56	55.30	2.66	n/a	n/a	n/a
Supernate: Supernate												
S96T001546	D	Silver-ICP-Acid Dil.	µg/mL	97.80	<1.00e-02	<4.010	<4.01e0	n/a	n/a	90.00	4.010	n/a
S96T001546	D	Aluminum-ICP- Aid Dil.	µg/mL	100.0	<5.00e-02	<20.10	<2.01e1	n/a	n/a	96.30	20.10	n/a
S96T001546	D	Arsenic-ICP-Acid Dil.	µg/mL	103.0	<1.00e-01	<40.10	<4.01e1	n/a	n/a	103.3	40.10	n/a
S96T001546	D	Boron-ICP-Acid Dil.	µg/mL	103.2	<5.00e-02	<20.10	<2.01e1	n/a	n/a	101.0	20.10	n/a
S96T001546	D	Barium-ICP-Acid Dil.	µg/mL	104.0	<5.00e-02	<20.10	<2.01e1	n/a	n/a	102.8	20.10	n/a
S96T001546	D	Beryllium-ICP- Acid Dil.	µg/mL	105.6	<5.00e-03	<2.000	<2.00e0	n/a	n/a	102.5	2.000	n/a
S96T001546	D	Bismuth-ICP-Acid Dil.	µg/mL	101.4	<1.00e-01	<40.10	<4.01e1	n/a	n/a	89.50	40.10	n/a
S96T001546	D	Calcium-ICP-Acid Dil.	µg/mL	103.2	<1.00e-01	<40.10	<4.01e1	n/a	n/a	104.2	40.10	n/a
S96T001546	D	Cadmium-ICP- Acid Dil.	µg/mL	99.60	<5.00e-03	<2.000	<2.00e0	n/a	n/a	94.80	2.000	n/a
S96T001546	D	Cerium-ICP-Acid Dil.	µg/mL	105.0	<1.00e-01	<40.10	<4.01e1	n/a	n/a	100.8	40.10	n/a
S96T001546	D	Cobalt-ICP-Acid Dil.	µg/mL	100.0	<2.00e-02	<8.020	<8.02e0	n/a	n/a	95.00	8.020	n/a
S96T001546	D	Chromium-ICP- Acid Dil.	µg/mL	98.80	<1.00e-02	<4.010	<4.01e0	n/a	n/a	94.80	4.010	n/a
S96T001546	D	Copper-ICP-Acid Dil.	µg/mL	105.0	<1.00e-02	<4.010	<4.01e0	n/a	n/a	102.3	4.010	n/a
S96T001546	D	Iron-ICP-Acid Dil.	µg/mL	102.0	<5.00e-02	<20.10	<2.01e1	n/a	n/a	100.0	20.10	n/a
S96T001546	D	Potassium-ICP- Acid Dil.	µg/mL	101.4	<5.00e-01	5.08e+02	496.0	502.0	2.39	81.20	200.0	n/a
S96T001546	D	Lanthanum-ICP- Acid Dil.	µg/mL	102.6	<5.00e-02	<20.10	<2.01e1	n/a	n/a	101.5	20.10	n/a
S96T001546	D	Lithium-ICP-Acid Dil.	µg/mL	106.4	<1.00e-02	<4.010	<4.01e0	n/a	n/a	100.0	4.010	n/a
S96T001546	D	Magnesium-ICP- Acid Dil.	µg/mL	97.00	<1.00e-01	<40.10	<4.01e1	n/a	n/a	92.00	40.10	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Supernate: Supernate (Continued)

Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T001546	D	Manganese-ICP- Acid Dil.	µg/mL	99.40	<1.00e-02	<4.010	<4.01e0	n/a	n/a	96.00	4.010	n/a
S96T001546	D	Molybdenum-ICP-Acid Dil.	µg/mL	100.2	<5.00e-02	21.80	21.80	21.80	0.00	95.60	20.10	n/a
S96T001546	D	Sodium-ICP-Acid Dil.	µg/mL	105.0	<1.00e-01	1.10e+05	1.06e+05	1.08e+05	3.70	n/a	40.10	n/a
S96T001546	D	Neodymium-ICP-Acid Dil.	µg/mL	108.4	<1.00e-01	<40.10	<4.01e1	n/a	n/a	109.5	40.10	n/a
S96T001546	D	Nickel-ICP-Acid Dil.	µg/mL	99.40	<2.00e-02	16.40	17.10	16.75	4.18	94.40	8.020	n/a
S96T001546	D	Phosphorus-ICP- Acid Dil.	µg/mL	102.0	<2.00e-01	2.92e+02	299.0	295.5	2.37	98.10	80.20	n/a
S96T001546	D	Lead-ICP-Acid Dil.	µg/mL	99.40	<1.00e-01	<40.10	<4.01e1	n/a	n/a	96.30	40.10	n/a
S96T001546	D	Sulfur-ICP-Acid Dil.	µg/mL	99.40	<1.00e-01	2.42e+03	2.35e+03	2.38e+03	2.94	26.40	40.10	n/a
S96T001546	D	Antimony-ICP- Acid Dil.	µg/mL	96.80	<6.00e-02	<24.10	<2.41e1	n/a	n/a	91.50	24.10	n/a
S96T001546	D	Selenium-ICP- Acid Dil.	µg/mL	106.0	<1.00e-01	<40.10	<4.01e1	n/a	n/a	112.2	40.10	n/a
S96T001546	D	Silicon-ICP-Acid Dil.	µg/mL	95.60	<5.00e-02	<20.10	<2.01e1	n/a	n/a	95.00	20.10	n/a
S96T001546	D	Samarium-ICP- Acid Dil.	µg/mL	105.8	<1.00e-01	<40.10	<4.01e1	n/a	n/a	109.0	40.10	n/a
S96T001546	D	Strontium-ICP- Acid Dil.	µg/mL	103.4	<1.00e-02	<4.010	<4.01e0	n/a	n/a	102.3	4.010	n/a
S96T001546	D	Titanium-ICP- Acid Dil.	µg/mL	99.00	<1.00e-02	<4.010	<4.01e0	n/a	n/a	96.50	4.010	n/a
S96T001546	D	Thallium-ICP- Acid Dil.	µg/mL	97.20	<2.00e-01	<80.20	<8.02e1	n/a	n/a	90.80	80.20	n/a
S96T001546	D	Uranium-ICP-Acid Dil.	µg/mL	100.0	<5.00e-01	1.76e+03	1.79e+03	1.78e+03	1.69	88.70	200.0	n/a
S96T001546	D	Vanadium-ICP- Acid Dil.	µg/mL	102.0	<5.00e-02	<20.10	<2.01e1	n/a	n/a	98.30	20.10	n/a
S96T001546	D	Zinc-ICP-Acid Dil.	µg/mL	100.0	<1.00e-02	4.320	<4.01e0	n/a	n/a	93.20	4.010	n/a
S96T001546	D	Zirconium-ICP- Acid Dil.	µg/mL	101.4	<1.00e-02	3.81e+02	377.0	379.0	1.06	93.50	4.010	n/a
S96T001546		Fluoride-IC- Dionex 4000i/4500	µg/mL	98.81	<1.30e-02	2.23e+02	212.0	217.3	5.06	125.6	14.44	n/a
S96T001546		Chloride-IC-Dionex4000i/4500	µg/mL	93.17	<1.70e-02	2.97e+02	295.0	295.8	0.68	99.75	18.89	n/a

