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ENGINEERING CHANGE NOTICE

Page 1 of 2

1 ECN 657277

Proj ECN

2 ECN Category (mark one) Supplemental <input type="checkbox"/> Direct Revision <input checked="" type="checkbox"/> Change ECN <input type="checkbox"/> Temporary <input type="checkbox"/> Standby <input type="checkbox"/> Supersedure <input type="checkbox"/> Cancel/Void <input type="checkbox"/>	3 Originator's Name Organization MSIN and Telephone No Duc M Nguyen Data Development and Interpretation R2-12 372-3042	4 USQ Required? <input checked="" type="checkbox"/> Yes <input type="checkbox"/> No USQ TF 99-412	5 Date 01/26/00	
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12a Modification Work <input type="checkbox"/> Yes (fill out Blk 12b) <input checked="" type="checkbox"/> No (NA Blks 12b 12c, 12d)	12b Work Package No N/A	12c Modification Work Complete N/A Design Authority/Cog Engineer Signature & Date	12d Restored to Original Condition (Temp or Standby ECN only) N/A Design Authority/Cog Engineer Signature & Date
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13a Description of Change
Complete revision

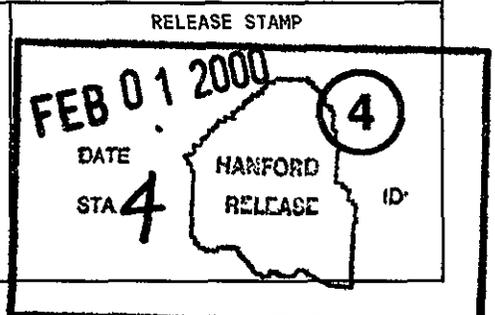
13b Design Baseline Document? Yes No

14a Justification (mark one)

Criteria Change <input checked="" type="checkbox"/>	Design Improvement <input type="checkbox"/>	Environmental <input type="checkbox"/>	Facility Deactivation <input type="checkbox"/>
As Found <input type="checkbox"/>	Facilitate Const <input type="checkbox"/>	Const Error/Omission <input type="checkbox"/>	Design Error/Omission <input type="checkbox"/>

14b Justification Details
This ECN incorporates lessons learned from the catch tank 241-ER-311 vapor sampling activities

15 Distribution (include name MSIN and no of copies)
See attached distribution



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16 Design Verification Required <input type="checkbox"/> Yes <input checked="" type="checkbox"/> No	17 Cost Impact <table style="width: 100%;"> <tr> <td style="text-align: center;">ENGINEERING</td> <td style="text-align: center;">CONSTRUCTION</td> </tr> <tr> <td>Additional <input type="checkbox"/> \$</td> <td>Additional <input type="checkbox"/> \$</td> </tr> <tr> <td>Savings <input type="checkbox"/> \$</td> <td>Savings <input type="checkbox"/> \$</td> </tr> </table>	ENGINEERING	CONSTRUCTION	Additional <input type="checkbox"/> \$	Additional <input type="checkbox"/> \$	Savings <input type="checkbox"/> \$	Savings <input type="checkbox"/> \$	18 Schedule Impact (days) Improvement <input type="checkbox"/> Delay <input type="checkbox"/>
ENGINEERING	CONSTRUCTION							
Additional <input type="checkbox"/> \$	Additional <input type="checkbox"/> \$							
Savings <input type="checkbox"/> \$	Savings <input type="checkbox"/> \$							

19 Change Impact Review Indicate the related documents (other than the engineering documents identified on Side 1) that will be affected by the change described in Block 13 Enter the affected document number in Block 20

SDD/DD <input type="checkbox"/>	Seismic/Stress Analysis <input type="checkbox"/>	Tank Calibration Manual <input type="checkbox"/>
Functional Design Criteria <input type="checkbox"/>	Stress/Design Report <input type="checkbox"/>	Health Physics Procedure <input type="checkbox"/>
Operating Specification <input type="checkbox"/>	Interface Control Drawing <input type="checkbox"/>	Spares Multiple Unit Listing <input type="checkbox"/>
Criticality Specification <input type="checkbox"/>	Calibration Procedure <input type="checkbox"/>	Test Procedures/Specification <input type="checkbox"/>
Conceptual Design Report <input type="checkbox"/>	Installation Procedure <input type="checkbox"/>	Component Index <input type="checkbox"/>
Equipment Spec <input type="checkbox"/>	Maintenance Procedure <input type="checkbox"/>	ASME Coded Item <input type="checkbox"/>
Const Spec <input type="checkbox"/>	Engineering Procedure <input type="checkbox"/>	Human Factor Consideration <input type="checkbox"/>
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OM Manual <input type="checkbox"/>	Operational Safety Requirement <input type="checkbox"/>	ICRS Procedure <input type="checkbox"/>
FSAR/SAR <input type="checkbox"/>	IEFD Drawing <input type="checkbox"/>	Process Control Manual/Plan <input type="checkbox"/>
Safety Equipment List <input type="checkbox"/>	Cell Arrangement Drawing <input type="checkbox"/>	Process Flow Chart <input type="checkbox"/>
Radiation Work Permit <input type="checkbox"/>	Essential Material Specification <input type="checkbox"/>	Purchase Requisition <input type="checkbox"/>
Environmental Impact Statement <input type="checkbox"/>	Fac Proc Samp Schedule <input type="checkbox"/>	Tickler File <input type="checkbox"/>
Environmental Report <input type="checkbox"/>	Inspection Plan <input type="checkbox"/>	<input type="checkbox"/>
Environmental Permit <input type="checkbox"/>	Inventory Adjustment Request <input type="checkbox"/>	<input type="checkbox"/>

20 Other Affected Documents (NOTE Documents listed below will not be revised by this ECN) Signatures below indicate that the signing organization has been notified of other affected documents listed below

Document Number/Revision	Document Number/Revision	Document Number Revision
N/A		

21 Approvals

	Signature	Date	Signature	Date
Design Authority			Design Agent	
Cog Eng D M Nguyen	<i>Duc M Nguyen</i>	<u>1/31/00</u>	PE	_____
Cog Mgr J G Field	<i>J G Field</i>	<u>1/31/00</u>	QA	_____
QA W L Adams	<i>W L Adams</i>	<u>1/31/00</u>	Safety	_____
Safety			Design	_____
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D D Wanner	<i>D D Wanner</i>	<u>1/31/00</u>		_____

DEPARTMENT OF ENERGY
 Signature or a Control Number that tracks the Approval Signature
ADDITIONAL _____

DISTRIBUTION SHEET

To Distribution	From Data Development and Interpretation	Page 1 of 1 Date 01/26/00
Project Title/Work Order HNF-4082 Rev 3 Test Plan for Measuring Ventilation Rates and Combustible Gas Levels in RPP Active Catch Tanks		EDT No N/A ECN No ECN-657277