Table A.2-1: Interim Results for Tank C-106 Grab Samples.
C-106 GRAB

Supernate: Supernate (Continued)												
Sample # R	A #	Analyte	Unit	Standard %	Blank	Result	Duplicate	Average	RPD %	Spk Rec %	Det Limit	Count Err %
S96T001546		Nitrite-IC-Dionex 4000i/4500	µg/mL	98.61	<1.07e-01	3.02e+04	3.04e+04	3.03e+04	0.66	96.88	118.9	n/a
S96T001546		Nitrate-IC-Dionex 4000i/4500	µg/mL	99.67	2.38e-01	1.00e+03	1.09e+03	1.05e+03	8.61	96.91	155.5	n/a
S96T001546		Phosphate-IC-Dionex 4000i/4500	µg/mL	100.7	<1.19e-01	5.13e+02	530.0	521.6	3.26	101.5	132.1	n/a
S96T001546		Sulfate by IC-Dionex 4000i/4500	µg/mL	99.53	<1.36e-01	7.88e+03	7.90e+03	7.89e+03	0.25	103.8	151.0	n/a
S96T001546		Oxalate by IC-Dionex 4000i	µg/mL	100.2	<1.05e-01	3.53e+03	3.50e+03	3.52e+03	0.85	101.1	116.7	n/a

APPENDIX A.3

DOSE MEASUREMENTS TAKEN DURING THE APRIL 19, 1986 CORE SAMPLING OF C-106

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APPENDIX A.3

DOSE MEASUREMENTS TAKEN DURING THE APRIL 19, 1986 CORE SAMPLING OF C-106

A summary of dose (mrem/hr) measurements obtained on the tank C-106 core samples taken April 19, 1986.

Table A.3-1. A Summary of Dose Measurements from April 19, 1986 Tank C-106 Core Samples.[1]

Description	Depth (19-in. segments - ~100% recovery)	Dose (mrem/hr) (through the drill string)
Top liquid layer	~8 in.; estimated as 12 in. supernate	Included with topmost solids
Topmost dark brown solids (BL waste)	Next ~15 in.	1,500
Dark brown soft solids (BL waste)	Next ~19 in.	2,100
Dark brown soft solids (PUREX AR waste)	Next ~12 in.	2,800
Dark brown solids overlaying hard solids (UR/CWP1 heels)	Next ~19 in.	2,000

Note:

[1]Fowler (1991)

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APPENDIX A.4

WORSE-CASE TOTAL ORGANIC CARBON MEASUREMENTS IN TANKS AY-102 AND C-106

(Excerpted from Castaing 1995)

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APPENDIX A.4

WORST-CASE TOTAL ORGANIC CARBON MEASUREMENTS IN TANKS AY-102 AND C-106

(Excerpted or summarized from Castaing 1995)

The worst-case values from Castaing (1995) were evaluated to determine whether any new information about their validity could be obtained. No further insight into the validity of the numbers reported could be obtained in the time available, but engineering judgment, coupled with recent sampling and speciation results, suggests that these results are to be treated as suspect as a basis for determination of a potential for propagating reaction in nitrate-nitrite-complexant systems.

AY-102

TOC = 3.82 mol/kg (Castaing [1995], Page 7). The other units reported in Castaing (1995) are in μg/kg. Mol/kg has not been a unit traditionally used in Hanford Site waste characterization.

Calculation: 3.82 moles (Carbon)/kg x 12 g/mole = 45.85 g/kg waste or 0.046 g/g of waste or 4.6% TOC wet basis or 9% if assumed to be 50% moisture in sludge

(If the units are reported as grams of carbon, then the actual TOC is 1/12 of the mole % basis calculated above, or 0.75%)

A Summary of AY-102 Chemistry

Scheele et al. (1990) reports on the analysis of four segment core samples taken in the second quarter of FY 1988 from tank AY-102. The bottom three segments were solids and the top segment was a mixture of supernatant fluid and solids. Chemical and physical properties of interest to retrieval were obtained (e.g., shear strength on each segment; density, percent water, percent solids, and percent oxides [pyrolysis at 1050 °C] on the core composite; and yield strength and shear stress [1:1 diluted composite]).

Detailed chemical analyses were obtained on the composited samples. The composited solids (data also summarized in Castaing [1995]) had a density of 1.4 g/mL, contained about 55% water as weight loss, and had a pH of 9.5. The composited solids are TRU waste having greater than 100 nCi/g transuranics.

The solid composite was dominated by sodium, aluminum and iron with fluoride, chloride and nitrate as major anions (assay methods do not measure oxyhydroxides, which would have to be estimated). The supernatant fluids contained potassium, sodium and uranium. All anions (nitrate, nitrite) other than phosphate were found in moderate quantities. The TOC (dry weight basis) was 0.83%.