Name	MSIN	Text With All Attach	Text Only	Attach / Appendix Only	EDT/ECN Only
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Test Plan for Measuring Ventilation Rates and Combustible Gas Levels in RPP Active Catch Tanks

D M Nguyen
CH2M HILL Hanford Group Inc Richland WA 99352
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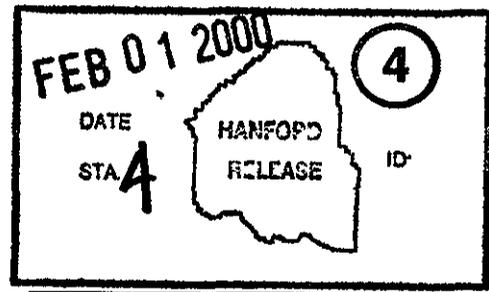
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HNF-4082
Revision 3

**TEST PLAN FOR MEASURING VENTILATION RATES AND
COMBUSTIBLE GAS LEVELS
IN RIVER PROTECTION PROJECT ACTIVE CATCH TANKS**

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CH2M HILL Hanford Group Inc

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LIST OF TERMS

CGM	combustible gas monitor
CPO	Characterization Project Operations
DB	diversion box
DQO	data quality objective
gal	gallon
HEPA	high-efficiency particulate air (filter)
LFL	lower flammability limit
OVM	organic vapor monitor
PNNL	Pacific Northwest National Laboratory
ppm	parts per million
%	percent
psig	pounds per square inch gauge
QA	quality assurance
QC	quality control
RPP	River Protection Project
SAP	sampling and analysis plan
WSCF	Waste Sampling and Characterization Facility

TEST PLAN FOR MEASURING VENTILATION RATES AND COMBUSTIBLE GAS LEVELS IN RIVER PROTECTION PROJECT ACTIVE CATCH TANKS

1 0 PURPOSE AND SCOPE

The purpose of this data collection activity is to obtain data for a screening of combustible gases in catch tanks that are currently operated by the River Protection Project (RPP). The results will be used to support closure of the flammable gas unreviewed safety question for these facilities. The data collection will be conducted in accordance with the *Tank Safety Screening Data Quality Objective* (Dukelow et al. 1995).

Combustible gas, ammonia, and organic vapor levels in the headspace of the catch tanks will be field-measured using hand-held instruments. If a combustible gas level measurement in a tank exceeds an established threshold, vapor grab samples (i.e., Hoke¹ and SUMMA¹) will be collected for laboratory analysis. In addition, ventilation rates of some catch tanks will be determined using the tracer gas injection method to evaluate removal of flammable gas by air flowing through the tanks.

This test plan identifies the field tests, sample collection, laboratory analysis, quality assurance, and reporting objectives for this data collection effort. The plan also provides step-by-step direction for field measurement of combustible gas concentrations and determination of ventilation rates.

2 0 BACKGROUND

In general, RPP catch tanks were designed to collect leaks, spills, condensation, and drainage that might occur during operation of tank farm diversion boxes (DBs), valve pits, and pipeline encasement. Volumes and constituents of the material in these tanks vary depending on the operations of the tank farm facilities. Most of these tanks are expected to contain small amounts of organic chemicals and low levels of radioactivity. Thus, flammable gases could be generated and accumulated in these tanks. A list of the RPP active catch tanks is shown in Table 2-1. A description of tank capacity, material of construction, and ventilation equipment is also provided.

¹ Hoke and SUMMA are registered trademarks of Hoke Incorporated of Cresskill, NJ and Moetrics Inc. of Cleveland, OH, respectively.

Table 2-1 River Protection Project Catch Tanks (2 Sheets)

Item No	Tank ID No	Historical Usage	Nominal Capacity (gal)	Construction Material	Ventilation Equipment
1	241-A 302A	Drainage from DB 241-A-151	8,400 gal	Carbon steel	None
2	241-A-350	Drainage from A Farm	800 gal	Stainless steel	Dip tubes ¹
3	241 A-417	Drainage from 241 AY/AZ vent	44,000 gal	Concrete vault with carbon steel liner	Breather filter and dip tubes
4	241-AX-152	Drainage from AX 152 diversion station, DB 241-AX-155, AY-501, and 702-A seal pot	11,000 gal	Concrete vault with steel liner	None (Known to benefit indirectly from 702-AZ vent system)
5	241-AZ 151	Drainage from DB 241 AZ-152, AZ vent Loop seals, leak detection pits, 801 AZ Instrumentation Building and precipitation/runoff	12,000 gal	Concrete vault with carbon steel liner	Yes (may benefit indirectly from 702 AZ system)
6	241-AZ-154	Drainage from AZ-101 and AZ-102 steam coils and precipitation/runoff	900 gal	Concrete vault with carbon steel liner	None
7	241-ER-311	Drainage from DBs 151-ER and 152-ER	18,000 gal	Carbon steel	None
8	204 AR-TK-1	Drainage from the 204-AR Waste Unloading Facility unloading canyon	1,500 gal	Stainless steel	Exhauster
9	241-S-304	Drainage from DB 241-S-151 and precipitation/runoff	6,000 gal	Carbon steel	Breather filter
10	241-TX-302C	Drainage from DB 241-TX-154 and precipitation/runoff	18,000 gal	Carbon steel	None

Table 2-1 River Protection Project Catch Tanks (2 Sheets)

Item No	Tank ID No	Historical Usage	Nominal Capacity (gal)	Construction Material	Ventilation Equipment
11	241-U-301B	Drainage from DBs 241-U-151, 241-U-152, 241-U-153, 241-U-252	36,000 gal	Concrete (unlined)	None
12	241-UX-302A	Drainage from DB 241-UX-154, 291 U stack, and precipitation/runoff	18,000 gal	Carbon steel	None
13	241 EW 151	Drainage from the former cross-site transfer vent station	800 gal	Carbon steel	Breather filter

¹Dip tubes are a liquid level measurement device based on differential air pressure. Air is forced through the tubes at 20 psig. The use of dip tubes provides a small ventilation rate.

3 0 OVERALL DESCRIPTION OF TEST

The flammable gas content of each catch tank and the ventilation rates in two of the tanks will be measured. Gas levels will be measured in the field using portable or hand-held gas meters. Ventilation rates will be determined using the tracer gas injection method. These methods have been used successfully for waste tanks and double-container receiver tanks (Bauer 1998 and Bauer and Hedengren 1999). The gas level and ventilation rate measurement methods are specified in Table 3-1.

Table 3-1 Data Needs and Associated Measurement Methods

Data Needs	Measurement Methods
Combustible gas level	Combustible Gas Monitor (CGM)
Ammonia	Calorimetric (Draeger) Tubes
Organic vapor	Organic Vapor Monitor
Ventilation Rate	Tracer gas (helium) injection

The appropriate tank access point (e.g., riser) and sample locations (i.e., depths) within the vapor space of each catch tank will be determined during the planning phase. Also, the sampling system must be purged to assure that the sample system tubing is filled only with gas from the headspace. The required duration for purging depends on the length of the system tubing. The sampling cognizant engineer shall determine the tank access point, sample locations, and the appropriate purging duration for each catch tank. The information shall be specified in the field work package.

Combustible gas, ammonia, and organic vapor concentrations will be measured three times at each sampling location. If a combustible (flammable) gas level measurement exceeds 25% of the lower flammability limit (LFL), Hoke™ and SUMMA™ samples will be collected for laboratory analysis. Also, for tanks with no known path for ventilation, the tank access shall be reconfigured to allow ventilation of the flammable gas instead of restoring the tank access point to the initial condition when sampling is complete (e.g., installing a flange or bag with air filter). Step-by-step directions for taking the field measurements and the grab samples are provided in Section 13.

The ventilation rates in the RPP active catch tanks are not known and are expected to vary. Seven of the thirteen tanks were installed with equipment that provides various degrees of ventilation. The equipment includes breather filters, dip tubes, and exhausters. The other tanks do not have installed ventilation equipment but some may be connected to other systems that have either active or passive ventilation. Two tanks, 241-AX-152 and 241-EW-151, have been selected for tracer gas injection to provide an indication of the range of gas removal rate due to airflow through the tanks.

Helium will be injected into the headspace of a designated tank through an assigned injection point as specified by the sampling cognizant engineer. The sampling cognizant engineer will specify the required volume of helium based on measured decrease in pressure of the gas supply. Two SUMMA™ samples will be collected after allowing the helium to disperse evenly throughout the tank headspace. One additional set of two SUMMA™ samples (and an optional third set of samples) will be collected at a time interval to be specified by the sampling cognizant engineer. These SUMMA™ samples will be analyzed only for helium concentration. Ventilation rate in the tank will be calculated based on the measured decay in helium concentration between these points in time. The calculation method is derived and described in Appendix A.

Note that the tests described in this plan will provide screening data only. A comprehensive evaluation of potential variables (i.e., factors that could affect combustible gas generation or retention in a catch tank), such as volume, composition, and temperature of the waste and atmospheric conditions, etc., are outside the scope of this effort. However, these data will be recorded if available.

4 0 EXPECTED RESULTS

For each catch tank, combustible gas level (in %LFL), ammonia concentration (in parts per million [ppm]), and organic vapor level (in ppm) will be measured and reported. The levels of these gases and vapors in the catch tanks are expected to be very low.

Tank 241-AX-152 headspace is indirectly connected to the 702-AZ ventilation system and, thus, is considered an actively ventilated tank. This tank is expected to have a much higher ventilation rate than that of the passively ventilated tank 241-EW-151.

5 0 TEST EQUIPMENT AND MATERIAL

Test equipment needed for each catch tank include:

- Combustible Gas Meter (CGM) for measuring combustible gas level,
 - Organic Vapor Monitor (OVM) for measuring organic vapor concentration,
 - Calorimetric (Draeger) tubes for measuring ammonia concentration, and
 - Two Hoke™ samplers and two SUMMA™ canisters (with the necessary tritium traps and canister particulate air filters) to collect gas samples in the event the combustible gas level in a tank exceeds the established threshold.
- A bag or flange with high-efficiency particulate air (HEPA) filter for venting the tank after sampling if flammable gas concentration exceeds 25% of the LFL. The venting device is needed only for tanks with no known path for ventilation (i.e., no exhausters, breather filters, or dip tubes).

In addition, tracer gas injections for tanks 241-AX-152 and 241-EW-151 will require the following equipment:

- Tracer gas injection and sampling systems as shown in Figures 1 and 2, respectively,
- A supply of bottled helium gas,
- SUMMA™ canisters (with canister particulate air filters),
- A tritium trap for each SUMMA™ canister and canister particulate air filters for radiation screening, and
- Temperature gauges to measure ambient and helium gas bottle temperatures.

Spare equipment for contingency will be available as required by standard operating procedures (SOPs) for the instruments or as determined by the sampling cognizant engineer.