The supernate is rich in cesium 137, while the solids contained appreciable insoluble cesium (associated with silicate) and a limited amount of strontium 90.

More recent core samples and grab samples from tank AY-102 have been obtained, as well as samples associated with raising the pH of the waste to avoid undue corrosion to the tank. When completed, the sampling event results will be incorporated into the tank characterization database.

C-106 - Worst-Case Assay Based Information

Highest TOC value in liquid = 20,020 mg/L supernate, maximum density = 1.22

Calculation: 20,020 mg/L ÷ 1,000 = 20.020 mg/mL ÷ 1.22 mg/mL (density) = 16.409 mg/g (x 100 and ÷ 1000) = 1.6% TOC wet basis or (assume 60% liquid in supernate - rest is solids). This would result in a dry weight basis of 4.0% dry weight basis.

C-106 - Average Case Assay Based Information

Average TOC value in liquid 11,260 mg/L supernate (Max) d = 1.22

Calculation: 11,260 mg/L ÷ 1,000 = 11.260 mg/mL ÷ 1.22 mg/mL (density) = 9.230 mg/g (x 100 and ÷ 1,000) = 0.9% TOC wet basis or (assume 60% liquid in supernate - rest is solids) ~2.3% dry weight basis.

High TOC value in composited solids 4,620 mg/l supernate (Max) d = 1.4

Calculation: 4,620 mg/kg ÷ 1,000 = 4.620 mg/g (x 100 and ÷ 1,000) = 0.46% TOC wet basis or 0.84% dry weight basis.

The only waste associated with high organics, based on flow sheet analysis, would be the wastes transferred to tank C-106 from B Plant. Only BL wastes should have contained organic complexants. Agnew (1995) estimated 0.12 mol/L citrate in the waste, which he associated with the BL waste estimating the TOC concentration to be 1.3 percent maximum as added to the tank. However, the B Plant flow sheet indicated that most of the citrate in the waste stream was destroyed by the B Plant evaporator.

If our model of the behavior of complexants in a high-temperature radiation field is accurate, then these conditions should have resulted in low energy waste with the water containing appreciable quantities of sodium oxalate. This insoluble materials would have been diluted during waste compositing, resulting in the low TOC values observed.

APPENDIX A.5

PRESENCE OF BIS (2-ETHYLHEXYL) PHOSPHATE-RELATED MATERIALS IN OTHER TANKS

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APPENDIX A.5

PRESENCE OF BIS (2-ETHYLHEXYL) PHOSPHATE-RELATED MATERIALS IN OTHER TANKS

Preliminary Evaluation of C-103 Samples For Phosphate Esters Related To D2EHP

Sample C-103 94-02002 X12 (received 1994) was retrieved from storage and a 30-mg aliquot taken of the organic layer present in the sample. This aliquot was dissolved in 2 mL methylene chloride and treated with an additional 2 mL diethyl ether that had been previously saturated with hydrochloric acid. This treatment appears to quantitatively transform sodium bis(2-ethylhexyl) phosphate in the sample into the free acid form; as evidenced by copious amounts of white precipitate (NaCl) forming in the vessel. Some precipitation was noted upon addition of acidified ether. The aliquots were then reduced in volume to 100 mL, cooled, and 3 mL of an uncalibrated solution of ethereal diazomethane added. (Diazomethane is produced by stirring an ethereal slurry of N-methyl-N-nitrosourea over a 40-percent KOH solution reference (Fieser and Fieser 1967). The esterification is essentially complete immediately; the colored diazomethane is used to visually confirm the presence of excess diazomethane. To ensure complete conversion, the sample was left for one hour in the presence of excess diazomethane before analysis.

Prior GC/MS analysis has tentatively identified other materials related to bis(2-ethylhexyl) phosphate in tank C-106 samples. The mass spectral signature ions (both EI and CI modes) for this group of organic analytes makes identification of these moieties relatively straightforward. We have evidence of the following molecules being present in samples containing D2EHP: butyl bis(2-ethylhexyl) phosphate, tris(2-ethylhexyl) phosphate, and butyl (2-ethylhexyl) phosphate.