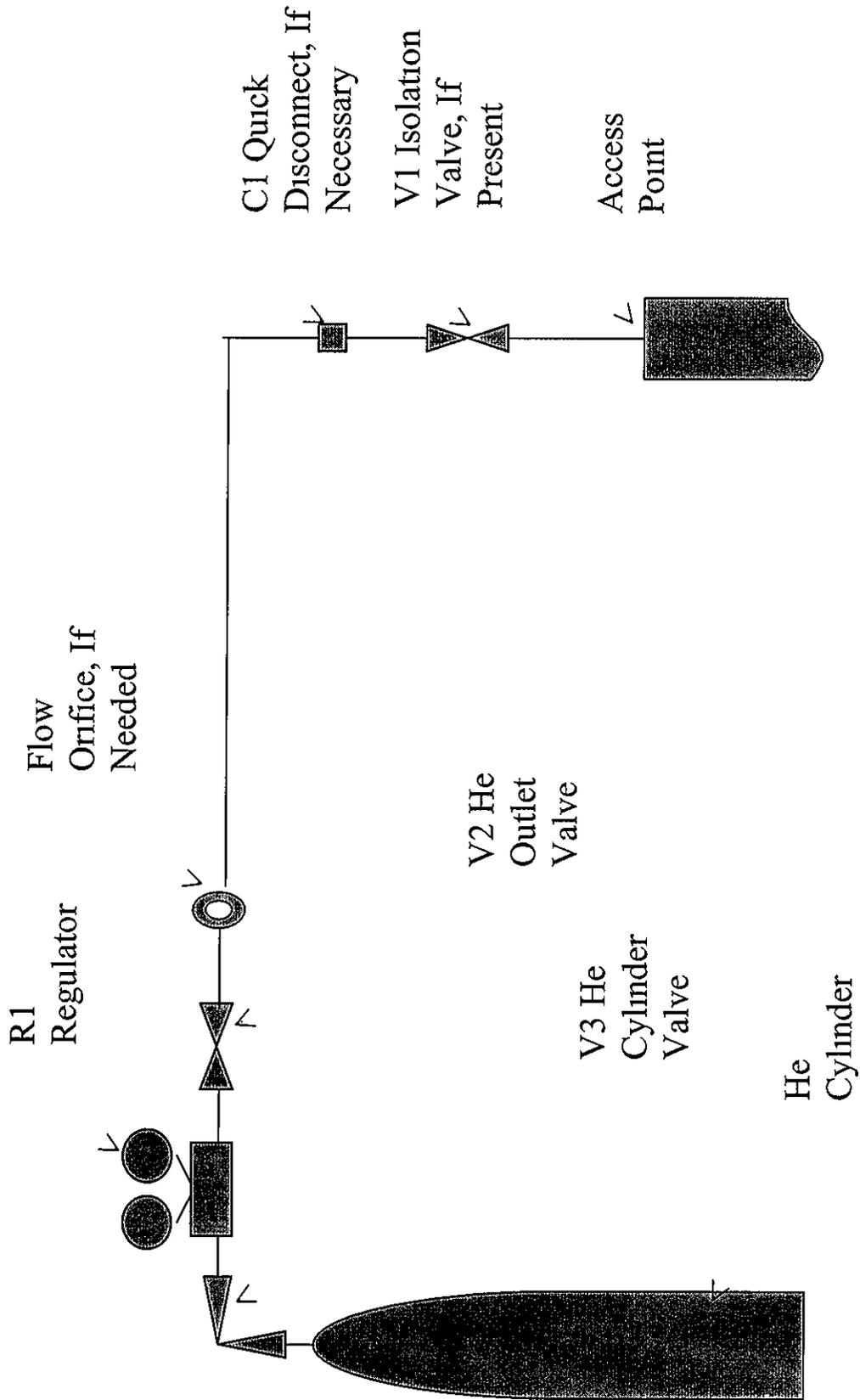


Figure 1. Helium Gas Injection System

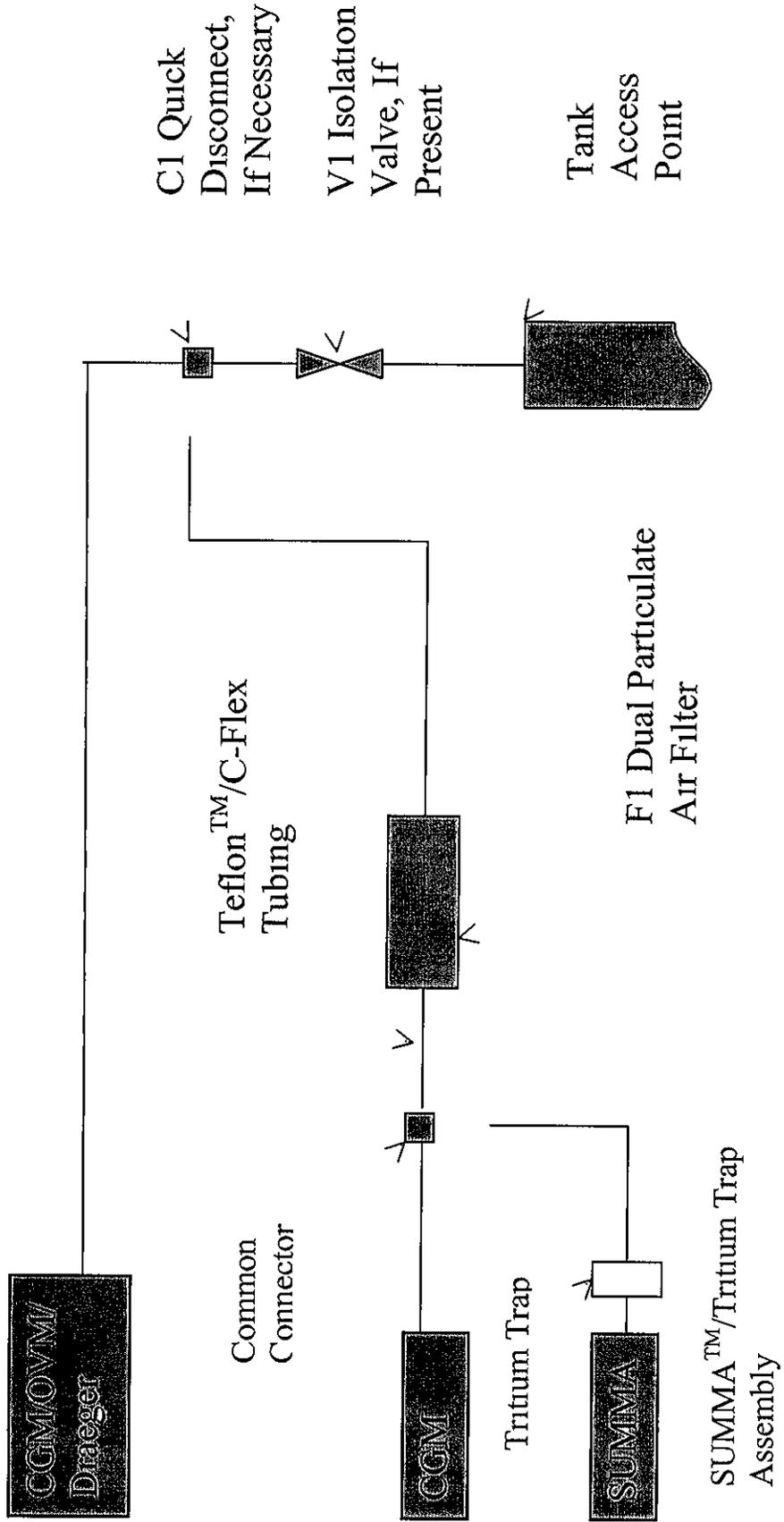


Figure 2 Sampling System

6 0 SAMPLE IDENTIFICATION

Each SUMMATM sample will be labeled with a unique identification number. This number will also be recorded in the appropriate box on the data sheet form (see Appendix B). Each sample identification number will have the following format:

VXXXXXX-YY-LLLL

Where,

V indicates that the sample is a vapor sample

XXXXXX indicates the tank number (e.g., UX302 or 0A350)

YY a two-digit sequential number (e.g., 01, 02, or 03). For samples used for tracer gas injection, the numbers are already specified on the data sheet.

LLLL a laboratory assigned code found on a tag attached to the SUMMATM canister.

If used, HokeTM samples shall be uniquely identified with the date, sequential numbers, and initials of the Industrial Hygiene and Safety (IH&S) technician.

Characterization Project Operations (CPO) shall initiate a chain-of-custody form for each tritium trap, HokeTM or SUMMATM sample collected. The sample number and location (e.g., riser and elevation) at which a grab sample was obtained shall be recorded. Also, pertinent sampling information (e.g., sampling problems) should be noted in the Comments section of the chain-of-custody form. The samples shall be shipped to the appropriate laboratory in accordance with the Job Control System (JCS) work package.

7 0 DATA REQUIREMENTS

7 1 REQUIREMENTS FOR FIELD DATA

Test data that will be required from field operations of the tracer gas injection system are identified in the data sheet shown in Appendix B. Anomalies and environmental conditions that could affect sampling results (e.g., usual odors, machinery in operation nearby, etc.) will be noted in the Comments/Observations section of the data sheet. Other data (combustible gas level, organic vapor and ammonia concentrations) shall be recorded as directed in the work packages.

7 2 REQUIREMENTS FOR LABORATORY DATA

Analytical requirements for the Hoke™ samples are specified in Table 7-1. The samples will be analyzed at the Pacific Northwest National Laboratory (PNNL) according to the procedure PNNL-98523-284 (current revision) (PNNL 1999a). Laboratory analysis shall be performed in accordance with the requirements in the Gas Analysis Task (Work Breakdown Structure 1.8) under the Flammable Gas Program.

Table 7-1 Required Analysis for Hoke™ Samples

Carbon Monoxide	Oxygen
Carbon Dioxide	Methane
Hydrogen	Nitrogen
Argon	Nitrous Oxide
Helium	Other Nitrogen Oxides
	Ammonia (estimated)

If data from the Hoke™ sample indicate that more extensive analyses (e.g., speciation of organic vapors) are needed, the SUMMA™ sample shall be analyzed at the Waste Sampling and Characterization Facility (WSCF) for components listed in Table 7-2. Organic analysis shall be performed per analytical procedure LA-523-404. Radiation screening of particulate filters shall be performed according to procedures LA-548-421 for total alpha, LA-508-415 for total beta, and LA-508-462 for gamma emitters. Tritium concentration in tritium traps shall be determined per LA-548-411 and LA-508-421.

It is anticipated that PNNL will analyze Hoke™ samples and WSCF will analyze SUMMA™ samples. In addition to these laboratories, other qualified laboratories may be selected by RPP Process Engineering to analyze the samples as necessary. All laboratories shall meet all the QA/QC requirements in this SAP.

Table 7-2 Suggested Analytical Methods and Laboratory Quality Control Requirements for SUMMA™ Samples (2 Sheets)

Analyte	Suggested Analytical Method	VPRQL ¹ (ppbv)	Precision (%RSD or %RPD) ²	Accuracy (% Recovery)
Freon 12	GC/MS ⁵	5 0	25	70 to 130
Methyl chloride	GC/MS ⁵	5 0	25	70 to 130
n-Butane	GC/MS ⁵	5 0	25	70 to 130
Ethyl chloride	GC/MS ⁵	5 0	25	70 to 130
Ethanol	GC/MS ⁵	5 0	25	70 to 130
Freon 11	GC/MS ⁵	5 0	25	70 to 130
Acetonitrile	GC/MS ⁵	5 0	25	70 to 130
Acetone	GC/MS ⁵	5 0	25	70 to 130
Furan	GC/MS ⁵	5 0	25	70 to 130
n-Pentane	GC/MS ⁵	5 0	25	70 to 130
2-Propanol	GC/MS ⁵	5 0	25	70 to 130
Dichloromethane	GC/MS ⁵	5 0	25	70 to 130
1-Propanol	GC/MS ⁵	5 0	25	70 to 130
2-Methyl-pentane	GC/MS ⁵	5 0	25	70 to 130
Propanenitrile	GC/MS ⁵	5 0	25	70 to 130
Butanal	GC/MS ⁵	5 0	25	70 to 130
1-Hexene	GC/MS ⁵	5 0	25	70 to 130
2-Butanone	GC/MS ⁵	5 0	25	70 to 130
n-Hexane	GC/MS ⁵	5 0	25	70 to 130
Chloroform	GC/MS ⁵	5 0	25	70 to 130
Tetrahydrofuran	GC/MS ⁵	5 0	25	70 to 130
1-Butanol	GC/MS ⁵	5 0	25	70 to 130
Benzene	GC/MS ⁵	5 0	25	70 to 130
Carbon tetrachloride	GC/MS ⁵	5 0	25	70 to 130
Butanenitrile	GC/MS ⁵	5 0	25	70 to 130
3-Methyl-hexane	GC/MS ⁵	5 0	25	70 to 130
2-Pentanone	GC/MS ⁵	5 0	25	70 to 130
n-Heptane	GC/MS ⁵	5 0	25	70 to 130
1,4-Dioxane	GC/MS ⁵	5 0	25	70 to 130
4-Methyl-2 pentanone	GC/MS ⁵	5 0	25	70 to 130
Toluene	GC/MS ⁵	5 0	25	70 to 130
2-Hexanone	GC/MS ⁵	5 0	25	70 to 130
n-Octane	GC/MS ⁵	5 0	25	70 to 130
Tetrachloroethylene	GC/MS ⁵	5 0	25	70 to 130
Chlorobenzene	GC/MS ⁵	5 0	25	70 to 130
Ethylbenzene	GC/MS ⁵	5 0	25	70 to 130
m,p-Xylene	GC/MS ⁵	5 0	25	70 to 130
3-Heptanone	GC/MS ⁵	5 0	25	70 to 130
2-Heptanone	GC/MS ⁵	5 0	25	70 to 130

Table 7-2 Suggested Analytical Methods and Laboratory Quality Control Requirements for SUMMA™ Samples (2 Sheets)

Analyte	Suggested Analytical Method	VPRQL ¹ (ppbv)	Precision (%RSD or %RPD) ²	Accuracy (% Recovery)
Cyclohexanone	GC/MS ⁵	5 0	25	70 to 130
Styrene	GC/MS ⁵	5 0	25	70 to 130
n Nonane	GC/MS ⁵	5 0	25	70 to 130
o-Xylene	GC/MS ⁵	5 0	25	70 to 130
1,1,2,2-Tetrachloroethane	GC/MS ⁵	5 0	25	70 to 130
2-Octanone	GC/MS ⁵	5 0	25	70 to 130
n-Decane	GC/MS ⁵	5 0	25	70 to 130
1,2,4-Trimethylbenzene	GC/MS ⁵	5 0	25	70 to 130

Notes

¹VPRQL Vapor Program Required Quantitation Limit

²RSD Relative Standard Deviation RPD Relative Percent Difference

³GC Gas Chromatography

⁴IC Ion Chromatography

⁵GC/MS Gas Chromatography/Mass Spectrometry

All sampling and analysis activities shall be performed in accordance with the quality assurance/quality control (QA/QC) requirements specified in this test plan. Data resulting from activities and conditions that do not conform to requirements specified in this test plan or references herein shall be controlled to prevent inadvertent use or flagged with appropriate cautions. Nonconforming sampling and analysis processes and information shall be identified, controlled, reported, and dispositioned as required by *Nonconforming Item Reporting and Control* (CHG 1999).

Laboratories performing analyses in support of this sampling and analysis plan (SAP) shall have approved and implemented quality assurance project plans. These QA plans shall meet the *Hanford Analytical Services Quality Assurance Requirements Document* (DOE 1998) minimum requirements for laboratory quality systems. The *PNNL QA Program for Conducting Analytical Work in Support of Regulatory Programs* (PNNL 1999b) and the *Waste Sampling and Characterization Facility Quality Assurance Program Plan* (Mezmarich 1999) specify the requirements for assuring the quality of sample analysis at PNNL and WSCF, respectively.