GC analysis was done using an HP 5890™ GC (FID) equipped with a low-polarity, thin phase capillary column (HP-5, 30m x 0.32 mm x 0.25 mm). The temperature was ramped from 50° to 260° at 8°/min, and held at 260° for 5 minutes, affording an adequate separation of the analytes previously observed in tank C-103 floating layer materials.

Inspection of the chromatogram reveals the presence of butyl bis(2-ethylhexyl) phosphate (retention time 24.31 min) and tris(2-ethylhexyl) phosphate (retention time 27.13 min) only. There does not appear to be an appreciable amount of D2EHP (retention time 22.2 min) in this sample. The ratios of these two materials, relative to each other, is similar to that observed in the tank C-106 analysis. The remainder of the chromatogram resembles the results previously reported by Pool and Bean (1994).

Unfortunately, standard materials are not available for butyl bis(2-ethylhexyl) phosphate (BuD2EHP) or tris(2-ethylhexyl) phosphate (T2EHP) at this time; the response observed for the analyte used for C-106 analysis (D2EHP) was used to calculated these minor components.

The resulting quantitation for these materials (per gram of sample) is as follows:

Component	mg/g amt.	mg Carbon/g amt.
BuD2EHP	0.003	0.0017
T2EHP	0.0005	0.0003

These materials comprise trace components in the mix of TBP and normal paraffinic hydrocarbons found in the C-103 matrix. By comparison, the TBP component has a FID response 50 times as large. In essence, the combination of these two components cannot represent more than 1 percent of the total carbon present in the sample.

It is significant to note the presence of BuD2EHP and T2EHP in these samples in the apparent absence of D2EHP. The presence of butylated species is highly indicative of trans-esterification from TBP or capture of butanol in the sample matrix over the life of the sample. These materials do not appear to be artifacts of sample preparation or analysis. An additional derivatization is warranted to determine if there were some reason for incomplete or inadequate derivatization of this sample.

In the original PNNL analytical scheme, the chemists were tasked with addition of diazomethane to the oil; Dr. Campbell of PNNL recalls a similar result. It is possible that the C-103 aqueous layer may contain D2EHP as the soluble sodium salt; however, this would appear to be unlikely owing to the near absence of D2EHP in the floating layer materials.

If funding permits, the recent samples of sludge from cores of C-103 will be speciated to see whether they contain, by analogy with C-106, appreciable amounts of materials derived from bis(2-ethylhexyl) phosphoric acid. Analytical requirements for speciation of some organics associated with sludge are also being added to the screening DQO, which is undergoing revision.

APPENDIX A.6

CALCULATION OF AMOUNT OF DISSOLVED SOLIDS

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APPENDIX A.6

CALCULATION OF AMOUNT OF DISSOLVED SOLIDS

Assumptions:

Interstitial liquor is 78.56% by weight water. (From Table 8-3)
Remainder of weight is dissolved solids.

Input Data

Not applicable.

Calculations

Weight % dissolved solids = 100 - 78.56 = 21.44%

21.44/78.56 = 0.273 grams of dissolved solids associated with every gram of water

Results

Weight % H_2O = 78.56 wt%

Weight % dissolved solids = 21.44 wt%

Each gram of water contains 0.273 grams of dissolved solids.

Conclusions

The results listed above will be utilized in other calculations.

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APPENDIX A.7

DISSOLUTION CALCULATIONS BASED ON LUMETTA

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APPENDIX A.7

DISSOLUTION CALCULATIONS BASED ON LUMETTA

Assumptions

The interstitial liquor is 78.56% water (Table 8-3)

Input Data

The following data comes from Figure 2.1 in the Lumetta (1996) document. The data will be followed with location of that number on Table 8-5.

15.14 g C-106 sludge (Column Start; Row Sludge)

28.8 g Water used with the sludge above to make a mixture.