Quality control requirements shall be consistent with the specified analytical procedures and QA plans. The laboratories shall use calibration and calibration check standards appropriate for the analytical instrumentation being used (see DOE 1998 for definitions of QC samples and standards). The criteria presented are goals for demonstrating reliable method performance. It is understood that the laboratories will follow established internal protocols for addressing QC failures. If sample QC failures occur or if some analyses cannot be performed (e.g., because of insufficient sample or of matrix interference), analysts shall consult with RPP Process Engineering to determine the proper action. The performing laboratory should provide a suggested course of action at that time. All sample QC failures and limitations on the associated data shall be discussed in the narrative of the data report. Proper notification of all data not meeting QC requirements shall be included with the data.

8 0 EXCEPTIONS, CLARIFICATIONS, AND ASSUMPTIONS

The Tank Safety Screening Data Quality Objective (DQO) addresses three potential safety issues: ferrocyanide and organics, criticality, and flammable gas. Only the flammable gas objectives are applicable to this data collection activity.

A combustible gas meter will be used to measure the flammable gas level in the headspace of a catch tank. The CGM will be calibrated using pentane gas. Actual CGM readings will be adjusted to percent LFL of hydrogen using a pentane to hydrogen conversion value recommended by the manufacturer. The assumption in the conversion is that the combustibility of the headspace vapor is due only to hydrogen. However, the presence of other combustible gases and vapors such as ammonia and organics could affect the results. Testing has shown that the CGM readings are conservative for gas mixtures (i.e., the instrument reports a higher percent LFL than that actually present for the gas mixtures tested) (Wilkins and Bauer 1996). Even so, it is desirable to determine whether or not the reported gas levels are due mainly to hydrogen or some other gases. Thus, ammonia and organic vapor concentrations will also be measured.

The main factors that could affect the concentration of combustible gas in a catch tank include the characteristics of the waste contents and the ventilation rate. These factors represent respectively the generation and removal of the gas from the tank headspace. Characteristics of the waste in the catch tanks will be examined in another activity that is outside the scope of this plan. Ventilation rate determines how fast combustible gas is removed from a tank by airflow through the headspace. Because most of the catch tanks are passively ventilated, the rate of gas removal varies according to ambient (atmospheric) conditions. Since ambient conditions change constantly, a number of measurements would be needed to accurately estimate the ventilation rates of individual catch tanks.

For the initial evaluation of combustible gas hazards in the catch tanks, only a rough indication of the range of ventilation rates is needed. Two tanks, one with active and another with passive ventilation, are selected for ventilation rate measurements. The ventilation rates in these tanks represent the approximate upper and lower bounds of the interested range. A known amount of helium gas will be injected into a tank headspace. Samples of headspace gas will be taken at measured time intervals. The ventilation rates of these tanks will be calculated based on the measured decrease in helium concentration between these points in time.

The DQO specifies that comparisons with the threshold value (i.e., 25% LFL) be made using one-sided 95% confidence level. Based on this requirement, the minimum number of needed measurements can be calculated if the mean concentration and the associated variance (a measure of the spatial variability of combustible gas in the headspace) are known. However, historical data are not available to estimate the mean percent LFL and the associated variance. Three measurements of combustible gas level in a tank are specified to support the initial hazard analysis. This number of measurements is adequate for the statistical analysis of the data and provides a contingency in the event one of the measurements must be discarded. Ammonia and organic concentrations will be measured each time a combustible gas level reading is taken (unless the 25% LFL threshold is exceeded).

Additional measurements may be needed to demonstrate that the combustible gas level in a catch tank is below the threshold at the 95% upper confidence level. However, it is expected that the combustible gas levels in the catch tanks are significantly below the threshold and that the spatial variability of combustible gas in a tank headspace is small. The required number of samples that is calculated based on a large difference between the mean concentration and the threshold and on a small data variance would be very small. Thus, three measurements are likely to be sufficient for the comparison.

The DQO states that “if combustible gas meter analysis results in >10% LFL, then a Type 3 or Type 4 vapor sample must be taken and analyzed to address the flammability issue.” Type 3 and Type 4 vapor samplers are not available at this time and the >10% LFL criteria is considered too conservative. For this data collection activity, if a combustible gas meter reading exceeds 25% LFL, Hoke™ and SUMMA™ samples will be collected and analyzed. This level is consistent with the flammable gas limit established in the *Tank Waste Remediation System Technical Safety Requirements* (LMHC 1999).

9 0 ROLES AND RESPONSIBILITIES

The organization and responsibility of key personnel involved in this data collection activity are shown in Table 9-1.

Table 9-1 Key Personnel for Sampling and Analysis of Catch Tanks

Responsibility	Organization	Individual
Manager, Inventory Control and Modeling	RPP Process Engineering	K M Hodgson, 373-3513
Technical Lead for Catch Tank Vapor Sampling	RPP Process Engineering	D M Nguyen, 372-3042 (fax 373-4641)
Field Sampling Cognizant Engineer	Characterization Field Engineering	D D Wanner, 373-3297
Laboratory Analysis	WSCF	K L Powell, 372-3909
	PNNL	J W Brothers, 375-2396
Field Sampling	Characterization Project Operations	J F Sickels, 373-0259
Safety Issue Resolution point of contact	Safety Issue Resolution	G D Johnson, 373-1324
On-Call Process Engineer	RPP Process Engineer	On-Call Process Engineer, Pager 85-9654
Tank Farms point of contact	Tank Farm Operations	Double-Shell Tank Farm Operations shift manager, 373-2689

10 0 DATA REPORTING AND DELIVERABLES

If a CGM reading exceeds 25% of the LFL, CPO shall immediately notify, via telephone, the Tank Farm Operations shift manager and/or the on-call process engineer. CPO shall provide electronic notification to the Tank Farm Operations shift manager, the Inventory Control and Modeling Manager, the technical lead for catch tank vapor sampling, and the Safety Issue Resolution point of contact as soon as practical. At a minimum, the electronic notification shall include the following information:

- The measured flammable gas concentration (in %LFL),
- The identification of the catch tank,
- The location of the measurements (e.g., riser and elevation),
- The final configurations of the tank access point (e.g., whether or not a bag or flange with HEPA filter was installed)

Hard copies of all field measurements shall be forwarded to the catch tank sampling technical lead within one week whether or not flammable gas concentration exceeds 25% of the LFL.