4.76 g Wt. Sludge Solids (Column Leaching; Row Total Solids)

2.24 g slurry Sample B (Column Sample B; Row Mixture)

4.45 g slurry Sample B1 (Column Sample B1; Row Mixture)

0.65 g slurry Sample C (Column Sample C; Row Mixture)

0.46 g slurry Sample D (Column Sample D; Row Mixture)

From sample B

0.772 g sludge initially (Column Sample B; Row Sludge)
0.295 g dried solids (Column Sample B; Row Total Solids)

From Sample B1

1.529 g sludge (Column Sample B1; Row Sludge)
0.587 g solids (Column Sample B1; Row Total Solids)
0.243 g washed solids (Column Sample B1; Row Undissolved Solids)

From the end of the leaching step

1.651 g dry solids (Column Leaching; Row Undissolved Solids)

Calculations

Calculate the mass of the mixture of the original sludge and water.

15.14 g + 28.8 g = 43.94 g (Column Start; Row Mixture)

Calculate the mass of the mixture which went to leaching. This was done be subtracting what went elsewhere (Samples B, B1, C, and D) from the original mass.

43.94 - 2.24 - 4.45 - 0.65 - 0.46 = 36.14 g (Column Leaching; Row Mixture)

Calculate the mass of sludge for each cell in the Row labeled Sludge. First calculate the sludge weight of each g of mixture.

15.14 g sludge/43.94 g mixture = 0.344 g sludge/g mixture

This ratio was then multiplied times the grams of mixture which went into the various samples. For example Sample B:

2.24 g mixture * 0.344 g sludge/g mixture = 0.771 g sludge

This is within roundoff error of the value 0.772 g sludge which is given by Lumetta.

Row labeled Sludge was completed using the step above.

Sample B was dried in an oven until constant weight. The remaining weight represents the amount of solids, both dissolved and undissolved, which were in the sludge. This is labeled total solids. To fill in the row labeled Total Solids the following calculations were made based on the information from Sample B.

0.295 g total solids/0.772 g sludge = 0.382 g total solids/g sludge

Using Sample B1 as an example:

1.529 g sludge*0.382 g total solids/g sludge = 0.58 g total solids

Using Leaching:
12.45 g sludge*0.382 g total solids/g sludge = 4.76 g total solids

This is the value given by Lumetta for the total solids so the method checks with his information.

The total solids contain both undissolved solids and dissolved solids which are in the interstitial liquor. To differentiate between dissolved solids and undissolved solids, the

percent moisture from the intersticial liquor is necessary. From Section 2.3.3, the wt% moisture in intersticial liquor is 78.56% which implies that there is 21.44 wt% dissolved solids.

21.44/78.56 = 0.273 g dissolved solid/g water

From above, there is 0.382 g total solids per gram sludge. This implies that there is 1 - 0.382 = 0.618 g water per gram of sludge.

$$\frac{0.618\ g\ water}{g\ sludge} \times \frac{0.273\ g\ diss.\ solids}{g\ water} = 0.169\ g\ diss.\ solids/g\ sludge \qquad (2)$$

This is used to calculate the amount of dissolved solids in each column. Using Sample B as an example:

0.772 g sludge * 0.169 g dissolved solids/g sludge = 0.13 g dissolved solids

The remaining row is filled in with similar means.

Sample B1 was washed with 0.01 M NaOH solution. This is enough caustic to prevent solids from dissolving due to a pH change but still represent what might be expected from the sluicing activity. The amount of undissolved solids which dissolved can be calculated by:

100*(1 - 0.243/0.326) = 25.5 %

The leaching study used two batches of about 3 M NaOH solution followed by three washes with a solution 0.01 M NaOH and 0.01 M $NaNO_2$. A similar calculation can be made.

Results

Table 8-5 in the document is a summary of the calculations made in this appendix.

Conclusions

This study shows that the sludge is only about 21% undissolved solids and about 62% water. About 25% of the undissolved solids may dissolve in the rather dilute waste being used for sluicing.

Reference

Lumetta, G. J., M. J. Wagner, F. V. Hoopes, and R. T. Steele, 1996, *Washing and Caustic Leaching of Hanford Tank C-106 Sludge*, PNNL-11381, Pacific Northwest National Laboratory, Richland, Washington.

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APPENDIX A.8

HEAT LOAD ADJUSTMENT FOR RADIOLOGICAL DECAY

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APPENDIX A.8

HEAT LOAD ADJUSTMENT FOR RADIOLOGICAL DECAY

Assumptions

The heat is proportional to the radioactive decay.

Strontium-90 decays with about 40% more heat than cesium-137.

There appears to be more strontium-90 than cesium-137 in the waste. Therefore, the strontium-90 provides the heat.

Heat rate in C-106 was 132,000 Btu/hr in 1994 and will be decayed to 1997 or 3 years.

Input

Strontium-90 has a 28.1 year half life. (Benedict 1981)
Cesium-137 has a 30. year half life. (Benedict 1981)

Calculations

Based on a 28.1 year half life.

Decay constant = ln(2)/28.1 = 0.025

Heat now = $132{,}000 * e^{-0.025*3} = 132{,}000 * 0.93$

Heat now = 123,000 Btu/hr

Results

The best basis heat is 123,000 Btu/hr.

Benedict, M., T. H. Pigford, H. W. Levi, Nuclear Chemical Engineering, McGraw-Hill Book Company, 2nd Edition, 1981.

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APPENDIX A.9

SETTLING TEST FLUFF FACTOR CALCULATIONS

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APPENDIX A.9

SETTLING TEST FLUFF FACTOR CALCULATIONS

Assumption

The sludge density is 1.5 g/mL

Input Data

Data is from Section 5.

9.96 g Sludge

Final volume from charts: 9 ml

Calculations

Initial volume:

9.96 g/1.5 g/mL = 6.65 mL

Fluff Factor:

9 mL/6.65 mL = 1.35

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APPENDIX A.10

HEATS OF SOLUTIONS

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APPENDIX A.10

HEATS OF SOLUTIONS

Assumptions:

1 liter of water is approximately 1 kilogram.

Molecular Weight of Water is 18 g/mole

Heat capacity (Cp) of the resulting brine is equivalent to water. This assumption can be modified if it is shown that a large temperature change happens. At most, the brine will not be different from water by a factor of 2 and generally tends to be less than water.

Cp = 1 cal/g*K = 4.187E-03 kJ/g*K

One mole of solids will dissolve in approximately one liter of liquid. This is conservative; most likely the final concentration will be much less than 1 mole/liter. However, this is a worst case situation for the dissolution. A lower concentration will mean slightly more energy change but a much larger mass of solution. In net, this means a lower final temperature.

Input Data

The heats of formation with the proper amounts of water are listed below. The data came from the reference given.

Table E-1. Thermodynamic Values for the Dissolution of Solids (Wagman 1982).

Species	State	Δh_f, kJ/mole
$NaNO_2$	crystal	-358.65
$NaNO_2$	in 50 mole H_2O	-346.14
Na_2CO_3	crystal	-1130.68
Na_2CO_3	in 50 mole H_2O	-1159.554

Calculations

Number of moles of water in 1 kilogram of water:

$$\frac{1000\ g}{18\ \frac{g}{mole}} = 55.6\ mole \tag{3}$$

Therefore, one mole salt in 50 moles water is approximately 1 M.

The heat of reaction is the heat of formation of the products minus the heat of formation of the reactants.

Heat of solution for $NaNO_2$ = -346.14 - (-358.65) = 12.51 kJ/mole $NaNO_2$

Heat of solution for Na_2CO_3 = -1159.554 - (-1130.68) = -28.874 kJ/mole Na_2CO_3

The heat of solution can be used to estimate the temperature change by:

$$\Delta H = mass \times Cp \times \Delta T \tag{4}$$

This can be solved for the change in temperature as:

$$\Delta T = \frac{\Delta H}{mass \times Cp} \tag{5}$$

For the purposes of this calculation the mass will be taken as 1000 grams and the heat capacity, Cp, will be taken as that of water.