The analytical laboratory for Hoke™ samples shall provide preliminary data via electronic mail to the technical lead for catch tank vapor sampling within two working days after the samples are received at the laboratory unless otherwise requested. Final reviewed data shall be transmitted formally within two weeks of receiving the sample(s). The final report shall contain the following information at a minimum:

- Sample identification,
- All analytical results,
- Estimate of analytical precision, and
- The analytical procedure used

The analytical laboratory for SUMMA™ samples shall provide preliminary data via electronic mail to the technical lead for catch tank vapor sampling within 3 weeks after the samples are received at the laboratory. The final data package shall be completed within 10 weeks after sample receipt. The final report shall contain the following information at a minimum:

- Sample identification,
- A brief discussion of the sample preparation, analysis, and quality assurance/quality control measures,
- Concentrations of target analytes for each sample,
- Quality control data to document achieved precision and accuracy,
- Appropriate required quantitation limit (RQL) if analyte is not detected, and

- Discussion of applicable analytical issues or data anomaly, resolution of each issue/anomaly and the impact on the data

Catch tank vapor sampling and analytical results shall be entered into the Tank Vapor Database (TVD). CGM results shall be entered from field documents. Each data report/package for a Hoke™ or a SUMMA™ sample shall be accompanied by an electronic version. The electronic version shall be in the standard electronic format specified in Bobrowski and Simonen (1999). The data shall be entered into the TVD and be available for viewing within 14 days after the data is received by RPP Process Engineering.

11 0 CHANGE CONTROL

All significant changes to the sampling, analysis, or QA/QC requirements in this SAP shall be documented by RPP Process Engineering in an engineering change notice or a letter. All such changes shall be clearly documented in the final data report. Minor changes may be documented by placing a notation in the appropriate permanent record (e.g., memorandum to file). The determination whether or not a change is significant shall be made by the technical lead for catch tank vapor sampling.

12 0 SAFETY CONSIDERATIONS

Pressurized helium in steel bottles will be used for the tracer gas injection. Proper precautions will be taken when handling pressurized gas bottles. The catch tanks may contain hazardous vapor and radionuclides. A survey for hazardous vapor will be performed prior to gaining access to a tank. Also, radiation and hazardous vapor will be monitored during the test as necessary.

13 0 TEST PROCEDURE

13 1 TRACER GAS INJECTION

Note For catch tanks 241-AX-152 and 241-EW-151, the combustible gas level measurements (See Section 13 2) must be completed prior to performing tracer gas injection

Helium Injection Procedure (Refer to Figure 1)

- A1 Verify that the gas cylinder contains helium at pressure <800 psig
- A2 Connect a single ended, shut-off, quick disconnect body (e g , Swagelok part #QC4), if necessary, to the assigned attachment point for the sample
- A3 Connect the helium injection system to the assigned tank access point at connection C1, if present, as directed by the work package
- A4 Verify that the helium outlet valve is closed
- A5 Measure the helium cylinder starting pressure by opening the helium cylinder valve (V3), and adjust the pressure regulator as specified in the work package
- A6 Record the starting helium cylinder starting pressure as indicated by the pressure regulator digital high-pressure stage gauge
- A7 Measure and record the helium cylinder temperature
- A8 Open the assigned sample line isolation valve (V1), if present
- A9 Begin tracer gas injection by opening the helium outlet valve (V2)
- A10 Observe the bottle pressure as indicated by the digital high-pressure stage gauge on the pressure regulator. When the pressure reaches the stopping pressure as specified in the work package, stop helium flow by closing the helium outlet valve (V2)
- A11 Close the assigned sample line isolation valve (V1), if present
- A12 Verify that the helium outlet valve (V2) is closed
- A13 Measure the helium cylinder final pressure using the digital high-pressure stage gauge, record the helium cylinder final pressure
- A14 Close the helium cylinder valve (V3)

A15 Disconnect the helium injection system as directed by the field work package

Procedure for Collecting the First Set of SUMMA™ Samples for Gas Injection (Refer to Figure 2)

A16 Verify that the specified time interval has elapsed since completion of the helium injection

A17 Connect (in series) two particulate air filters to the sample line as shown in Figure 2. The particulate air filters (F1) shall be closest to the tank access point

A18 Place a short piece of Teflon™ (or c-flex) tubing down stream of the dual particulate air filter (F1)

A19 Connect the CGM/OVM to the Teflon™ (or c-flex) tubing

A20 Open the sample line isolation valve (V1), if present

A21 Purge the sample line using the CGM/OVM for the duration specified in the field work package

A22 Close the isolation valve (V1), if present

A23 Disconnect the CGM/OVM from the Teflon™ (or c-flex) tubing

A24 Connect the SUMMA™ tritium trap assembly

A25 Open the isolation valve (V1), if present

A26 Collect the first SUMMA™ sample per field work package and record the data required on the data sheet

A27 Close the isolation valve (V1), if present

A28 Disconnect the SUMMA™/tritium trap assembly from the Teflon™ (or c-flex) tubing

A29 Repeat Steps A24 through A28 to collect the second SUMMA™ sample

A30 Configure the assigned tank access point to the condition specified in the fieldwork package

Procedure for Collecting the Second Set of SUMMA™ Samples for Gas Injection (Refer to Figure 2)

- A31 Verify that the specified time interval has elapsed since completing collection of the first set of SUMMA™ samples
- A32 Repeat Steps A17 through A30 to collect the second set of SUMMA™ samples

Procedure for Collecting the Optional Third Set of SUMMA™ Samples for Gas Injection (Refer to Figure 2)

- A33 Verify that the specified time interval has elapsed since completing collection of the second set of SUMMA™ samples
- A34 Repeat Steps A17 through A30 to collect the optional third set of SUMMA™ samples

13.2 FIELD COMBUSTIBLE GAS LEVEL MEASUREMENTS

Three measurements of flammable gas, ammonia, and organic vapor concentrations shall be obtained at each sampling location according to the following steps

Note At any time during sampling, if a combustible (flammable) gas level measurement exceeds 25% of the LFL, Steps B1 through B11 will no longer apply. If the measurement is taken from within the riser, proceed with Steps C1 through C12. If the measurement is from within the tank headspace, proceed with Steps D1 through D8. Also, instead of restoring the tank access point to the initial condition when sampling is complete, the tank access shall be reconfigured to allow ventilation of the flammable gas (e.g., installing a flange or bag with HEPA filter) if the tank has no known ventilation paths.

- B1 Lower the sampling line approximately 1 foot into the selected riser
- B2 Purge the sample line with gas in the riser using the CGM for the duration specified in the work package
- B3 Measure the concentrations of combustible gas, ammonia, and organic vapor. Record the data as directed in the work package
- B4 If flammable gas concentration in the riser is greater than 25% of the LFL, perform Steps C1 through C12
- B5 Repeat Step B3 twice

- B6 Lower the sampling line into the tank headspace to the depth specified in the work package
- B7 Purge the sample line with gas in the tank headspace using the CGM for the duration specified in the work package
- B8 Measure the concentrations of combustible gas, ammonia, and organic vapor Record the data
- B9 If flammable gas concentration in the tank headspace is greater than 25% of the LFL, perform Steps D1 through D8
- B10 Repeat Step B8 twice
- B11 Configure the assigned tank access point to the condition as specified in the work package

If the flammable gas level in the access riser as measured by a CGM exceeds 25% of the LFL, then perform the following steps

- C1 Connect a Hoke™ sampler to the sampling line
- C2 Purge the line through the Hoke™ sampler for the duration specified in the work package
- C3 Obtain a Hoke™ sample
- C4 Install particulate air filter(s) on the sample line
- C5 Purge the sample line for the duration specified in the field work package
- C6 Connect a SUMMA™/tritium trap assembly to the sample line and obtain a SUMMA™ sample
- C7 Disconnect the SUMMA™/tritium trap assembly and the particulate air filter from the sample line
- C8 Lower the sample line into the tank headspace to the depth specified in the work package
- C9 Purge the sample line
- C10 Measure the concentration of combustible gas using the CGM and record the data
- C11 Repeat Steps C1 through C7

- C12 If the tank has no known ventilation paths and if it is necessary to leave the open riser unattended, install a flange or bag with HEPA filter over the tank access point. Otherwise, the tank access shall be reconfigured as directed by engineering.

If the flammable gas concentration in the tank headspace exceeds 25%, then perform the following steps:

- D1 Connect a Hoke™ sampler to the sampling line.
- D2 Purge the line through the Hoke™ sampler for the duration specified in the field work package.
- D3 Obtain a Hoke™ sample.
- D4 Install particulate air filter(s) on the sample line.
- D5 Purge the sample line.
- D6 Connect a SUMMA™/tritium trap assembly to the sample line and obtain a SUMMA™ sample.
- D7 Disconnect the SUMMA™/tritium trap assembly and the particulate air filter from the sample line.
- D8 If the tank has no known ventilation paths and if it is necessary to leave the open riser unattended, install a flange or bag with HEPA filter over the tank access point. Otherwise, the tank access shall be reconfigured as directed by engineering.

13.3 RADIATION SCREENING

Tritium traps and particulate air filter assemblies will be shipped by CPO to WSCF for analysis. The tritium traps will be analyzed for tritium, the air filters will be analyzed for total alpha, total beta, and gamma energy analyses. Radiation Protection will use the data to determine whether or not the SUMMA™ samples can be radiologically released (and therefore can be accepted by the laboratory). CPO will store the SUMMA™ samples until they are released and will ship them to the laboratory at that time.

14 0 REFERENCES

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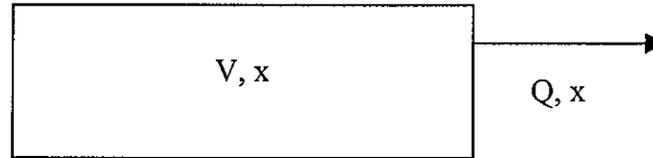
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APPENDIX A

METHOD FOR CALCULATING VENTILATION RATE IN A CATCH TANK

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METHOD FOR CALCULATING VENTILATION RATE IN A CATCH TANK



Where V volume of headspace (volume of tank – volume of liquid)

Q ventilation rate

x concentration of helium at any given time after gas injection

Mass balance for helium

Rate of helium out – Rate of helium in = Rate of helium loss

The rate of helium entering the tank after completion of gas injection can be considered negligible. The mass balance equation can be re written as

$$Qx = -V \frac{dx}{dt} \quad (1)$$

$$\text{Or } dt = \frac{-V}{Q} \frac{dx}{x} \quad (2)$$

Integration of Equation 2 gives

$$\int dt = \frac{-V}{Q} \int \frac{dx}{x}$$

$$\Delta t = \frac{-V}{Q} (\ln x_2 - \ln x_1)$$

$$\Delta t = \frac{V}{Q} \ln \frac{x_1}{x_2}$$

$$\text{Or } Q = \frac{V}{\Delta t} \ln \frac{x_1}{x_2} \quad (3)$$

x_1 and x_2 will be determined from analysis of the SUMMA™ samples Δt is the time interval between collection of the two sample sets

Equation 3 can be re-written as follow for the period between gas injection and collection of the first set of SUMMA™ samples (Δt_o)

$$Q = \frac{V}{\Delta t_o} \ln \frac{x_o}{x_1} \quad (4)$$

x_o the initial concentration of helium in the tank, can be estimated as follows

Assume helium behaves as an ideal gas

$$PV = nRT$$

$$nR = \frac{P_c V_c}{T_c} = \frac{P_o V_o}{T_o} \quad (5)$$

Where P_c , V_c , and T_c are pressure, volume, and temperature of helium in the gas cylinder and P_o , V_o , and T_o are the same properties of helium in the catch tank immediately after injection

Equation 5 can be re-arranged to

$$V_o = V_c \frac{P_c}{P_o} \frac{T_o}{T_c} \quad (6)$$

The initial concentration of helium in the catch tank after completion of the gas injection is

$$x_o = \frac{V_o}{V} \quad (7)$$

Three significant assumptions are associated with the calculation of x_o (1) helium behaves like an ideal gas, (2) ambient temperature is the same as that in the tank vapor space (this assumption is necessary because there are no temperature probes in the catch tanks), and (3) the rate of helium loss during gas injection is negligible. Because of these assumptions, ventilation rates should be calculated based on data from analyses of the SUMMA™ samples. If necessary, calculation of the ventilation rate using helium gas bottle data will be performed for verification

APPENDIX B

DATA SHEET FOR USE WITH TRACER GAS INJECTION

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TRACER GAS INJECTION DATA SHEET							
Catch Tank Number							
Data Description	Sample No	Date	Time		Pressure		Recorded By
			Start	Stop	Start	Stop	
Gas Injection	NA ¹						
Gas Cylinder Temperature _____ °F				NA	NA	NA	
Ambient Air Temperature _____ °F				NA	NA	NA	
Sample Set 1	Canister 1 # V _____ -A1- _____				NA	NA	
	Canister 2 # V _____ A2 _____				NA	NA	
Ambient Air Temperature _____ °F				NA	NA	NA	
Sample Set 2	Canister 1 # V _____ -B1- _____				NA	NA	
	Canister 2 # V _____ -B2- _____				NA	NA	
Ambient Air Temperature _____ °F				NA	NA	NA	
Sample Set 3 (Optional)	Canister 1 # V _____ -C1- _____				NA	NA	
	Canister 2 # V _____ -C2- _____				NA	NA	
Ambient Air Temperature _____ °F				NA	NA	NA	
Comments or Observations							

¹NA Not Applicable

Note Temperature measurements should be performed during (or as close as possible to) the gas injection or sampling

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