Temperature change for $NaNO_2$:

$$\Delta T = \frac{12.51\ kJ/mole}{1000\ g \times 4.187E{-}3\ kJ/g\ K} = 3\ K \tag{6}$$

Temperature change for Na_2CO_3:

$$\Delta T = \frac{-28.874}{1000\ g \times 4.187E{-}3\ kJ/g\ K} = -6.9\ K \tag{7}$$

Results

The convention is that a positive heat of solution will need that much heat taken into the system. A negative heat of solution will evolve or give up that heat up to the surroundings. The heat of solutions show that dissolving sodium nitrite is endothermic and will take heat in and dissolving sodium carbonate is exothermic and will give off heat.

This means that dissolving one mole of sodium nitrite in one kilogram of water will lower the temperature by 3 K. Dissolving one mole of sodium carbonate in one kilogram of water will increase in temperature by about 7 K. In actual fact, both will be dissolving in the same water and will tend to counter act each other.

Conclusions

The above calculations are for a worst case situation where the final brine would end up about 1 M in either sodium nitrite or sodium carbonate. In actual sluicing, the sodium nitrite and sodium carbonate would be much more dilute. This would mean that the heat would be spread over a much larger mass of solution and the temperature changes would be much smaller than calculated above.

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APPENDIX A.11

HEATS OF DILUTION CONSIDERATIONS

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APPENDIX A.11

HEATS OF DILUTION CONSIDERATIONS

Assumptions

The supernate from AY-102 will be 0.5 M in hydroxide. This may be less in actual practice.

1 liter of water is approximately 1 kilogram.

Molecular Weight of Water is 18 g/mole

Heat capacity of resulting brine is equivalent to water. This assumption can be modified if it is shown that a large temperature change happens. At most, the brine will not be different from water by a factor of 2 and generally tends to be less than water.

Cp = 1 cal/g*K = 4.187E-03 kJ/g*K

The supernate from AY-102 will be diluted somewhat with liquid in C-106. For this calculation, it is assumed that approximately two liters of AY-102 will be mixed with approximately one liter of C-106. The result will be approximately 3 liters.

Input Data

The heats of formation with the proper amounts of water are listed below. The data came from the reference given.

Table F-1
Thermodynamic Values for the Dissolution of NaOH

Species	State	Δh_p kJ/mole (Wagman 1982)
NaOH	in 100 mole H_2O	-469.646
NaOH	in 150 mole H_2O	-469.621

Calculations

Number of moles of water in 1 kilogram of water is 55.6 moles from above.

If the NaOH is 0.5 moles per liter, then that is equivalent to 1 mole NaOH in two liters. Two liters of water is equivalent to 112 moles. For this calculation, the value for 1 mole NaOH with 100 moles of water is adequate.

The AY-102 waste will be diluted somewhat with the liquid in C-106. It is assumed that the 1 mole of NaOH per 100 moles of water will be diluted to 1 mole of NaOH per 150 moles of water.

Heat of Dilution of NaOH = -469.621-(-469.646) = 0.025 kJ/mole of NaOH

The heat of solution can be used to estimate the temperature change by:

$$\Delta H = mass \times Cp \times \Delta T \tag{8}$$

This can be solved for the change in temperature as:

$$\Delta T = \frac{\Delta H}{mass \times Cp} \tag{9}$$

For the purposes of this calculation the mass will be taken as 3000 grams (approximately 3 liter) and the heat capacity, Cp, will be taken as that of water.

Temperature change for NaOH:

$$\Delta T = \frac{0.025\ kJ/mole}{3000\ g \times 4.187E\text{-}3\ kJ/g\ K} = 0.002\ K \tag{10}$$

Results

The convention is that a positive heat of solution will need that much heat taken into the system. A negative heat of solution will evolve or give up that heat up to the surroundings. The heat of solutions show that diluting sodium hydroxide is endothermic in this concentration range and will take heat in.

This means that diluting one mole of sodium hydroxide in two kilogram of water by adding an additional kilogram of water will lower the temperature by 0.002 K.

Conclusions

The above calculations are for a worst case. The heat of dilution resulting from this process will result in an undetectable temperature change.

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